



SOURCE TEST REPORT

Emissions Testing of Metal Melting "Facility C" for Selected Metals and Particulate Matter

Facility ID: [REDACTED]

Prepared for:
South Coast Air Quality Management District
21865 Copley Drive
Diamond Bar, CA 91765

Equipment Location:
Metal Melting Facility C
[REDACTED] CA [REDACTED]

Test Date(s): August 13-16, 2019

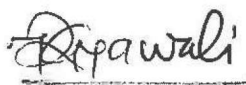
Report Date: November 8, 2019

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1.0 EXECUTIVE SUMMARY

Key project information is provided in the summary below. Test results are summarized in Table 1-1 and Table 1-2.

Customer:	South Coast Air Quality Management District (SCAQMD) 21865 East Copley Drive Diamond Bar, CA 91765-4182 Contact: Mr. Michael Garibay, (909) 396-2249
Facility & Location:	Metal Melting Facility C [REDACTED] CA
Facility ID:	[REDACTED]
Equipment:	Inlets (Furnace and Upstream to Baghouse) / HEPA Baghouse Outlet
Test Objective:	To determine the Particulate Matter (PM), Arsenic, Cadmium, Nickel, Chromium, and Hexavalent Chromium (Cr ⁶⁺) emissions from the chromium alloy melting operations
Test Requested by:	South Coast Air Quality Management District (SCAQMD)
Test Date(s):	August 13-16, 2019
Test Personal	Neal Conroy, Morgan Nguyen, Dorian Johnson, William Bryant, Luke Barrow, and Mark Rowlett of Almega Environmental & Technical Services
Testing Firm:	Almega Environmental & Technical Services 10602 Walker Street Cypress, CA 90630 Contact: Mr. Charles Figueroa, tel (714) 889-4000
Regulatory Agency:	South Coast Air Quality Management District (SCAQMD) 21865 East Copley Drive Diamond Bar, CA 91765-4182 Contact: Mr. Brian Speaks, (909) 396-3212
Measurements: Volumetric flow rates Selected Metals (As, Cd, Cr, & Ni) Chromium (Hex/Total) Particulate Matter (PM)	SCAQMD Methods 1.1 - 4.1 CARB Method 436 CARB Method 425 SCAQMD Method 5.1

TABLE 1-1. SUMMARY OF TEST RESULTS

Facility: Metal Melting Facility C
City, State: ████████ CA
Test Location: Baghouse Outlet & Inlets
Test Date(s): August 13-16, 2019

Test Data	Units	Baghouse Outlet	Inlet 1 Furnace (Inside)	Inlet 2 (Upstream to Baghouse)
<u>CARB Method 436</u>				
<u>Sampling Data</u>				
Stack Temperature	°F	3-Run Avg. 08/13-14/19 100	3-Run Avg. 08/13-14/19 114	3-Run Avg. 08/13-14/19 95
Sample Volume	dscf	79	89	96
Stack Flow Rate	acfm	8,115	1,151	6,507
Stack Flow Rate	dscfm	7,499	1,033	5,989
<u>Concentration (CARB 436)</u>				
Arsenic	ug/dscm	< 0.451	< 3.45	< 0.850
Cadmium	ug/dscm	< 0.451	< 0.399	< 0.367
Chromium	ug/dscm	1.43	2060	503
Nickel	ug/dscm	0.55	61.0	16.7
<u>Mass Emissions (CARB 436)</u>				
Arsenic	lb/hr	< 1.27E-05	< 1.33E-05	< 1.92E-05
Cadmium	lb/hr	< 1.27E-05	< 1.66E-06	< 8.84E-06
Chromium	lb/hr	4.09E-05	7.97E-03	1.12E-02
Nickel	lb/hr	1.56E-05	2.36E-04	3.74E-04
<u>CARB Method 425</u>				
<u>Sampling Data</u>				
Stack Temperature	°F	3-Run Avg. 08/14-15/19 103	3-Run Avg. 08/14-15/19 129	3-Run Avg. 08/14-15/19 98.4
Sample Volume	dscf	76.4	88.1	93.1
Stack Flow Rate	acfm	7,893	1,172	6,296
Stack Flow Rate	dscfm	7,245	1,030	5,771
<u>Concentration (CARB 425)</u>				
Chromium VI	ug/dscm	< 0.062	5.79	1.52
Total Chromium	ug/dscm	< 0.270	530	106
<u>Mass Emissions (CARB 425)</u>				
Chromium VI	lb/hr	< 1.62E-06	2.26E-05	3.30E-05
Total Chromium	lb/hr	< 7.27E-06	2.00E-03	2.25E-03
<u>SCAQMD Method 5.1</u>				
<u>Sampling Data</u>				
Stack Temperature	°F	Single Run 08/16/19 88	Single Run 08/16/19 101	Single Run 08/16/19 93
Sample Volume	dscf	40	53	56
Stack Flow Rate	acfm	6,705	1,147	6,412
Stack Flow Rate	dscfm	6,240	1,040	5,825
Particulate Catch	mg	6.57	105.6	45.2
Particulate Concentration	gr/dscf	0.0026	0.0305	0.0126
Particulate Emission Rates	lb/hr	0.136	0.271	0.628
	lb/day	3.28	6.52	15.06

Flags
 ND or "<" - Not detected, reporting limit reported.

**TABLE 1-2. SUMMARY OF TEST RESULTS
(INLET 1 INSIDE)**

Facility: AQMD Facility C
 City: ████████ CA
 Source: Baghouse
 Location: Inlet 1 Furnace (Inside)

Test Data	Units	Source Test Results			Average
		Run 1	Run 2	Run 3	
Run Number	--				
CARB Method 436					
Sampling Data		08/13/19	08/13/19	08/14/19	3-Run Avg.
Stack Temperature	°F	116	126	101	114
Sample Volume	dscf	86.7	88.8	90.1	88.6
Stack Flow Rate	acfm	1,132	1,177	1,144	1,151
Stack Flow Rate	dscfm	1,012	1,035	1,052	1,033
Material Charged (25CH)	lbs/hr	3000	3000	3000	3000
CARB Method 436					
MASS EMISSION RATE		Total	Total	Total	
Arsenic	lb/hr	2.32E-05	1.19E-05	4.63E-06	1.32E-05
Cadmium	lb/hr	ND	1.54E-06	1.88E-06	< 1.66E-06
Chromium	lb/hr	6.79E-03	1.09E-02	6.17E-03	7.97E-03
Nickel	lb/hr	1.43E-04	3.68E-04	1.99E-04	2.37E-04
Emissions Factor (lb/lbs)					
Arsenic	lb-As/lb-25CH	7.72E-09	3.96E-09	1.54E-09	1.55E-05
Cadmium	lb-Cd/lb-25CH	ND	5.14E-10	6.28E-10	ND 1.29E-06
Chromium	lb-Cr/lb-25CH	2.26E-06	3.65E-06	2.06E-06	1.60E-06
Nickel	lb-Ni/lb-25CH	4.77E-08	1.23E-07	6.62E-08	4.91E-07
CARB Method 425					
Sampling Data		08/14/19	08/15/19	08/15/19	3-Run Avg.
Stack Temperature	°F	131	114	142	129
Sample Volume	dscf	85.3	92.6	86.3	88.1
Stack Flow Rate	acfm	1,142	1,201	1,174	1,172
Stack Flow Rate	dscfm	998	1,083	1,008	1,030
Material Charged (25CH)	lbs/hr	3000	3000	3000	3000
Mass Emissions (CARB 425)					
Chromium VI	lb/hr	1.27E-06	3.39E-05	3.28E-05	2.26E-05
Total Chromium	lb/hr	3.93E-03	5.11E-04	1.56E-03	2.00E-03
Emissions Factor (lb/lbs)					
Chromium VI	lb-Cr+6/lb-25CH	4.22E-10	1.13E-08	1.09E-08	7.55E-09
Total Chromium	lb-Cr/lb-25CH	1.31E-06	1.70E-07	5.18E-07	6.67E-07
SCAQMD Method 5.1					
Sampling Data		08/16/19			Single Run
Stack Temperature	°F	101			101
Sample Volume	dscf	53.5			53.5
Stack Flow Rate	acfm	1,147			1,147
Stack Flow Rate	dscfm	1,040			1,040
Material Charged (25CH)	lbs/hr	3000			3000
PM Emissions					
Emission Rate	lb/hr	0.271			2.71E-01
Emissions Factor (lb/lbs)					
PM Emissions	lb-PM/lb-25CH	9.05E-05			9.05E-05

2.0 INTRODUCTION

Almega Environmental & Technical Services (Almega) was contracted by South Coast Air Quality Management District (SCAQMD) to conduct stationary source emissions testing of the baghouse serving the chromium alloy melting operations at facility designated as “Facility C” located in ██████████ California. The purpose of the test program is to determine the Particulate Matter (PM), Arsenic, Cadmium, Nickel, Chromium, and Hexavalent Chromium (Cr⁶⁺) emissions from the chromium alloy melting operations.

Due to the rising level of hexavalent chromium in the ambient air in the city of Paramount and its vicinity, SCAQMD staff initiated the rule development process to amend Rule 1407 to address toxic air contaminant emissions from ferrous metal melting operations and update existing requirements for non-ferrous metal melting operations currently regulated under the rule. Through working group meetings with industry stakeholders, it was requested that the rule be separated in to two rules for (1) ferrous and (2) non-ferrous metal melting. After additional input and working group meetings, the SCAQMD staff decided to bifurcate the rule and reclassify characterization into (1) non-chromium alloy (Rule 1407) and (2) chromium alloy (Rule 1407.1) metal melting. In regards to the chromium alloy melting, additional data from melting operations of metals with a chromium content greater than 0.5% is needed to quantify the conversion rate of chromium to hexavalent chromium and quantify toxic air contaminant emissions from these facilities to aid in the rulemaking process. Three facilities have agreed to allow source testing for the purposes of collecting this data [Ref. SCAQMD Source Test Plan to be conducted at Metal Melting facilities].

Almega was selected as a third-party source test contractor to perform a portion of this testing. The test matrix employed during the testing is presented in Table 2-1.

TABLE 2-1. TEST MATRIX

PARAMETER	TEST METHOD	# OF TEST RUNS	TEST TIME	LOCATION
Traverse Points	SCAQMD Methods 1.1 & 2.1	3 Per Location	120 min.	Simultaneous testing at the outlet and two inlets of the HEPA/Baghouse
Molecular Weight and Excess Air	SCAQMD Method 10.1	1 each Location	60 min.	
Moisture Content	Method 4.1 (Inclusive in the CARB M436, M425, & SCAQMD M5.1)	3 Per Location	120 min.	
Hexavalent and Total Chromium	CARB Method 425	3 Per Location	120 min.	
Selected Metals (As, Cd, Cr, & Ni)	CARB Method 436	3 Per Location	120 min.	
Particulate Matter (PM)	SCAQMD Method 5.1	3 Per Location	72 min.	
Fugitive Emissions	Determination of overall capture efficiency	--	n/a	HEPA/Baghouse Inlets

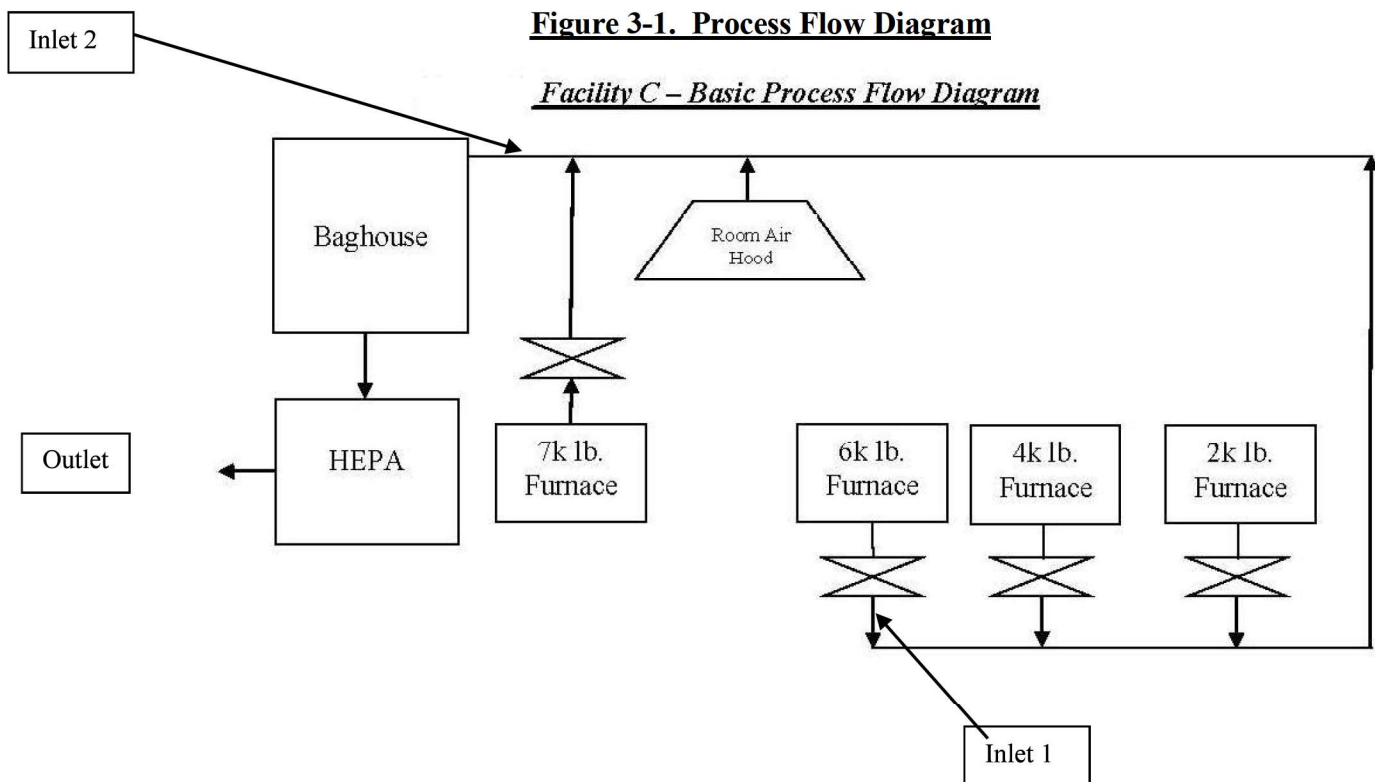
Almega performed source testing at the outlet and the two designated inlets of the baghouse simultaneously over a three-day period August 13 - 16, 2019. The sampling was conducted in triplicate at each of the three (3) sampling locations for metals and chromium with just a single test conducted for the particulate matter. Testing was conducted as specified in the reference methods and Source Test Plan prepared by SCAQMD. The source test plan is included in the Appendix I for reference. Capture/Collection efficiency test was conducted by the SCAQMD personal and provided to Almega for the inclusion in the source test report. All pertinent process data was collected and provided by the facility and included in the Appendix H.

2.1 Document Outline

This report is organized as follows. Section 1.0 is a summary of the project and test results. Section 2.0 describes the project, its objectives and approach. Section 3.0 describes the equipment tested and applicable sampling locations. Section 4.0 describes the sampling and analysis procedures used to conduct the testing. Section 5.0 describes Quality Assurance and Quality Control activities performed, and section 6.0 discusses test results. The Appendices contain test results, calculated data, raw field data, analytical data, calibration records, and certification documents.

3.0 EQUIPMENT AND PROCESS DESCRIPTION

The metal melting facility C uses electric induction furnaces for the processing of white iron, cast iron, ductile iron, and stainless steel. A general schematic of the test locations follows:



Note: Courtesy of SCAQMD Source Test Plan

3.1 Process and Equipment Description

The facility C has four electric induction furnaces in sizes as follows:

- 7,000 lbs material capacity with a power rating of 1,500 KW
- 6,000 lbs material capacity with a power rating of 1,500 kW
- 4,000 lbs material capacity with a power rating of 1,000 kW
- 2,000 lbs material capacity with a power rating of 400 kW

90% of facility operations involve melting of various irons and approximately 10% percent of operations are stainless steel melts. Raw materials for iron melts are frequently re-runs while the stainless melts tend to be new certified material. The facility normally runs 2 furnaces at a time, most frequently the 7,000 lbs and 6,000 lbs furnaces. Stainless steels are only processed in either the 4,000 lbs or 2,000 lbs furnace. The furnaces are loaded with the applicable material and the heat begins. Electrical current is applied and the material becomes molten. Typical temperatures are in the 2400-2700°F range during iron melting operations and in the 3000°F range during stainless steel melting operations. Material from the furnace is poured in to pre-heated ladles for transport by forklift to the casting area. All casting at the facility is green sand casting. The casting area is in a separate location within the building.

During the melting process emissions are captured by an exhaust system which mounts to the furnace and utilizes a slot design. Suction is provided by the blower which is part of the baghouse and HEPA system. Each furnace has a closable damper installed which allows for isolation from the system when a furnace is not in use. In the exhaust header there is one non closable exhaust hood which pulls room air into the system. The HEPA filters are installed between the baghouse and the exhaust stack. The facility has modified the outlet such that a straight run of duct is now provided downstream of the exhaust muffler to meet the requirements of at least two duct diameters downstream and one half of a diameter upstream of any flow disturbances.

The facility does approximately 4-5 heats a day. The iron heats performed in the 7,000 lbs and 6,000 lbs furnaces take 1.5 – 2 hours. The stainless heats performed in the smaller 4,000 lbs and 2,000 lbs furnaces take up to 3 hours [Ref. SCAQMD Source Test Plan to be conducted at Metal Melting facilities].

3.2 Operating Conditions during Test

Testing was performed during the processing of chrome iron (25CH) in 6K furnace (Furnace 3). The individual exhaust duct that vents Furnace 3 was designated as “Inlet 1”. The control device is a slot exhaust system mounted on the base of the furnace’s lid. Furnaces No. 3 and 4 were operated during the test program. The Inlet 2 (Upstream to Baghouse) location is the general inlet that vents all four furnaces to the control device.

The process data including process material, baghouse differential pressure, HEPA filter

differential pressure, ambient conditions, etc are included in the Appendix H.

3.3 Sampling Locations

Inlet 1 (Inside) Furnace #3:

The reference method sampling locations meet the following specifications:

Sampling Location Configuration – Inlet Furnace (Inlet Inside)	
Distance from Upstream Disturbance	120 in. (> 8 duct diameter)-B
Distance from Downstream Disturbance	48 in. (> 2 duct diameter)-A
Port Length	0.0 in. (measured from outside wall)-L
Port Inside Diameter	3 in. - d
Number of sampling ports	2 (located at 90° intervals)
Stack Diameter	13 in. (internal diameter)-D

Sampling locations comply with the requirements of SCAQMD Method 1.1.

Inlet 2 (Upstream to Baghouse):

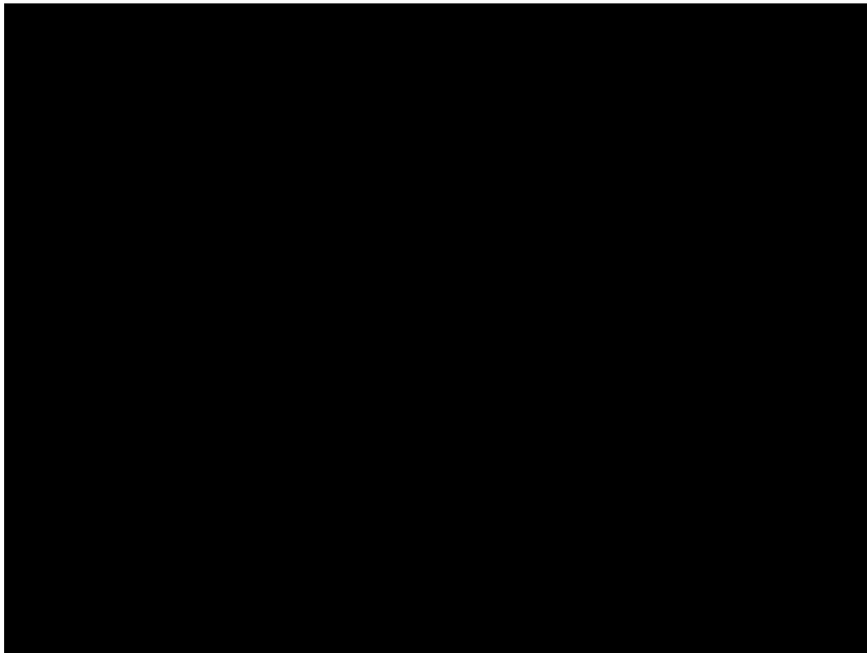
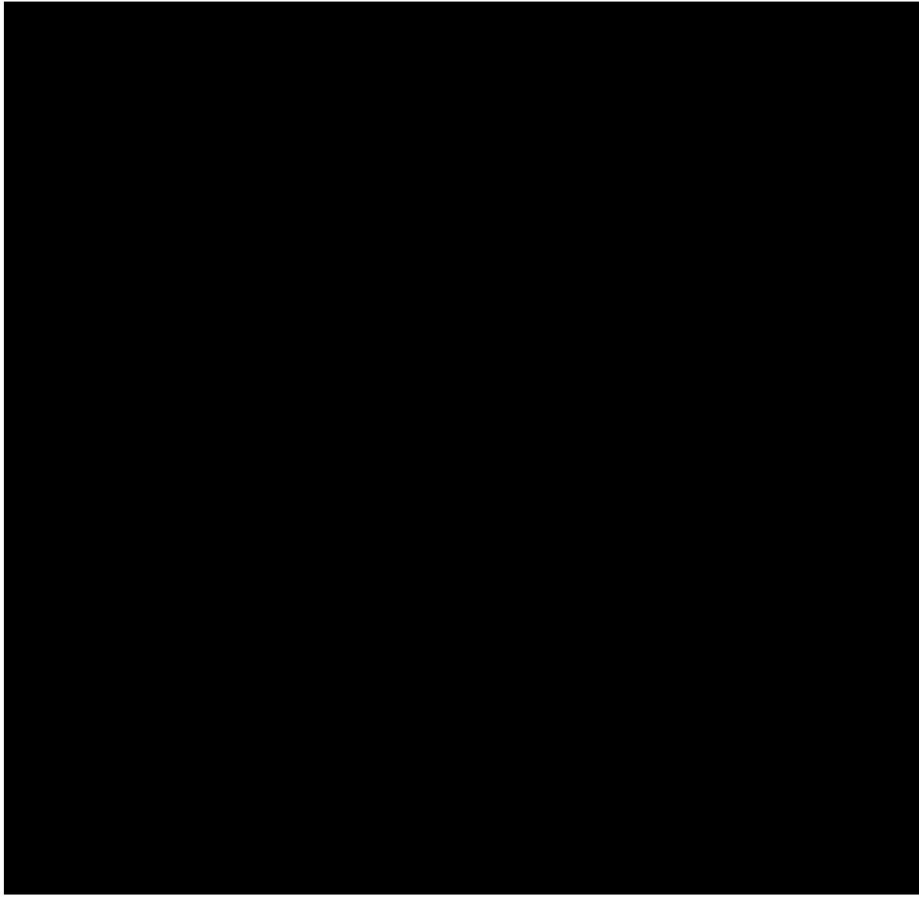
Sampling Location Configuration – Inlet 2 Outside (Upstream of Baghouse)	
Distance from Upstream Disturbance	42.0 in. (2.63 duct diameter)-B
Distance from Downstream Disturbance	196 in. (12.3 duct diameter)-A
Port Length	6 in. (measured from outside wall)-L
Port Inside Diameter	3.0 in.-d
Number of sampling ports	2 (located at 90° intervals)
Stack Diameter	16 in. (internal diameter)-D

Sampling locations comply with the requirements of SCAQMD Method 1.1.

Outlet:

Sampling Location Configuration – Outlet	
Distance from Upstream Disturbance	126 in. (2.63 duct diameter)-B
Distance from Downstream Disturbance	50 in. (1.04 duct diameter)-A
Port Length	6 in. (measured from outside wall)-L
Port Inside Diameter	3.0 in.-d
Number of sampling ports	2 (located at 90° intervals)
Stack Diameter	48 in. (internal diameter)-D

Sampling locations comply with the requirements of SCAQMD Method 1.1.



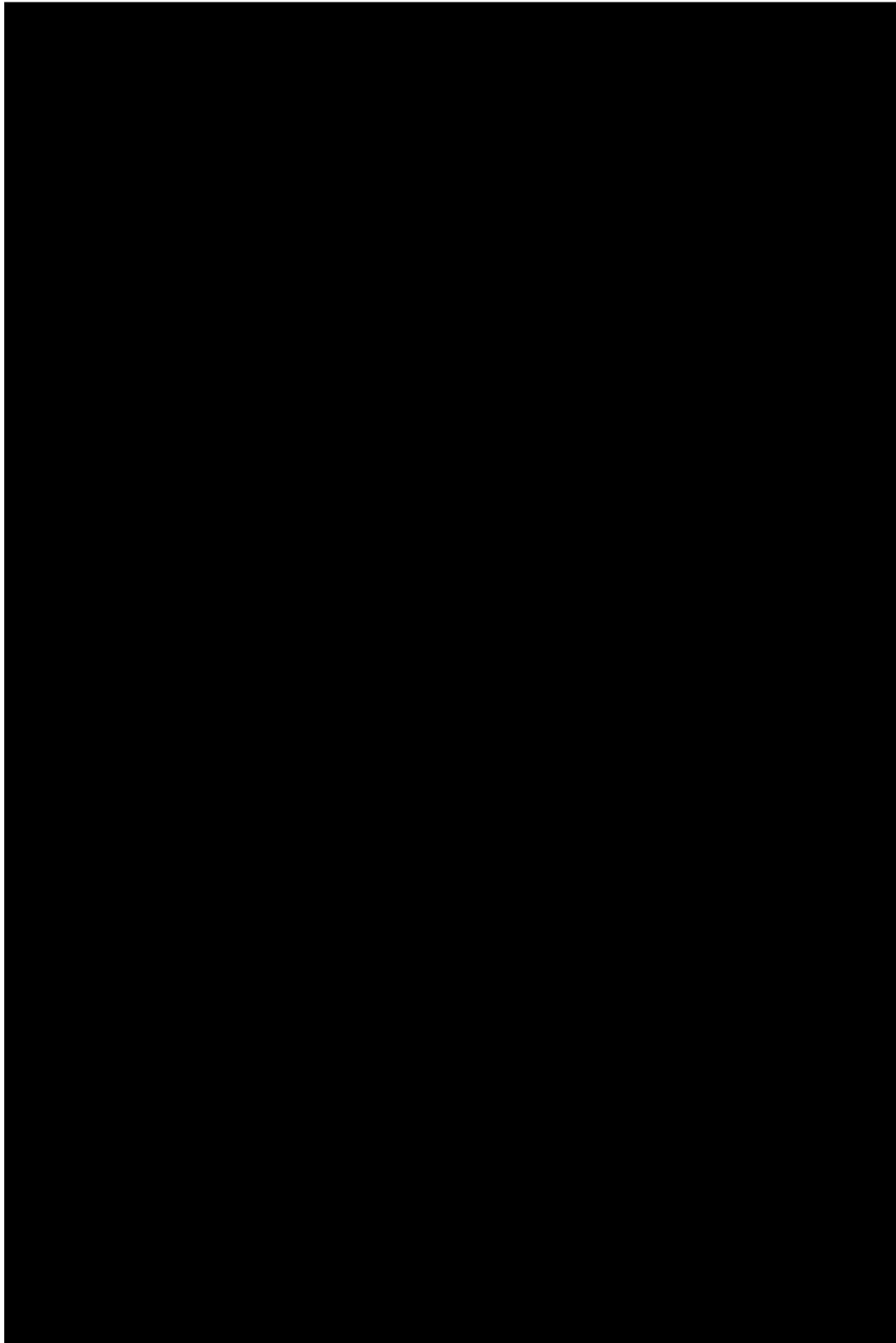
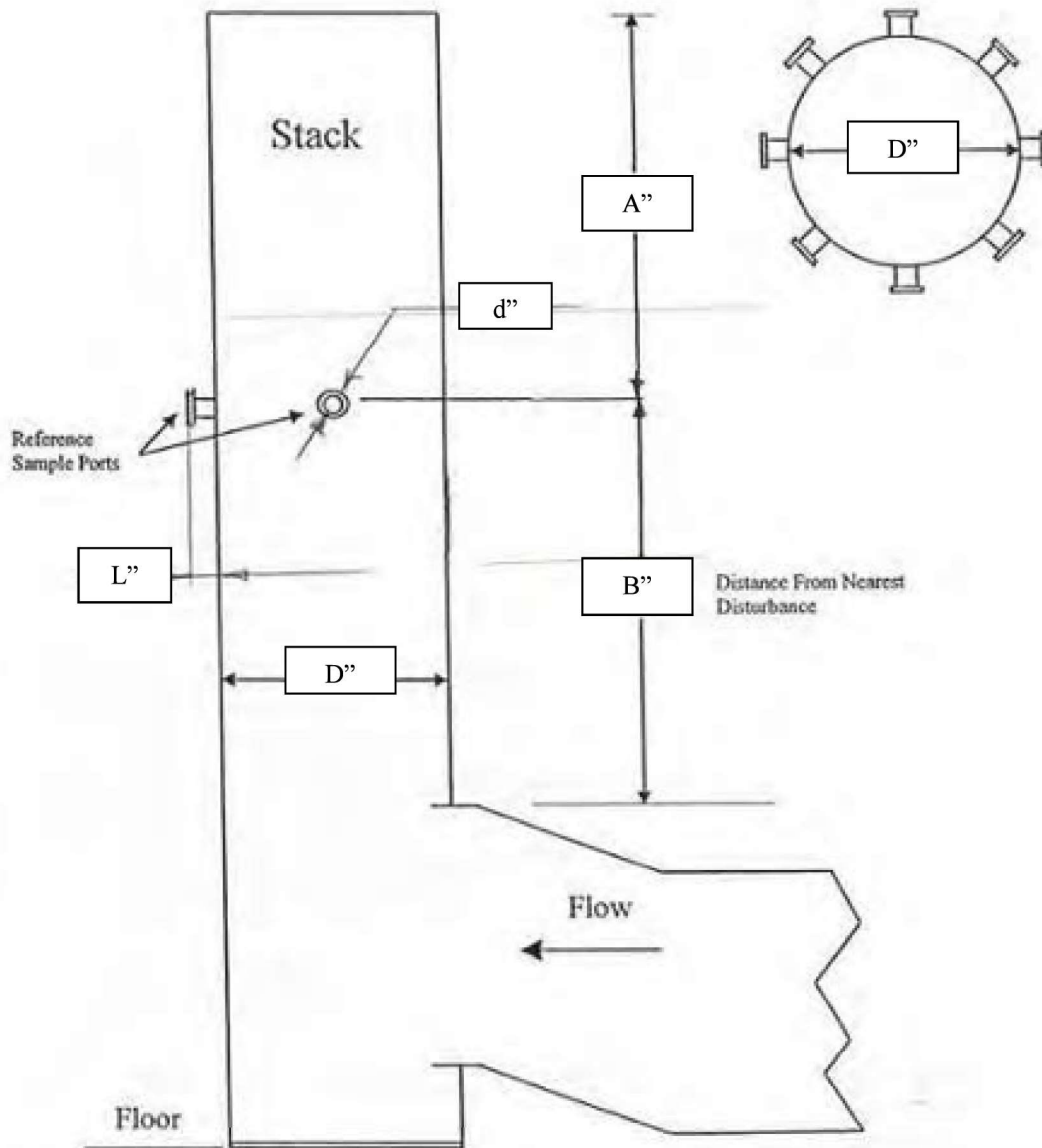


Figure 3-3. General Stack Schematic



4.0 SAMPLING AND ANALYTICAL PROCEDURES

Test measurements were performed according to sampling and analysis procedures promulgated by the South Coast Air Quality Management District (SCAQMD), California Air Resources Board (CARB), or US Environmental Protection Agency (EPA). The sampling and analysis procedures used for this test program are summarized below. Any modifications or deviations not addressed herein are discussed in Section 3 of this report.

- 4.1 SCAQMD Methods 1.1-4.1 – Determination of Stack Gas Volumetric Flow Rate, Molecular Weight, and Moisture Content
 - 4.1.1 SCAQMD Method 1.1 – Sampling Traverse Points
 - 4.1.2 SCAQMD Method 2.1 – Stack Gas Flow Rate
 - 4.1.3 SCAQMD Method 3.1 – Stack Gas Molecular Weight
 - 4.1.4 SCAQMD Method 4.1 – Stack Gas Moisture Content
- 4.2 SCAQMD Method 5.1 – Particulate Matter (PM)
- 4.3 SCAQMD Method 10.1 – Integrated Gas Sampling (O₂/CO₂)
- 4.4 CARB Method 425 – Total and Hexavalent Chromium
- 4.5 CARB Method 436 – Multiple Metal Emissions
- 4.6 Capture/Collection Efficiency

4.1 SCAQMD Methods 1.1-4.1 – Determination of Stack Gas Volumetric Flow Rate, Molecular Weight, and Moisture Content

The flue gas flow characteristics (i.e. flow rate, molecular weight, and moisture content) were determined according to SCAQMD Methods 1.1 through 4.1. The testing was conducted as follows:

4.1.1 SCAQMD Method 1.1/1.2 – Sampling and Velocity Traverse Points

The number and location of traverse points are determined according to SCAQMD Method 1.1/1.2 based on the physical dimensions of the sampling location and process parameters. In principle, the stack cross-section is divided into equal areas, each of which is represented by a “traverse point”. Generally, the number of traverse points diminishes as the flow profile at the sampling location becomes uniform. In most cases, the maximum number of sampling points is 24 for particulate/metals testing and 16 for velocity traverses. Fewer traverse points are permitted as described in the method.

4.1.2 SCAQMD Method 2.1 – Gas Velocity and Traverse Points

The velocity and volumetric flow rate of the laser exhaust was determined according to SCAQMD Method 2.1. In this method, the velocity head (differential pressure) and temperature is measured at the required traverse points. The stack gas differential pressure head was determined using an "S" type Pitot tube and inclined liquid manometer. The temperature was measured using a type "K" thermocouple and digital temperature readout.

Prior to testing, the measurement system was set-up and leak-checked. Then the velocity head and temperature was recorded at predetermined traverse points. After the last traverse is completed, the system was again leak-checked. After completion of the traverse, the static pressure in the stack was determined near the centroid of the stack. The stack gas velocity was calculated using the velocity head, and stack gas temperature, pressure and molecular weight.

QA/QC for the method included field performance checks, and periodic calibrations of test equipment including the Pitot tube, differential pressure gauge, TC and TC-readout. A swirl check was also performed to assess cyclonic flow.

4.1.3 SCAQMD Method 3.1 - Gas Molecular Weight

The stack gas molecular weight (MW) was calculated based on the fraction of its major constituents including: oxygen (O₂), carbon dioxide, (CO₂), nitrogen (N₂), carbon monoxide (CO), and water (H₂O). The dry MW was calculated based on the partial fractions of O₂, CO₂, N₂, and CO. Specifically, the O₂ and CO₂ fractions were determined by CEMS, integrated sampling, or grab sampling, and the balance was assumed to be N₂ and CO. The wet MW was calculated based on the fractions of dry gas and water vapor. The dry and wet MW were calculated according to the following equations:

$$MW_{\text{DRY}} = 0.32 \times \%O_2 + 0.44 \times \%CO_2 + 0.28 \times (\%N_2 + \%CO)$$

$$MW_{\text{WET}} = 0.18 \times \%H_2O + MW_{\text{DRY}} \times (1 - \%H_2O/100)$$

where: MW_{DRY} = stack gas molecular weight, dry-basis
 MW_{WET} = stack gas molecular weight, wet-basis
 0.32 = molecular weight fraction for O₂
 0.44 = molecular weight fraction for CO₂
 0.28 = molecular weight fraction for N₂ and CO
 0.18 = molecular weight fraction for H₂O (water vapor)
 %X = fraction of X in stack gas, dry basis, where X = O₂, CO₂, N₂, CO
 %H₂O = fraction of water vapor in stack gas, wet-basis

For this test, single bag sample was collected at each test location over a period of 60 minutes. These samples were analyzed for oxygen and carbon dioxide via SCAQMD Method 10.1. The analysis of those bag samples shows that the O₂/CO₂ concentration for all sampling locations is in ambient level.

4.1.4 SCAQMD Method 4.1- Gas Moisture Content

The stack gas moisture content was determined according to SCAQMD Method 4.1. In this method, water vapor is collected in a condenser while the dry stack gas volume is measured using a dry gas meter. The volume of water vapor was calculated from the amount of water condensed and the total gas volume is the sum of water vapor plus dry stack gas. The moisture content was determined as a fraction of the total wet stack gas volume. The following calculations were used.

$$B_{WS} = \frac{V_{W,Std}}{V_{M,Std} + V_{W,Std}}$$

$$V_{W,Std} = K_1 \times V_{H_2O}$$

$$V_{M,Std} = T_{Std}/P_{Std} \times Y_M \times V_M \times P_M/T_M$$

- where:
- B_{WS} = Fraction of water vapor in stack gas
 - $V_{W,Std}$ = Volume of water vapor (scf)
 - $V_{M,Std}$ = Volume of stack gas sampled (dscf)
 - K_1 = Unit volume of water vapor (0.04707 scf @68°F or 0.0464 scf @60°F)
 - T_{Std} = Standard Temperature (528°R or 520°R)
 - P_{Std} = Standard Pressure, 29.92 in. Hg
 - Y_M = Dry gas meter calibration factor
 - V_M = Measured volume of stack gas sampled
 - P_M = Dry gas meter pressure (in. Hg)
 - T_M = Dry gas meter temperature (°R)

The moisture content was simultaneously determined if sampling was performed isokinetically otherwise performed as follows:

Moisture was collected in a sampling train consisting of a probe, TFE line, four impingers in an ice bath, a leak-free pump, a vacuum gauge and a dry gas meter. Figure 4-1 is a schematic of a typical moisture train. Initially, impingers #1 and #2 contained 100 ml of water, impinger #3 was empty, and impinger #4 contained a known amount (approximately 300 g) of desiccant (e.g. Silica Gel). Prior to sampling, a leak check of the sampling train was performed. Then, the sampling probe was inserted into the centroid of the stack, the initial meter readings (volume, temperatures, etc.) were recorded, the sample pump is started and the sampling rate is adjusted to the desired sampling rate (typically 0.75 dry cfm). Sampling was conducted until at least 22 dry cubic feet were collected. After sampling, the final meter readings were recorded and the impinger train was recovered. The change in volume and/or weight of the impinger train components was used to determine the amount of moisture condensed. The volume of water vapor and the corrected volume of dry gas sampled were used to calculate the moisture fraction as described above.

4.2 SCAQMD Method 5.1 - Total Particulate Matter

Measurements to determine total particulate matter were performed according to SCAQMD Method 5.1. In this method, a stack gas sample is isokinetically extracted from the stack through a stainless-steel nozzle and probe and transported to an impinger train in an ice bath. Entrained particulates were collected in the impingers and on a back-up filter placed between the 3rd and 4th impingers. Figure 4-3 is a schematic of the sampling apparatus.

Prior to testing, a series of measurements were made to determine location and number of traverse points, gas velocity, MW, and moisture content. The results of these measurements were used to determine the appropriate nozzle size for isokinetic sampling. The sampling rate was adjusted to maintain isokinetic conditions based on pitot and TC measurements.

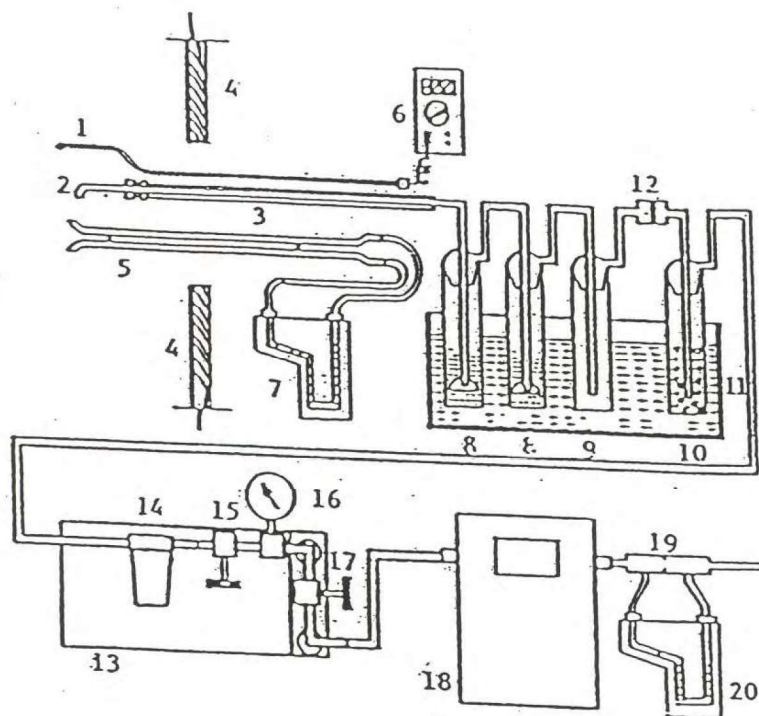
The sampling train was prepared by charging impingers # 1 and # 2 with 100 ml of D.I. water and impinger # 4 with approximately 200 g of silica gel. Impinger # 3 was left empty. Finally, the sampling train was sealed, transported to the sampling location, and leak-checked. Sampling was performed at each traverse point. After completing the test, the Method 5.1 sample was taken to a secured area (i.e., Mobile test van or Almega's laboratory) and recovered.

The recovered samples were entered into Almega's Sample Custody Program and delivered to the laboratory for analysis. At the laboratory, samples were analyzed as follows:

The filter was removed and placed in a desiccator until completely dry. Following drying, the filter was weighed to determine the fraction of sample acquired on the filter. The probe, nozzle, sampling lines, and impingers were washed with deionized water and methylene chloride, and the washing solutions were combined with the impinger solutions. The combined solution was extracted with methylene chloride. The aqueous fraction was heated to boil off water, and the organic fraction was allowed to evaporate at room temperature. Residues from both fractions were weighed and combined with the sample weight from the filter to determine the total particulate sample weight. Samples were stored at 4 °C until analyzed at the Almega in-house laboratory.

Field and laboratory data were used to calculate sample volume corrected to standard conditions, stack gas flow rate, and particulate emissions. Emissions were reported in gr/dscf and lb/hr.

Figure 4-1. Sampling Apparatus for Particulate Matter



- | | |
|--|--|
| 1. Temperature Sensor | 11. Ice Bath |
| 2. Nozzle | 12. Filter |
| 3. Glass Lined Stainless Steel Probe | 13. Sealed Pump (Leak Free) |
| 4. S-type Pitot Tube | 14. Filter for Pump |
| 5. Stack Wall | 15. Metering Valve |
| 6. Temperature Sensor Meter | 16. Vacuum Gauge |
| 7. Pitot Tube Inclined Manometer | 17. By-pass Valve |
| 8. Impinger with 100 ml H ₂ O | 18. Temperature Compensated
Dry Gas Meter |
| 9. Empty Bubbler | 19. Orifice |
| 10. Bubbler with Silica Gel | 20. Orifice Inclined Manometer |

4.3 SCAQMD METHOD 10.1 – INTEGRATED GAS SAMPLING (O₂ & CO₂)

In this method, gaseous components of the stack gas (e.g. O₂, & CO₂) are measured using integrated sampling in accordance with the procedures specified in SCAQMD Method 10.1. Sample was collected in a Tedlar bag for each test event and analyzed by Almega's in-house laboratory via GC.

4.4 Total and Hexavalent Chromium (CARB Method 425)

Hexavalent chromium and total chromium were measured according to CARB Method 425. The sampling was conducted isokinetically for 2-hours in order to achieve target detection limits. After sampling, the sampling train was recovered and analyzed for both total chromium and hexavalent chromium.

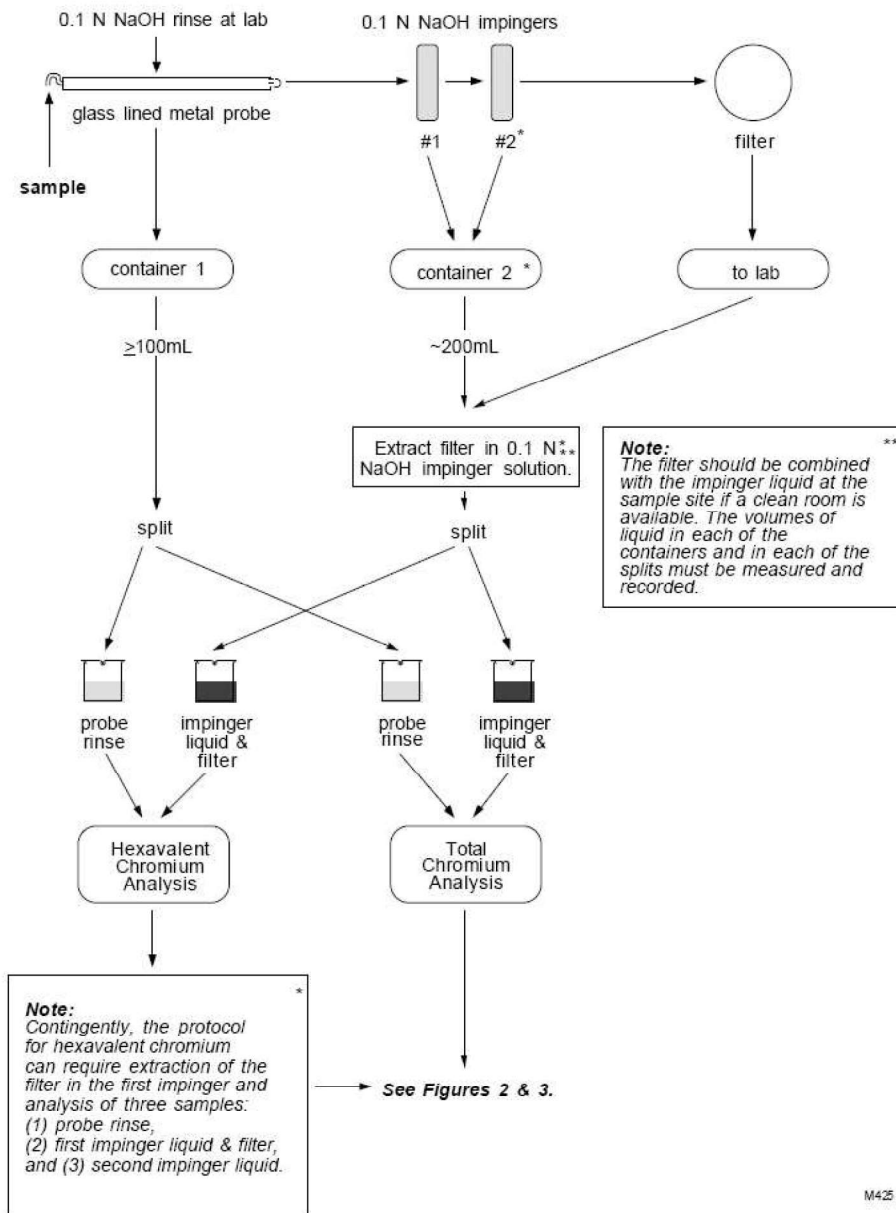
The sampling apparatus included a glass probe, a Teflon union, a flexible Teflon sample line from the probe to the first impinger, two Greenburg-Smith impingers each containing 100 ml of 0.1N NaHCO₃ solution, an empty modified impinger, and a modified impinger containing silica gel. The glass probe is fitted with a glass nozzle for isokinetic sampling. The remaining components of the sampling apparatus included an umbilical line, a vacuum pump, a dry gas meter, and a calibrated orifice connected to an inclined manometer. The sampling train is shown in Figure 4-3.

The volume of the impinger solution and the weight of the silica gel were recorded before and after the tests to determine the moisture content of the stack gas. All sample weights were recorded on the sampling data sheet during charging and sample recovery. Leak checks were performed before and after each test.

Volumetric flow rates at the sampling locations were calculated from the measured velocity head and the cross-sectional area of the duct. As each traverse point was sampled, the velocity head of the flue gas was measured with an S-type pitot tube connected to an inclined manometer, and the temperature of the flue gas was measured with a type "K" thermocouple and a digital readout (SCAQMD Method 2.1). This information was used to adjust the sampling rate to isokinetic conditions.

After the test, the contents of the impingers were recovered as described in the method and stored in pre-cleaned sample bottles. The final pH of the sample was verified using multiple-field pH paper. The samples were then stored at 4°C or less until delivered to the Laboratory for analysis. Samples were analyzed for hexavalent chromium as described in the method. Hexavalent chromium was determined by ion chromatography (IC) by Weck Laboratories, Inc. located in City of Industry, California. No sodium bicarbonate reagent blank was submitted since the values from the same sodium bicarbonate batch were on file from a previous test event. All samples are accompanied by a chain of custody until disposed.

Figure 4-2 CARB Method 425 Sampling



Note: 0.1NaHCO₃ was used instead 0.1NaOH.

4.5 CARB METHOD 436 - DETERMINATION OF MULTIPLE METALS EMISSIONS

Multiple metals samples were collected isokinetically in accordance with CARB Method 436, “Determination of Multiple Metals Emissions from Stationary Sources.” Stack sample was withdrawn from the source, with particulate emissions collected in the probe and on a heated filter and gaseous emissions collected in a series of chilled impingers containing an aqueous solution of dilute nitric acid combined with dilute hydrogen peroxide in two impingers.

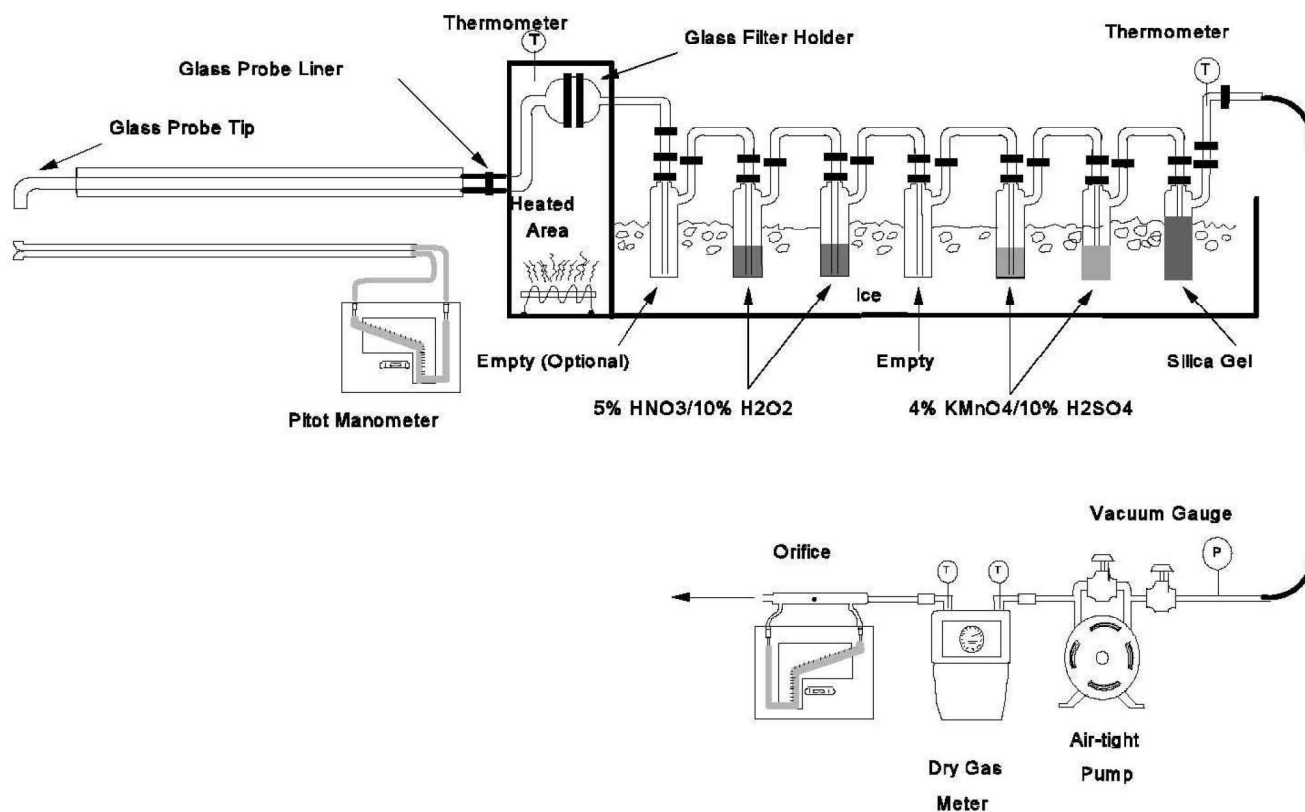
A schematic of the sampling apparatus is shown in Figure 4-2. The sampling train consists of a nozzle, heated probe, heated filter, and a series of three impingers immersed in an ice bath and a silica gel impinger. The probe is made of borosilicate glass with a heating system of maintaining an exit gas temperature during sampling of $248 \pm 25^\circ\text{F}$.

The Teflon line was used to transfer the sample from the filter to the impingers. The impinger train was setup as follows: the first and second impingers each contained 100 mL of a nitric acid/hydrogen peroxide solution (5% HNO_3 /10% H_2O_2), the third was empty, the last impinger contained silica gel (for moisture collection), and an umbilical line connected to an isokinetic sampling console. The sampling console includes a vacuum pump, a dry gas meter, and additional monitors and controls for collecting a sample. A thermometer capable of measuring to within 1°C (2°F) was placed at the outlet of the last impinger.

Sampling train components were recovered into separate front and back half fractions and acid digested using conventional digestion techniques to dissolve inorganic and to remove organic constituents that created analytical interferences. After digestion, portions of the probe catch, filter catch, and nitric acid/hydrogen peroxide catch were combined into a single composite sample and analyzed for all target metals according to ICP/MS as prescribed by the Method. Sample analyses were performed by Weck Laboratory in City of Industry, California.

Quality assurance samples include field blanks and reagent blanks. Quality control samples include laboratory method blanks and duplicates. Field sampling and laboratory data were used to calculate emissions concentrations and mass emission rates as described in the Method. Although no nitric reagent blank was submitted for this set of tests, the test results were corrected for background levels found in reagent blank results on-file from a previous test (same nitric batch). Results are reported for concentration in milligram per dry standard cubic meter (mg/dscm). Analysis results that are below the limit of detection (i.e. not detected or ND) were substituted for the one-half of detection limit in calculating three-run averages.

Figure 4-3. CARB Method 436 Sampling Apparatus



Note: Impingers 5 and 6 containing 4% KMnO₄/10% H₂SO₄ were not used in actual sampling since Mercury was not measured.

4.6 Verification of Capture/Collection Efficiency

SCAQMD conducted the verification of the capture and collection. The collection was deemed adequate for us to continue with the testing program. Detailed summary of the collection is available upon request.

5.0 QUALITY ASSURANCE AND QUALITY CONTROL

Almega applies stringent quality assurance and quality control (QA/QC) procedures to ensure the validity of measurements for all test methods. The following section discusses general and project-specific QA/QC measures.

5.1 General QA/QC

Almega's QA/QC procedures follow guidelines from the "Quality Assurance Handbook for Air Pollution Measurement Systems," Volume I through III. And, procedures for pretest preparation and calibration of sampling equipment are followed. Standardized written procedures, calculator programs, and computer spreadsheets are used for test planning, pre-survey, equipment checklist, preliminary calculations, testing, data analysis, and reporting. Pretest equipment preparation and maintenance include organization of the following equipment prior to testing:

- Mobile RM CEM test van: Check fluids, fuel, mechanical conditions, verify operation of CEM instruments, sample lines and sample conditioner prior to the date of the source test.
- Sampling Equipment: Check meter boxes, pitot tubes, manometers and thermocouples to ensure in good working conditions and in proper calibrations. Preclean sampling trains and seal all openings prior to use.

Calibrations are performed in accordance with Chapter III of the SCAQMD Source Test Manual (March 1989). Table 5-1 shows the test equipment calibration schedules. Table 5-2 shows the test equipment maintenance schedules.

5.2 Project-Specific QA/QC

This project included specific QA/QC activities required to validate the test results. These QA/QC activities are based on the test methods discussed in Section 5 and generally acceptable test procedures. Reference Methods used for source testing are promulgated by the South Coast Air Quality Management District (SCAQMD), the California Air Resource Board (CARB), or the US Environmental Protection Agency (EPA). Any deviations from published Methods are approved in advance by the regulatory agency (i.e. SCAQMD), prior to implementation if possible. Project-specific QA/QC activities and results that may impact test results are discussed in Section 3.

TABLE 5-1. TEST EQUIPMENT CALIBRATION SCHEDULE

Equipment	Calibration Period	Standard or Method of Calibration
Thermocouples	6 Months and 2 Months	Mercury Thermometer, three point (ice, boiling water, hot oil)
Dry Gas Meters	6 Months and 2 Months	Critical orifice
Field Barometers	6 Months, Check prior to usage	Mercury Barometer
S-Type Pitot	6 Months Check prior to usage	EPA Method 2, Measure physical configuration. Reshape pitot tips or calibrate if configuration does not meet the limits.
Pressure gauges	6 Months	Five-point calibration against manometer
	2 Months	Three-point check
Temp. Meters	6 Months	Precision Potentiometer
CEM Systems	Bimonthly, or as needed	Specified by Manufacturer

TABLE 5-2. TEST EQUIPMENT MAINTENANCE

Equipment	Check For	Correction	Frequency
CEM Systems	Absence of malfunction, noise, drift, conversion efficiency for NOx anlzr.	As required by the manufacture, or depending on performance	Bimonthly
Pumps	Absence of leakage, flow, proper vacuum	Replace parts, inspect, clean	300 hours of usage
Flow Devices	Levelling, zeroing, obstruction, deformation	Clean, replace, or re-calibrate	300 hours of usage
Calibration Gases	Expiration date, tank pressure	Re-certify, order new gases	2 months and prior to field testing
Regulators	Malfunction, Gauge precision	Repair or replace	3 months and prior to field testing
Gas Divider	Malfunction, precision	Repair or replace	Monthly and before field testing
Condensers	Leakage, temperature	Repair or replace	Monthly and before field testing
Heated lines	Leakage, temperature, cleanliness	Repair, replace, clean	Monthly and before field testing

6.0 TEST RESULTS AND DISCUSSION

The testing was conducted on August 13 through 16, 2019. The sampling locations and equipment were prepared prior to initiating the sampling activities. Testing was conducted after the arrival of Almega's test personnel and set-up of test equipment.

6.1 DISCUSSION

The scope of work included the testing to determine the emissions of Particulate Matter (PM) and selected metals (As, Cd, Ni, Cr, and Cr⁺⁶) at the two designated inlets and the outlet of the baghouse/HEPA system. The metals testing were conducted in triplicate with just a single run conducted for PM.

Test calculations are corrected to 68°F for CARB methods and 60°F for SCAQMD methods. The sampling system was setup on August 12, 2019. Sampling was conducted for all three locations on August 13 through 16, 2019.

The metals and PM emissions in the stack gas effluent were reported in micrograms per dry standard cubic meter ($\mu\text{g}/\text{dscm}$), microgram per dry standard cubic feet ($\mu\text{g}/\text{dscf}$), and pounds per hours (lbs/hr). The results are summarized in Table 1-1. Test-specific results for all three sampling locations are presented in Tables 6-1 through 6-9. Supporting data including calculations, field test data, laboratory analysis reports, and QA/QC data are found in the Appendices.

6.1.1 TEST RESULTS – CARB METHOD 436 MULTIPLE METALS

Sampling and analysis for Multiple Metals was conducted for the selected metals in triplicate according to CARB Method 436. The mercury testing option was not used. The CARB Method 436 sampling was conducted simultaneously for all three locations. The sampling duration for each run was two hours. The first and second runs were conducted on August 13 and the third run was conducted on August 14, 2019. The field blank was prepared and collected on August 13 before Run 1. Only Arsenic, Cadmium, Chromium, and Nickel were analyzed as purpose in this testing program. One set of reagent blank was analyzed for those selected metals and the reported results are corrected with the detectable results.

The detailed test results are presented in Table 6-1 for the outlet and Tables 6-4 and 6-7 for the inlets.

6.1.2 TEST RESULTS – CARB M425 HEXAVALENT CHROMIUM AND TOTAL CHROMIUM

Sampling and analysis for hexavalent chromium and total chromium was conducted in triplicate according to CARB Method 425 simultaneously at all three locations. The sampling duration for each run was two hours. The first run was conducted on August 14 with the remaining two runs conducted on August 15, 2019. The field blank was prepared and collected on August 14 before

Run 1. The CARB Method 425 test method used was modified to include the absorbing solution of 0.1N sodium bicarbonate. One set of reagent blank was analyzed for hexavalent chromium and total chromium, the reagent blank results were not detected, and no correction was necessary.

These samples were analyzed within the holding time recommended by the method. However, the samples were re-analyzed to achieve a lower reporting limit without dilution and that second analysis exceeded the recommended holding time (see detail in CARB Method 425 lab report).

The detailed test results are presented in Table 6-2 for the outlet and Tables 6-5 and 6-8 for the inlets.

6.1.3 TEST RESULTS – PARTICULATE MATTER

The single run sampling and analysis for particulate matter was conducted according to SCAQMD Method 5.1. The sampling duration for the test run was 72-minutes. The sampling for PM was conducted simultaneously for all three locations on August 16, 2019. The field blank was prepared and collected prior to sampling.

The detailed test results are presented in Table 6-3 for the outlet and Tables 6-6 and 6-9 for the inlets.

6.2 OTHERS

- Filter and probe temperatures were maintained at $248 \pm 25^{\circ}\text{F}$ for CARB Method 436 isokinetic sampling.
- Each impinger solution was maintained at a pH greater than eight (8) for CARB Method 425.
- Impinger trains and XAD temperatures, where applicable, were maintained below 68°F for all sampling event.
- Percent (%) Isokinetics was within the allowable range of 90-110% for all isokinetic sampling events.
- Cyclonic flow check was performed prior to sampling. No cyclonic flow was found.
- The single bag sample was collected at each test location over a period of 60 minutes. These samples were analyzed for oxygen and carbon dioxide via SCAQMD Method 10.1. The analysis of those bag samples shows that the O_2/CO_2 concentration for all sampling locations is in ambient level.
- No unusual operating conditions or field-testing observations were reported. Field data and calculations for all the emissions are presented in respective appendices.

- Although no nozzle diameters were recorded on the Method 436 data sheets for Runs 2 and 3, the nozzles were the same as used for Run 1 and hence the same diameter.
- The measured flow rates (dP) at the exhaust test location were approaching the reporting limits of the inclined manometer system used for the measurements. Upon request by the District, a direct comparison of the flows across the stack was collected between the “as-used” inclined manometer and a low-flow ADM electronic meter (Appendix G). The results of the comparison show the readings from the inclined manometer were within 10% (7.8%) of the ADM average values and could be considered as “biased low”.

Testing was performed as specified in the reference methods and the SCAQMD Source Test Plan. No modifications to proposed sampling and analysis procedures other than those noted above were required.

6.3 TEST CHRONOLOGY

All testing was conducted during the periods listed below:

Parameter Measurement	Test Date	Time	Run No.
CARB Method 436 Baghouse Outlet, Inlet 1 (inside), and Inlet 2 (upstream to Baghouse)	08/13/19	08:50 – 10:55	Run 1
	08/13/19	11:55 – 14:00	Run 2
	08/14/19	08:25 – 10:30	Run 3
CARB Method 425 Baghouse Outlet, Inlet 1 (inside), and Inlet 2 (upstream to Baghouse)	08/14/19	11:25 – 13:30	Run 1
	08/15/19	08:10 – 10:15	Run 2
	08/15/19	10:55 – 13:10	Run 3
SCAQMD Method 5.1 Baghouse Outlet, Inlet 1 (inside), and Inlet 2 (upstream to Baghouse)	08/16/19	07:40 – 08:56	Run 1

**TABLE 6-1. TEST RESULTS
CARB 436 (Multiple Metals)**

Facility: AQMD Facility C
 City: ████████ CA
 Source: Baghouse
 Location: Outlet

Test Data	Units	Source Test Results			Average				
Run Number	--	Run 1	Run 2	Run 3					
Test Date	mm/dd/yy	08/13/19	08/13/19	08/14/19	--				
Test Time	hh:mm	08:50 - 10:55	11:55 - 14:00	08:25 - 10:30	--				
<u>Sampling Data*</u>									
Stack Temperature	°F	93.9	109	96.5	99.8				
Moisture	%	1.9	2.1	2.1	2.0				
Sample Volume	dscf	82.4	73.1	80.1	78.5				
Oxygen**	% v/v	20.9	20.9	20.9	20.9				
Carbon Dioxide**	% v/v	< 0.3	< 0.3	< 0.3	< 0.3				
Gas Velocity	ft/min	671	608	658	646				
Stack Flow Rate	acfm	8,436	7,642	8,268	8,115				
Stack Flow Rate	dscfm	7,883	6,940	7,674	7,499				
<u>CARB Method 436</u>									
<u>CONCENTRATION</u>									
			<u>Total</u>		<u>Total</u>				
Arsenic	ug/dscm	ND	0.43	ND	0.48	ND	0.44	<	0.45
	ug/dscf	ND	0.012	ND	0.014	ND	0.012	<	0.013
Cadmium	ug/dscm	ND	0.43	ND	0.48	ND	0.44	<	0.45
	ug/dscf	ND	0.024	ND	0.027	ND	0.025	<	0.026
Chromium	ug/dscm		1.63		0.68		1.98		1.43
	ug/dscf		0.05		0.02		0.06		0.04
Nickel	ug/dscm		0.69		0.34		0.62		0.55
	ug/dscf		0.019		0.010		0.017		0.015
<u>CARB Method 436</u>									
<u>MASS EMISSION RATE</u>									
			<u>Total</u>		<u>Total</u>		<u>Total</u>		
Arsenic	lb/hr	ND	1.27E-05	ND	1.26E-05	ND	1.27E-05	<	1.26E-05
Cadmium	lb/hr	ND	1.27E-05	ND	1.26E-05	ND	1.27E-05	<	1.26E-05
Chromium	lb/hr		4.81E-05		1.76E-05		5.70E-05		4.09E-05
Nickel	lb/hr		2.02E-05		8.79E-06		1.77E-05		1.56E-05

Notes:

* Performed during isokinetic sampling (e.g. CARB Method 436).

** Measured via SCAQMD Method 10.1.

ND or "<" - Not detected, reporting limit reported.

**TABLE 6-2. TEST RESULTS
CARB 425 (Hexavalent & Total Chromium)**

Facility: AQMD Facility C
 City: ████████ CA
 Source: Baghouse
 Location: Outlet

TEST DATA	UNITS	TEST RESULTS			AVERAGE
		Run 1	Run 2	Run 3	
Run Number	-	Run 1	Run 2	Run 3	
Test Date	mm/dd/yy	8/14/19	8/14/19	8/15/19	--
Test Time	hh:mm	11:25 - 13:30	08:10 - 10:15	10:55 - 13:10	--
<u>Sampling Data*</u>					
Stack Temperature	°F	117.1	87.1	104.6	102.9
Moisture	%	2.3	1.9	2.4	2.2
Sample Volume	dscf	73.1	85.3	70.8	76.4
Oxygen**	% v/v	20.9	20.9	20.9	20.9
Carbon Dioxide**	% v/v	<0.3	<0.3	<0.3	<0.3
Gas Velocity	ft/min	613.6	685.1	585.5	628
Stack Flow Rate	acfm	7,711	8,609	7,358	7,893
Stack Flow Rate	dscfm	6,885	8,143	6,708	7,245
<u>Total Catch (CARB 425)</u>					
Chromium VI	ug	< 0.312	< 0.032	< 0.046	< 0.13
Total Chromium	ug	< 0.550	< 0.590	< 0.600	< 0.58
<u>Concentration (CARB 425)</u>					
Chromium VI	ug/dscm	< 0.151	< 0.013	< 0.023	< 0.062
	ug/dscf	< 0.004	< 0.0004	< 0.001	< 0.0018
Total Chromium	ug/dscm	< 0.266	< 0.244	< 0.299	< 0.270
	ug/dscf	< 0.0075	< 0.0069	< 0.0085	< 0.0076
<u>Mass Emissions (CARB 425)</u>					
Chromium VI	ug/hr	< 1763	< 180	< 261	< 735
Chromium VI	mg/hr	< 1.76	< 0.18	< 0.26	< 0.73
Chromium VI	lb/hr	< 3.89E-06	< 3.98E-07	< 5.76E-07	< 1.62E-06
Total Chromium	ug/hr	< 3107	< 3380	< 3410	< 3299
Total Chromium	mg/hr	< 3.11	< 3.38	< 3.41	< 3.30
Total Chromium	lb/hr	< 6.85E-06	< 7.45E-06	< 7.52E-06	< 7.27E-06

Notes:

* Performed during isokinetic sampling by CARB 425.

** O2/CO2 was measured via SCAQMD Method 10.1 by GC.

"<" Indicates an analytical result of non-detect (ND) and the use of laboratory MRL for emission calculations.

**TABLE 6-3. TEST RESULTS
SCAQMD Method 5.1 (Particulate Matter)**

Facility: AQMD Facility C

City: [REDACTED] CA

Source: Baghouse

Location: Outlet

Run Number	1	
Run Date	08/16/19	
Run Start Time	7:40	
Run Stop Time	8:56	
Test Train Parameters		AVERAGE
Volume of Dry Gas Sample, SCF*	39.73	39.73
Flue Gas Parameters		
CO ₂ , Percent By Volume, Dry**	< 0.30	< 0.30
O ₂ , Percent By Volume, Dry**	20.90	20.90
Temperature, Degrees F	87.6	87.6
Moisture, %	1.93	1.93
Air Flow Rate, Wet ACFM	6,705	6,705
Air Flow Rate, Dry SCFM*	6,240	6,240
Total Particulate		
Catch, mg	6.57	6.57
Concentration, Gr/DSCF	0.002552	0.002552
Emission Rate, lb/hr	0.136	0.136

Notes:

* 60 Degrees F and 29.92 Inches of Mercury

** O₂/CO₂ was sampled in Tedlar bag and analyzed via SCAQMD Method 10.1 by GC.

**TABLE 6-4. TEST RESULTS
CARB 436 (Multiple Metals)**

Facility: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Test Data	Units	Source Test Results			Average
		Run 1	Run 2	Run 3	
Run Number	--				
Test Date	mm/dd/yy	08/13/19	08/13/19	08/14/19	--
Test Time	hh:mm	08:50 - 10:55	11:55 - 14:00	08:25 - 10:30	--
<u>Sampling Data*</u>					
Stack Temperature	°F	116	126	101	114
Moisture	%	2.0	2.1	1.9	2.0
Sample Volume	dscf	86.7	88.8	90.1	88.6
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	< 0.3	< 0.3	< 0.3	< 0.3
Gas Velocity	ft/min	1,228	1,277	1,241	1,249
Stack Flow Rate	acfm	1,132	1,177	1,144	1,151
Stack Flow Rate	dscfm	1,012	1,035	1,052	1,033
<u>CARB Method 436</u>					
<u>CONCENTRATION</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	ug/dscm	6.11	3.06	1.18	3.45
	ug/dscf	0.173	0.087	0.033	0.098
Cadmium	ug/dscm	ND 0.407	ND 0.398	ND 0.392	< 0.399
	ug/dscf	ND 0.023	ND 0.023	ND 0.022	< 0.023
Chromium	ug/dscm	1790.9	2822.2	1567	2060
	ug/dscf	50.71	79.92	44.38	58.33
Nickel	ug/dscm	37.7	94.90	50.4	61.0
	ug/dscf	1.069	2.687	1.428	1.728
<u>CARB Method 436</u>					
<u>MASS EMISSION RATE</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	lb/hr	2.32E-05	1.19E-05	4.63E-06	1.32E-05
Cadmium	lb/hr	ND 1.54E-06	ND 1.54E-06	ND 1.88E-06	< 1.66E-06
Chromium	lb/hr	6.79E-03	1.09E-02	6.17E-03	7.97E-03
Nickel	lb/hr	1.43E-04	3.68E-04	1.99E-04	2.37E-04

Notes:

* Performed during isokinetic sampling (e.g. CARB Method 436).

** Measured via SCAQMD Method 10.1.

ND or "<" - Not detected, reporting limit reported.

**TABLE 6-5. TEST RESULTS
CARB 425 (Hexavalent & Total Chromium)**

Facility: AQMD Facility C
 City: ████████ CA
 Source: Baghouse
 Location: Inlet 1

TEST DATA	UNITS	TEST RESULTS			AVERAGE
		Run 1	Run 2	Run 3	
Run Number	-	Run 1	Run 2	Run 3	
Test Date	mm/dd/yy	8/14/19	8/14/19	8/15/19	--
Test Time	hh:mm	11:25 - 13:30	08:10 - 10:15	10:55 - 13:10	--
<u>Sampling Data*</u>					
Stack Temperature	°F	131	114	142	129
Moisture	%	1.6	1.6	1.7	1.7
Sample Volume	dscf	85.3	92.6	86.3	88.1
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	0.30	0.30	0.30	0.30
Gas Velocity	ft/min	1,238.5	1,303.0	1,273.8	1,272
Stack Flow Rate	acfm	1,142	1,201	1,174	1,172
Stack Flow Rate	dscfm	998	1,083	1,008	1,030
<u>Total Catch (CARB 425)</u>					
Chromium VI	ug	0.82	21.9	21.2	14.6
Total Chromium	ug	2540	330	1007	1292
<u>Concentration (CARB 425)</u>					
Chromium VI	ug/dscm	0.34	8.35	8.68	5.79
	ug/dscf	0.010	0.237	0.246	0.164
Total Chromium	ug/dscm	1052	125.9	412.1	529.9
	ug/dscf	29.78	3.56	11.67	15.00
<u>Mass Emissions (CARB 425)</u>					
Chromium VI	ug/hr	575	15369	14859	10268
Chromium VI	mg/hr	0.57	15.37	14.9	10.3
Chromium VI	lb/hr	1.27E-06	3.39E-05	3.28E-05	2.26E-05
Total Chromium	ug/hr	1784014	231584	705479	907026
Total Chromium	mg/hr	1784	232	705	907
Total Chromium	lb/hr	3.93E-03	5.11E-04	1.56E-03	2.00E-03

Notes:

* Performed during isokinetic sampling by CARB 425.

** O2/CO2 was measured via SCAQMD Method 10.1 by GC.

**TABLE 6-6. TEST RESULTS
SCAQMD Method 5.1 (Particulate Matter)**

Facility: AQMD Facility C

City: [REDACTED] CA

Source: Baghouse

Location: Inlet 1

Run Number	1	
Run Date	08/16/19	
Run Start Time	7:40	
Run Stop Time	8:56	
Test Train Parameters		AVERAGE
Volume of Dry Gas Sample, SCF*	53.50	53.50
Flue Gas Parameters		
CO2, Percent By Volume, Dry**	< 0.30	< 0.30
O2, Percent By Volume, Dry**	20.80	20.80
Temperature, Degrees F	100.8	100.8
Moisture, %	1.80	1.80
Air Flow Rate, Wet ACFM	1,147	1,147
Air Flow Rate, Dry SCFM*	1,040	1,040
Total Particulate		
Catch, mg	105.57	105.57
Concentration, Gr/DSCF	0.0305	0.0305
Emission Rate, lb/hr	0.271	0.271

Notes:

* 60 Degrees F and 29.92 Inches of Mercury

** O2/CO2 was sampled in Tedlar bag and analyzed via SCAQMD Method 10.1 by GC.

**TABLE 6-7. TEST RESULTS
CARB 436 (Multiple Metals)**

Facility: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2

Test Data	Units	Source Test Results			Average
Run Number	--	Run 1	Run 2	Run 3	
Test Date	mm/dd/yy	08/13/19	08/13/19	08/14/19	--
Test Time	hh:mm	08:50 - 10:55	11:55 - 14:00	08:25 - 10:30	--
<u>Sampling Data*</u>					
Stack Temperature	°F	91.9	99.0	95.5	95.5
Moisture	%	2.1	2.0	2.3	2.1
Sample Volume	dscf	98.9	95.5	94.1	96.2
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	< 0.3	< 0.3	< 0.3	< 0.3
Gas Velocity	ft/min	4,765	4,649	4,568	4,661
Stack Flow Rate	acfm	6,653	6,491	6,379	6,507
Stack Flow Rate	dscfm	6,164	5,942	5,861	5,989
<u>CARB Method 436</u>					
<u>CONCENTRATION</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	ug/dscm	1.32	0.67	0.56	0.85
	ug/dscf	0.037	0.019	0.016	0.024
Cadmium	ug/dscm	ND 0.357	ND 0.370	ND 0.375	< 0.367
	ug/dscf	ND 0.020	ND 0.021	ND 0.021	< 0.021
Chromium	ug/dscm	356.4	553.9	600	503
	ug/dscf	10.09	15.68	16.99	14.25
Nickel	ug/dscm	11.0	19.11	20.2	16.7
	ug/dscf	0.310	0.541	0.571	0.474
<u>CARB Method 436</u>					
<u>MASS EMISSION RATE</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	lb/hr	3.05E-05	1.48E-05	1.24E-05	1.92E-05
Cadmium	lb/hr	ND 8.24E-06	ND 8.23E-06	ND 1.01E-05	< 8.84E-06
Chromium	lb/hr	8.23E-03	1.23E-02	1.32E-02	1.12E-02
Nickel	lb/hr	2.53E-04	4.25E-04	4.42E-04	3.74E-04

Notes:

* Performed during isokinetic sampling (e.g. CARB Method 436).

** Measured via SCAQMD Method 10.1.

ND or "<" - Not detected, reporting limit reported.

**TABLE 6-8. TEST RESULTS
CARB 425 (Hexavalent & Total Chromium)**

Facility: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2

TEST DATA	UNITS	TEST RESULTS			AVERAGE
		Run 1	Run 2	Run 3	
Run Number	-				
Test Date	mm/dd/yy	8/14/19	8/14/19	8/15/19	--
Test Time	hh:mm	11:25 - 13:30	08:10 - 10:15	10:55 - 13:10	--
<u>Sampling Data*</u>					
Stack Temperature	°F	112.3	86.1	96.9	98.4
Moisture	%	2.0	2.1	1.9	2.0
Sample Volume	dscf	89.8	97.3	92.2	93.1
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	0.30	0.30	0.30	0.30
Gas Velocity	ft/min	4,481.7	4,560.9	4,485.3	4,509
Stack Flow Rate	acfm	6,258	6,368	6,263	6,296
Stack Flow Rate	dscfm	5,597	5,958	5,757	5,771
<u>Total Catch (CARB 425)</u>					
Chromium VI	ug	2.89	5.30	3.90	4.03
Total Chromium	ug	469	70.0	280	273
<u>Concentration (CARB 425)</u>					
Chromium VI	ug/dscm	1.14	1.92	1.49	1.52
	ug/dscf	0.032	0.054	0.042	0.043
Total Chromium	ug/dscm	184.50	25.42	107.29	105.7
	ug/dscf	5.22	0.72	3.04	2.99
<u>Mass Emissions (CARB 425)</u>					
Chromium VI	ug/hr	10812	19479	14618	14969
Chromium VI	mg/hr	10.8	19.48	14.6	15.0
Chromium VI	lb/hr	2.38E-05	4.29E-05	3.22E-05	3.30E-05
Total Chromium	ug/hr	1754573	257267	1049466	1020435
Total Chromium	mg/hr	1755	257	1049	1020
Total Chromium	lb/hr	3.87E-03	5.67E-04	2.31E-03	2.25E-03

Notes:

* Performed during isokinetic sampling by CARB 425.

** O2/CO2 was measured via SCAQMD Method 10.1 by GC.

**TABLE 6-9. TEST RESULTS
SCAQMD Method 5.1 (Particulate Matter)**

Facility: AQMD Facility C

City: [REDACTED] CA

Source: Baghouse

Location: Inlet 2

Run Number	1	
Run Date	08/16/19	
Run Start Time	7:40	
Run Stop Time	8:56	
Test Train Parameters		AVERAGE
Volume of Dry Gas Sample, SCF*	55.51	55.51
Flue Gas Parameters		
CO ₂ , Percent By Volume, Dry**	< 0.30	< 0.30
O ₂ , Percent By Volume, Dry**	20.80	20.80
Temperature, Degrees F	93.2	93.2
Moisture, %	2.26	2.26
Air Flow Rate, Wet ACFM	6,412	6,412
Air Flow Rate, Dry SCFM*	5,825	5,825
Total Particulate		
Catch, mg	45.22	45.22
Concentration, Gr/DSCF	0.0126	0.0126
Emission Rate, lb/hr	0.628	0.628

Notes:

* 60 Degrees F and 29.92 Inches of Mercury

** O₂/CO₂ was sampled in Tedlar bag and analyzed via SCAQMD Method 10.1 by GC.

APPENDICES

APPENDIX A
GENERAL CALCULATIONS AND FORMULAE

GENERAL CALCULATIONS

Standard conditions: 29.92 in.Hg, 68 °F for CARB, 60°F for SCAQMD

Gas Moisture at standard conditions (scf): $V_{WTR} = K2 * V_{COND}$
 $K2 = 0.04707 @ 68 °F, 0.0464 @ 60 °F$

Sample volume at standard conditions (scf):
 $V_{mstd} = K1 * V_{macf} * Y_m * (P_{bar} + dH/13.6) / (T_m + 460)$
 $K1 = 17.64 @ 68 °F, 17.38 @ 60 °F$

Percent of water: $\%H_2O = 100 * V_{mstd} / (V_{mstd} + V_{wtr})$

Dry molecular weight: $M_d = (44 * \%CO_2 + 32 * \%O_2 + 28 * (\%N_2 + \%CO)) / 100$

Wet molecular weight: $M_w = M_d * (1 - \%H_2O / 100) + 18 * (\%H_2O / 100)$

Stack gas pressure (In. Hg): $P_{stk} = P_{bar} + P_{sta} / 13.6$

Average velocity head: $Ave. dP = \{SQRT(dP)\}^2$

Stack gas velocity (fps): $V = 85.49 * C_p * SQRT(dP) * SQRT((T_s + 460) / (P_{STK} * M_w))$

Percent of excess air: $\%EXCA = 100 * (\%O_2 - 0.5\%CO) / (0.264(\%N_2 - (\%O_2 - 0.5\%CO)))$

Stack gas flow (scfm): $Q_{STK} = 60(1 - \%H_2O / 100) * V * A * (528 / (T_s + 460)) * P_{stk} / 29.92$

Concentration at 3% O₂: $PPM @ 3\% O_2 = PPM_{measured} * 17.9 / (20.9 - \%O_2)$

Emissions lb/MMBtu:
 $lb/MMBtu = PPM * 10^{-6} * (MW \text{ lb/lb-mole}) / SV \text{ Mole} * F_d * 20.9 / (20.9 - \%O_2)$

Emissions lb/hr:
 $lb/hr = PPM * 10^{-6} * ((MW \text{ lb/lb-mole}) / SV) * F_d * FF * (1050 \text{ Btu/scf}) * 20.9 / (20.9 - \%O_2)$

Concentration (ug/dscm), $C_i = M_i / V_{mStd} * 35.315$

Metals Mass Emission Rate (ug/hr), $E_{i,m} = C_i * Q_{sdm} * 60,$

Metals Mass Emission Rate (lbs/hr) = $E_i / 453.6 / 1000000$

DEFINITIONS

A:	Stack cross area, Square feet
Cp:	Pitot coefficient
@h:	Orifice Pressure, In. H2O
MW:	Molecular weight
Md:	Dry molecular weight of flue gas
Mw:	Wet molecular weight of flue gas
Pbar:	Barometric pressure, In. Hg
Psta:	Static Pressure, In. H2O
Pstk:	Stack pressure, In, Hg
P:	Stack differential pressure, In. H2O
Qstk:	Stack gas flow, scfm
Tm:	Meter temperature, F
Ts:	Stack gas temperature, F
Vcond:	Volume of water condensation, ml
Vm:	Meter volume, acf
Vmstd:	Sample gas at standard conditions, scf
Vwtr:	Water vapor volume, scf
Ym:	Meter correction factor
SV:	Specific molar volume, 379.5 dscf/Lb.mole at 60F, or 385.3 dscf/Lb.mole at 68F
FF:	Fuel Flow Rate (SCF/HR)
Fd:	Dry Fuel Factor, for natural gas $F_d=8710 \text{ Dscf/MMBTU}$ at 68F.

APPENDIX B
APPROVALS AND CERTIFICATIONS

APPENDIX B1
SCAQMD AND CARB TESTING APPROVALS



South Coast Air Quality Management District

21865 Copley Drive, Diamond Bar, CA 91765-4178
(909) 396-2000 · www.aqmd.gov



May 29, 2019

Mr. John W. Phillips
Almega Environmental
10602 Walker Street
Cypress, CA 90630

Subject: LAP Approval Notice
Reference # 93LA0827

Dear Mr. Phillips:

We completed our review of the renewal application you submitted for approval under the South Coast Air Quality Management District's Laboratory Approval Program (LAP). We are pleased to inform you that your firm is approved for the period beginning June 30, 2019, and ending June 30, 2020 for the following methods, subject to the requirements in the LAP Conditions For Approval Agreement and conditions listed in the attachment to this letter:

SCAQMD Methods 1-4	SCAQMD Method 7.1
SCAQMD Method 10.1	SCAQMD Rule 1121/ 1146.2 Protocols
SCAQMD Method 100.1	SCAQMD Rule 1420/1420.1/ 1420.2 – (Lead) Source Sampling
SCAQMD Method 25.1 (Sampling)	SCAQMD Rule 1420/1420.1/ 1420.2 – (Lead) Ambient Sampling
SCAQMD Method 25.1 (Analysis)	SCAQMD Rule 462 Testing
SCAQMD Method 25.3 (Analysis)	ASTM D6522-00/ USEPA CTM-030
SCAQMD Methods 5.1 and 6.1	

Thank you for participating in the LAP. Your cooperation helps us to achieve the goal of the LAP: to maintain high standards of quality in the sampling and analysis of source emissions. You may direct any questions or information to LAP Coordinator, Glenn Kasai. He may be reached by telephone at (909) 396-2271, or via e-mail at gkasai@aqmd.gov.

Sincerely,

Dipankar Sarkar
Program Supervisor
Source Test Engineering

GK/gk

190529 LapRenewal.doc

ATTACHMENT
Conditions For Almega Environmental's
LAP Approval

- 1) **Almega shall adhere to the following requirements when conducting portable analyzer tests using CTM-030 or ASTM D6522:**
 - a) **Deviations to CTM-030 or ASTM D6522 shall be documented in the Test Critique section of the test report;**
 - b) **The test report shall be formatted and organized in a manner consistent with the example portable analyzer test report, dated September 24, 2011, and the Source Test Manual, Chapter II; and,**
 - c) **NO₂ measurements may be quantified to 10% of the NO₂ span under the following conditions:**
 - **Calibrations shall be conducted per Sections 7.3 and 7.6 of CTM-030 at the span, mid-span (40-60% of span), low-span (10% of span), and zero level. The low-span calibration shall satisfy the requirements in Section 4.2 of CTM-030;**
 - **A linearity check shall be conducted once every five days using the low-span calibration gas; and,**
 - **If the measured NO₂ emission is less than 10% of the NO₂ span, it shall be reported as less than 10% of the span, and added to the NO emission to determine the total NO_x concentration.**

State of California
Air Resources Board
Approved Independent Contractor
Almega Environmental & Technical Services, Incorporated

This is to certify that the company listed above has been approved by the California Air Resources Board to conduct compliance testing pursuant to California Code of Regulations, title 17, section 91207, through June 30, 2020, for the test methods listed below:

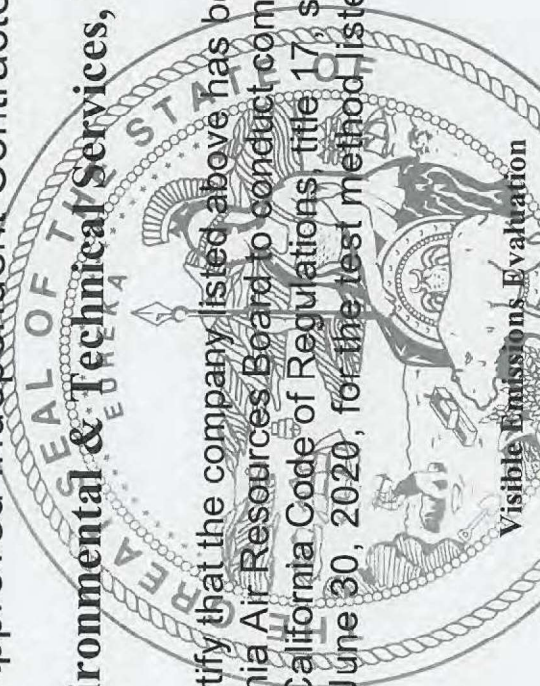


Catherine Dunwoody

Catherine Dunwoody, Chief
Monitoring and Laboratory Division

State of California
Air Resources Board
Approved Independent Contractor
Almega Environmental & Technical Services, Incorporated

This is to certify that the company listed above has been approved by the California Air Resources Board to conduct compliance testing pursuant to California Code of Regulations, title 17, section 91207, through June 30, 2020, for the test method listed below:



Catherine Dunwoody

Catherine Dunwoody, Chief
Monitoring and Laboratory Division

APPENDIX B2
CERTIFICATION OF NO CONFLICT-OF-INTEREST

Certification of No Conflict-of-Interest

Almega Environmental & Technical Services
10602 Walker Street
Cypress, CA 90630

I certify that I am responsible for the testing operations of Almega and am authorized to sign this certificate on the Company's behalf.

Almega may conduct tests as an independent tester pursuant to SCAQMD Rule 304(k). I further certify that Almega has no conflict-of-interests and is not related or owned in any way to the company being tested.

Company being tested: Metal Melting Facility C

Facility Location: [REDACTED]

Facility ID: [REDACTED]

Signature: *Charles M. Figueroa*

Name (printed or typed): Charles M. Figueroa

Title: Senior Project Manager

Date: November 8, 2019

APPENDIX C

CARB METHOD 436 – MULTIPLE METAL EMISSIONS

APPENDIX C1

MULTIPLE METAL EMISSIONS – RESULTS AND CALCULATIONS

Location: Baghouse Outlet

TEST RESULTS CARB 436 (Multiple Metals)

Facility: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Test Data	Units	Source Test Results						Average
Run Number	--	Run 1		Run 2		Run 3		
Test Date	mm/dd/yy	08/13/19		08/13/19		08/14/19		--
Test Time	hh:mm	08:50 - 10:55		11:55 - 14:00		08:25 - 10:30		--
<u>Sampling Data*</u>								
Stack Temperature	°F	93.9		109		96.5		99.8
Moisture	%	1.9		2.1		2.1		2.0
Sample Volume	dscf	82.4		73.1		80.1		78.5
Oxygen**	% v/v	20.9		20.9		20.9		20.9
Carbon Dioxide**	% v/v	< 0.3		< 0.3		< 0.3		< 0.3
Gas Velocity	ft/min	671		608		658		646
Stack Flow Rate	acfm	8,436		7,642		8,268		8,115
Stack Flow Rate	dscfm	7,883		6,940		7,674		7,499
<u>CARB Method 436</u>								
<u>CONCENTRATION</u>								
			<u>Total</u>		<u>Total</u>		<u>Total</u>	
Arsenic	ug/dscm	ND	0.43	ND	0.48	ND	0.44	< 0.45
	ug/dscf	ND	0.012	ND	0.014	ND	0.012	< 0.013
Cadmium	ug/dscm	ND	0.43	ND	0.48	ND	0.44	< 0.45
	ug/dscf	ND	0.024	ND	0.027	ND	0.025	< 0.026
Chromium	ug/dscm		1.63		0.68		1.98	1.43
	ug/dscf		0.05		0.02		0.06	0.04
Nickel	ug/dscm		0.69		0.34		0.62	0.55
	ug/dscf		0.019		0.010		0.017	0.015
<u>CARB Method 436</u>								
<u>MASS EMISSION RATE</u>								
			<u>Total</u>		<u>Total</u>		<u>Total</u>	
Arsenic	lb/hr	ND	1.27E-05	ND	1.26E-05	ND	1.27E-05	< 1.26E-05
Cadmium	lb/hr	ND	1.27E-05	ND	1.26E-05	ND	1.27E-05	< 1.26E-05
Chromium	lb/hr		4.81E-05		1.76E-05		5.70E-05	4.09E-05
Nickel	lb/hr		2.02E-05		8.79E-06		1.77E-05	1.56E-05

Notes:

* Performed during isokinetic sampling (e.g. CARB Method 436).

** Measured via SCAQMD Method 10.1.

ND or "<" - Not detected, reporting limit reported.

CARB METHOD 436 DATA AND CALCULATIONS

Plant:	AQMD Facility C	Test Date(s):	08/13-14/19
City:	██████████ CA	Operator:	NC
Source:	Baghouse	Entered by:	TG
Location:	Outlet	Checked by:	CF

Metals Catch, Mi		Run 1		Run 2		Run 3		Field Blank		Reagent Blank	
Fraction		Results		Results		Results		Results		Results	
Arsenic	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.0	ND	1.00
Cadmium	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.0	ND	1.00
Chromium	ug		5.3		2.9		6.0		1.6		1.50
Nickel	ug		2.9		2.0		2.7		1.4		1.30

Reagent Blank		Run 1		Run 2		Run 3		Field Blank		
Fraction		Results		Results		Results		Results		
Arsenic	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.0	
Cadmium	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.0	
Chromium	ug		1.5		1.5		1.50		1.5	
Nickel	ug		1.3		1.3		1.30		1.3	

Reagent Blank Corrected Values		Run 1		Run 2		Run 3		Field Blank		Reporting Limit*
Fraction		Results		Results		Results		Results		
Arsenic	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.0	
Cadmium	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.0	
Chromium	ug		3.8		1.4		4.5		0.10	0.30
Nickel	ug		1.6		0.7		1.4		0.10	0.30

*Reporting limit is based on three times the FB values.

CARB METHOD 436 DATA AND CALCULATIONS

Plant:	AQMD Facility C	Test Date(s):	08/13-14/19
City:	██████████ CA	Operator:	NC
Source:	Baghouse	Entered by:	TG
Location:	Outlet	Checked by:	CF

Metals Catch, Mi		Run 1		Run 2		Run 3		Field Blank	Reagent Blank
Fraction		Total		Total		Total		Total	Total
Arsenic	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.00
Cadmium	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.00
Chromium	ug	B	3.8	B	1.4	B	4.5	1.5	1.50
Nickel	ug	B	1.6	B	0.7	B	1.4	1.3	1.30
Metals Molecular Weight, MW		Run 1		Run 2		Run 3			
Fraction		Total		Total		Total			
Arsenic	g/g-mole	74.92		74.92		74.92			
Cadmium	g/g-mole	112.41		112.41		112.41			
Chromium	g/g-mole	51.995		51.995		51.995			
Nickel	g/g-mole	58.69		58.69		58.69			
Concentration (ug/dscm), Ci = Mi/VmStd *35.315e-3cf/dscm									
Fraction		Total		Total		Total			
Arsenic	ug/dscm	ND	0.43	ND	0.48	ND	0.44		
Cadmium	ug/dscm	ND	0.4285	ND	0.4829	ND	0.4410		
Chromium	ug/dscm	1.628		0.676		1.985			
Nickel	ug/dscm	0.6857		0.3381		0.617			
Metals Mass Emission Rate (ug/hr), Ei,m Ei = Ci*Qsdm*60									
Fraction		Total		Total		Total			
Arsenic	ug/hr	ND	5.74E+03	ND	5.69E+03	ND	5.75E+03		
Cadmium	ug/hr	ND	5.74E+03	ND	5.69E+03	ND	5.75E+03		
Chromium	ug/hr	2.18E+04		7.97E+03		2.59E+04			
Nickel	ug/hr	9.18E+03		3.99E+03		8.05E+03			
Metals Mass Emission Rate (lb/hr), Ei Ei = Ci*Qsdm*60/453600/1000									
Fraction		Total		Total		Total			
Arsenic	lb/hr	ND	1.27E-05	ND	1.26E-05	ND	1.27E-05		
Cadmium	lb/hr	ND	1.27E-05	ND	1.26E-05	ND	1.27E-05		
Chromium	lb/hr	4.81E-05		1.76E-05		5.70E-05			
Nickel	lb/hr	2.02E-05		8.79E-06		1.77E-05			

Flags
 ND or "<" - Not detected, reporting limit reported.
 B - Reagent blank corrected value.
 NDb - Reagent blank corrected result is less than RL. RL is substituted.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Test Date(s): 08/13-14/19
 Operator: NC
 Entered by: TG
 Checked by: CF

DATA ENTRY	Symbol	units	08/13/19	08/13/19	08/14/19
			DATA	DATA	DATA
Run Number			Run 1	Run 2	Run 3
Stack Dimensions: Round Stack Diameter	Ds	in.	48.0	48.0	48.0
Rectangular Stack, Length	L	in.			
Width	W	in.			
Nozzle Diameter	Dn	in.	0.450	0.450	0.450
Standard Temperature	Tstd	°F	68	68	68
Universal (molar) Gas Constant	Renglish	in. Hg-cu.ft./°R-lbmole	21.85	21.85	21.85
Average Stack Temperature (measured)	Fs	°F	93.9	109.0	96.5
Average Meter Temperature (measured)	Fm	°F	92.0	109.5	79.0
Standard Pressure	Pstd	in.Hg	29.92	29.92	29.92
Barometric Pressure	Pbar	in.Hg	29.90	29.90	29.90
Stack Static Pressure	Pg	in.WC	-0.020	-0.020	-0.020
Average Meter Orifice Head (Delta-H)	dH	in.WC	1.45	1.13	1.36
Average RMS Velocity Head (Delta-P)	dP	in.WC	0.038	0.030	0.036
Pitot Coefficient	Cp	—	0.84	0.84	0.84
Net Volume of Gas Metered	Vm	cu.ft.	82.774	75.832	78.550
Dry Gas Meter Calibration Factor (gamma, Y)	Y	—	1.0379	1.0379	1.0379
NET Sampling Time	min	min.	120	120	120
Stack Gas: Oxygen Content *	O2,m	%	20.9	20.9	20.9
Carbon Dioxide Content *	CO2,m	%	< 0.3	< 0.3	< 0.3
Total Impinger Gain	Ww	g	33.7	32.6	36.3
CALCULATED DATA					
Nozzle Area: $An = \pi/4 \cdot dn^2$	An	sq.in.	0.1590	0.1590	0.1590
Stack Area (round): $As = \pi/576 \cdot ds^2$	As	sq.ft.	12.57	12.57	12.57
(rectangular): $As = L \cdot W/144$					
Absolute Stack Temperature: $Ts = Fs+460$	Ts	°R	553.9	569.0	556.5
Absolute Meter Temperature: $Tm = Fm+460$	Tm	°R	552.0	569.5	539.0
Standard Temperature: $Tstd = Tstd+460$	Tstd	°R	528.0	528.0	528.0
Gas Sample Volume at Standard Conditions: $Vm(std) = Y \cdot (Vm/Tm) \cdot (Pbar + dH/13.6 \text{ in H}_2\text{O/in Hg}) \cdot (Tstd/Pstd)$	VmStd	cu.ft.	82.408	73.125	80.071
Vol. of Water Vapor, $Vw(std) = Ww/453.59 \cdot Renglish/18 \cdot Tstd / Pstd$	VwStd	cu.ft.	1.592	1.540	1.714
Moisture Fraction: $Bws = VwStd/(VmStd+VwStd)$	Bws	—	0.019	0.021	0.021
Stack Gas MW, Dry Basis: $Md = 0.32 \cdot O_{2,m} + 0.44 \cdot CO_{2,m} + 0.28 \cdot (100 - O_{2,m} - CO_{2,m})$	Md	g/mole	28.88	28.88	28.88
Stack Gas MW, Wet Basis: $Mw = Md \cdot (1 - Bws) + 18 \cdot Bws$	Mw	g/mole	28.68	28.66	28.66
Stack Pressure: $Ps = Pbar + Pg/13.6$	Ps	in.Hg	29.90	29.90	29.90
Stack Gas Velocity, measured $vs = 85.49 \cdot Cp \cdot \sqrt{(dP \cdot Ts / Ps / Mw)}$ $vm = 0.3048 \text{ m/ft} \cdot vs$	vs	ft/s	11.19	10.14	10.97
	vsm	m/s	3.41	3.09	3.34
Stack Gas Volumetric Flow Rate: $Q = 60 \cdot vs \cdot As$	Q	acfm	8,436	7,642	8,268
Stack Gas Volumetric Flow Rate, corrected: $Qsd = Q \cdot (1 - Bws) \cdot (Ps / Ts) \cdot (Tstd / Pstd)$ $Qsdm = Qsd / 35.315$	Qsd	dscfm	7,883	6,940	7,674
	Qsdm	dscmm	223.2	196.5	217.3
Isokinetic Sampling Rate: $I = 144 \cdot 100 \cdot Ts \cdot Vmstd \cdot Pstd / [60 \cdot Tstd \cdot vs \cdot \min \{ An \cdot Ps \cdot (1 - Bws) \}]$	I	%	99.1	99.9	98.9

* O2/CO2 is based on SCAQMD Method 10.1 analysis.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Run No.: 1
 Test Date: 08/13/19
 Times: 08:50 - 10:55

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	87	9.3	0.080	0.283	2.93	71	72
2	90	9.5	0.080	0.283	2.96	82	75
3	91	9.5	0.070	0.265	2.55	85	77
4	91	9.5	0.050	0.224	1.86	88	79
5	92	9.6	0.040	0.200	1.49	90	81
6	92	9.6	0.040	0.200	1.49	90	82
7	92	9.6	0.040	0.200	1.50	91	84
8	92	9.6	0.040	0.200	1.50	93	85
9	93	9.6	0.040	0.200	1.50	94	87
10	93	9.6	0.030	0.173	1.13	95	88
11	94	9.7	0.030	0.173	1.13	96	89
12	94	9.7	0.030	0.173	1.13	97	90
B-1	93	9.6	0.030	0.173	1.13	92	92
2	95	9.7	0.030	0.173	1.13	99	92
3	95	9.7	0.030	0.173	1.13	100	93
4	96	9.8	0.030	0.173	1.13	100	94
5	96	9.8	0.030	0.173	1.14	101	95
6	96	9.8	0.030	0.173	1.14	102	96
7	96	9.8	0.030	0.173	1.14	102	96
8	96	9.8	0.030	0.173	1.14	103	96
9	97	9.8	0.030	0.173	1.14	103	97
10	97	9.8	0.030	0.173	1.14	104	97
11	98	9.9	0.030	0.173	1.14	104	98
12	99	9.9	0.030	0.173	1.13	104	97
Average:	93.9		0.0376		1.45		92.0

DGM Reading (cu.ft.): Final-1:	443.624	Impinger Weight (g): #1 Final:	746.4
Initial-1:	360.850	#1 Initial:	742.6
Final-2:		#2 Final:	767.6
Initial-2:		#2 Initial:	757.2
Final-3:		#3 Final:	636.0
Initial-3:		#3 Initial:	632.7
Final-4:		#4 Final:	876.7
Initial-4:		#4 Initial:	860.5
Final-5:		#5 Final:	
Initial-5:		#5 Initial:	
Volume:	82.774	#6 Final:	
		#6 Initial:	
		#7 Final:	
		#7 Initial:	
		#8 Final:	
		#8 Initial:	
		Total wt of impingers:	33.7

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Run No.: 2
 Test Date: 08/13/19
 Times: 11:55 - 14:00

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	99	9.9	0.030	0.173	1.13	99	99
2	108	10.4	0.030	0.173	1.12	106	99
3	108	10.4	0.030	0.173	1.13	109	101
4	108	10.4	0.030	0.173	1.13	110	102
5	110	10.5	0.030	0.173	1.13	111	103
6	110	10.5	0.030	0.173	1.13	112	104
7	110	10.5	0.030	0.173	1.13	113	105
8	110	10.5	0.030	0.173	1.13	113	106
9	109	10.4	0.030	0.173	1.13	114	106
10	109	10.4	0.030	0.173	1.13	114	107
11	109	10.4	0.030	0.173	1.13	114	107
12	110	10.5	0.030	0.173	1.13	114	108
B-1	110	10.5	0.030	0.173	1.13	108	108
2	112	10.6	0.030	0.173	1.13	114	107
3	112	10.6	0.030	0.173	1.13	115	107
4	111	10.5	0.030	0.173	1.13	115	108
5	111	10.5	0.030	0.173	1.13	116	108
6	110	10.5	0.030	0.173	1.14	115	109
7	110	10.5	0.030	0.173	1.14	116	109
8	109	10.4	0.030	0.173	1.14	116	109
9	109	10.4	0.030	0.173	1.14	116	109
10	109	10.4	0.030	0.173	1.14	116	109
11	108	10.4	0.030	0.173	1.14	116	109
12	106	10.3	0.030	0.173	1.14	116	109
Average:	109.0		0.030		1.13		109.5

DGM Reading (cu.ft.): Final-1:	524.682	Impinger Weight (g): #1 Final:	727.3
Initial-1:	448.850	#1 Initial:	739.7
Final-2:		#2 Final:	781.6
Initial-2:		#2 Initial:	761.5
Final-3:		#3 Final:	657.8
Initial-3:		#3 Initial:	650.9
Final-4:		#4 Final:	768.3
Initial-4:		#4 Initial:	750.3
Final-5:		#5 Final:	
Initial-5:		#5 Initial:	
Volume:	75.832	#6 Final:	
		#6 Initial:	
		#7 Final:	
		#7 Initial:	
		#8 Final:	
		#8 Initial:	
		Total wt of impingers:	32.6

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Run No.: 3
 Test Date: 08/14/19
 Times: 08:25 - 10:30

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	93	9.6	0.060	0.245	2.15	66	66
2	98	9.9	0.060	0.245	2.14	69	66
3	98	9.9	0.060	0.245	2.15	74	67
4	100	10.0	0.060	0.245	2.15	77	68
5	93	9.6	0.030	0.173	1.09	79	69
6	94	9.7	0.030	0.173	1.09	79	71
7	93	9.6	0.030	0.173	1.10	80	72
8	92	9.6	0.030	0.173	1.02	81	73
9	92	9.6	0.030	0.173	1.10	82	73
10	93	9.6	0.030	0.173	1.10	83	75
11	93	9.6	0.030	0.173	1.10	84	75
12	95	9.7	0.030	0.173	1.10	84	76
B-1	99	9.9	0.030	0.173	1.09	78	77
2	96	9.8	0.030	0.173	1.10	85	77
3	99	9.9	0.030	0.173	1.10	86	78
4	97	9.8	0.030	0.173	1.10	87	79
5	97	9.8	0.030	0.173	1.10	87	79
6	98	9.9	0.030	0.173	1.10	87	80
7	98	9.9	0.030	0.173	1.11	88	82
8	98	9.9	0.020	0.141	0.74	89	81
9	99	9.9	0.020	0.141	0.73	88	81
10	100	10.0	0.020	0.141	0.73	88	82
11	101	10.0	0.060	0.245	2.20	89	82
12	101	10.0	0.090	0.300	3.31	92	83
Average:	96.5		0.0359		1.36		79.0

DGM Reading (cu.ft.): Final-1:	607.525	Impinger Weight (g): #1 Final:	745.9
Initial-1:	528.975	#1 Initial:	743.0
Final-2:		#2 Final:	769.3
Initial-2:		#2 Initial:	755.6
Final-3:		#3 Final:	635.2
Initial-3:		#3 Initial:	632.4
Final-4:		#4 Final:	894.0
Initial-4:		#4 Initial:	877.1
Final-5:		#5 Final:	
Initial-5:		#5 Initial:	
Volume:	78.550	#6 Final:	
		#6 Initial:	
		#7 Final:	
		#7 Initial:	
		#8 Final:	
		#8 Initial:	
		Total wt of impingers:	36.3

Location: Inlet 1 (Inside)

TEST RESULTS CARB 436 (Multiple Metals)

Facility: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Test Data	Units	Source Test Results			Average
Run Number	--	Run 1	Run 2	Run 3	
Test Date	mm/dd/yy	08/13/19	08/13/19	08/14/19	--
Test Time	hh:mm	08:50 - 10:55	11:55 - 14:00	08:25 - 10:30	--
<u>Sampling Data*</u>					
Stack Temperature	°F	116	126	101	114
Moisture	%	2.0	2.1	1.9	2.0
Sample Volume	dscf	86.7	88.8	90.1	88.6
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	< 0.3	< 0.3	< 0.3	< 0.3
Gas Velocity	ft/min	1,228	1,277	1,241	1,249
Stack Flow Rate	acfm	1,132	1,177	1,144	1,151
Stack Flow Rate	dscfm	1,012	1,035	1,052	1,033
<u>CARB Method 436</u>					
<u>CONCENTRATION</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	ug/dscm	6.11	3.06	1.18	3.45
	ug/dscf	0.173	0.087	0.033	0.098
Cadmium	ug/dscm	ND 0.407	ND 0.398	ND 0.392	< 0.399
	ug/dscf	ND 0.023	ND 0.023	ND 0.022	< 0.023
Chromium	ug/dscm	1790.9	2822.2	1567	2060
	ug/dscf	50.71	79.92	44.38	58.33
Nickel	ug/dscm	37.7	94.90	50.4	61.0
	ug/dscf	1.069	2.687	1.428	1.728
<u>CARB Method 436</u>					
<u>MASS EMISSION RATE</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	lb/hr	2.32E-05	1.19E-05	4.63E-06	1.32E-05
Cadmium	lb/hr	ND 1.54E-06	ND 1.54E-06	ND 1.88E-06	< 1.66E-06
Chromium	lb/hr	6.79E-03	1.09E-02	6.17E-03	7.97E-03
Nickel	lb/hr	1.43E-04	3.68E-04	1.99E-04	2.37E-04

Notes:

* Performed during isokinetic sampling (e.g. CARB Method 436).

** Measured via SCAQMD Method 10.1.

ND or "<" - Not detected, reporting limit reported.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C Test Date(s): 08/13-14/19
 City: ██████████ CA Operator: DJ
 Source: Baghouse Entered by: TG
 Location: Inlet 1 Checked by: CF

Metals Catch, Mi		Run 1	Run 2	Run 3	Field Blank	Reagent Blank
Fraction		Results	Results	Results	Results	Results
Arsenic	ug	15.0	7.7	3.0	ND 1.0	ND 1.00
Cadmium	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0	ND 1.00
Chromium	ug	4,400	7,100	4,000	1.6	1.50
Nickel	ug	94	240	130	1.4	1.30

Reagent Blank		Run 1	Run 2	Run 3	Field Blank	
Fraction		Results	Results	Results	Results	
Arsenic	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0	
Cadmium	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0	
Chromium	ug	1.5	1.5	1.50	1.5	
Nickel	ug	1.3	1.3	1.30	1.3	

Reagent Blank Corrected Values		Run 1	Run 2	Run 3	Field Blank	Reporting Limit*
Fraction		Results	Results	Results	Results	
Arsenic	ug	15.0	7.7	3.0	ND 1.0	
Cadmium	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0	
Chromium	ug	4,398.5	7,098.5	3,998.5	0.10	0.30
Nickel	ug	92.7	238.7	128.7	0.10	0.30

*Reporting limit is based on three times the FB values.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C Test Date(s): 08/13-14/19
 City: ██████████ CA Operator: DJ
 Source: Baghouse Entered by: TG
 Location: Inlet 1 Checked by: CF

Metals Catch, Mi		Run 1		Run 2		Run 3		Field Blank		Reagent Blank	
Fraction		Total		Total		Total		Total		Total	
Arsenic	ug	15.0		7.7		3.0		ND	1.00	ND	1.00
Cadmium	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.00	ND	1.00
Chromium	ug	B	4,398.5	B	7,098.5	B	3,998.5		1.6		1.50
Nickel	ug	B	92.7	B	238.7	B	128.7		1.4		1.30
Metals Molecular Weight, MW		Run 1		Run 2		Run 3					
Fraction		Total		Total		Total					
Arsenic	g/g-mole	74.92		74.92		74.92					
Cadmium	g/g-mole	112.41		112.41		112.41					
Chromium	g/g-mole	51.995		51.995		51.995					
Nickel	g/g-mole	58.69		58.69		58.69					
Concentration (ug/dscm), Ci = Mi/VmStd *35.315e-3cf/dscm											
Fraction		Total		Total		Total					
Arsenic	ug/dscm	6.11		3.06		1.18					
Cadmium	ug/dscm	ND	0.4072	ND	0.3976	ND	0.3919				
Chromium	ug/dscm	1,790.927		2,822.222		1,567.145					
Nickel	ug/dscm	37.7444		94.9024		50.442					
Metals Mass Emission Rate (ug/hr), Ei,m Ei,m = Ci*Qsdm*60											
Fraction		Total		Total		Total					
Arsenic	ug/hr	1.05E+04		5.38E+03		2.10E+03					
Cadmium	ug/hr	ND	7.00E+02	ND	6.99E+02	ND	7.00E+02				
Chromium	ug/hr	3.08E+06		4.96E+06		2.80E+06					
Nickel	ug/hr	6.49E+04		1.67E+05		9.01E+04					
Metals Mass Emission Rate (lb/hr), Ei Ei = Ci*Qsdm*60/453600/1000											
Fraction		Total		Total		Total					
Arsenic	lb/hr	2.32E-05		1.19E-05		4.63E-06					
Cadmium	lb/hr	ND	1.54E-06	ND	1.54E-06	ND	1.54E-06				
Chromium	lb/hr	6.79E-03		1.09E-02		6.17E-03					
Nickel	lb/hr	1.43E-04		3.68E-04		1.99E-04					

Flags
 ND or "<" - Not detected, reporting limit reported.
 B - Reagent blank corrected value.
 NDb - Reagent blank corrected result is less than RL. RL is substituted.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Test Date(s): 08/13-14/19
 Operator: DJ
 Entered by: TG
 Checked by: CF

DATA ENTRY	Symbol	Units	08/13/19	08/13/19	08/14/19
			DATA	DATA	DATA
Run Number			Run 1	Run 2	Run 3
Stack Dimensions: Round Stack Diameter	Ds	in.	13.0	13.0	13.0
Rectangular Stack, Length	L	in.			
Width	W	in.			
Nozzle Diameter	Dn	in.	0.348	0.348	0.348
Standard Temperature	Tstd	°F	68	68	68
Universal (molar) Gas Constant	Renglish	in. Hg-cu.ft/ °R-lbmole	21.85	21.85	21.85
Average Stack Temperature (measured)	Fs	°F	116.2	125.7	101.2
Average Meter Temperature (measured)	Fm	°F	99.6	103.8	96.5
Standard Pressure	Pstd	in.Hg	29.92	29.92	29.92
Barometric Pressure	Pbar	in.Hg	29.90	29.90	29.90
Stack Static Pressure	Pg	in.WC	-1.50	-1.50	-1.50
Average Meter Orifice Head (Delta-H)	dH	in.WC	1.85	1.93	1.97
Average RMS Velocity Head (Delta-P)	dP	in.WC	0.12	0.13	0.13
Pitot Coefficient	Cp	—	0.84	0.84	0.84
Net Volume of Gas Metered	Vm	cu.ft.	88.093	90.864	90.987
Dry Gas Meter Calibration Factor (gamma, Y)	Y	—	1.0395	1.0395	1.0395
NET Sampling Time	min	min.	120	120	120
Stack Gas: Oxygen Content *	O2,m	%	20.8	20.8	20.8
Carbon Dioxide Content *	CO2,m	%	< 0.3	< 0.3	< 0.3
Total Impinger Gain	Ww	g	36.7	39.4	36.2
CALCULATED DATA					
Nozzle Area: $An = \pi/4 * dn^2$	An	sq.in.	0.0951	0.0951	0.0951
Stack Area (round): $As = \pi/576 * ds^2$ (rectangular): $As = L * W / 144$	As	sq.ft.	0.92	0.92	0.92
Absolute Stack Temperature: $Ts = Fs + 460$	Ts	°R	576.2	585.7	561.2
Absolute Meter Temperature: $Tm = Fm + 460$	Tm	°R	559.6	563.8	556.5
Standard Temperature: $Tstdr = Tstd + 460$	Tstdr	°R	528.0	528.0	528.0
Gas Sample Volume at Standard Conditions: $Vm(std) = Y * (Vm / Tm) * (Pbar + dH / 13.6 \text{ in H}_2\text{O} / \text{in Hg}) * (Tstdr / Pstd)$	VmStd	cu.ft.	86.733	88.825	90.105
Vol. of Water Vapor, $Vw(std) = Ww / 453.59 * Renglish / 18 * Tstdr / Pstd$	VwStd	cu.ft.	1.733	1.861	1.710
Moisture Fraction: $Bws = VwStd / (VmStd + VwStd)$	Bws	—	0.020	0.021	0.019
Stack Gas MW, Dry Basis: $Md = 0.32 * O_{2,m} + 0.44 * CO_{2,m} + 0.28 * (100 - O_{2,m} - CO_{2,m})$	Md	g/mole	28.88	28.88	28.88
Stack Gas MW, Wet Basis: $Mw = Md * (1 - Bws) + 18 * Bws$	Mw	g/mole	28.67	28.66	28.68
Stack Pressure: $Ps = Pbar + Pg / 13.6$	Ps	in.Hg	29.79	29.79	29.79
Stack Gas Velocity, measured $vs = 85.49 * Cp * \sqrt{(dP * Ts / Ps / Mw)}$ $vm = 0.3048 \text{ m} / \text{ft} * vs$	vs	ft/s	20.46	21.28	20.69
	vsm	m/s	6.24	6.49	6.31
Stack Gas Volumetric Flow Rate: $Q = 60 * vs * As$	Q	acfm	1,132	1,177	1,144
Stack Gas Volumetric Flow Rate, corrected: $Qsd = Q * (1 - Bws) * (Ps / Ts) * (Tstdr / Pstd)$ $Qsdm = Qsd / 35.315$	Qsd	dscfm	1,012	1,035	1,052
	Qsdm	dscmm	28.7	29.3	29.8
Isokinetic Sampling Rate: $I = 144 * 100 * Ts * Vmstd * Pstd / [60 * Tstdr * vs * \text{min} * An * Ps * (1 - Bws)]$	I	%	99.7	99.8	99.6

* O2/CO2 is based on SCAQMD Method 10.1 analysis.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Run No.: 1
 Test Date: 08/13/19
 Times: 08:50 - 10:55

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	121	11.0	0.160	0.400	2.35	89	89
2	124	11.1	0.150	0.387	2.20	90	90
3	124	11.1	0.180	0.424	2.65	92	92
4	123	11.1	0.100	0.316	1.48	94	94
5	123	11.1	0.100	0.316	1.48	95	95
6	123	11.1	0.080	0.283	1.19	95	95
7	120	11.0	0.100	0.316	1.49	96	96
8	120	11.0	0.110	0.332	1.65	97	97
9	119	10.9	0.080	0.283	1.20	98	98
10	93	9.6	0.160	0.400	2.52	99	99
11	88	9.4	0.100	0.316	1.59	100	100
12	90	9.5	0.090	0.300	1.43	101	101
B-1	130	11.4	0.190	0.436	2.80	99	99
2	134	11.6	0.170	0.412	2.49	99	99
3	130	11.4	0.180	0.424	2.67	101	101
4	130	11.4	0.180	0.424	2.68	103	103
5	139	11.8	0.130	0.361	1.91	104	104
6	128	11.3	0.110	0.332	1.64	104	104
7	126	11.2	0.100	0.316	1.50	105	105
8	118	10.9	0.091	0.302	1.37	105	105
9	92	9.6	0.120	0.346	1.92	106	106
10	101	10.0	0.110	0.332	1.73	106	106
11	103	10.1	0.080	0.283	1.25	106	106
12	102	10.1	0.080	0.283	1.26	107	107
Average:	116.2		0.1203		1.85		99.6
DGM Reading (cu.ft.): Final-1:			332.124	Impinger Weight (g): #1 Final:			765.6
Initial-1:			244.031	#1 Initial:			766.1
Final-2:				#2 Final:			746.6
Initial-2:				#2 Initial:			729.5
Final-3:				#3 Final:			658.6
Initial-3:				#3 Initial:			655.9
Final-4:				#4 Final:			880.0
Initial-4:				#4 Initial:			862.6
Final-5:				#5 Final:			
Initial-5:				#5 Initial:			
Volume:			88.093	#6 Final:			
				#6 Initial:			
				#7 Final:			
				#7 Initial:			
				#8 Final:			
				#8 Initial:			
				Total wt of impingers:			36.7

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Run No.: 2
 Test Date: 08/13/19
 Times: 11:55 - 14:00

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	125	11.2	0.150	0.387	2.20	92	92
2	125	11.2	0.140	0.374	2.07	95	95
3	125	11.2	0.160	0.400	2.39	96	96
4	127	11.3	0.150	0.387	2.22	98	98
5	125	11.2	0.140	0.374	2.08	99	99
6	125	11.2	0.110	0.332	1.64	100	100
7	125	11.2	0.100	0.316	1.49	101	101
8	126	11.2	0.090	0.300	1.34	102	102
9	126	11.2	0.140	0.374	2.10	104	104
10	130	11.4	0.140	0.374	2.08	104	104
11	120	11.0	0.100	0.316	1.52	105	105
12	110	10.5	0.120	0.346	1.85	105	105
B-1	128	11.3	0.180	0.424	2.69	104	104
2	128	11.3	0.160	0.400	2.39	105	105
3	130	11.4	0.150	0.387	2.24	106	106
4	136	11.7	0.140	0.374	2.07	107	107
5	128	11.3	0.110	0.332	1.65	108	108
6	130	11.4	0.100	0.316	1.50	108	108
7	129	11.4	0.140	0.374	2.11	109	109
8	126	11.2	0.120	0.346	1.81	108	108
9	125	11.2	0.100	0.316	1.51	108	108
10	124	11.1	0.110	0.332	1.67	108	108
11	124	11.1	0.100	0.316	1.52	109	109
12	120	11.0	0.150	0.387	2.29	109	109
Average:	125.7		0.128		1.93		103.8

DGM Reading (cu.ft.): Final-1:	423.546	Impinger Weight (g): #1 Final:	625.7
Initial-1:	332.682	#1 Initial:	616.0
Final-2:		#2 Final:	744.0
Initial-2:		#2 Initial:	735.0
Final-3:		#3 Final:	657.5
Initial-3:		#3 Initial:	651.0
Final-4:		#4 Final:	889.3
Initial-4:		#4 Initial:	875.1
Final-5:		#5 Final:	
Initial-5:		#5 Initial:	
Volume:	90.864	#6 Final:	
		#6 Initial:	
		#7 Final:	
		#7 Initial:	
		#8 Final:	
		#8 Initial:	
		Total wt of impingers:	39.4

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Run No.: 3
 Test Date: 08/14/19
 Times: 08:25 - 10:30

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	126	11.2	0.18	0.424	2.59	82	82
2	116	10.8	0.15	0.387	2.20	83	83
3	112	10.6	0.16	0.400	2.37	84	84
4	104	10.2	0.14	0.374	2.11	87	87
5	99	9.9	0.14	0.374	2.14	90	90
6	98	9.9	0.13	0.361	2.00	91	91
7	104	10.2	0.12	0.346	1.83	93	93
8	94	9.7	0.11	0.332	1.71	94	94
9	90	9.5	0.10	0.316	1.57	94	94
10	86	9.3	0.08	0.283	1.27	95	95
11	90	9.5	0.10	0.316	1.57	96	96
12	87	9.3	0.09	0.300	1.42	96	96
B-1	103	10.1	0.17	0.412	2.60	94	94
2	108	10.4	0.18	0.424	2.79	105	105
3	106	10.3	0.15	0.387	2.32	103	103
4	103	10.1	0.16	0.400	2.49	102	102
5	104	10.2	0.12	0.346	1.87	103	103
6	103	10.1	0.10	0.316	1.56	103	103
7	96	9.8	0.12	0.346	1.89	103	103
8	100	10.0	0.11	0.332	1.72	103	103
9	96	9.8	0.10	0.316	1.58	103	103
10	99	9.9	0.10	0.316	1.57	104	104
11	100	10.0	0.12	0.346	1.88	104	104
12	110	10.5	0.14	0.374	2.20	105	105
Average:	101.2		0.1264		1.97		96.5

DGM Reading (cu.ft.): Final-1:	515.006	Impinger Weight (g): #1 Final:	760.3
Initial-1:	424.019	#1 Initial:	765.0
Final-2:		#2 Final:	747.4
Initial-2:		#2 Initial:	731.5
Final-3:		#3 Final:	659.8
Initial-3:		#3 Initial:	655.8
Final-4:		#4 Final:	893.6
Initial-4:		#4 Initial:	872.6
Final-5:		#5 Final:	
Initial-5:		#5 Initial:	
Volume:	90.987	#6 Final:	
		#6 Initial:	
		#7 Final:	
		#7 Initial:	
		#8 Final:	
		#8 Initial:	
		Total wt of impingers:	36.2

Location: Inlet 2 (Upstream to Baghouse)

TEST RESULTS CARB 436 (Multiple Metals)

Facility: AQMD Facility C
 City: ████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Test Data	Units	Source Test Results			Average
Run Number	--	Run 1	Run 2	Run 3	
Test Date	mm/dd/yy	08/13/19	08/13/19	08/14/19	--
Test Time	hh:mm	08:50 - 10:55	11:55 - 14:00	08:25 - 10:30	--
<u>Sampling Data*</u>					
Stack Temperature	°F	91.9	99.0	95.5	95.5
Moisture	%	2.1	2.0	2.3	2.1
Sample Volume	dscf	98.9	95.5	94.1	96.2
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	< 0.3	< 0.3	< 0.3	< 0.3
Gas Velocity	ft/min	4,765	4,649	4,568	4,661
Stack Flow Rate	acfm	6,653	6,491	6,379	6,507
Stack Flow Rate	dscfm	6,164	5,942	5,861	5,989
<u>CARB Method 436</u>					
<u>CONCENTRATION</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	ug/dscm	1.32	0.67	0.56	0.85
	ug/dscf	0.037	0.019	0.016	0.024
Cadmium	ug/dscm	ND 0.357	ND 0.370	ND 0.375	< 0.367
	ug/dscf	ND 0.020	ND 0.021	ND 0.021	< 0.021
Chromium	ug/dscm	356.4	553.9	600	503
	ug/dscf	10.09	15.68	16.99	14.25
Nickel	ug/dscm	11.0	19.11	20.2	16.7
	ug/dscf	0.310	0.541	0.571	0.474
<u>CARB Method 436</u>					
<u>MASS EMISSION RATE</u>					
		<u>Total</u>	<u>Total</u>	<u>Total</u>	
Arsenic	lb/hr	3.05E-05	1.48E-05	1.24E-05	1.92E-05
Cadmium	lb/hr	ND 8.24E-06	ND 8.23E-06	ND 1.01E-05	< 8.84E-06
Chromium	lb/hr	8.23E-03	1.23E-02	1.32E-02	1.12E-02
Nickel	lb/hr	2.53E-04	4.25E-04	4.42E-04	3.74E-04

Notes:

* Performed during isokinetic sampling (e.g. CARB Method 436).

** Measured via SCAQMD Method 10.1.

ND or "<" - Not detected, reporting limit reported.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C Test Date(s): 08/13-14/19
 City: ██████████ CA Operator: WB
 Source: Baghouse Entered by: TG
 Location: Inlet 2 (Upstream to) Checked by: CF

Metals Catch, Mi		Run 1	Run 2	Run 3	Field Blank	Reagent Blank
Fraction		Results	Results	Results	Results	Results
Arsenic	ug	3.7	1.8	1.5	ND 1.0	ND 1.00
Cadmium	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0	ND 1.00
Chromium	ug	1,000	1,500	1,600	1.6	1.50
Nickel	ug	32.0	53.0	55.0	1.4	1.30

Reagent Blank		Run 1	Run 2	Run 3	Field Blank
Fraction		Results	Results	Results	Results
Arsenic	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0
Cadmium	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0
Chromium	ug	1.5	1.5	1.50	1.5
Nickel	ug	1.3	1.3	1.30	1.3

Reagent Blank Corrected Values		Run 1	Run 2	Run 3	Field Blank	Reporting Limit*
Fraction		Results	Results	Results	Results	
Arsenic	ug	3.7	1.8	1.5	ND 1.0	
Cadmium	ug	ND 1.0	ND 1.0	ND 1.0	ND 1.0	
Chromium	ug	998.5	1,498.5	1,598.5	0.1	0.30
Nickel	ug	30.7	51.7	53.7	0.1	0.30

*Reporting limit is based on three times the FB values.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C Test Date(s): 08/13-14/19
 City: ██████████ CA Operator: WB
 Source: Baghouse Entered by: TG
 Location: Inlet 2 (Upstream to Bag) Checked by: CF

Metals Catch, Mi		Run 1		Run 2		Run 3		Field Blank		Reagent Blank	
Fraction		Total		Total		Total		Total		Total	
Arsenic	ug		3.7		1.8		1.5	ND	1.00	ND	1.00
Cadmium	ug	ND	1.0	ND	1.0	ND	1.0	ND	1.00	ND	1.00
Chromium	ug	B	998.5	B	1,498.5	B	1,598.5		1.6		1.50
Nickel	ug	B	30.7	B	51.7	B	53.7		1.4		1.30
Metals Molecular Weight, MW		Run 1		Run 2		Run 3					
Fraction		Total		Total		Total					
Arsenic	g/g-mole		74.92		74.92		74.92				
Cadmium	g/g-mole		112.41		112.41		112.41				
Chromium	g/g-mole		51.995		51.995		51.995				
Nickel	g/g-mole		58.69		58.69		58.69				
Concentration (ug/dscm), Ci = Mi/VmStd *35.315e-3cf/dscm											
Fraction		Total		Total		Total					
Arsenic	ug/dscm		1.32		0.67		0.56				
Cadmium	ug/dscm	ND	0.3569	ND	0.3696	ND	0.3753				
Chromium	ug/dscm		356.380		553.886		599.977				
Nickel	ug/dscm		10.9573		19.1097		20.156				
Metals Mass Emission Rate (ug/hr), Ei,m Ei,m = Ci*Qsdm*60											
Fraction		Total		Total		Total					
Arsenic	ug/hr		1.38E+04		6.72E+03		5.61E+03				
Cadmium	ug/hr	ND	3.74E+03	ND	3.73E+03	ND	3.74E+03				
Chromium	ug/hr		3.73E+06		5.59E+06		5.97E+06				
Nickel	ug/hr		1.15E+05		1.93E+05		2.01E+05				
Metals Mass Emission Rate (lb/hr), Ei Ei = Ci*Qsdm*60/453600/1000											
Fraction		Total		Total		Total					
Arsenic	lb/hr		3.05E-05		1.48E-05		1.24E-05				
Cadmium	lb/hr	ND	8.24E-06	ND	8.23E-06	ND	8.24E-06				
Chromium	lb/hr		8.23E-03		1.23E-02		1.32E-02				
Nickel	lb/hr		2.53E-04		4.25E-04		4.42E-04				

Flags
 ND or "<" - Not detected, reporting limit reported.
 B - Reagent blank corrected value.
 NDb - Reagent blank corrected result is less than RL. RL is substituted.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Test Date(s): 08/13-14/19
 Operator: WB
 Entered by: TG
 Checked by: CF

DATA ENTRY	Symbol	Units	08/13/19	08/13/19	08/14/19
			DATA	DATA	DATA
Run Number			Run 1	Run 2	Run 3
Stack Dimensions: Round Stack Diameter	Ds	in.	16.0	16.0	16.0
Rectangular Stack, Length	L	in.			
Width	W	in.			
Nozzle Diameter	Dn	in.	0.184	0.184	0.184
Standard Temperature	Tstd	°F	68	68	68
Universal (molar) Gas Constant	Renglish	in. Hg-cu.ft/ °R-lbmole	21.85	21.85	21.85
Average Stack Temperature (measured)	Fs	°F	91.9	99.0	95.5
Average Meter Temperature (measured)	Fm	°F	89.3	106.0	86.7
Standard Pressure	Pstd	in.Hg	29.92	29.92	29.92
Barometric Pressure	Pbar	in.Hg	29.90	29.90	29.90
Stack Static Pressure	Pg	in.WC	-4.200	-4.200	-4.200
Average Meter Orifice Head (Delta-H)	dH	in.WC	2.30	2.18	2.05
Average RMS Velocity Head (Delta-P)	dP	in.WC	1.88	1.77	1.71
Pitot Coefficient	Cp	—	0.84	0.84	0.84
Net Volume of Gas Metered	Vm	cu.ft.	98.720	98.246	93.476
Dry Gas Meter Calibration Factor (gamma, Y)	Y	—	1.0376	1.0376	1.0376
NET Sampling Time	min	min.	120	120	120
Stack Gas: Oxygen Content *	O2,m	%	20.8	20.8	20.8
Carbon Dioxide Content *	CO2,m	%	< 0.3	< 0.3	< 0.3
Total Impinger Gain	Ww	g	44.4	41.2	46.0
CALCULATED DATA					
Nozzle Area: $An = \pi/4 \cdot dn^2$	An	sq.in.	0.0266	0.0266	0.0266
Stack Area (round): $As = \pi/576 \cdot ds^2$ (rectangular): $As = L \cdot W/144$	As	sq.ft.	1.40	1.40	1.40
Absolute Stack Temperature: $Ts = Fs + 460$	Ts	°R	551.9	559.0	555.5
Absolute Meter Temperature: $Tm = Fm + 460$	Tm	°R	549.3	566.0	546.7
Standard Temperature: $Tstdr = Tstd + 460$	Tstdr	°R	528.0	528.0	528.0
Gas Sample Volume at Standard Conditions: $Vm(std) = Y \cdot (Vm/Tm) \cdot (Pbar + dH/13.6 \text{ in H}_2\text{O/in Hg}) \cdot (Tstdr/Pstd)$	VmStd	cu.ft.	98.945	95.542	94.089
Vol. of Water Vapor, $Vw(std) = Ww/453.59 \cdot Renglish/18 \cdot Tstdr / Pstd$	VwStd	cu.ft.	2.097	1.946	2.172
Moisture Fraction: $Bws = VwStd/(VmStd+VwStd)$	Bws	—	0.021	0.020	0.023
Stack Gas MW, Dry Basis: $Md = 0.32 \cdot O_{2,m} + 0.44 \cdot CO_{2,m} + 0.28 \cdot (100 - O_{2,m} - CO_{2,m})$	Md	g/mole	28.88	28.88	28.88
Stack Gas MW, Wet Basis: $Mw = Md \cdot (1 - Bws) + 18 \cdot Bws$	Mw	g/mole	28.65	28.66	28.63
Stack Pressure: $Ps = Pbar + Pg/13.6$	Ps	in.Hg	29.59	29.59	29.59
Stack Gas Velocity, measured $vs = 85.49 \cdot Cp \cdot \sqrt{(dP \cdot Ts / Ps / Mw)}$ $vm = 0.3048 \text{ m/ft} \cdot vs$	vs	ft/s	79.41	77.48	76.14
	vsm	m/s	24.21	23.61	23.21
Stack Gas Volumetric Flow Rate: $Q = 60 \cdot vs \cdot As$	Q	acfm	6,653	6,491	6,379
Stack Gas Volumetric Flow Rate, corrected: $Qsd = Q \cdot (1 - Bws) \cdot (Ps / Ts) \cdot (Tstdr / Pstd)$ $Qsdm = Qsd / 35.315$	Qsd	dscfm	6,164	5,942	5,861
	Qsdm	dscmm	174.6	168.3	166.0
Isokinetic Sampling Rate: $I = 144 \cdot 100 \cdot Ts \cdot Vmstd \cdot Pstd / [60 \cdot Tstdr \cdot vs \cdot \min \cdot An \cdot Ps \cdot (1 - Bws)]$	I	%	101.1	101.3	101.2

* O2/CO2 is based on SCAQMD Method 10.1 analysis.

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Run No.: 1
 Test Date: 08/13/19
 Times: 08:50 - 10:55

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	93	9.6	2.60	1.612	3.10	74	74
2	94	9.7	2.55	1.597	3.05	75	75
3	93	9.6	2.75	1.658	3.25	77	77
4	93	9.6	2.90	1.703	3.45	79	79
5	93	9.6	2.45	1.565	2.90	81	81
6	93	9.6	2.65	1.628	3.15	84	84
7	93	9.6	1.90	1.378	2.25	86	86
8	91	9.5	1.50	1.225	1.80	87	87
9	89	9.4	1.25	1.118	1.50	88	88
10	86	9.3	1.20	1.095	1.45	89	89
11	84	9.2	1.19	1.091	1.30	90	90
12	77	8.8	1.20	1.095	1.45	90	90
B-1	94	9.7	2.15	1.466	2.55	90	90
2	95	9.7	2.25	1.500	2.65	90	90
3	95	9.7	2.35	1.533	2.80	91	91
4	94	9.7	2.40	1.549	2.85	93	93
5	96	9.8	2.30	1.517	2.75	94	94
6	96	9.8	2.35	1.533	2.98	96	96
7	98	9.9	2.10	1.449	2.50	97	97
8	98	9.9	1.50	1.225	1.80	98	98
9	96	9.8	1.20	1.095	1.45	98	98
10	95	9.7	1.15	1.072	1.35	99	99
11	87	9.3	1.20	1.095	1.45	99	99
12	84	9.2	1.20	1.095	1.45	99	99
Average:	91.9		1.8789		2.30		89.3
DGM Reading (cu.ft.): Final-1:			98.912	Impinger Weight (g): #1 Final:			752.5
Initial-1:			0.192	#1 Initial:			758.7
Final-2:				#2 Final:			754.2
Initial-2:				#2 Initial:			732.9
Final-3:				#3 Final:			656.9
Initial-3:				#3 Initial:			650.4
Final-4:				#4 Final:			791.6
Initial-4:				#4 Initial:			768.8
Final-5:				#5 Final:			
Initial-5:				#5 Initial:			
Volume:			98.720	#6 Final:			
				#6 Initial:			
				#7 Final:			
				#7 Initial:			
				#8 Final:			
				#8 Initial:			
				Total wt of impingers:			44.4

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Run No.: 2
 Test Date: 08/13/19
 Times: 11:55 - 14:00

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	102	10.1	2.20	1.483	3.20	93	93
2	101	10.0	2.45	1.565	2.90	93	93
3	103	10.1	2.65	1.628	3.15	95	95
4	104	10.2	2.60	1.612	3.10	97	97
5	103	10.1	2.50	1.581	2.95	99	99
6	105	10.2	2.50	1.581	2.95	102	102
7	102	10.1	1.80	1.342	2.15	103	103
8	99	9.9	1.50	1.225	1.80	105	105
9	100	10.0	1.20	1.095	1.45	106	106
10	96	9.8	1.10	1.049	1.30	107	107
11	95	9.7	1.10	1.049	1.30	108	108
12	98	9.9	1.05	1.025	1.25	108	108
B-1	101	10.0	2.20	1.483	2.60	107	107
2	100	10.0	2.30	1.517	2.75	108	108
3	100	10.0	2.30	1.517	2.75	109	109
4	98	9.9	2.45	1.565	2.90	110	110
5	98	9.9	1.90	1.378	2.25	111	111
6	99	9.9	1.85	1.360	2.20	112	112
7	99	9.9	1.80	1.342	2.15	112	112
8	100	10.0	1.35	1.162	1.60	113	113
9	97	9.8	1.10	1.049	1.30	112	112
10	95	9.7	1.20	1.095	1.45	112	112
11	90	9.5	1.20	1.095	1.45	111	111
12	92	9.6	1.20	1.095	1.45	111	111
Average:	99.0		1.766		2.18		106.0

DGM Reading (cu.ft.): Final-1:	197.206	Impinger Weight (g): #1 Final:	656.2
Initial-1:	98.960	#1 Initial:	646.2
Final-2:		#2 Final:	774.8
Initial-2:		#2 Initial:	763.2
Final-3:		#3 Final:	631.0
Initial-3:		#3 Initial:	628.4
Final-4:		#4 Final:	844.8
Initial-4:		#4 Initial:	827.8
Final-5:		#5 Final:	
Initial-5:		#5 Initial:	
Volume:	98.246	#6 Final:	
		#6 Initial:	
		#7 Final:	
		#7 Initial:	
		#8 Final:	
		#8 Initial:	
		Total wt of impingers:	41.2

CARB METHOD 436 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Run No.: 3
 Test Date: 08/14/19
 Times: 08:25 - 10:30

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	99	9.9	1.95	1.396	2.30	71	71
2	100	10.0	2.35	1.533	2.75	72	72
3	97	9.8	2.60	1.612	3.05	74	74
4	99	9.9	2.40	1.549	2.80	76	76
5	96	9.8	2.20	1.483	2.60	78	78
6	96	9.8	2.40	1.549	2.80	80	80
7	97	9.8	2.25	1.500	2.65	82	82
8	95	9.7	1.40	1.183	1.65	84	84
9	92	9.6	1.20	1.095	1.40	85	85
10	87	9.3	1.20	1.095	1.40	86	86
11	89	9.4	1.20	1.095	1.40	87	87
12	90	9.5	1.15	1.072	1.35	87	87
B-1	93	9.6	1.70	1.304	2.00	87	87
2	94	9.7	1.85	1.360	2.15	88	88
3	95	9.7	2.10	1.449	2.45	89	89
4	95	9.7	2.20	1.483	2.60	90	90
5	96	9.8	1.80	1.342	2.10	93	93
6	97	9.8	2.10	1.449	2.45	93	93
7	100	10.0	1.80	1.342	2.10	94	94
8	102	10.1	1.50	1.225	1.75	96	96
9	98	9.9	1.30	1.140	1.55	96	96
10	97	9.8	1.10	1.049	1.30	97	97
11	94	9.7	1.05	1.025	1.25	97	97
12	94	9.7	1.20	1.095	1.40	98	98
Average:	95.5		1.7148		2.05		86.7

DGM Reading (cu.ft.): Final-1:	291.049	Impinger Weight (g): #1 Final:	746.2
Initial-1:	197.573	#1 Initial:	759.0
Final-2:		#2 Final:	760.9
Initial-2:		#2 Initial:	735.9
Final-3:		#3 Final:	660.1
Initial-3:		#3 Initial:	651.5
Final-4:		#4 Final:	822.4
Initial-4:		#4 Initial:	797.2
Final-5:		#5 Final:	
Initial-5:		#5 Initial:	
Volume:	93.476	#6 Final:	
		#6 Initial:	
		#7 Final:	
		#7 Initial:	
		#8 Final:	
		#8 Initial:	
		Total wt of impingers:	46.0

APPENDIX C2
MULTIPLE METAL EMISSIONS – FIELD DATA

Location: Baghouse Outlet

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ██████████ CA
 SAMPLING LOCATION: Outlet
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 54.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 6.00 inches
 DEPTH OF STACK OR DUCT, D: 48.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

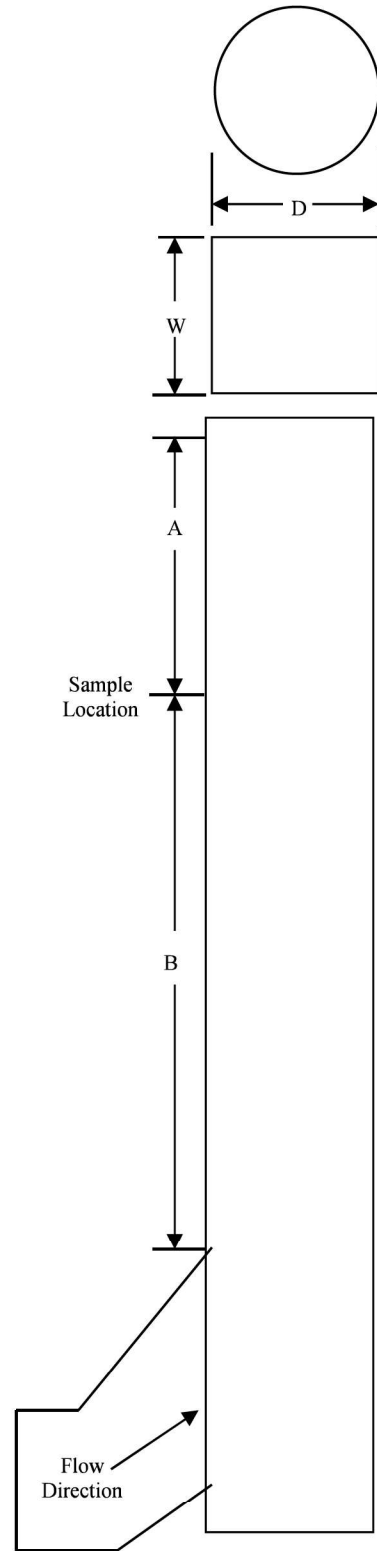
EQUIVALENT DIAMETER
 $De = 2 * (DEPTH) * (WIDTH) / (DEPTH + WIDTH) =$ 48.00 inches

STACK/DUCT AREA = 12.57 sq.feet 1809.6 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	<u>B</u>	<u>A</u>
# OF INCHES	126.00	50.00
# OF DIAMETERS	2.63	1.04

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	1.01	7
2	6.7	3.22	9 1/4
3	11.8	5.66	11 5/8
4	17.7	8.50	14 1/2
5	25.0	12.00	18
6	35.6	17.09	23 1/8
7	64.4	30.91	36 7/8
8	75.0	36.00	42
9	82.3	39.50	45 1/2
10	88.2	42.34	48 3/8
11	93.3	44.78	50 3/4
12	97.9	46.99	53



DRAWING NOT TO SCALE

Run #: 2	Pilot ID: 73	Impinger #	Initial	Final	Net	Pilot Leak Check Initial: <input checked="" type="checkbox"/> <input checked="" type="checkbox"/> Final: <input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Date: 8-13-19	Pilot Coeff.: 0.84	1	742.6	746.4		
Client: SCAQMD C	Meter Box #: A-3	2	757.2	767.6		Meter Box Leak Check Initial: 0.00 12 Final: 0.00 12
Unit: Outlet	Meter @ Dh: 1.583	3	632.7	636.0		
Operator: Nc	Meter Y: 1.0379	4	860.5	876.7		
Stack Dia: 48"	TC #: 73	5				
Amb. Press: 29.9	Start Time: 8:50	H2O Gain =			Filter:	
Static Press: 0.02	Stop Time: 10:55					

A West

950

Bas South

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mr. Inlet Temp. (F)	Mr. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	0.08	87	2.93	360.856	71	72	252	251	55	3	N/A	N/A
11	5	0.08	90	2.96	365.7	82	75	252	251	56	4		
10	10	0.07	91	2.55	370.7	85	77	248	252	56	↓		
9	15	0.05	91	1.86	375.3	88	79	249	253	56	↓		
8	20	0.04	92	1.49	379.2	90	81	250	251	56	3		
7	25	0.04	92	1.49	382.7	90	82	251	253	56	↓		
6	30	0.04	92	1.50	386.2	91	84	251	250	56	↓		
5	35	0.04	92	1.50	389.7	93	85	249	253	56	↓		
4	40	0.04	93	1.50	393.3	94	87	251	249	56	↓		
3	45	0.03	93	1.13	396.9	95	88	248	252	56	↓		
2	50	0.03	94	1.13	400.0	96	89	249	250	56	↓		
1	55	0.03	94	1.13	403.1	97	90	248	251	56	↓		
	60				406.214								
12	0	0.03	93	1.13	406.214	92	92	249	250	56	3	N/A	N/A
11	5	0.03	95	1.13	409.3	99	92	248	249	57	↓		
10	10	0.03	95	1.13	412.4	100	93	250	252	57	↓		
9	15	0.03	96	1.13	415.5	100	94	249	250	57	↓		
8	20	0.03	96	1.14	418.6	101	95	248	249	57	↓		
7	25	0.03	96	1.14	421.7	102	96	248	251	57	↓		
6	30	0.03	96	1.14	424.8	102	96	249	252	57	↓		
5	35	0.03	96	1.14	427.9	103	96	247	250	57	↓		
4	40	0.03	97	1.14	431.05	103	97	248	252	57	↓		
3	45	0.03	97	1.14	434.2	104	97	250	250	58	↓		
2	50	0.03	98	1.14	437.35	104	98	251	249	58	↓		
1	55	0.03	99	1.13	440.49	104	97	249	250	58	↓		
	60				443.624								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: **88**

Estimated Stack Temp: **90**

Estimated Delta P: **0.04**

Estimated Moisture Content: **2**

Estimated O2: **20.8**

Estimated CO2: **0.05**

Equipment Evaluation, OK/YY or N

Ambient Temp: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

	1	2	3	4
DGM Initial:				
Vacuum:				
Leak Rate:				
DGM Final:				

Nozzle Information

Nozzle ID: _____

Nozzle Dia: **0.450**

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #: 2	Pilot ID: 73	Impinger #	Initial	Final	Net	Pilot Leak Check Initial: <input checked="" type="checkbox"/> <input checked="" type="checkbox"/> Final: <input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Date: 8-13-19	Pilot Coeff.: 0.84	1	739.7	727.3		
Client: SCAQMD C	Meter Box #: A-3	2	761.5	746.6		Meter Box Leak Check Initial: 0.00 12 Final: 0.00 12
Unit: Baghouse - outlet	Meter @ Dh: 1.533	3	650.9	652.8		
Operator: NC	Meter Y: 1.0379	4	750.3	768.3		
Stack Dia: 48"	TC #: -3	5				
Amb. Press: 29.9	Start Time: 11:55	H2O Gain =				
Static Press: -0.02	Stop Time: 14:00	Filter:				

155A East

1255 B

Transverse Points	Time (Minute)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp. (F)	Mt. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	0.03	99	1.13	448.850	99	99	248	250	55	2	N/A	N/A
11	5	0.03	108	1.12	452.0	106	99	249	251	55			
10	10	0.03	108	1.13	455.1	109	101	250	252	55			
9	15	0.03	108	1.13	458.2	110	102	248	250	55			
8	20	0.03	110	1.13	461.3	111	103	248	249	55			
7	25	0.03	110	1.13	464.4	112	104	249	251	55			
6	30	0.03	110	1.13	467.5	113	105	251	252	56			
5	35	0.03	110	1.13	470.65	113	106	249	250	56			
4	40	0.03	109	1.13	473.8	114	106	252	253	56			
3	45	0.03	109	1.13	477.0	114	107	251	250	56			
2	50	0.03	109	1.13	480.2	114	107	248	249	57			
1	55	0.03	110	1.13	483.3	114	108	249	251	57			
	60				486.460								
12	0	0.03	110	1.13	486.460	108	108	249	250	57	2	N/A	N/A
11	5	0.03	112	1.13	489.6	114	107	250	252	57			
10	10	0.03	112	1.13	492.8	115	107	251	251	57			
9	15	0.03	111	1.13	496.0	115	108	249	252	57			
8	20	0.03	111	1.13	499.2	116	108	248	250	57			
7	25	0.03	110	1.14	502.3	115	109	249	251	57			
6	30	0.03	110	1.14	505.5	116	109	248	252	57			
5	35	0.03	109	1.14	508.7	116	109	249	250	57			
4	40	0.03	109	1.14	511.9	116	109	251	249	57			
3	45	0.03	109	1.14	515.1	116	109	249	249	57			
2	50	0.03	108	1.14	518.3	116	109	248	251	57			
1	55	0.03	106	1.14	521.5	116	109	249	252	56			
	60				524.682								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 110

Estimated Stack Temp: 110

Estimated Delta P: 0.03

Estimated Moisture Content: 2

Estimated O2: 20.8

Estimated CO2: 0.05

Equipment Evaluation, OK? Y or N

Ambient Temp: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

	1	2	3	4
DGM Initial:				
Vacuum:				
Leak Rate:				
DGM Final:				

Nozzle Information

Nozzle ID: _____

Nozzle Dia: 0.450

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #:	3	Pilot ID:	23	Impinger #	Initial	Final	Net	Pilot Leak Check	
Date:	8-18-19	Pilot Coeff.:	0.84	1	743.0	745.9		Initial:	<input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Client:	SCAQMD C	Meter Box #:	A-3	2	755.6	769.3		Final:	<input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Unit:	Outlet	Meter @ Dh:	1.583	3	632.4	635.2		Meter Box Leak Check	
Operator:	NC	Meter Y:	1.0379	4	777.1	894.0		Rate	"HG
Stack Dia:	48"	TC #:	73	5				Initial:	0.00 12
Amb. Press:	29.9	Start Time:	8:25	H2O Gain =				Final:	6.00 15
Static Press:	-0.02	Stop Time:	10:30	Filter:					

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp. (F)	Mt. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
A 12	0	0.06	93	2.15	528.75	66	66	248	251	55	3	N/A	N/A
11	5	0.06	98	2.14	533.15	69	66	249	248	49			
10	10	0.06	98	2.15	537.3	74	67	250	250	50			
9	15	0.06	100	2.15	541.5	77	68	249	252	52			
8	20	0.03	93	1.09	545.7	79	69	248	250	52			
7	25	0.03	94	1.09	548.7	79	71	247	249	54	2		
6	30	0.03	93	1.10	551.7	80	72	251	248	54			
5	35	0.03	92	1.02	554.7	81	73	250	251	55			
4	40	0.03	92	1.10	557.5	82	73	252	250	55			
3	45	0.03	93	1.10	560.5	83	75	248	249	55			
2	50	0.03	93	1.10	563.5	84	75	249	249	55			
1	55	0.03	96	1.10	566.5	84	76	249	251	55			
	60				569.520								
B 12	0	0.03	99	1.09	569.520	78	77	248	252	55	2	N/A	N/A
11	5	0.03	96	1.10	572.5	85	77	252	251	55			
10	10	0.03	99	1.10	575.5	86	78	252	250	56			
9	15	0.03	97	1.10	578.5	87	79	250	249	56			
8	20	0.03	97	1.10	581.5	87	79	252	250	57			
7	25	0.03	98	1.10	584.5	87	80	248	252	57			
6	30	0.03	98	1.11	587.5	88	82	249	250	57			
5	35	0.02	98	0.74	590.55	89	81	252	251	57			
4	40	0.02	99	0.73	593.0	88	81	249	251	57			
3	45	0.02	100	0.73	595.5	88	82	251	249	57			
2	50	0.04	107	2.20	598.0	89	82	248	251	58			
1	55	0.09	101	3.31	602.25	92	83	249	252	58			
	60				607.525								

Isokinetic Factor Setup Estimated Dry Gas Meter Temp: 80 Estimated Stack Temp: 90 Estimated Delta P: 0.04 Estimated Moisture Content: 2 Estimated O2: 20.8 Estimated CO2: 0.05	Equipment Evaluation, OK? Y or N Ambient Temp.: TC Check: Pilot Check: Tedlar Bag: Pilot Exp Date: TC Exp Date:	Dry Gas Meter Leak Checks DGM Initial: Vacuum: Leak Rate: DGM Final:	Nozzle Information Nozzle ID: Nozzle Dia: 0.450
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Location: Inlet 1 (Inside)

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ██████████ CA
 SAMPLING LOCATION Inlet 1
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 13.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 0.0 inches
 DEPTH OF STACK OR DUCT, D: 13.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

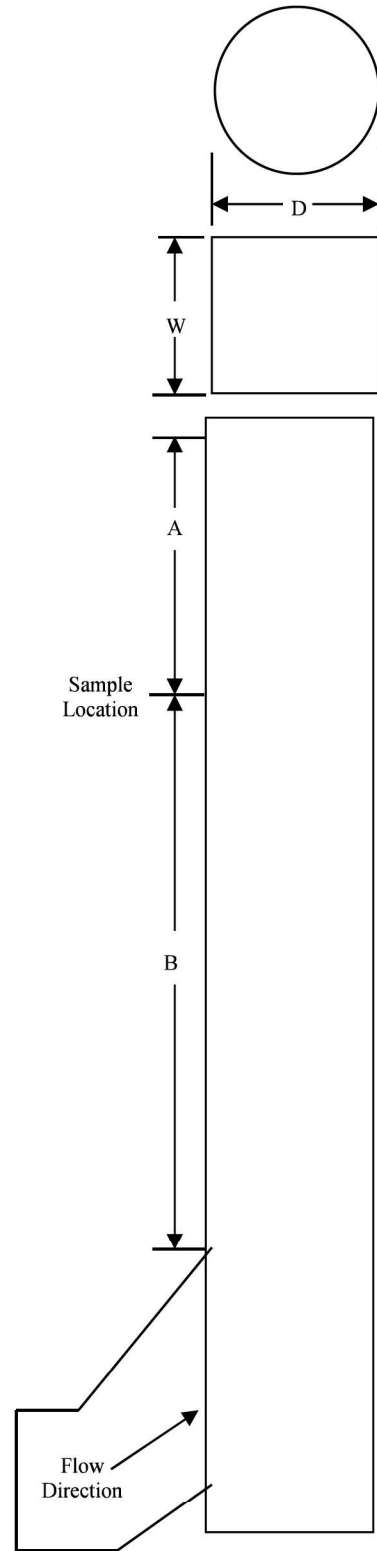
EQUIVALENT DIAMETER
 $De = 2*(DEPTH)*(WIDTH)/(DEPTH+WIDTH) =$ 13.00 inches

STACK/DUCT AREA = 0.92 sq.feet 132.7 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	<u>B</u>	<u>A</u>
# OF INCHES	>26.0	>6.5
# OF DIAMETERS	>2.00	>0.50

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	0.50	0 1/2
2	6.7	0.87	0 7/8
3	11.8	1.53	1 1/2
4	17.7	2.30	2 1/4
5	25.0	3.25	3 1/4
6	35.6	4.63	4 5/8
7	64.4	8.37	8 3/8
8	75.0	9.75	9 3/4
9	82.3	10.70	10 3/4
10	88.2	11.47	11 1/2
11	93.3	12.13	12 1/8
12	97.9	12.50	12 1/2



DRAWING NOT TO SCALE

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #:	1	Pitot ID:	85	Impinger #:	Initial	Final	Net	Pitot Leak Check		
Date:	8-12-19	Pitot Coeff.:	0.84	1:	766.2	765.6		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMD C	Meter Box #:	A-8	2:	729.5	746.6		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Unit 1	Meter @ Dh:	1.834	3:	655.9	658.6		Meter Box Leak Check		
Operator:	DJ	Meter Y:	1.0395	4:	862.6	880.0		Drate:		7HG:
Stack Dia:	7'-8" 13"	TC #:	85	5:				Initial:	002	18"
Amb. Press:	29.90	Start Time:	8:30	H2O Gain =				Final:	002	18"
Static Press:	-1.5	Stop Time:	10:55	Filter:						

Traverse Points	Time (Minutes)	Delta P (7HG)	Stack Temp. (F)	Set delta H (7HG)	Meter Volume (scf)	Mr. Inlet Temp. (F)	Mr. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (7HG)	TE Cooler Temp. (F)	Cyclonic Flow (7HG)
0	0				214.021								Jumped
1	5	.16	121	2.35	248.164	89	89	256	253	54	3	250	
2	10	.15	124	2.26	252.168	90	96	249	250	54	3	251	
3	15	.18	124	2.65	256.564	92	92	254	252	54	3	253	
4	20	.10	123	1.48	259.866	94	94	252	256	54	2.5	250	
5	25	.10	123	1.48	263.172	95	95	251	254	54	2.5	253	
6	30	.08	123	1.19	266.138	95	95	249	251	54	2	250	
7	35	.10	120	1.49	269.462	96	96	253	256	54	2.5	249	
8	40	.11	126	1.65	272.954	97	97	248	251	55	2.5	250	
9	45	.08	119	1.26	275.946	98	98	253	258	54	2	250	
10	50	.16	93	2.62	280.267	99	99	254	253	54	3	253	
11	55	.10	88	1.59	283.784	100	100	254	252	54	2.5	249	
12	60	.09	90	1.43	286.975	101	101	255	257	54	2.5	251	
0	0				286.975								
1	5	.19	130	2.80	291.528	99	99	252	258	54	3.5	250	
2	10	.17	134	2.49	295.815	99	99	253	256	54	3.5	249	
3	15	.18	130	2.67	306.258	101	101	254	253	54	3.5	249	
4	20	.18	130	2.68	304.715	103	103	253	256	54	3.5	250	
5	25	.13	139	1.91	308.498	104	104	253	252	54	3/	250	
6	30	.11	128	1.64	312.083	104	104	254	254	55	3	251	
7	35	.10	126	1.56	315.368	108	105	254	256	55	3	250	
8	40	.09	118	1.37	318.571	105	105	253	258	55	3	249	
9	45	.12	92	1.92	322.364	106	106	255	252	55	3	251	
10	50	.11	101	1.73	325.968	106	106	254	254	55	3	253	
11	55	.08	103	1.25	329.044	106	106	252	259	55	2.5	254	
12	60	.08	102	1.26	332.124	107	107	252	254	55	2.5	253	

ELD @ 7:50
st 7:55

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 110
 Estimated Stack Temp: 106
 Estimated Delta P: 2.0%
 Estimated Moisture Content: 208
 Estimated O2: 20.5
 Estimated CO2: 0.05

Equipment Evaluation, OK? Y or N

Ambient Temp.:
 TC Check:
 Pitot Check:
 Tedlar Bag: N/A
 Pitot Exp Date:
 TC Exp Date:

Dry Gas Meter Leak Checks

1	2	3	4

Nozzle Information

DGM Initial: Nozzle ID: #85
 Vacuum: Nozzle Dia: 1.348
 Leak Rate:
 DGM Final:

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #:	2	Pilot ID:	85	Impinger #:	Initial	Final	Not		
Date:	8-13-19	Pilot Coeff.:	0.94	1:	46.0	625.7		Initial:	Pilot Leak Check
Client:	SCAQMD	Meter Box #:	A-8	2:	735.0	744.0		Final:	<input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Unit:	Inlet 1	Meter @ Ch:	1.834	3:	651.0	652.5			
Operator:	DS	Meter Y:	1.0395	4:	875.1	889.3			
Stack Dia:	13" I	TC #:	85	5:					
Amb. Press:	29.90	Start Time:	11:55	H2O Gain =				Initial:	Meter Box Leak Check
Static Press:	-1.5	Stop Time:	14:00	Filter:				Final:	Rate: 19" Hg

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp (F)	Mt. Outlet Temp (F)	Oven Temp (F)	Probe Temp (F)	Impinger Temp (F)	Pump Vac (H2O)	TE Cooler Temp (F)	Cyclonic Flow (H2O)
0	0				332.682								Temp
1	5	.15	125	2.20	336.697	92	92	254	256	54	6	250	
2	10	.14	125	2.09	340.593	95	95	256	253	54	6	251	
3	15	.16	125	2.39	344.761	96	96	250	251	54	6	250	
4	20	.15	127	2.22	348.816	98	98	252	251	54	6	253	
5	25	.14	125	2.08	352.713	99	99	254	253	54	6	251	
6	30	.11	125	1.64	356.238	100	100	252	251	54	6	250	
7	35	.10	125	1.49	359.571	101	101	254	250	54	5	251	
8	40	.09	126	1.34	362.715	102	102	256	252	54	5	250	
9	45	.14	126	2.10	366.703	104	104	250	250	54	6	251	
10	50	.14	130	2.08	370.648	104	104	251	251	54	6	252	
11	55	.10	120	1.52	374.025	105	105	252	253	54	5	253	
12	60	.12	110	1.85	377.754	105	105	253	256	54	5.5	251	
0	0				377.754								
1	5	.18	128	2.69	382.226	104	104	251	250	54	6.5	250	
2	10	.16	128	2.39	386.452	105	105	254	251	54	6	250	
3	15	.15	130	2.24	390.558	106	106	255	253	54	6	248	
4	20	.14	136	2.07	394.501	107	107	256	254	55	6	251	
5	25	.11	128	1.65	398.034	108	108	254	250	55	5	250	
6	30	.10	130	1.50	401.390	108	108	260	253	55	5	250	
7	35	.14	129	2.11	405.378	109	109	251	255	55	6	254	
8	40	.12	126	1.81	409.078	108	108	254	251	55	5	251	
9	45	.10	125	1.51	412.457	108	108	250	253	55	5	250	
10	50	.11	124	1.67	416.602	108	108	254	251	56	5	251	
11	55	.10	124	1.52	419.388	109	109	255	250	56	5	252	
12	60	.15	120	2.29	423.546	109	109	250	251	56	6	253	

END @ 12:55
SF @ 13:00

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 110
 Estimated Stack Temp: 130
 Estimated Delta P:
 Estimated Moisture Content: 2.4%
 Estimated O2: 20.8
 Estimated CO2: .15

Equipment Evaluation, OK? Y or N

Ambient Temp: 83
 TC Check:
 Pilot Check:
 Tedlar Bag: N/A
 Pilot Exp Date:
 TC Exp Date:
 DGM Initial:
 Vacuum:
 Leak Rate:
 DGM Final:
 Nozzle ID: A85
 Nozzle Dia: .342

Dry Gas Meter Leak Checks

1	2	3	4

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #:	3	Pilot ID:	85	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-14-19	Pilot Coeff:	0.84	1	765.0	760.3		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMD C	Meter Box #:	A-8	2	731.5	747.4		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Inlet 1	Meter @ Dh:	1.834	3	665.8	659.4		Meter Box Leak Check		
Operator:	DJ	Meter Y:	1.0395	4	872.6	893.6		Rate	"HG	
Stack Dia:	13.0"	TC #:	85	5				Initial:	0.02	0.05"
Amb. Press:	29.90	Start Time:	8:25	H2O Gain =			Final:	0.00	16"	
Static Press:	-1.6	Stop Time:	10:30	Filter:						

Traverse Points	Time (Minutes)	Delta P ("H2O)	Stack Temp. (F)	Std Delta H ("H2O)	Meter Volume (scf)	Mt. Inlet Temp. (F)	Mt. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. ("HG)	Wet Cell Temp. (F)	Cyclonic Flow ("H2O)
0	0				424.019								
1	5	.18	126	2.59	438.324	82	82	252	251	54	3	250	
2	10	.15	116	2.26	432.308	83	83	251	253	54	3	251	
3	15	.16	112	2.37	436.431	84	84	250	251	54	3	250	
4	20	.14	104	2.11	440.348	87	87	248	250	54	3	249	
5	25	.14	99	2.14	444.305	90	90	253	250	54	3	250	
6	30	.13	98	2.00	448.128	91	91	253	250	54	3	250	
7	35	.12	104	1.83	451.993	93	93	250	256	54	2.5	251	
8	40	.11	94	1.71	455.346	94	94	249	251	54	2.5	252	
9	45	.10	96	1.57	458.743	94	94	250	249	54	2.5	251	
10	50	.08	86	1.27	461.807	95	95	248	249	54	2	253	
11	55	.10	90	1.57	465.214	96	96	255	252	54	2.5	253	
12	60	.09	87	1.42	468.453	96	96	253	250	54	2	251	
0	0				468.453								
1	5	.17	103	2.60	472.815	94	94	250	249	54	4	250	
2	10	.18	108	2.79	477.319	105	105	256	257	54	4	249	
3	15	.15	106	2.32	481.532	103	103	256	250	54	4	251	
4	20	.16	103	2.49	485.838	102	102	254	253	54	4	252	
5	25	.12	104	1.89	489.571	103	103	251	250	54	2.5	251	
6	30	.10	103	1.56	492.986	103	103	253	258	54	2.5	253	
7	35	.12	96	1.89	496.942	103	103	254	250	55	2.5	251	
8	40	.11	100	1.72	500.328	103	103	251	254	55	2.5	250	
9	45	.10	96	1.58	503.765	103	103	255	250	55	2.5	250	
10	50	.10	99	1.57	507.198	104	104	255	252	55	2.5	254	
11	55	.12	100	1.88	510.953	104	104	250	254	55	2.5	253	
12	60	.14	100	2.20	515.206	105	105	250	253	55	4	251	

2nd @
7:25
st @
7:30

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 110

Estimated Stack Temp: 130

Estimated Delta P:

Estimated Moisture Content: 2.6

Estimated O2: 20.8

Estimated CO2: 1.6

Equipment Evaluation, OK? Y or N

Ambient Temp: 63

TC Check:

Pilot Check:

Tedlar Bag: N/A

Pilot Exp Date:

TC Exp Date:

Dry Gas Meter Leak Checks

1	2	3	4

Nozzle Information

Nozzle ID: 85

Nozzle Dia: .348

DGM Initial:

Vacuum:

Leak Rate:

DGM Final:

Location: Inlet 2 (Upstream to Baghouse)

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ██████████ CA
 SAMPLING LOCATION Inlet 2
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 22.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 6.00 inches
 DEPTH OF STACK OR DUCT, D: 16.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

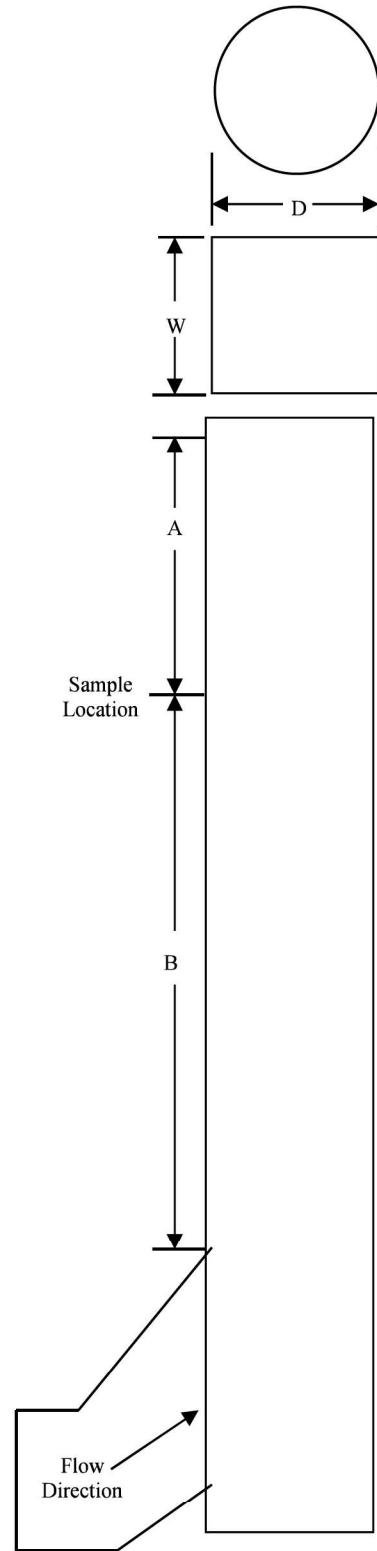
EQUIVALENT DIAMETER
 $De = 2 * (DEPTH) * (WIDTH) / (DEPTH + WIDTH) =$ 16.00 inches

STACK/DUCT AREA = 1.40 sq.feet 201.1 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	<u>B</u>	<u>A</u>
# OF INCHES	42.00	196.00
# OF DIAMETERS	2.63	12.25

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	0.50	6 1/2
2	6.7	1.07	7 1/8
3	11.8	1.89	7 7/8
4	17.7	2.83	8 7/8
5	25.0	4.00	10
6	35.6	5.70	11 3/4
7	64.4	10.30	16 1/4
8	75.0	12.00	18
9	82.3	13.17	19 1/8
10	88.2	14.11	20 1/8
11	93.3	14.93	20 7/8
12	97.9	15.50	21 1/2



DRAWING NOT TO SCALE

Run #: 1	Pilot ID: 28	Impinger #	Initial	Final	Net	Pilot Leak Check	
Date: 8-13-19	Pilot Coeff.: 0.84	1	758.7	752.5		Initial:	<input checked="" type="checkbox"/>
Client: SCAQMD C	Meter Box #: A6	2	732.9	754.2		Final:	<input checked="" type="checkbox"/>
Unit: INLET 2	Meter @ Dh: 1.785	3	650.4	656.9		Meter Box Leak Check	
Operator: WB	Meter Y: 1.0376	4	768.8	791.6		Rate	15
Stack Dia: 26	TC #: 28	5				Final:	10
Amb. Press: 29.9	Start Time: 0850	H2O Gain =				TIG	
Static Press: -4.2	Stop Time: 1055	Filter:				0.002	

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp (F)	Set delta H (H2O)	Meter Volume (scf)	Mr. Inlet Temp (F)	Mr. Outlet Temp (F)	Oven Temp (F)	Probe Temp (F)	Impinger Temp (F)	Pump Vac (H2O)	TE Cooler Temp (F)	Cyclonic Flow (H2O)
12	0.0	2.60	93	3.10	0.192	74	74	252	247	46	8		
11	5	2.55	94	3.05	4.97	75	75	254	249	48	8		
10	10	2.75	93	3.25	9.74	77	77	257	257	51	8		
9	15	2.90	93	3.45	14.58	79	79	254	249	52	8		
8	20	2.45	93	2.90	19.57	81	81	254	251	54	8		
7	25	2.65	93	3.15	24.31	84	84	249	249	56	8		
6	30	1.90	93	2.25	29.16	86	86	255	251	55	6		
5	35	1.50	91	1.80	33.35	87	87	254	250	57	5		
4	40	1.25	89	1.50	37.00	88	88	249	251	58	5		
3	45	1.20	86	1.45	40.42	89	89	251	251	59	5		
2	50	1.10	84	1.30	45.70	90	90	249	252	60	4		
1	55	1.20	77	1.45	46.88	90	90	253	250	60	4		
12	60	2.15	94	2.55	50.16	90	90	251	253	48	7		
11	65	2.25	95	2.65	54.54	90	90	252	251	49	7		
10	70	2.35	95	2.80	59.06	91	91	250	249	51	7		
9	75	2.40	94	2.85	63.69	93	93	256	254	53	7		
8	80	2.30	98	2.75	68.36	94	94	249	251	53	7		
7	85	2.35	96	2.80	72.96	96	96	250	253	55	7		
6	90	2.10	98	2.50	77.57	97	97	253	250	56	6		
5	95	1.50	98	1.80	81.98	98	98	250	248	57	5		
4	100	1.20	96	1.45	85.68	98	98	256	251	58	5		
3	105	1.15	95	1.35	88.97	99	99	249	252	59	5		
2	110	1.20	82	1.45	92.22	99	99	256	249	60	5		
1	115	1.20	84	1.45	95.52	99	99	256	251	60	5		
END	120				98.912								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: _____

Estimated Stack Temp: _____

Estimated Delta P: _____

Estimated Moisture Content: _____

Estimated O2: _____

Estimated CO2: _____

Equipment Evaluation - OK? Y or N

Ambient Temp: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

1	2	3	4
DGM Initial:			
Vacuum:			
Leak Rate:			
DGM Final:			

Nozzle Information

Nozzle ID: **G372**

Nozzle Dia: **0.184**

Run #:	2	Pilot ID:	-28	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-13-19	Pilot Coeff.:	0.84	1	646.2	656.2		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMDC	Meter Box #:	A-6	2	763.2	774.8		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	IMUS 2	Meter @ Dh:	1.789	3	628.4	631.0		Meter Box Leak Check		
Operator:	WB	Meter Y:	1.0376	4	827.8	844.8		Rate	*HG	
Stack Dia:	16"	TC #:	28	5				Initial:	15	0.002
Amb. Press:	29.90	Start Time:	1155	H2O Gain =			Final:	10	0.000	
Static Press:	-4.2	Stop Time:	1400	Filter:						

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mtr. Inlet Temp. (F)	Mtr. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	2.70	102	3.20	98.960	95	93	280	251	49	0.87		
11	5	2.45	101	2.90	103.91	93	93	287	253	50	0.87		
10	10	2.65	103	3.05	108.67	95	95	286	250	50	7		
9	15	2.60	104	3.10	113.57	97	97	249	252	51	7		
8	20	2.50	105	2.95	118.49	94	94	251	250	52	7		
7	25	2.50	105	2.75	123.26	102	102	253	248	53	7		
6	30	1.80	102	2.15	128.05	103	103	252	250	54	6		
5	35	1.50	99	1.80	132.10	105	105	252	251	55	5		
4	40	1.20	100	1.45	135.82	106	106	254	250	56	5		
3	45	1.10	96	1.30	139.27	107	107	252	253	57	5		
2	50	1.10	95	1.50	142.44	108	108	253	253	58	5		
1	55	1.05	98	1.25	145.76	108	108	257	249	57	5		
12	60	2.20	101	2.60	149.89	107	107	251	252	52	7		
11	65	2.30	100	2.75	153.42	108	108	252	253	52	7		
10	70	2.30	100	2.75	158.10	107	107	257	250	54	7		
9	75	2.45	98	2.90	162.75	110	110	253	250	55	7		
8	80	1.90	98	2.25	167.05	111	111	253	248	56	6		
7	85	1.85	99	2.20	171.88	112	112	252	250	56	6		
6	90	1.80	99	2.15	176.04	112	112	257	252	56	6		
5	95	1.35	100	1.60	180.11	113	113	255	251	56	6		
4	100	1.10	97	1.30	183.79	112	112	252	249	57	5		
3	105	1.20	95	1.45	187.02	112	112	255	252	58	5		
2	110	1.20	90	1.45	190.41	111	111	254	250	58	5		
1	115	1.20	92	1.45	193.75	111	111	257	249	59			
ENV	120				197.206								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: _____

Estimated Stack Temp: _____

Estimated Delta P: _____

Estimated Moisture Content: _____

Estimated O2: _____

Estimated CO2: _____

Equipment Evaluation, OK? Y or N

Ambient Temp: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

	1	2	3	4	
DGM Initial:					Nozzle ID: _____
Vacuum:					Nozzle Dia: _____
Leak Rate:					
DGM Final:					

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #:	3	Pilot ID:	# 28	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-14-19	Pilot Coeff.:	0.84	1	759.0	746.2		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCARMDC	Meter Box #:	A-6	2	735.9	760.9		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Inlet 2	Meter @ Dh:	1.789	3	651.5	660.1		Meter Box Leak Check		
Operator:	WR	Meter Y:	1.0376	4	797.2	822.4		Rate	7HG	
Stack Dia:	26	TC #:	28	5				Initial:	15	0.007
Amb. Press:	29.9	Start Time:	0825	H2O Gain =				Final:	10	0.000
Static Press:	-4.2	Stop Time:	1030	Filter:						

Transverse Points	Time (Minutes)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp. (F)	Mt. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	1.95	99	2.30	197.573	71	71	251	248	47	6		
11	5	2.35	100	2.75	201.59	72	72	255	251	46	7		
10	10	2.60	97	3.05	206.10	74	74	255	253	48	7		
9	15	2.40	99	2.80	210.78	76	76	249	252	50	7		
8	20	2.20	96	2.60	215.33	78	78	248	250	51	6		
7	25	2.40	96	2.80	219.73	80	80	252	251	53	6		
6	30	2.25	97	2.65	224.32	82	82	255	249	55	6		
5	35	1.40	95	1.65	228.74	84	84	256	254	55	5		
4	40	1.20	92	1.40	232.26	85	85	249	251	56	4		
3	45	1.20	87	1.40	235.52	86	86	254	254	58	4		
2	50	1.20	89	1.40	238.77	87	87	255	249	60	4		
1	55	1.15	90	1.35	242.09	87	87	251	253	61	4		
12	60	1.70	93	2.00	245.26	87	87	255	250	53	5		
11	65	1.85	94	2.15	249.11	88	88	252	248	53	5		
10	70	2.10	95	2.45	253.10	89	89	255	251	54	6		
9	75	2.20	95	2.60	257.37	90	90	251	250	56	6		
8	80	1.80	96	2.10	261.88	93	93	248	250	58	6		
7	85	2.10	97	2.45	265.88	93	93	249	252	59	6		
6	90	1.80	100	2.10	270.19	94	94	256	250	59	6		
5	95	1.50	102	1.75	274.34	96	96	257	254	59	5		
4	100	1.30	98	1.55	277.90	96	96	252	251	59	5		
3	105	1.10	97	1.30	281.45	97	97	249	253	58	5		
2	110	1.05	94	1.25	284.64	97	97	256	251	55	5		
1	115	1.20	94	1.40	287.77	98	98	255	256	55	5		
12	120				291.049								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: _____

Estimated Stack Temp: _____

Estimated Delta P: _____

Estimated Moisture Content: _____

Estimated O2: _____

Estimated CO2: _____

Equipment Evaluation, OK? Y or N

Ambient Temp: _____

TC Check: _____

Pitot Check: _____

Tedlar Bag: _____

Pitot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

1	2	3	4
DGM Initial:			
Vacuum:			
Leak Rate:			
DGM Final:			

Nozzle Information

Nozzle ID: _____

Nozzle Dia: _____

APPENDIX C3

MULTIPLE METAL EMISSIONS – LABORATORY DATA

Mehod 436 Lab Data Summary								
				I1	I2	Outlet		
				Inlet 1 (Inside)	Inlet 2 (Outside)	Outlet	RB	FB
				1	Upstream of Baghouse			
Run 1	Arsenic	As	ug	15	3.7	<1	<1	<1
	Cadmium	Cd	ug	<1	<1	<1	<1	<1
	Chromium	Cr	ug	4400	1000	5.3	1.5	1.6
	RB Corrected	Cr	ug	4398.5	998.5	3.8		
	Nickel	Ni	ug	94	32	2.9	1.3	1.4
	RB Corrected	Ni	ug	92.7	30.7	1.6		
Run 2	Arsenic	As	ug	7.7	1.8	<1		
	Cadmium	Cd	ug	<1	<1	<1		
	Chromium	Cr	ug	7100	1500	2.9		
	RB Corrected	Cr	ug	7098.5	1498.5	1.4		
	Nickel	Ni	ug	240	53	2		
	RB Corrected	Ni	ug	238.7	51.7	0.70		
Run 3	Arsenic	As	ug	3.0	1.5	<1		
	Cadmium	Cd	ug	<1	<1	<1		
	Chromium	Cr	ug	4000	1600	6		
	RB Corrected	Cr	ug	3998.5	1598.5	4.5		
	Nickel	Ni	ug	130	55	2.7		
	RB Corrected	Ni	ug	128.7	53.7	1.4		
AVG	Arsenic	As	ug	8.6	2.33	<1		
	Cadmium	Cd	ug	<1.0	<1.0	<1.0		
	Chromium RB Corr.	Cr	ug	5165.2	1365.2	3.23		
	Nickel RB Corr.	Ni	ug	153.4	45.4	1.23		

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Project Number: 10562/IN(I)/In(O)/Out

Reported:
06/20/2019 07:57

Project Manager: Almega Environmental & Technical Services

Sample Summary

Sample Name	Sampled By	Lab ID	Matrix	Sampled	Qualifiers
105462 - M436 - C1 - In(O) - FB	Client	9E30032-01	Filter	05/21/19 09:00	
105462 - M436 - C1 - In(I) - R1	Client	9E30032-04	Filter	05/21/19 12:10	
105462 - M436 - C1 - In(O) - R1	Client	9E30032-07	Filter	05/21/19 12:10	
105462 - M436 - C1 - Out - R1	Client	9E30032-10	Filter	05/21/19 12:10	
105462 - M436 - C1 - In(I) - R2	Client	9E30032-13	Filter	05/21/19 15:10	
105462 - M436 - C1 - In(O) - R2	Client	9E30032-16	Filter	05/21/19 15:10	
105462 - M436 - C1 - Out - R2	Client	9E30032-19	Filter	05/21/19 15:10	
105462 - M436 - C1 - In(I) - R3	Client	9E30032-22	Filter	05/22/19 08:30	
105462 - M436 - C1 - In(O) - R3	Client	9E30032-25	Filter	05/22/19 08:30	
105462 - M436 - C1 - Out - R3	Client	9E30032-28	Filter	05/22/19 08:30	
105462-M436-RB-Filter	Client	9E30032-31	Filter	05/22/19 09:30	



WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Project Number: 10562/IN(I)/In(O)/Out

Project Manager: Almega Environmental & Technical Services

Reported:
06/20/2019 07:57

Sample Results

(Continued)

Sample: 105462 - M436 - C1 - In(O) - R3
9E30032-25 (Filter) Sampled: 05/22/19 8:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W9F0681	Instr: ICPMS03	Prepared: 06/12/19 16:26	Analyst: ALN		
Arsenic, Total	ND	1.0	ug/filter	5	06/17/19 15:03	
Cadmium, Total	ND	1.0	ug/filter	5	06/17/19 15:03	
Chromium, Total	60	0.20	ug/filter	1	06/17/19 13:48	
Nickel, Total	44	0.20	ug/filter	1	06/17/19 13:48	

Sample: 105462 - M436 - C1 - Out - R3
9E30032-28 (Filter) Sampled: 05/22/19 8:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W9F0681	Instr: ICPMS03	Prepared: 06/12/19 16:26	Analyst: ALN		
Arsenic, Total	ND	1.0	ug/filter	5	06/17/19 15:05	
Cadmium, Total	ND	1.0	ug/filter	5	06/17/19 15:05	
Chromium, Total	2.1	0.20	ug/filter	1	06/17/19 14:02	
Nickel, Total	1.9	0.20	ug/filter	1	06/17/19 14:02	

Sample: 105462-M436-RB-Filter
9E30032-31 (Filter) Sampled: 05/22/19 9:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W9F0681	Instr: ICPMS03	Prepared: 06/12/19 16:26	Analyst: ALN		
Arsenic, Total	ND	1.0	ug/filter	5	06/17/19 14:18	
Cadmium, Total	ND	1.0	ug/filter	5	06/17/19 14:18	
Chromium, Total	1.6	0.20	ug/filter	1	06/17/19 13:31	
Nickel, Total	1.3	0.20	ug/filter	1	06/17/19 13:31	

Work Orders: 9H26086

Report Date: 10/14/2019

Project: 10566 Baghouse SCAQMD-C

Received Date: 8/19/2019

Turnaround Time: Normal

Phones: (714) 889-4000

Fax: (714) 889-7030

Attn: Almega Environmental & Technical Services

P.O. #:

Client: Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Billing Code:

ELAP-CA #1132 • EPA-UCMR #CA00211 • Guam-EPA #17-008R • HW-DOH # • ISO 17025 #L2457.01 • LACSD #10143 •
NELAP-CA #04229CA • NELAP-OR #4047 • NJ-DEP #CA015 • NV-DEP #NAC 445A • SCAQMD #93LA1006

This is a complete final report. The information in this report applies to the samples analyzed in accordance with the chain-of-custody document. Weck Laboratories certifies that the test results meet all requirements of TNI unless noted by qualifiers or written in the Case Narrative. This analytical report must be reproduced in its entirety.

Dear Almega Environmental & Technical Services,

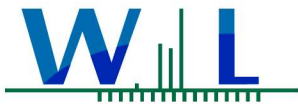
Enclosed are the results of analyses for samples received 8/19/19 with the Chain-of-Custody document. The samples were received in good condition, at 5.1 °C. All analyses met the method criteria except as noted in the case narrative or in the report with data qualifiers.

Reviewed by:



Brandon Gee
Operations Manager/Senior PM





WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Certificate of Analysis

Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

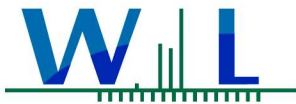
Reported:

10/14/2019 13:56

Project Manager: Almega Environmental & Technical Services

Sample Summary

Sample Name	Sampled By	Lab ID	Matrix	Sampled	Qualifiers
10566-M436-FB-C1	Client	9H26086-01	Filter	08/13/19 07:30	
10566-M436-I1-R1-C1	Client	9H26086-04	Filter	08/13/19 10:55	
10566-M436-I2-R1-C1	Client	9H26086-07	Filter	08/13/19 10:55	
10566-M436-O-R1-C1	Client	9H26086-10	Filter	08/13/19 10:55	
10566-M436-I1-R2-C1	Client	9H26086-13	Filter	08/13/19 14:00	
10566-M436-I2-R2-C1	Client	9H26086-16	Filter	08/13/19 14:00	
10566-M436-O-R2-C1	Client	9H26086-19	Filter	08/13/19 14:00	
10566-M436-I1-R3-C1	Client	9H26086-22	Filter	08/14/19 10:30	
10566-M436-I2-R3-C1	Client	9H26086-25	Filter	08/14/19 10:30	
10566-M436-O-R3-C1	Client	9H26086-28	Filter	08/14/19 10:30	



WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Certificate of Analysis

Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:

10/14/2019 13:56

Project Manager: Almega Environmental & Technical Services

Sample Results

Sample: 10566-M436-FB-C1
9H26086-01 (Filter) Sampled: 08/13/19 7:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	ND	1.0	ug/filter	5	10/04/19 16:06	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:06	
Chromium, Total	1.6	0.20	ug/filter	1	10/04/19 18:58	
Nickel, Total	1.4	0.20	ug/filter	1	10/04/19 18:58	

Sample: 10566-M436-I1-R1-C1
9H26086-04 (Filter) Sampled: 08/13/19 10:55 by Client

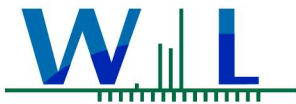
Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	15	1.0	ug/filter	5	10/04/19 16:10	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:10	
Chromium, Total	4400	100	ug/filter	500	10/04/19 17:56	
Nickel, Total	94	0.20	ug/filter	1	10/04/19 19:02	

Sample: 10566-M436-I2-R1-C1
9H26086-07 (Filter) Sampled: 08/13/19 10:55 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	3.7	1.0	ug/filter	5	10/04/19 16:15	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:15	
Chromium, Total	1000	100	ug/filter	500	10/04/19 18:01	
Nickel, Total	32	0.20	ug/filter	1	10/04/19 19:11	

Sample: 10566-M436-O-R1-C1
9H26086-10 (Filter) Sampled: 08/13/19 10:55 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	ND	1.0	ug/filter	5	10/04/19 16:19	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:19	
Chromium, Total	5.3	0.20	ug/filter	1	10/04/19 19:16	
Nickel, Total	2.9	0.20	ug/filter	1	10/04/19 19:16	



WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Certificate of Analysis

Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:
10/14/2019 13:56

Project Manager: Almega Environmental & Technical Services

Sample Results

(Continued)

Sample: 10566-M436-I1-R2-C1
9H26086-13 (Filter) Sampled: 08/13/19 14:00 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	7.7	1.0	ug/filter	5	10/04/19 16:24	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:24	
Chromium, Total	7100	500	ug/filter	2500	10/04/19 18:05	
Nickel, Total	240	1.0	ug/filter	5	10/04/19 16:24	

Sample: 10566-M436-I2-R2-C1
9H26086-16 (Filter) Sampled: 08/13/19 14:00 by Client

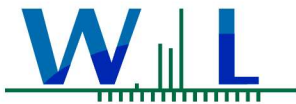
Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	1.8	1.0	ug/filter	5	10/04/19 16:29	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:29	
Chromium, Total	1500	100	ug/filter	500	10/04/19 18:10	
Nickel, Total	53	0.20	ug/filter	1	10/04/19 19:29	

Sample: 10566-M436-O-R2-C1
9H26086-19 (Filter) Sampled: 08/13/19 14:00 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	ND	1.0	ug/filter	5	10/04/19 16:33	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:33	
Chromium, Total	2.9	0.20	ug/filter	1	10/04/19 19:34	
Nickel, Total	2.0	0.20	ug/filter	1	10/04/19 19:34	

Sample: 10566-M436-I1-R3-C1
9H26086-22 (Filter) Sampled: 08/14/19 10:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	3.0	1.0	ug/filter	5	10/04/19 16:38	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:38	
Chromium, Total	4000	100	ug/filter	500	10/04/19 18:15	
Nickel, Total	130	1.0	ug/filter	5	10/04/19 16:38	



WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Certificate of Analysis

Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:
10/14/2019 13:56

Project Manager: Almega Environmental & Technical Services

Sample Results

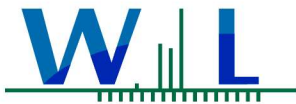
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Sample: 10566-M436-I2-R3-C1
9H26086-25 (Filter) Sampled: 08/14/19 10:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	1.5	1.0	ug/filter	5	10/04/19 16:42	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:42	
Chromium, Total	1600	100	ug/filter	500	10/04/19 18:35	
Nickel, Total	55	0.20	ug/filter	1	10/04/19 19:47	

Sample: 10566-M436-O-R3-C1
9H26086-28 (Filter) Sampled: 08/14/19 10:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020	Batch ID: W910712	Instr: ICPMS03	Prepared: 09/12/19 12:49	Analyst: aln		
Arsenic, Total	ND	1.0	ug/filter	5	10/04/19 16:47	
Cadmium, Total	ND	1.0	ug/filter	5	10/04/19 16:47	
Chromium, Total	6.0	0.20	ug/filter	1	10/04/19 19:52	
Nickel, Total	2.7	0.20	ug/filter	1	10/04/19 19:52	



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Almega Environmental & Technical Services
10602 Walker St
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Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:

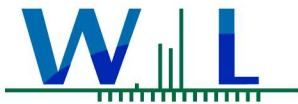
10/14/2019 13:56

Project Manager: Almega Environmental & Technical Services

Quality Control Results

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Analyte	Result	MRL	Units	Spike Level	Source Result	%REC	Limits	RPD	RPD Limit	Qualifier
Batch: W910712 - EPA 6020										
Blank (W910712-BLK1)				Prepared: 09/12/19 Analyzed: 10/04/19						
Arsenic, Total	ND	0.20	ug/filter							
Cadmium, Total	ND	0.40	ug/filter							
Chromium, Total	ND	0.20	ug/filter							
Nickel, Total	ND	0.20	ug/filter							
LCS (W910712-BS1)				Prepared: 09/12/19 Analyzed: 10/04/19						
Arsenic, Total	4.86	1.0	ug/filter	5.00		97	80-120			
Cadmium, Total	4.88	1.0	ug/filter	5.00		98	80-120			
Chromium, Total	5.63	0.20	ug/filter	5.00		113	80-120			
Nickel, Total	5.56	0.20	ug/filter	5.00		111	80-120			
LCS Dup (W910712-BSD1)				Prepared: 09/12/19 Analyzed: 10/04/19						
Arsenic, Total	4.83	1.0	ug/filter	5.00		97	80-120	0.7	20	
Cadmium, Total	5.02	1.0	ug/filter	5.00		100	80-120	3	20	
Chromium, Total	5.56	0.20	ug/filter	5.00		111	80-120	1	20	
Nickel, Total	5.47	0.20	ug/filter	5.00		109	80-120	2	20	



WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Project Number: 10566 Baghouse SCAQMD-C

Project Manager: Almega Environmental & Technical Services

Certificate of Analysis

Almega REPORT
ENVIRONMENTAL

Reported:
10/14/2019 13:56



Notes and Definitions

Item	Definition
% Rec	Percent Recovery
Dil	Dilution
dry	Sample results reported on a dry weight basis
MDA	Minimum Detectable Activity
MDL	Method Detection Limit
MRL	The minimum levels, concentrations, or quantities of a target variable (e.g., target analyte) that can be reported with a specified degree of confidence. The MRL is also known as Limit of Quantitation (LOQ)
ND	NOT DETECTED at or above the Method Reporting Limit (MRL). If Method Detection Limit (MDL) is reported, then ND means not detected at or above the MDL.
NR	Not Reportable
RPD	Relative Percent Difference
Source	Sample that was matrix spiked or duplicated.
TIC	Tentatively Identified Compound (TIC) using mass spectrometry. The reported concentration is relative concentration based on the nearest internal standard. If the library search produces no matches at, or above 85%, the compound is reported as unknown.

Any remaining sample(s) will be disposed of one month from the final report date unless other arrangements are made in advance.

An Absence of Total Coliform meets the drinking water standards as established by the California State Water Resources Control Board (SWRCB)

All results are expressed on wet weight basis unless otherwise specified.

All samples collected by Weck Laboratories have been sampled in accordance to laboratory SOP Number MIS002.

9426086



INVOICE TO: _____ **REPORT TO:** _____ **PO #** 10566

ALMEGA Environmental & Technical Services
 10602 Walker St.
 Cypress, CA 90630
 (714) 889-4000 Fax (714) 889-7030
 lab@almegaenv.com

ATTN: Charles **Contact:** _____

Job #	10566	Unit #	Baghouse	Client	SCAQMD - C	Location: Inlet & Outlet	ANALYSIS REQUESTED				Turnaround Time
							Standard:	Other:	Return or Dispose	REMARKS	
Unit Information:							LAB M436 CR N. DLS				
Project Manager: Morgan Nguyen											
Sample Date	Sample Time	Sample Identification	Lab Sample #	Type Of Sample	Liquid	Gas	Solid	No of Containers			
8/13/2019	7:30	10566-M436-FB-C1					X	1			
		10566-M436-FB-C2		X				1			combine
		10566-M436-FB-C3		X				1			
8/13/2019	8:50 - 10:55	10566-M436-I1-R1-C1					X	1			
		10566-M436-I1-R1-C2		X				1			combine
		10566-M436-I1-R1-C3		X				1			
8/13/2019	8:50 - 10:55	10566-M436-I2-R1-C1					X	1			
		10566-M436-I2-R1-C2		X				1			combine
		10566-M436-I2-R1-C3		X				1			
8/13/2019	8:50 - 10:55	10566-M436-O-R1-C1					X	1			
		10566-M436-O-R1-C2		X				1			combine
		10566-M436-O-R1-C3		X				1			
Relinquished by: _____							Received by: _____				
Date:	8/16/2019	Time	11:30	Date:	8/16/2019	Time:	11:40	Date:	8/19/19	Time:	13:45
Relinquished by:	_____			Relinquished by:	_____			Relinquished by:	_____		
Date:	8/19/19	Time	14:25	Date:	8/19/19	Time:	14:25	Date:	8/19/19	Time:	13:45

5:10 Form

9H26086

INVOICE TO:		REPORT TO:		PO # 10566		Turnaround Time											
		ALMEGA Environmental & Technical Services				Standard: <input checked="" type="checkbox"/> Other: _____											
		10602 Walker St.				Rush: _____											
		Cypress, CA 90630				Depends on # of Samples											
		(714) 889-4000 Fax (714) 889-7030				5 - 10 days _____											
		lab@almegaenv.com				3 - 7 days _____											
ATTN: Charles		Contact:				Return or Dispose											
Job #	10566	Unit #	Baghouse	Client	SCAQMD - C	Location:	Inlet & Outlet										
Unit Information:																	
Project Manager:	Morgan Nguyen																
Sample Date	Sample Time	Sample Identification	Lab Sample #	Type Of Sample	Liquid	Gas	Solid										
				No of Containers													
8/14/2019	8:25 - 10:30	10566-M436-11-R3-C1					X	1									
		10566-M436-11-R3-C2				X		1									combine
		10566-M436-11-R3-C3				X		1									
8/14/2019	8:25 - 10:30	10566-M436-12-R3-C1					X	1									
		10566-M436-12-R3-C2				X		1									combine
		10566-M436-12-R3-C3				X		1									
8/14/2019	8:25 - 10:30	10566-M436-O-R3-C1					X	1									
		10566-M436-O-R3-C2				X		1									combine
		10566-M436-O-R3-C3				X		1									
Relinquished by:				Received by:													
Date:	8/16/2019	Time	11:30	Date:	8/16/19	Time:	11:40	Relinquished by:				Received by:					
Relinquished by:				Received by:													
Date:	8/16/19	Time	14:25	Date:	8/16/19	Time:	14:25	Relinquished by:				Received by:					

Handwritten notes: CAPD, M436, 10566, 10566

Handwritten notes: Received by: [Signature], Date: 8/16/19, Time: 11:40; Relinquished by: [Signature], Date: 8/16/19, Time: 14:25; S-112 T-0222

APPENDIX C4
O₂/CO₂ RESULTS – FIELD & LABORATORY DATA

LABORATORY REPORT
Carbon Dioxide & Oxygen by TCD
by Modified SCAQMD Method 25.3 (TCA/FID)

Client: AQMD
Project No.: c10566
Unit Tested: Facility C
Sampling Date: 13-Aug-19
Analyzed Date: 20-Aug-19
Lab No.: A 085

Client Sample ID	Lab ID	Almega Sample ID	CO ₂ % v/v by TCD	O ₂ % v/v by TCD
		Tank		
Facility C				
10566-M10.1-I2-O2/CO2	A 085 - 01	29	ND	20.8
10566-M10.1-II-O2/CO2	A 085 - 02	14	ND	20.8
10566-M10.1-O-O2/CO2	A 085 - 03	37	ND	20.9
Detection Limit			0.3	0.3

* NOTE - the BIAS FACTOR (of 1.086) is NOT applied in these results.

ND=Not Detected

TGMNEO concentration values are reported in ppm (v.v) as Methane (carbon#=1).

The sample cylinder is analyzed for NMNEO, CO, CH₄, CO₂ and C₃H₆. It is then directed to a separation column where all heavy organics (C₃+) separate from the light organics (CO, CO₂, CH₄ and C₃H₆). The light organics are then passed through a reduction catalyst to convert CO and CO₂ to CH₄, and are then directed to a FID for detection and quantification. The heavy organics are backflushed off the holding column, passed through an oxidation catalyst, which convert all organics to CO₂, then through a reduction catalyst to convert CO₂ to CH₄ and then to a FID for detection and quantification.

Reviewed by: _____



CALCULATIONS



Client: AQMD
Project No.: c10566
Unit Tested: Facility C
Sampling Date: 13-Aug-19
Date tested: 20-Aug-19

Lab No.: A 085

Parameter	Symbol	Units	Run #1 10566-M10.1-12-O2/CO2 A 085 - 01	Run #2 10566-M10.1-11-O2.CO2 A 085 - 02
Sample ID				
Lab ID				
<u>Sample Tank</u>				
Tank No			29	14
Sample Tank Volume	V_T	L	12.085	12.035
Barometric Pressure	P_b	mm Hg	763	763
Pre-test Pressure	P_{T1}	mm Hg (abs)	2.00	2.00
Pre-test Temperature	t_{T1}	°C	21	21
Abs. Pre-test Temperature	T_{T1}	°K	294	294
Post-test Pressure	P_{T2}	mm Hg (abs)	372	330
Post-test Temperature	t_{T2}	°C	21	21
Abs. Post-test Temperature	c	°K	294	294
Final Pressure	P_{TF}	mm Hg (abs)	926	930
Abs. Final Temperature	T_{TF}	°K	293	293
Dilution Factor	DF_T		2.51	2.85
Sample Volume	V_s	L	5.778	5.101

Calculations

$$V_s = k_1 \cdot V_T \cdot (P_{T2}/T_{T2} - P_{T1}/T_{T1})$$

$$k_1 = (273 + 15.56) / 760 = 0.3799$$

$$C_{SAT} = DF \cdot C_{SA}$$

$$C_{CO2} = DF \cdot C_{CO}$$

$$DF = (P_{TF}/T_{TF}) / (P_{T2}/T_{T2} - P_{T1}/T_{T1})$$

CALCULATIONS

Client:	AQMD	Lab No.:
Project No.:	c10566	A 085
Unit Tested:	Facility C	
Sampling Date:	13-Aug-19	
Date tested:	20-Aug-19	

Parameter	Symbol	Units	Run #3
Sample ID			10566-M10.1-O-O2/CO2
Lab ID			A 085 - 03
<u>Sample Tank</u>			
Tank No			37
Sample Tank Volume	V_T	L	12.085
Barometric Pressure	P_b	mm Hg	763
Pre-test Pressure	P_{T1}	mm Hg (abs)	2.00
Pre-test Temperature	t_{T1}	°C	21
Abs. Pre-test Temperature	T_{T1}	°K	294
Post-test Pressure	P_{TS}	mm Hg (abs)	416
Post-test Temperature	t_{TS}	°C	21
Abs. Post-test Temperature	T_{TS}	°K	294
Final Pressure	P_{TF}	mm Hg (abs)	932
Abs. Final Temperature	T_{TF}	°K	293
Dilution Factor	DF_T		2.26

Sample Volume	V_s	L	6.465
---------------	-------	---	-------

Calculations

$$V_s = k_1 * V_T * (P_{TS}/T_{TS} - P_{TF}/T_{TF})$$

$$k_1 = (273 + 15.56) / 760 = 0.3799$$

$$DF = (P_{TF}/T_{TF}) / (P_{TS}/T_{TS} - P_{TF}/T_{TF})$$

$$C_{SAT} = DF * C_{SA}$$

$$C_{COT} = DF * C_{CO}$$

QA/QC SUMMARY
(Repeat Analysis)



Client Project No.: c10566
 Sampling Date: 13-Aug-19
 Run #1

Lab No.: A 085
 Analyzed Date: 20-Aug-19

Analyte	Sample ID	Area Count #1	Area Count #2	Area % diff (±20%)	Conc # 1	Conc # 2	Mean Conc ppm	% diff from Mean
Tank Analysis								
CO2*	A 085 - 01	ND	ND	ND	ND	ND	ND	ND
O2*	A 085 - 01	1598972	1573856	1.57	8.3	8.2	8.3	1.58

Run #2

Analyte	Sample ID	Area Count #1	Area Count #2	Area Count #3	Conc # 1	Conc # 2	Mean Conc ppm	% diff from Mean
Tank Analysis								
CO2*	A 085 - 02	ND	ND	ND	ND	ND	ND	ND
O2 *	A 085 - 02	1398715	1399520	-0.06	7.3	7.3	7.3	-0.06

* - by GC/TCD

$$\text{Conc}_{\text{CO}} \text{ in tank} = \text{MeanConc}_{\text{CO}} * \text{DF}$$

$$\text{Conc}_{\text{CO}_2} \text{ in tank} = \text{MeanConc}_{\text{CO}_2} * \text{DF}$$

$$\text{Conc}_{\text{O}_2} \text{ in tank} = \text{MeanConc}_{\text{O}_2} * \text{DF}$$

QA/QC SUMMARY
(Repeat Analysis)



Client Project No.:	c10566	Lab No.:	A 085
Sampling Date:	13-Aug-19	Analyzed Date:	20-Aug-19
Run #3			

Analyte	Sample ID	Area Count #1	Area Count #2	Area Count #3	Conc # 1	Conc # 2	Mean Conc ppm	% diff from Mean
Tank Analysis								
CO2*	A 085 - 03	ND	ND	ND	ND	ND	ND	ND
O2*	A 085 - 03	1750794	1792895	-2.40	9.1	9.4	9.2	-2.38

* - by GC/TCD

$$\text{Conc}_{\text{CO}} \text{ in tank} = \text{MeanConc}_{\text{CO}} * \text{DF}$$

$$\text{Conc}_{\text{CO}_2} \text{ in tank} = \text{MeanConc}_{\text{CO}_2} * \text{DF}$$

$$\text{Conc}_{\text{O}_2} \text{ in tank} = \text{MeanConc}_{\text{O}_2} * \text{DF}$$

Lot # A085



Almega ENVIRONMENTAL
CHAIN OF CUSTODY RECORDS

INVOICE TO:		REPORT TO:		PO #		Turnaround Time		
		ALMEGA Environmental & Technical Services 10602 Walker St. Cypress, CA 90630 (714) 889-4000 Fax (714) 889-7030 lab@almegaenv.com				Standard: <input checked="" type="checkbox"/> X Other: _____ Rush: _____ Depends on # of Samples 5 - 10 days 3 - 7 days		
Unit Information:		ANALYSIS REQUESTED		REMARKS		Return or Dispose		
Job #	10566	Unit #	Baghouse	Client:	SCAQMD - C	Location:	Inlet & Outlet	
Project Manager:	Morgan Nguyen	Sample Date	Sample Time	Sample Identification	Lab Sample #	Type Of Sample	No of Containers	
						LIQUID GAS SOLID		
8/13/2019	13:00 - 14:00	10566-M10.1-12-O2/CO2	A085-01			x	1	TK# 29
8/13/2019	11:55 - 12:55	10566-M10.1-11-O2/CO2	-02			x	1	TK# 14
8/13/2019	11:55 - 12:55	10566-M10.1-O-O2/CO2	-03			x	1	TK# 37
Relinquished by:		Received by:		Relinquished by:		Received by:		
Date: 8/16/2019	Time: 11:30	Date: 08/15/19	Time: 11:40	Date:	Time:	Date:	Time:	
Relinquished by:		Received by:		Relinquished by:		Received by:		
Date:	Time:	Date:	Time:	Date:	Time:	Date:	Time:	

Standard Receipt
Sample LOG in Checklist

Project No: 210366

Method: NIOSH 151

Lab ID: A085

Sampling Date: 8/12 - 8/16

Location: AQMD-C Int: _____

Date & Time Rc'd: 8/16/19 11:40

Location: LAB Int: DN

Arrived By: (circle) FedEx UPS Drop Off (Int) OK Other _____

Condition of Package(s): (comment): OK Package Type: Box Cooler Other: _____

Number of Sample Container(s): 8, 3 Correct Containers (per Method): Y N

Preservation: (circle) ICE DryICE ICEPacks None

Sample Conditions:

Sample Temp (C): 21

Ambient Temp (C): 21

Sample Temp (C): _____

Filter Condition: OK - Dirty

PH: _____

Components Sealed: Y N

Sample Recovery Completed On: (date & time) _____

Recovered In: (circle) Field Lab Other _____

Silica Gel Condition: _____

Tedlar Bags -

Condensation: Y N

Comments:

Container(s) Requested: Glass _____ Plastic _____

Additional Comments:

A085-22-02 = hard to extract, Black residue stuck to bottle
need vial to collect it. Separator

SAMPLE INVENTORY REPORT

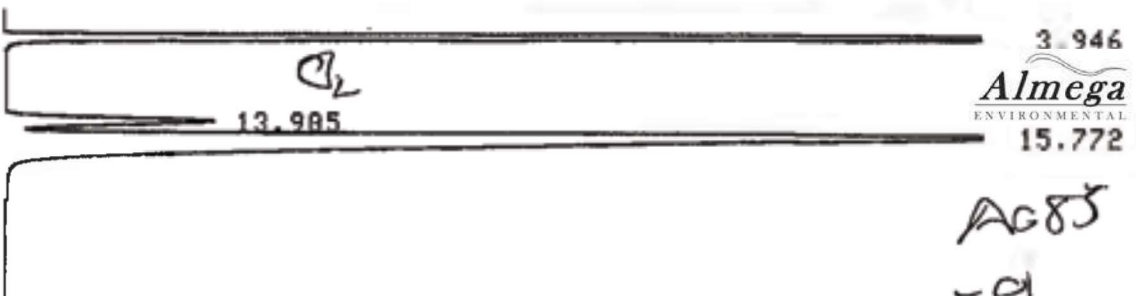
Method 25.3 Sampling Train

Project No.: c10566
 Client: AQMD

Lab No.: A 085
 Sampling Date: 13-Aug-19

Laboratory ID	Client ID	Component ID
Run #1		
A 085 - 01	10566-M10.1-I2-O2/CO2	Tank # 29
Run #2		
A 085 - 02	10566-M10.1-I1-O2/CO2	Tank # 14
Run #3		
A 085 - 03	10566-M10.1-O-O2/CO2	Tank # 37

**CHROMATOGRAM
TEST SAMPLES**



SHIMADZU

AG85
-9

CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC
CHANNEL NO 1
SAMPLE NO 0
REPORT NO 84

FILE 0
METHOD 41

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.946	8115064			34.9591	
2	13.905	1598972			6.8883	
3	15.772	13498974	V		58.1526	
TOTAL		23213008			100	



AG85
-01
dup

CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC
CHANNEL NO 1
SAMPLE NO 0
REPORT NO 85

FILE 0
METHOD 41

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.935	8095080			35.2841	
2	13.807	1573856			6.86	
3	15.649	13273628	V		57.8559	
TOTAL		22942562			100	

012



15.642

AOPS
SZ

CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC

CHANNEL NO 1 FILE 0
SAMPLE NO 0 METHOD 41
REPORT NO 86

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.923	8147198			35.4486	
2	13.887	1398715			6.0858	
3	15.642	13437182	V		58.4655	
TOTAL		22983096			100	



3.928

AOPS
SZ
dy

15.665

CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC

CHANNEL NO 1 FILE 0
SAMPLE NO 0 METHOD 41
REPORT NO 87

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.928	8145182			35.3557	
2	13.792	1399520			6.0749	
3	15.665	13493086	V		58.5694	
TOTAL		23037786			100	

13.825

Almaga ENVIRONMENTAL

15.688

A085
03

CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC
CHANNEL NO 1
SAMPLE NO 0
REPORT NO 88

FILE 0
METHOD 41

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.928	8175739			35.4135	
2	13.825	1750794			7.5836	
3	15.688	13159960	V		57.0029	
TOTAL		23086492			100	

0 3

223-02037-01

7:25:11A

SHIMADZU



CHROMATOGRAM 1 MEMORIZED

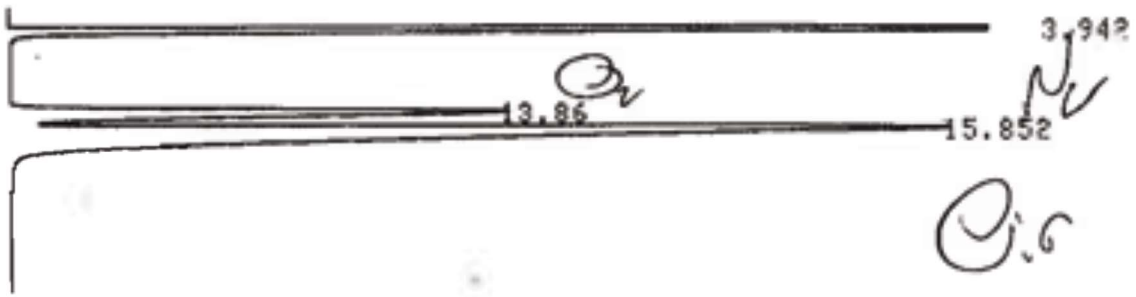
C-R5A CHROMATOPAC
CHANNEL NO 1
SAMPLE NO 0
REPORT NO 89

FILE 0
METHOD 41

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.947	8114429			35.1026	
2	13.882	1792895			7.756	
3	15.752	13208964	V		57.1414	
TOTAL		23116288			100	

A085
03
03

QAQC

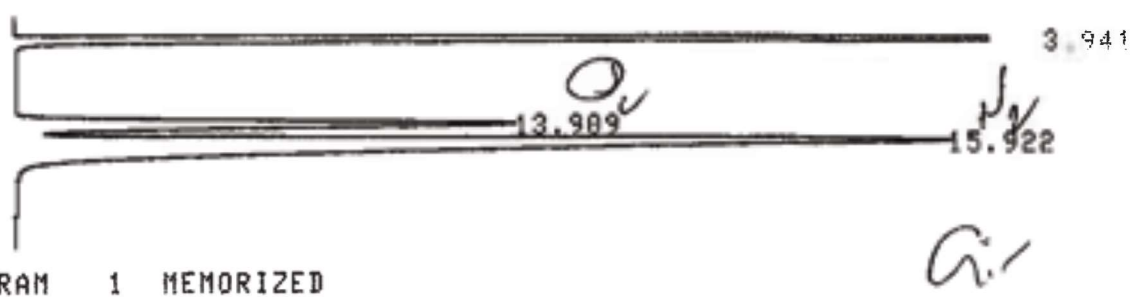


CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC
 CHANNEL NO 1
 SAMPLE NO 0
 REPORT NO 80

FILE 0
 METHOD 41

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.942	8343058			35.5278	
2	13.86	3861772			16.4448	
3	15.852	11278388	Y		48.0274	
TOTAL		23483210			100	



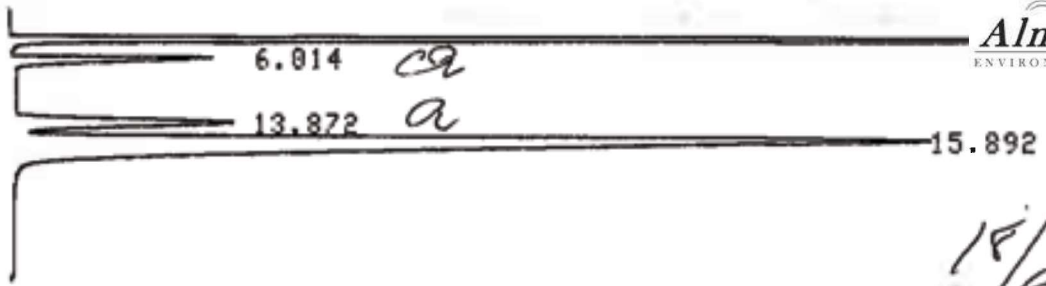
CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC
 CHANNEL NO 1
 SAMPLE NO 0
 REPORT NO 81

FILE 0
 METHOD 41

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.941	8320981			35.1658	
2	13.909	3909554			16.5224	
3	15.922	11431600	Y		48.3118	
TOTAL		23662134			100	

010 223-02037-01 712541A SHIMADZU

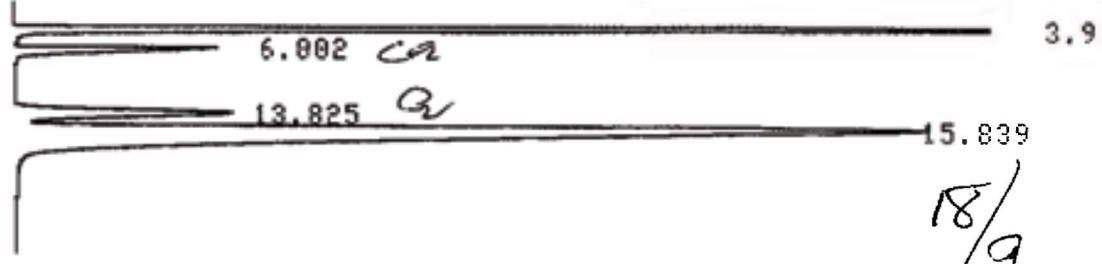


CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC

CHANNEL NO 1 FILE 0
 SAMPLE NO 6 METHOD 41
 REPORT NO 82

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.905	6823786			33.4419	
2	6.014	989505			4.8494	
3	13.872	1680226			8.2344	
4	15.892	10911366	V		53.4743	
TOTAL		20404880			100	



CHROMATOGRAM 1 MEMORIZED

C-R5A CHROMATOPAC

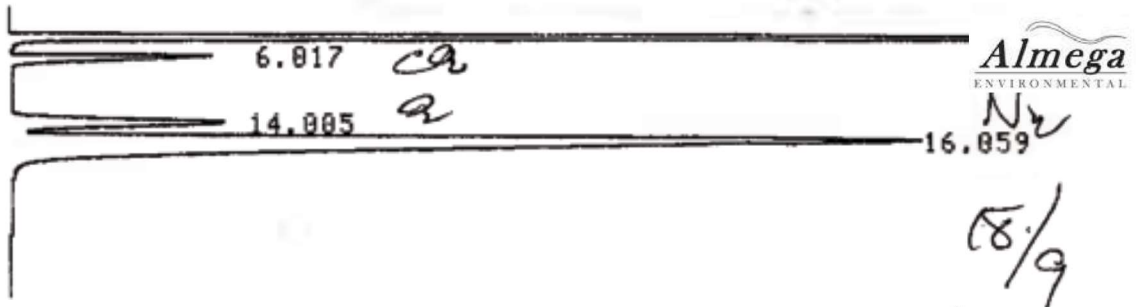
CHANNEL NO 1 FILE 0
 SAMPLE NO 0 METHOD 41
 REPORT NO 83

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.9	6801570			33.5435	
2	6.002	993231			4.8983	
3	13.825	1662400			8.1985	
4	15.839	10819684	V		53.3597	
TOTAL		20276884			100	

011

223-02037-01

712541A



CHROMATOGRAM MEMORIZED

C-R5A CHROMATOPAC

CHANNEL NO 1

FILE 0

SAMPLE NO 0

METHOD 41

REPORT NO 90

PKNO	TIME	AREA	MK	IDNO	CONC	NAME
1	3.91	6831713			33.3318	
2	6.017	1000349			4.8807	
3	14.005	1691962			8.2551	
4	16.059	10972030	V		53.5324	
TOTAL		20496652			100	

TANK PREPARATION

TANK PREPARATIONS

Client: AQMD
 Project No.: c10566
 Unit Tested: Facility C
 Sampling Date: 13-Aug-19
 Date pressurized: 16-Aug-19

Lab No.: A 085

Tank ID	Sample ID	Pre-test pressure mm Hg		Post-test pressure mm Hg	Final Pressure	Comments
		1	2			
29	A 085 - 01	-758	-758	-388	166	Run #1
14	A 085 - 02	-758	-758	-430	170	Run #2
37	A 085 - 03	-758	-758	-344	172	Run #3

* - Post -test Pressure is less then 200 mm Hg.



VOC FIELD DATA SHEET - SCAQMD METHOD 10.1 (Modified)

Date: 8-13-19 Test No.: 1
 Client: SCAQMD C Barometric Pressure (in. Hg): 29.9
 Unit: Inlet 1 Baghouse Pretest Leak Check:
 Operator Name: DJ A: X B: _____
 Fuel: Stack gas Post-test Leak check:
 Location: Inlet 1 A: X B: _____

RUN # 1

RUN # _____

Time 24 Hours	Start Time	Tank # <u>29</u> Control ID: <u>1213</u>	Flow ml/min.	Vacuum inch Hg
0	<u>11:55</u>	}		<u>28</u>
10				<u>24</u>
20				<u>20</u>
30				<u>20</u>
40				<u>18</u>
50				<u>16</u>
60			<u>12:55</u>	

Time 24 Hours	Start Time	Tank # _____ Control ID: _____	Flow ml/min.	Vacuum inch Hg

APPENDIX D

CARB METHOD 425 – CHROMIUM EMISSIONS (HEX/TOTAL)

APPENDIX D1

CHROMIUM EMISSIONS (HEX/TOTAL) – RESULTS AND CALCULATIONS

Location: Baghouse Outlet

TEST RESULTS

CARB 425 (Hexavalent & Total Chromium)

Facility: AQMD Facility C
 City: ████████ CA
 Source: Baghouse
 Location: Outlet

TEST DATA	UNITS	TEST RESULTS			AVERAGE
		Run 1	Run 2	Run 3	
Run Number	-				
Test Date	mm/dd/yy	8/14/19	8/15/19	8/15/19	--
Test Time	hh:mm	11:25 - 13:30	08:10 - 10:15	10:55 - 13:10	--
<u>Sampling Data*</u>					
Stack Temperature	°F	117.1	87.1	104.6	102.9
Moisture	%	2.3	1.9	2.4	2.2
Sample Volume	dscf	73.1	85.3	70.8	76.4
Oxygen**	% v/v	20.9	20.9	20.9	20.9
Carbon Dioxide**	% v/v	<0.3	<0.3	<0.3	<0.3
Gas Velocity	ft/min	613.6	685.1	585.5	628
Stack Flow Rate	acfm	7,711	8,609	7,358	7,893
Stack Flow Rate	dscfm	6,885	8,143	6,708	7,245
<u>Total Catch (CARB 425)</u>					
Chromium VI	ug	< 0.312	< 0.032	< 0.046	< 0.13
Total Chromium	ug	< 0.550	< 0.590	< 0.600	< 0.58
<u>Concentration (CARB 425)</u>					
Chromium VI	ug/dscm	< 0.151	< 0.013	< 0.023	< 0.062
	ug/dscf	< 0.004	< 0.0004	< 0.001	< 0.0018
Total Chromium	ug/dscm	< 0.266	< 0.244	< 0.299	< 0.270
	ug/dscf	< 0.0075	< 0.0069	< 0.0085	< 0.0076
<u>Mass Emissions (CARB 425)</u>					
Chromium VI	ug/hr	< 1763	< 180	< 261	< 735
Chromium VI	mg/hr	< 1.76	< 0.18	< 0.26	< 0.73
Chromium VI	lb/hr	< 3.89E-06	< 3.98E-07	< 5.76E-07	< 1.62E-06
Total Chromium	ug/hr	< 3107	< 3380	< 3410	< 3299
Total Chromium	mg/hr	< 3.11	< 3.38	< 3.41	< 3.30
Total Chromium	lb/hr	< 6.85E-06	< 7.45E-06	< 7.52E-06	< 7.27E-06

Notes:

* Performed during isokinetic sampling by CARB 425.

** O2/CO2 was measured via SCAQMD Method 10.1 by GC.

"<" Indicates an analytical result of non-detect (ND) and the use of laboratory MRL for emission calculations.

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Test Date(s): 08/14 to 08/15/19
 Operator: NC
 Entered by: TG
 Checked by: CF

Lab Results	Units	Run 1	Run 2	Run 3	Average
Chromium VI	ug	< 0.31	< 0.032	< 0.046	< 0.130
Total Chromium	μg	< 0.55	< 0.59	< 0.60	< 0.580
Chromium VI, Molecular Weight	g/g-mole	51.995	51.995	51.995	--
Total Chromium, Molecular Weight	g/g-mole	51.995	51.995	51.995	--
Concentration (ug/dscm), $C_i = M_i/V_mStd * 35.315 \text{ cf/dscm}$					
Chromium VI	ug/dscm	< 0.151	< 0.013	< 0.023	< 0.062
Total Chromium	ug/dscm	< 0.266	< 0.244	< 0.299	< 0.270
Metals Mass Emission Rate (lb/hr), $E_i = C_i * Q_{sdm} * 60 / 453600 / 1000$					
Chromium VI	lb/hr	< 3.89E-06	< 3.98E-07	< 5.76E-07	< 1.62E-06
Total Chromium	lb/hr	< 6.85E-06	< 7.45E-06	< 7.52E-06	< 7.27E-06

MV₁ = 24.05 L/g-mole @68°F, 23.68 L/g-mole @60°F

"<" Indicates an analytical result of non-detect (ND) and the use of laboratory MRL for emission calculations.

B - Reagent blank corrected value.

Lab Data - CARB 425

Facility: AQMD Facility C

Source: Baghouse Outlet

Analytical Results - Cr+6					
Run Number:	Run 1	Run 2	Run 3	RB	
Rinse C1, ug	ND, MRL 0.220	ND, MRL 0.0095	ND, MRL 0.009	ND, MRL 0.010	Cr+6 C1
Impingers C2, ug	0.092	ND, MRL 0.022	0.037	ND, MRL 0.020	C2
Total catch, ug	<0.312	<0.0315	<0.046		

Analytical Results - Total Chromium					
Run Number:	Run 1	Run 2	Run 3	RB	
Rinse C1, ug	ND, MRL 0.31	ND, MRL 0.35	ND, MRL 0.36	ND, MRL 1.00	Cr C1
Impingers C2, ug	ND, MRL 0.24	ND, MRL 0.24	ND, MRL 0.24	ND, MRL 1.00	C2
Total catch, ug	<0.55	<0.59	<0.60		

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Test Date(s): 08/14 to 08/15/19
 Operator: NC
 Entered by: TG
 Checked by: CF

			08/14/19	08/15/19	08/15/19
DATA ENTRY	symbol	units	DATA	DATA	DATA
Run Number			1	2	3
Stack Dimensions: Round Stack Diameter	Ds	in.	48.00	48.00	48.00
Rectangular Stack, Length	L	in.			
Width	W	in.			
Nozzle Diameter	Dn	in.	0.450	0.450	0.450
Standard Temperature	Tstd	°F	68	68	68
Universal (molar) Gas Constant	Renglish	in. Hg-cu.ft/ °R-lbmole	21.85	21.85	21.85
Average Stack Temperature (measured)	Fs	°F	117.1	87.1	104.6
Average Meter Temperature (measured)	Fm	°F	93.9	76.0	89.9
Standard Pressure	Pstd	in.Hg	29.92	29.92	29.92
Barometric Pressure	Pbar	in.Hg	29.90	29.90	29.90
Stack Static Pressure	Pg	in.WC	-0.02	-0.02	-0.02
Average Meter Orifice Head (Delta-H)	dH	in.WC	1.16	1.49	1.09
Average RMS Velocity Head (Delta-P)	dP	in.WC	0.030	0.040	0.028
Pitot Coefficient	Cp	—	0.84	0.84	0.84
Net Volume of Gas Metered	Vm	cu.ft.	73.752	83.153	70.924
Dry Gas Meter Calibration Factor (gamma, Y)	Y	—	1.0379	1.0379	1.0379
NET Sampling Time	min	min.	120	120	120
Stack Gas: Oxygen Content*	O2,m	%	20.90	20.90	20.90
Carbon Dioxide Content*	CO2,m	%	<0.30	<0.30	<0.30
Total Impinger Gain	Ww	g	37.2	35.3	37.5
CALCULATED DATA					
Nozzle Area: $An = \pi/4 \cdot dn^2$	An	sq.in.	0.1590	0.1590	0.1590
Stack Area (round): $As = \pi/576 \cdot ds^2$ (rectangular): $As = L \cdot W/144$	As	sq.ft.	12.57	12.57	12.57
Absolute Stack Temperature: $Ts = Fs + 460$	Ts	°R	577.1	547.1	564.6
Absolute Meter Temperature: $Tm = Fm + 460$	Tm	°R	553.9	536.0	549.9
Standard Temperature: $Tstdr = Tstd + 460$	Tstdr	°R	528.0	528.0	528.0
Gas Sample Volume at Standard Conditions: $Vm(std) = Y \cdot (Vm/Tm) \cdot (Pbar + dH/13.6 \text{ in H}_2\text{O/in Hg}) \cdot (Tstdr/Pstd)$	VmStd	cu.ft.	73.1	85.3	70.8
Vol. of Water Vapor: $Vw(std) = Ww/453.59 \cdot Renglish/18 \cdot Tstdr / Pstd$	VwStd	cu.ft.	1.757	1.667	1.771
Moisture Fraction: $Bws = VwStd/(VmStd + VwStd)$	Bws	—	0.0235	0.019	0.0244
Stack Gas MW, Dry Basis: $Md = 0.32 \cdot O_{2,m} + 0.44 \cdot CO_{2,m} + 0.28 \cdot (100 - O_{2,m} - CO_{2,m})$	Md	g/mole	28.88	28.88	28.88
Stack Gas MW, Wet Basis: $Mw = Md \cdot (1 - Bws) + 18 \cdot Bws$	Mw	g/mole	28.63	28.68	28.62
Stack Pressure: $Ps = Pbar + Pg/13.6$	Ps	in.Hg	29.90	29.90	29.90
Stack Gas Velocity, measured $vs = 85.49 \cdot Cp \cdot \sqrt{(dP \cdot Ts / Ps \cdot Mw)}$ $vm = 0.3048 \text{ m/ft} \cdot vs$	vs vsm	ft/s m/s	10.23 3.12	11.42 3.48	9.76 2.97
Stack Gas Volumetric Flow Rate: $Q = 60 \cdot vs \cdot As$	Q	acfm	7,711	8,609	7,358
Stack Gas Volumetric Flow Rate, corrected: $Qsd = Q \cdot (1 - Bws) \cdot (Ps / Ts) \cdot (Tstdr / Pstd)$ $Qsdm = Qsd / 35.315$	Qsd Qsdm	dscfm dscmm	6,885 195.0	8,143 230.6	6,708 190.0
Isokinetic Sampling Rate: $I = 144 \cdot 100 \cdot Ts \cdot Vmstd \cdot Pstd / [60 \cdot Tstdr \cdot vs \cdot \min \cdot An \cdot Ps \cdot (1 - Bws)]$	I	%	100.7	99.3	100.1

* O2/CO2 was measured via SCAQMD Method 10.1 by GC.

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Run No.: 1
 Test Date: 08/14/19
 Times: 11:25 - 13:30

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	108	10.4	0.060	0.24	2.17	84	84
2	111	10.5	0.050	0.22	1.81	93	85
3	111	10.5	0.050	0.22	1.82	95	86
4	117	10.8	0.050	0.22	1.80	96	87
5	116	10.8	0.050	0.22	1.81	97	88
6	114	10.7	0.030	0.17	1.09	97	89
7	119	10.9	0.030	0.17	1.09	97	89
8	119	10.9	0.030	0.17	1.08	97	90
9	118	10.9	0.030	0.17	1.08	97	90
10	119	10.9	0.030	0.17	1.08	98	91
11	119	10.9	0.020	0.14	0.72	98	91
12	119	10.9	0.020	0.14	0.72	98	91
B-1	118	10.9	0.020	0.14	0.72	92	93
2	121	11.0	0.020	0.14	0.72	97	91
3	121	11.0	0.020	0.14	0.72	98	92
4	121	11.0	0.020	0.14	0.72	99	92
5	122	11.0	0.020	0.14	0.72	99	92
6	122	11.0	0.020	0.14	0.72	100	92
7	123	11.1	0.020	0.14	0.72	99	93
8	121	11.0	0.020	0.14	0.72	100	93
9	113	10.6	0.030	0.17	1.10	100	93
10	115	10.7	0.030	0.17	1.10	101	94
11	112	10.6	0.050	0.22	1.84	101	94
12	112	10.6	0.030	0.17	1.84	101	94
Average:		117.1		0.0301	1.16		93.9

DGM Reading (cu.ft.):	Final-1:	681.850	Impinger Weight (g):	#1 Final:	774.6
	Initial-1:	608.098		#1 Initial:	760.0
	Final-2:			#2 Final:	770.4
	Initial-2:			#2 Initial:	767.8
	Final-3:			#3 Final:	620.8
	Initial-3:			#3 Initial:	620.3
	Final-4:			#4 Final:	790.0
	Initial-4:			#4 Initial:	770.5
	Final-5:			#5 Final:	
	Initial-5:			#5 Initial:	
	NET Volume:	73.752		#6 Final:	
				#6 Initial:	
				#7 Final:	
				#7 Initial:	
				#8 Final:	
				#8 Initial:	
			Total wt of impingers:		37.2

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Run No.: 2
 Test Date: 08/15/19
 Times: 08:10 - 10:15

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	78	8.8	0.05	0.224	1.84	66	66
2	82	9.1	0.05	0.224	1.84	75	64
3	82	9.1	0.06	0.245	2.22	76	66
4	82	9.1	0.05	0.224	1.85	78	67
5	83	9.1	0.05	0.224	1.85	79	68
6	82	9.1	0.04	0.200	1.49	80	69
7	82	9.1	0.05	0.224	1.86	80	70
8	83	9.1	0.04	0.200	1.49	80	70
9	85	9.2	0.05	0.224	1.85	80	71
10	86	9.3	0.04	0.200	1.48	81	71
11	86	9.3	0.04	0.200	1.48	81	72
12	86	9.3	0.04	0.200	1.48	82	72
B-1	85	9.2	0.03	0.173	1.11	75	73
2	87	9.3	0.03	0.173	1.11	80	72
3	90	9.5	0.03	0.173	1.10	80	73
4	91	9.5	0.03	0.173	1.10	81	73
5	91	9.5	0.03	0.173	1.10	82	73
6	93	9.6	0.03	0.173	1.10	82	74
7	92	9.6	0.02	0.141	0.74	83	75
8	93	9.6	0.03	0.173	1.10	82	75
9	93	9.6	0.03	0.173	1.11	84	76
10	94	9.7	0.03	0.173	1.10	85	76
11	93	9.6	0.06	0.245	2.22	86	77
12	94	9.7	0.06	0.245	2.22	88	78
Average:		87.1		0.0396	1.49		76.0

DGM Reading (cu.ft.):	Final-1:	767.625	Impinger Weight (g):	#1 Final:	773.3
	Initial-1:	684.472		#1 Initial:	760.1
	Final-2:			#2 Final:	770.9
	Initial-2:			#2 Initial:	766.8
	Final-3:			#3 Final:	621.1
	Initial-3:			#3 Initial:	619.4
	Final-4:			#4 Final:	805.2
	Initial-4:			#4 Initial:	788.9
	Final-5:			#5 Final:	
	Initial-5:			#5 Initial:	
	NET Volume:	83.153		#6 Final:	
				#6 Initial:	
				#7 Final:	
				#7 Initial:	
				#8 Final:	
				#8 Initial:	
			Total wt of impingers:		35.3

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Outlet

Run No.: 3
 Test Date: 08/15/19
 Times: 10:55 - 13:10

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	98	9.9	0.04	0.200	1.46	79	79
2	98	9.9	0.04	0.200	1.46	84	79
3	98	9.9	0.04	0.200	1.47	87	80
4	97	9.8	0.03	0.173	1.10	89	81
5	97	9.8	0.03	0.173	1.11	90	82
6	97	9.8	0.02	0.141	0.74	90	83
7	99	9.9	0.02	0.141	0.74	91	84
8	99	9.9	0.03	0.173	1.11	91	84
9	100	10.0	0.02	0.141	0.74	93	86
10	101	10.0	0.02	0.141	0.74	93	86
11	106	10.3	0.02	0.141	0.73	93	86
12	107	10.3	0.02	0.141	0.73	94	86
B-1	109	10.4	0.02	0.141	0.73	88	87
2	109	10.4	0.02	0.141	0.73	94	88
3	110	10.5	0.02	0.141	0.73	96	88
4	110	10.5	0.02	0.141	0.73	96	89
5	111	10.5	0.02	0.141	0.73	96	89
6	111	10.5	0.02	0.141	0.73	97	90
7	111	10.5	0.02	0.141	0.73	97	91
8	111	10.5	0.02	0.141	0.73	98	91
9	111	10.5	0.02	0.141	0.73	98	91
10	108	10.4	0.06	0.245	2.21	99	92
11	107	10.3	0.07	0.265	2.59	101	93
12	107	10.3	0.07	0.265	2.60	102	94
Average:		104.6		0.0280	1.09		89.9

DGM Reading (cu.ft.):	Final-1: 838.859	Impinger Weight (g):	#1 Final: 776.3
	Initial-1: 767.935		#1 Initial: 753.3
	Final-2:		#2 Final: 756.0
	Initial-2:		#2 Initial: 754.6
	Final-3:		#3 Final: 542.0
	Initial-3:		#3 Initial: 541.2
	Final-4:		#4 Final: 871.9
	Initial-4:		#4 Initial: 859.6
	Final-5:		#5 Final:
	Initial-5:		#5 Initial:
NET Volume:	70.924		#6 Final:
			#6 Initial:
			#7 Final:
			#7 Initial:
			#8 Final:
			#8 Initial:
		Total wt of impingers:	37.5

Location: Inlet 1 (Inside)

TEST RESULTS

CARB 425 (Hexavalent & Total Chromium)

Facility: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

TEST DATA	UNITS	TEST RESULTS			AVERAGE
		Run 1	Run 2	Run 3	
Run Number	-				
Test Date	mm/dd/yy	8/14/19	8/15/19	8/15/19	--
Test Time	hh:mm	11:25 - 13:30	08:10 - 10:15	10:55 - 13:10	--
<u>Sampling Data*</u>					
Stack Temperature	°F	131	114	142	129
Moisture	%	1.6	1.6	1.7	1.7
Sample Volume	dscf	85.3	92.6	86.3	88.1
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	0.30	0.30	0.30	0.30
Gas Velocity	ft/min	1,238.5	1,303.0	1,273.8	1,272
Stack Flow Rate	acfm	1,142	1,201	1,174	1,172
Stack Flow Rate	dscfm	998	1,083	1,008	1,030
<u>Total Catch (CARB 425)</u>					
Chromium VI	ug	0.82	21.9	21.2	14.6
Total Chromium	ug	2540	330	1007	1292
<u>Concentration (CARB 425)</u>					
Chromium VI	ug/dscm	0.34	8.35	8.68	5.79
	ug/dscf	0.010	0.237	0.246	0.164
Total Chromium	ug/dscm	1052	125.9	412.1	529.9
	ug/dscf	29.78	3.56	11.67	15.00
<u>Mass Emissions (CARB 425)</u>					
Chromium VI	ug/hr	575	15369	14859	10268
Chromium VI	mg/hr	0.57	15.37	14.9	10.3
Chromium VI	lb/hr	1.27E-06	3.39E-05	3.28E-05	2.26E-05
Total Chromium	ug/hr	1784014	231584	705479	907026
Total Chromium	mg/hr	1784	232	705	907
Total Chromium	lb/hr	3.93E-03	5.11E-04	1.56E-03	2.00E-03

Notes:

* Performed during isokinetic sampling by CARB 425.

** O2/CO2 was measured via SCAQMD Method 10.1 by GC.

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Test Date(s): 08/14 to 08/15/19
 Operator: DJ
 Entered by: TG
 Checked by: CF

Lab Results	Units	Run 1	Run 2	Run 3	Average
Chromium VI	ug	0.818	21.9	21.2	14.64
Total Chromium	μg	2540	330.0	1007	1292.3
Chromium VI, Molecular Weight	g/g-mole	51.995	51.995	51.995	--
Total Chromium, Molecular Weight	g/g-mole	51.995	51.995	51.995	--
Concentration (ug/dscm), $C_i = M_i/V_mStd * 35.315 \text{ cf/dscm}$					
Chromium VI	ug/dscm	0.34	8.35	8.68	5.8
Total Chromium	ug/dscm	1,051.65	125.86	412.06	530
Metals Mass Emissino Rate (lb/hr), $E_i = C_i * Q_{sdm} * 60 / 453600 / 1000$					
Chromium VI	lb/hr	1.27E-06	3.39E-05	3.28E-05	2.26E-05
Total Chromium	lb/hr	3.93E-03	5.11E-04	1.56E-03	2.00E-03

MV₁ = 24.05 L/g-mole @68°F, 23.68 L/g-mole @60°F

Lab Data - CARB 425

Facility: AQMD Facility C

Source: Baghouse Inlet 1

Analytical Results - Cr+6						
Run Number:	Run 1	Run 2	Run 3	RB		
Rinse C1, ug	0.068	0.90	0.21	ND, MRL	0.010	Cr+6 C1
Impingers C2, ug	0.75	21.0	21.0	ND, MRL	0.020	C2
Total catch, ug	0.818	21.9	21.21			

Analytical Results - Total Chromium						
Run Number:	Run 1	Run 2	Run 3	RB		
Rinse C1, ug	240	50	27.0	ND, MRL	1.00	Cr C1
Impingers C2, ug	2300	280	980	ND, MRL	1.00	C2
Total catch, ug	2540	330	1007			

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Test Date(s): 08/14 to 08/15/19
 Operator: DJ
 Entered by: TG
 Checked by: CF

			08/14/19	08/15/19	08/15/19
DATA ENTRY	symbol	units	DATA	DATA	DATA
Run Number			1	2	3
Stack Dimensions: Round Stack Diameter	Ds	in.	13.00	13.00	13.00
Rectangular Stack, Length	L	in.			
Width	W	in.			
Nozzle Diameter	Dn	in.	0.348	0.348	0.348
Standard Temperature	Tstd	°F	68	68	68
Universal (molar) Gas Constant	Renglish	in. Hg-cu.ft/ °R-lbmole	21.85	21.85	21.85
Average Stack Temperature (measured)	Fs	°F	131.4	113.5	142.0
Average Meter Temperature (measured)	Fm	°F	114.0	94.4	107.9
Standard Pressure	Pstd	in.Hg	29.92	29.92	29.92
Barometric Pressure	Pbar	in.Hg	29.90	29.90	29.90
Stack Static Pressure	Pg	in.WC	-1.60	-1.50	-1.40
Average Meter Orifice Head (Delta-H)	dH	in.WC	1.82	2.07	1.84
Average RMS Velocity Head (Delta-P)	dP	in.WC	0.119	0.136	0.124
Pitot Coefficient	Cp	—	0.84	0.84	0.84
Net Volume of Gas Metered	Vm	cu.ft.	88.858	93.119	88.950
Dry Gas Meter Calibration Factor (gamma, Y)	Y	—	1.0395	1.0395	1.0395
NET Sampling Time	min	min.	120	120	120
Stack Gas: Oxygen Content*	O2,m	%	20.80	20.80	20.80
Carbon Dioxide Content*	CO2,m	%	<0.30	<0.30	<0.30
Total Impinger Gain	Ww	g	29.0	32.4	32.5
CALCULATED DATA					
Nozzle Area: $An = \pi/4 \cdot dn^2$	An	sq.in.	0.0951	0.0951	0.0951
Stack Area (round): $As = \pi/576 \cdot ds^2$ (rectangular): $As = L \cdot W/144$	As	sq.ft.	0.92	0.92	0.92
Absolute Stack Temperature: $Ts = Fs + 460$	Ts	°R	591.4	573.5	602.0
Absolute Meter Temperature: $Tm = Fm + 460$	Tm	°R	574.0	554.4	567.9
Standard Temperature: $Tstdr = Tstd + 460$	Tstdr	°R	528.0	528.0	528.0
Gas Sample Volume at Standard Conditions: $Vm(std) = Y \cdot (Vm/Tm) \cdot (Pbar + dH/13.6 \text{ in H}_2\text{O/in Hg}) \cdot (Tstdr/Pstd)$	VmStd	cu.ft.	85.3	92.6	86.3
Vol. of Water Vapor: $Vw(std) = Ww/453.59 \cdot Renglish/18 \cdot Tstdr / Pstd$	VwStd	cu.ft.	1.370	1.530	1.535
Moisture Fraction: $Bws = VwStd/(VmStd + VwStd)$	Bws	—	0.0158	0.016	0.0175
Stack Gas MW, Dry Basis: $Md = 0.32 \cdot O_{2,m} + 0.44 \cdot CO_{2,m} + 0.28 \cdot (100 - O_{2,m} - CO_{2,m})$	Md	g/mole	28.88	28.88	28.88
Stack Gas MW, Wet Basis: $Mw = Md \cdot (1 - Bws) + 18 \cdot Bws$	Mw	g/mole	28.71	28.70	28.69
Stack Pressure: $Ps = Pbar + Pg/13.6$	Ps	in.Hg	29.78	29.79	29.80
Stack Gas Velocity, measured $vs = 85.49 \cdot Cp \cdot \sqrt{(dP \cdot Ts / Ps \cdot Mw)}$ $vm = 0.3048 \text{ m/ft} \cdot vs$	vs vsm	ft/s m/s	20.64 6.29	21.72 6.62	21.23 6.47
Stack Gas Volumetric Flow Rate: $Q = 60 \cdot vs \cdot As$	Q	acfm	1,142	1,201	1,174
Stack Gas Volumetric Flow Rate, corrected: $Qsd = Q \cdot (1 - Bws) \cdot (Ps / Ts) \cdot (Tstdr / Pstd)$ $Qsdm = Qsd / 35.315$	Qsd Qsdm	dscfm dscmm	998 28.3	1,083 30.7	1,008 28.5
Isokinetic Sampling Rate: $I = 144 \cdot 100 \cdot Ts \cdot Vmstd \cdot Pstd / [60 \cdot Tstdr \cdot vs \cdot \min \cdot An \cdot Ps \cdot (1 - Bws)]$	I	%	99.3	99.4	99.6

* O2/CO2 was measured via SCAQMD Method 10.1 by GC.

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Run No.: 1
 Test Date: 08/14/19
 Times: 11:25 - 13:30

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	128	11.3	0.170	0.41	2.53	101	101
2	146	12.1	0.150	0.39	2.17	102	102
3	149	12.2	0.160	0.40	2.31	104	104
4	150	12.2	0.130	0.36	1.87	105	105
5	139	11.8	0.110	0.33	1.63	107	107
6	135	11.6	0.100	0.32	1.49	108	108
7	126	11.2	0.090	0.30	1.36	109	109
8	127	11.3	0.100	0.32	1.51	110	110
9	126	11.2	0.120	0.35	1.82	111	111
10	126	11.2	0.140	0.37	2.12	111	111
11	122	11.0	0.130	0.36	1.99	111	111
12	120	11.0	0.110	0.33	1.69	112	112
B-1	139	11.8	0.150	0.39	2.23	111	111
2	138	11.7	0.160	0.40	2.38	112	112
3	153	12.4	0.140	0.37	2.06	119	119
4	144	12.0	0.140	0.37	2.09	119	119
5	144	12.0	0.130	0.36	1.95	121	121
6	130	11.4	0.110	0.33	1.69	122	122
7	131	11.4	0.080	0.28	1.23	123	123
8	119	10.9	0.090	0.30	1.41	124	124
9	116	10.8	0.110	0.33	1.73	123	123
10	116	10.8	0.100	0.32	1.58	124	124
11	123	11.1	0.080	0.28	1.25	123	123
12	113	10.6	0.100	0.32	1.58	123	123
Average:		131.4		0.1194	1.82		114.0

DGM Reading (cu.ft.):	Final-1: 604.228	Impinger Weight (g):	#1 Final: 734.4
	Initial-1: 515.370		#1 Initial: 721.9
	Final-2:		#2 Final: 537.1
	Initial-2:		#2 Initial: 535.4
	Final-3:		#3 Final: 648.5
	Initial-3:		#3 Initial: 646.7
	Final-4:		#4 Final: 887.5
	Initial-4:		#4 Initial: 874.5
	Final-5:		#5 Final:
	Initial-5:		#5 Initial:
NET Volume:	88.858		#6 Final:
			#6 Initial:
			#7 Final:
			#7 Initial:
			#8 Final:
			#8 Initial:
		Total wt of impingers:	29.0

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Run No.: 2
 Test Date: 08/15/19
 Times: 08:10 - 10:15

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	122	11.0	0.19	0.436	2.81	93	93
2	132	11.5	0.18	0.424	2.62	93	93
3	128	11.3	0.18	0.424	2.64	94	94
4	104	10.2	0.16	0.400	2.45	95	95
5	101	10.0	0.14	0.374	2.16	97	97
6	97	9.8	0.13	0.361	2.02	97	97
7	94	9.7	0.11	0.332	1.73	98	98
8	96	9.8	0.12	0.346	1.88	98	98
9	89	9.4	0.10	0.316	1.58	98	98
10	88	9.4	0.13	0.361	2.07	99	99
11	85	9.2	0.15	0.387	2.40	100	100
12	89	9.4	0.14	0.374	2.22	100	100
B-1	114	10.7	0.17	0.412	2.53	89	89
2	118	10.9	0.18	0.424	2.67	90	90
3	121	11.0	0.16	0.400	2.36	90	90
4	119	10.9	0.16	0.400	2.37	91	91
5	126	11.2	0.11	0.332	1.61	92	92
6	131	11.4	0.12	0.346	1.75	93	93
7	127	11.3	0.10	0.316	1.47	93	93
8	129	11.4	0.10	0.316	1.46	93	93
9	132	11.5	0.09	0.300	1.31	93	93
10	131	11.4	0.11	0.332	1.60	93	93
11	131	11.4	0.13	0.361	1.89	93	93
12	137	11.7	0.15	0.387	2.17	94	94
Average:		113.5		0.1363	2.07		94.4

DGM Reading (cu.ft.):	Final-1: 697.568	Impinger Weight (g):	#1 Final: 736.5
	Initial-1: 604.449		#1 Initial: 724.1
	Final-2:		#2 Final: 631.3
	Initial-2:		#2 Initial: 630.0
	Final-3:		#3 Final: 649.9
	Initial-3:		#3 Initial: 647.4
	Final-4:		#4 Final: 902.1
	Initial-4:		#4 Initial: 885.9
	Final-5:		#5 Final:
	Initial-5:		#5 Initial:
NET Volume:	93.119		#6 Final:
			#6 Initial:
			#7 Final:
			#7 Initial:
			#8 Final:
			#8 Initial:
		Total wt of impingers:	32.4

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 1

Run No.: 3
 Test Date: 08/15/19
 Times: 10:55 - 13:10

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	127	11.3	0.18	0.424	2.70	105	105
2	128	11.3	0.17	0.412	2.55	107	107
3	125	11.2	0.16	0.400	2.43	111	111
4	133	11.5	0.14	0.374	2.11	113	113
5	137	11.7	0.13	0.361	1.94	112	112
6	138	11.7	0.11	0.332	1.64	112	112
7	140	11.8	0.10	0.316	1.49	113	113
8	127	11.3	0.11	0.332	1.64	112	112
9	126	11.2	0.13	0.361	1.98	112	112
10	127	11.3	0.12	0.346	1.82	112	112
11	131	11.4	0.11	0.332	1.65	110	110
12	134	11.6	0.10	0.316	1.49	108	108
B-1	149	12.2	0.17	0.412	2.44	101	101
2	149	12.2	0.16	0.400	2.30	101	101
3	154	12.4	0.15	0.387	2.15	104	104
4	154	12.4	0.13	0.361	1.86	104	104
5	155	12.4	0.12	0.346	1.72	105	105
6	156	12.5	0.10	0.316	1.43	106	106
7	155	12.4	0.10	0.316	1.43	106	106
8	156	12.5	0.09	0.300	1.29	107	107
9	152	12.3	0.10	0.316	1.44	107	107
10	152	12.3	0.11	0.332	1.59	107	107
11	154	12.4	0.10	0.316	1.44	107	107
12	154	12.4	0.12	0.346	1.73	107	107
Average:		142.0		0.1241	1.84		107.9

DGM Reading (cu.ft.):	Final-1: 790.926	Impinger Weight (g):	#1 Final: 740.0
	Initial-1: 701.976		#1 Initial: 728.9
	Final-2:		#2 Final: 752.5
	Initial-2:		#2 Initial: 749.7
	Final-3:		#3 Final: 619.1
	Initial-3:		#3 Initial: 618.1
	Final-4:		#4 Final: 877.1
	Initial-4:		#4 Initial: 859.5
	Final-5:		#5 Final:
	Initial-5:		#5 Initial:
NET Volume:	88.950		#6 Final:
			#6 Initial:
			#7 Final:
			#7 Initial:
			#8 Final:
			#8 Initial:
		Total wt of impingers:	32.5

Location: Inlet 2 (Upstream to Baghouse)

TEST RESULTS

CARB 425 (Hexavalent & Total Chromium)

Facility: AQMD Facility C
 City: ████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

TEST DATA	UNITS	TEST RESULTS			AVERAGE
		Run 1	Run 2	Run 3	
Run Number	-				
Test Date	mm/dd/yy	8/14/19	8/15/19	8/15/19	--
Test Time	hh:mm	11:25 - 13:30	08:10 - 10:15	10:55 - 13:10	--
<u>Sampling Data*</u>					
Stack Temperature	°F	112.3	86.1	96.9	98.4
Moisture	%	2.0	2.1	1.9	2.0
Sample Volume	dscf	89.8	97.3	92.2	93.1
Oxygen**	% v/v	20.8	20.8	20.8	20.8
Carbon Dioxide**	% v/v	0.30	0.30	0.30	0.30
Gas Velocity	ft/min	4,481.7	4,560.9	4,485.3	4,509
Stack Flow Rate	acfm	6,258	6,368	6,263	6,296
Stack Flow Rate	dscfm	5,597	5,958	5,757	5,771
<u>Total Catch (CARB 425)</u>					
Chromium VI	ug	2.89	5.30	3.90	4.03
Total Chromium	ug	469	70.0	280	273
<u>Concentration (CARB 425)</u>					
Chromium VI	ug/dscm	1.14	1.92	1.49	1.52
	ug/dscf	0.032	0.054	0.042	0.043
Total Chromium	ug/dscm	184.50	25.42	107.29	105.7
	ug/dscf	5.22	0.72	3.04	2.99
<u>Mass Emissions (CARB 425)</u>					
Chromium VI	ug/hr	10812	19479	14618	14969
Chromium VI	mg/hr	10.8	19.48	14.6	15.0
Chromium VI	lb/hr	2.38E-05	4.29E-05	3.22E-05	3.30E-05
Total Chromium	ug/hr	1754573	257267	1049466	1020435
Total Chromium	mg/hr	1755	257	1049	1020
Total Chromium	lb/hr	3.87E-03	5.67E-04	2.31E-03	2.25E-03

Notes:

* Performed during isokinetic sampling by CARB 425.

** O2/CO2 was measured via SCAQMD Method 10.1 by GC.

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Test Date(s): 08/14 to 08/15/19
 Operator: WB
 Entered by: TG
 Checked by: CF

Lab Results	Units	Run 1	Run 2	Run 3	Average
Chromium VI	ug	2.89	5.30	3.90	4.03
Total Chromium	μg	469	70.0	280	273
Chromium VI, Molecular Weight	g/g-mole	51.995	51.995	51.995	--
Total Chromium, Molecular Weight	g/g-mole	51.995	51.995	51.995	--
Concentration (ug/dscm), $C_i = M_i/V_mStd * 35.315 \text{ cf/dscm}$					
Chromium VI	ug/dscm	1.14	1.92	1.49	1.5
Total Chromium	ug/dscm	184.50	25.42	107.29	106
Metals Mass Emissino Rate (lb/hr), $E_i = C_i * Q_{sdm} * 60 / 453600 / 1000$					
Chromium VI	lb/hr	2.38E-05	4.29E-05	3.22E-05	3.30E-05
Total Chromium	lb/hr	3.87E-03	5.67E-04	2.31E-03	2.25E-03

MV₁ = 24.05 L/g-mole @68°F, 23.68 L/g-mole @60°F

Lab Data - CARB 425

Facility: AQMD Facility C

Source: Baghouse Inlet 2 (Upstream to Baghouse)

Analytical Results - Cr+6						
Run Number:	Run 1	Run 2	Run 3	RB		
Rinse C1, ug	0.29	0.20	1.9	ND, MRL	0.010	Cr+6 C1
Impingers C2, ug	2.60	5.10	2.0	ND, MRL	0.020	C2
Total catch, ug	2.89	5.3	3.9			

Analytical Results - Total Chromium						
Run Number:	Run 1	Run 2	Run 3	RB		
Rinse C1, ug	59	14.0	110	ND, MRL	1.00	Cr C1
Impingers C2, ug	410	56.0	170	ND, MRL	1.00	C2
Total catch, ug	469	70.0	280			

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Test Date(s): 08/14 to 08/15/19
 Operator: WB
 Entered by: TG
 Checked by: CF

			08/14/19	08/15/19	08/15/19
DATA ENTRY	symbol	units	DATA	DATA	DATA
Run Number			1	2	3
Stack Dimensions: Round Stack Diameter	Ds	in.	16.00	16.00	16.00
Rectangular Stack, Length	L	in.			
Width	W	in.			
Nozzle Diameter	Dn	in.	0.181	0.181	0.181
Standard Temperature	Tstd	°F	68	68	68
Universal (molar) Gas Constant	Renglish	in. Hg-cu.ft/ °R-lbmole	21.85	21.85	21.85
Average Stack Temperature (measured)	Fs	°F	112.3	86.1	96.9
Average Meter Temperature (measured)	Fm	°F	103.2	80.9	96.9
Standard Pressure	Pstd	in.Hg	29.92	29.92	29.92
Barometric Pressure	Pbar	in.Hg	29.90	29.90	29.90
Stack Static Pressure	Pg	in.WC	-4.20	-4.30	-4.30
Average Meter Orifice Head (Delta-H)	dH	in.WC	1.93	2.28	2.16
Average RMS Velocity Head (Delta-P)	dP	in.WC	1.604	1.739	1.650
Pitot Coefficient	Cp	—	0.84	0.84	0.84
Net Volume of Gas Metered	Vm	cu.ft.	91.912	95.555	93.259
Dry Gas Meter Calibration Factor (gamma, Y)	Y	—	1.0376	1.0376	1.0376
NET Sampling Time	min	min.	120	120	120
Stack Gas: Oxygen Content*	O2,m	%	20.80	20.80	20.80
Carbon Dioxide Content*	CO2,m	%	<0.30	<0.30	<0.30
Total Impinger Gain	Ww	g	38.3	45.0	38.3
CALCULATED DATA					
Nozzle Area: $An = \pi/4 \cdot dn^2$	An	sq.in.	0.0257	0.0257	0.0257
Stack Area (round): $As = \pi/576 \cdot ds^2$ (rectangular): $As = L \cdot W/144$	As	sq.ft.	1.40	1.40	1.40
Absolute Stack Temperature: $Ts = Fs + 460$	Ts	°R	572.3	546.1	556.9
Absolute Meter Temperature: $Tm = Fm + 460$	Tm	°R	563.2	540.9	556.9
Standard Temperature: $Tstdr = Tstd + 460$	Tstdr	°R	528.0	528.0	528.0
Gas Sample Volume at Standard Conditions: $Vm(std) = Y \cdot (Vm/Tm) \cdot (Pbar + dH/13.6 \text{ in H}_2\text{O/in Hg}) \cdot (Tstdr/Pstd)$	VmStd	cu.ft.	89.8	97.3	92.2
Vol. of Water Vapor: $Vw(std) = Ww/453.59 \cdot Renglish/18 \cdot Tstdr / Pstd$	VwStd	cu.ft.	1.809	2.125	1.809
Moisture Fraction: $Bws = VwStd/(VmStd + VwStd)$	Bws	—	0.0198	0.021	0.0192
Stack Gas MW, Dry Basis: $Md = 0.32 \cdot O_{2,m} + 0.44 \cdot CO_{2,m} + 0.28 \cdot (100 - O_{2,m} - CO_{2,m})$	Md	g/mole	28.88	28.88	28.88
Stack Gas MW, Wet Basis: $Mw = Md \cdot (1 - Bws) + 18 \cdot Bws$	Mw	g/mole	28.67	28.65	28.67
Stack Pressure: $Ps = Pbar + Pg/13.6$	Ps	in.Hg	29.59	29.58	29.58
Stack Gas Velocity, measured $vs = 85.49 \cdot Cp \cdot \sqrt{(dP \cdot Ts / Ps \cdot Mw)}$ $vm = 0.3048 \text{ m/ft} \cdot vs$	vs	ft/s	74.70	76.02	74.75
	vsm	m/s	22.77	23.17	22.79
Stack Gas Volumetric Flow Rate: $Q = 60 \cdot vs \cdot As$	Q	acfm	6,258	6,368	6,263
Stack Gas Volumetric Flow Rate, corrected: $Qsd = Q \cdot (1 - Bws) \cdot (Ps / Ts) \cdot (Tstdr / Pstd)$ $Qsdm = Qsd / 35.315$	Qsd	dscfm	5,597	5,958	5,757
	Qsdm	dscmm	158.5	168.7	163.0
Isokinetic Sampling Rate: $I = 144 \cdot 100 \cdot Ts \cdot Vmstd \cdot Pstd / [60 \cdot Tstdr \cdot vs \cdot \min \cdot An \cdot Ps \cdot (1 - Bws)]$	I	%	104.4	106.3	104.2

* O2/CO2 was measured via SCAQMD Method 10.1 by GC.

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Run No.: 1
 Test Date: 08/14/19
 Times: 11:25 - 13:30

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	108	10.4	1.90	1.38	2.25	91	91
2	110	10.5	1.80	1.34	2.10	92	92
3	111	10.5	1.90	1.38	2.25	93	93
4	113	10.6	1.90	1.38	2.25	94	94
5	114	10.7	1.75	1.32	2.05	96	96
6	113	10.6	2.50	1.58	2.95	98	98
7	111	10.5	1.70	1.30	2.00	100	100
8	109	10.4	1.20	1.10	1.40	101	101
9	106	10.3	1.00	1.00	1.15	103	103
10	104	10.2	1.00	1.00	1.15	103	103
11	107	10.3	1.05	1.02	1.25	104	104
12	107	10.3	1.00	1.00	1.15	104	104
B-1	110	10.5	1.95	1.40	2.30	104	104
2	110	10.5	2.00	1.41	2.35	104	104
3	115	10.7	2.25	1.50	2.65	105	105
4	118	10.9	2.15	1.47	2.50	106	106
5	114	10.7	1.90	1.38	2.25	108	108
6	123	11.1	2.30	1.52	2.70	109	109
7	119	10.9	1.80	1.34	2.10	110	110
8	122	11.0	1.60	1.26	1.90	110	110
9	116	10.8	1.30	1.14	1.55	111	111
10	113	10.6	1.20	1.10	1.40	111	111
11	115	10.7	1.05	1.02	1.25	110	110
12	108	10.4	1.10	1.05	1.30	110	110
Average:		112.3		1.6036	1.93		103.2

DGM Reading (cu.ft.):	Final-1:	382.967	Impinger Weight (g):	#1 Final:	757.7
	Initial-1:	291.055		#1 Initial:	743.0
	Final-2:			#2 Final:	773.7
	Initial-2:			#2 Initial:	769.0
	Final-3:			#3 Final:	630.9
	Initial-3:			#3 Initial:	628.0
	Final-4:			#4 Final:	841.3
	Initial-4:			#4 Initial:	825.3
	Final-5:			#5 Final:	
	Initial-5:			#5 Initial:	
	NET Volume:	91.912		#6 Final:	
				#6 Initial:	
				#7 Final:	
				#7 Initial:	
				#8 Final:	
				#8 Initial:	
			Total wt of impingers:		38.3

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Run No.: 2
 Test Date: 08/15/19
 Times: 08:10 - 10:15

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	88	9.4	1.90	1.378	2.45	67	67
2	89	9.4	2.50	1.581	3.20	68	68
3	88	9.4	2.60	1.612	3.30	69	69
4	87	9.3	2.45	1.565	3.15	71	71
5	86	9.3	1.90	1.378	2.45	74	74
6	85	9.2	2.80	1.673	3.60	75	75
7	86	9.3	1.90	1.378	2.45	77	77
8	86	9.3	1.50	1.225	1.95	79	79
9	84	9.2	1.40	1.183	1.80	80	80
10	77	8.8	1.10	1.049	1.40	81	81
11	74	8.6	1.20	1.095	1.55	81	81
12	75	8.7	1.20	1.095	1.55	82	82
B-1	87	9.3	1.80	1.342	2.30	81	81
2	88	9.4	2.15	1.466	2.75	81	81
3	88	9.4	2.20	1.483	2.80	83	83
4	89	9.4	2.35	1.533	3.00	84	84
5	90	9.5	1.70	1.304	2.15	85	85
6	91	9.5	1.90	1.378	2.45	86	86
7	92	9.6	2.00	1.414	2.55	87	87
8	92	9.6	1.50	1.225	1.90	89	89
9	89	9.4	1.25	1.118	1.60	89	89
10	87	9.3	1.15	1.072	1.45	90	90
11	85	9.2	1.10	1.049	1.40	91	91
12	85	9.2	1.10	1.049	1.40	91	91
Average:		86.1		1.7389	2.28		80.9

DGM Reading (cu.ft.):	Final-1:	478.870	Impinger Weight (g):	#1 Final:	763.9
	Initial-1:	383.315		#1 Initial:	745.1
	Final-2:			#2 Final:	650.7
	Initial-2:			#2 Initial:	645.1
	Final-3:			#3 Final:	630.8
	Initial-3:			#3 Initial:	628.7
	Final-4:			#4 Final:	816.2
	Initial-4:			#4 Initial:	797.7
	Final-5:			#5 Final:	
	Initial-5:			#5 Initial:	
	NET Volume:	95.555		#6 Final:	
				#6 Initial:	
				#7 Final:	
				#7 Initial:	
				#8 Final:	
				#8 Initial:	
			Total wt of impingers:		45.0

CARB METHOD 425 DATA AND CALCULATIONS

Plant: AQMD Facility C
 City: ██████████ CA
 Source: Baghouse
 Location: Inlet 2 (Upstream to Baghouse)

Run No.: 3
 Test Date: 08/15/19
 Times: 10:55 - 13:10

point	Stack Temp (°F)		Velocity Head (in.WC)		dH (in.WC)	DGM Temperature (°F)	
	Fs	sqrt (Fs)	dP	sqrt (dP)		Fm,in	Fm,out
A-1	98	9.9	2.10	1.449	2.70	84	84
2	98	9.9	2.45	1.565	3.15	85	85
3	97	9.8	2.50	1.581	3.20	86	86
4	97	9.8	2.60	1.612	3.30	88	88
5	99	9.9	1.85	1.360	2.35	91	91
6	97	9.8	2.60	1.612	3.30	92	92
7	97	9.8	1.80	1.342	2.30	94	94
8	97	9.8	1.40	1.183	1.80	95	95
9	96	9.8	1.20	1.095	1.55	96	96
10	93	9.6	1.10	1.049	1.40	97	97
11	94	9.7	1.10	1.049	1.40	98	98
12	84	9.2	1.10	1.049	1.40	99	99
B-1	101	10.0	1.70	1.304	2.15	98	98
2	102	10.1	2.05	1.432	2.60	97	97
3	103	10.1	2.25	1.500	2.90	98	98
4	104	10.2	1.90	1.378	2.45	100	100
5	103	10.1	1.65	1.285	2.10	101	101
6	105	10.2	2.00	1.414	2.55	102	102
7	105	10.2	1.70	1.304	2.15	103	103
8	106	10.3	1.15	1.072	1.45	104	104
9	88	9.4	1.10	1.049	1.40	104	104
10	85	9.2	1.10	1.049	1.40	104	104
11	92	9.6	1.10	1.049	1.40	105	105
12	88	9.4	1.10	1.049	1.40	105	105
Average:		96.9		1.6503	2.16		96.9

DGM Reading (cu.ft.):	Final-1: 572.316	Impinger Weight (g):	#1 Final: 762.4
	Initial-1: 479.057		#1 Initial: 748.6
	Final-2:		#2 Final: 694.1
	Initial-2:		#2 Initial: 689.3
	Final-3:		#3 Final: 666.4
	Initial-3:		#3 Initial: 665.7
	Final-4:		#4 Final: 808.3
	Initial-4:		#4 Initial: 789.3
	Final-5:		#5 Final:
	Initial-5:		#5 Initial:
NET Volume:	93.259		#6 Final:
			#6 Initial:
			#7 Final:
			#7 Initial:
			#8 Final:
			#8 Initial:
		Total wt of impingers:	38.3

APPENDIX D2

CHROMIUM EMISSIONS (HEX/TOTAL) – FIELD DATA

Location: Baghouse Outlet

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ██████████ CA
 SAMPLING LOCATION: Outlet
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 54.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 6.00 inches
 DEPTH OF STACK OR DUCT, D: 48.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

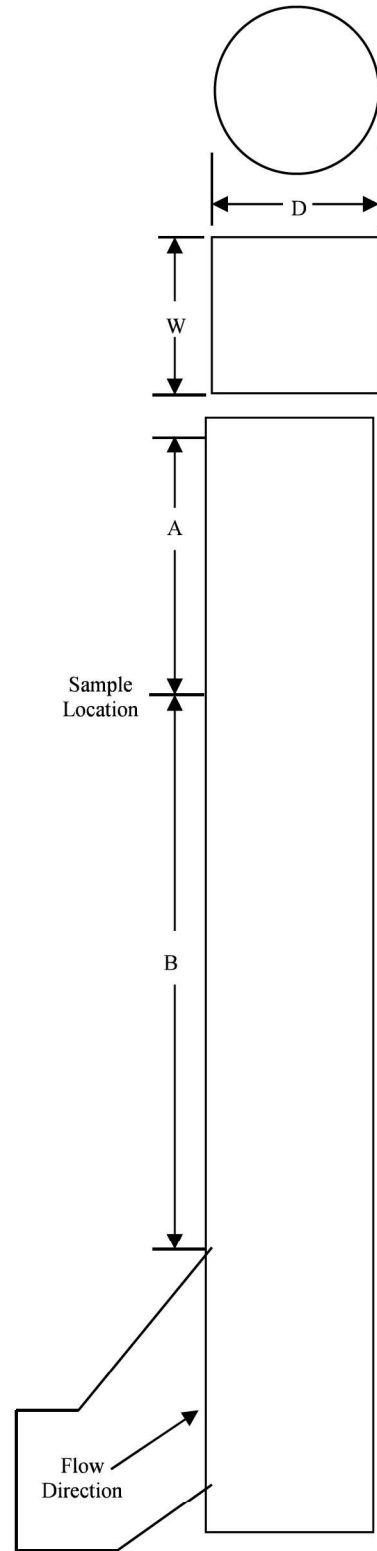
EQUIVALENT DIAMETER
 $De = 2*(DEPTH)*(WIDTH)/(DEPTH+WIDTH) =$ 48.00 inches

STACK/DUCT AREA = 12.57 sq.feet 1809.6 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	<u>B</u>	<u>A</u>
# OF INCHES	126.00	50.00
# OF DIAMETERS	2.63	1.04

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	1.01	7
2	6.7	3.22	9 1/4
3	11.8	5.66	11 5/8
4	17.7	8.50	14 1/2
5	25.0	12.00	18
6	35.6	17.09	23 1/8
7	64.4	30.91	36 7/8
8	75.0	36.00	42
9	82.3	39.50	45 1/2
10	88.2	42.34	48 3/8
11	93.3	44.78	50 3/4
12	97.9	46.99	53



DRAWING NOT TO SCALE

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #: 1	Pilot ID: 73	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date: 8-14-19	Pilot Coeff.: 0.84	1	762.6	774.6		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client: SCAQMD C	Meter Box #: A-3	2	767.8	770.4		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit: Outlet	Meter @ Dh: 1.583	3	620.3	620.8		Meter Box Leak Check		
Operator: NL	Meter Y: 1.0379	4	770.5	790.0		Rate	"HG	
Stack Dia: 48.0	TC #: 73	5	770.5			Initial:	0.00	9"
Amb. Press: 29.9	Start Time: 1125	H2O Gain =				Final:	0.00	12
Static Press: 29.9 - 0.02	Stop Time: 1330	Filter:						

Reverse Points	Time (Minute)	Delta P (HG)	Stack Temp. (F)	Set delta H (HG)	Meter Volume (scf)	Mtr. Inlet Temp. (F)	Mtr. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (HG)
A 12	0	0.06	108	2.17	608.058	84	84	N/A	N/A	50	7	N/A	N/A
11	5	0.05	114	1.81	612.3	93	85			46			
10	10	0.05	111	1.82	616.2	95	86			47			
9	15	0.05	117	1.80	620.1	96	87			47			
8	20	0.05	116	1.81	624.0	97	88			48			
7	25	0.03	114	1.09	627.9	97	89			47			
6	30	0.03	119	1.09	631.0	97	89			47	4		
5	35	0.03	119	1.08	634.0	97	90			48			
4	40	0.03	118	1.06	637.0	97	90			48			
3	45	0.03	119	1.06	640.0	98	91			48			
2	50	0.02	119	0.72	643.0	98	91			49			
1	55	0.02	119	0.72	645.5	98	91			50			
	60				647.981								
1230 B 12	0	0.02	118	0.72	647.981	92	93	N/A	N/A	52	3	N/A	N/A
11	5	0.02	121	0.72	650.4	97	91			52			
10	10	0.02	121	0.72	652.9	98	92			52			
9	15	0.02	121	0.72	655.4	99	92			52			
8	20	0.02	122	0.72	658	99	92			52			
7	25	0.02	122	0.72	660.4	100	92			52			
6	30	0.02	123	0.72	662.9	99	93			53			
5	35	0.02	121	0.72	665.35	100	93			54			
4	40	0.03	113	1.10	667.8	100	93			54	4		
3	45	0.03	115	1.10	670.85	101	94			54			
2	50	0.05	112	1.84	673.9	101	94			53	7		
1	55	0.05	112	1.84	677.83	101	94			55	7		
	60				681.85								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 92

Estimated Stack Temp: 110

Estimated Delta P: 0.04

Estimated Moisture Content: 2

Estimated O2: 20.8

Estimated CO2: 0.05

Equipment Evaluation, OK? Y or N

Ambient Temp.: _____

TC Check: _____

Pitot Check: _____

Tedlar Bag: _____

Pitot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

	1	2	3	4
DGM Initial:				
Vacuum:				
Leak Rate:				
DGM Final:				

Nozzle Information

Nozzle ID: _____

Nozzle Dia: 0.450

Run #:	2	Pilot ID:	73	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-14-19	Pilot Coeff.:	0.84	1	760.1	773.3		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMD C	Meter Box #:	A-3	2	766.8	770.9		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Outlet	Meter @ Dh:	1.583	3	619.4	621.6		Meter Box Leak Check		
Operator:	NC	Meter Y:	6.0379	4	790.0	805.2		Rate:		7HG
Stack Dia:	480	TC #:	73	5				Initial:	0.00	12
Amb. Press:	29.9	Start Time:	0810	H2O Gain =				Final:	8.00	12
Static Press:	-0.02	Stop Time:	1015	Filter:						

910 A

910

915 B

Reverse Point	Time (Minute)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mr. Inlet Temp. (F)	Mr. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	0.05	78	1.84	684.472	66	66	N/A	N/A	49	3	N/A	N/A
11	5	0.05	82	1.84	698.3	75	64			49			
10	10	0.06	82	2.22	692.2	76	66			51			
9	15	0.05	82	1.85	696.45	78	67			52			
8	20	0.05	83	1.85	700.3	79	68			53			
7	25	0.04	82	1.49	704.2	80	69			54			
6	30	0.05	82	1.86	707.7	80	70			54			
5	35	0.04	83	1.49	711.6	80	70			54			
4	40	0.05	85	1.85	715.1	80	71			54			
3	45	0.04	86	1.48	719.0	81	71			53			
2	50	0.04	86	1.48	722.5	81	72			53			
1	55	0.04	86	1.48	726.0	82	72			53			
	60				729.494								
12	0	0.03	85	1.11	729.494	75	73	N/A	N/A	53	2	N/A	N/A
11	5	0.03	87	1.11	732.5	80	72			53			732.52
10	10	0.03	90	1.10	735.5	80	73			53			735
9	15	0.03	91	1.10	738.5	81	73			53			738.52
8	20	0.03	91	1.10	741.5	82	73			53			741.52
7	25	0.03	93	1.10	744.5	82	74			53			744.53
6	30	0.02	92	0.74	747.52	83	75			53			747.52
5	35	0.03	93	1.10	750.0	82	75			52			750.00
4	40	0.03	93	1.11	753.0	84	76			52			753.03
3	45	0.03	94	1.10	756.0	85	76			53			756.03
2	50	0.06	93	2.22	759.0	86	77			54			759.03
1	55	0.06	94	2.22	763.3	88	78			54			763.29
	60				767.625								767.60

Isokinetic Factor Setup Estimated Dry Gas Meter Temp: 80 Estimated Stack Temp: 80 Estimated Delta P: 0.04 Estimated Moisture Content: 2 Estimated O2: 20.8 Estimated CO2: 0.05	Equipment Evaluation, OK? Y or N Ambient Temp.: TC Check: Pilot Check: Tedlar Bag: Pilot Exp Date: TC Exp Date:	Dry Gas Meter Leak Checks DGM Initial: [] [] [] [] Vacuum: [] [] [] [] Leak Rate: [] [] [] [] DGM Final: [] [] [] []	Nozzle Information Nozzle ID: Nozzle Dia: 0.450
---	--	---	--

Run #:	3	Pilot ID:	73	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-15-19	Pilot Coeff.:	0.84	1	753.3	776.3		Initial:	✓	✓
Client:	SCAQMD C	Meter Box #:	A-3	2	754.6	756.0		Final:	✓	✓
Unit:	Inlet Outlet	Meter @ Dh:	1.583	3	541.2	542.0		Meter Box Leak Check		
Operator:	NC	Meter Y:	1.0379	4	859.6	871.9		Rate	"HG	
Stack Dia:	48.0"	TC #:	73	5				Initial:	0.00	12
Amb. Press:	29.9	Start Time:	1055	H2O Gain =			Final:	0.00	12	
Static Press:	-0.0 Z	Stop Time:	1310	Filter:						

1055A

Traverse Points	Time (Minutes)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp. (F)	Mt. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	0.04	98	1.46	767.935	79	79	N/A	N/A	51	4	N/A	N/A
11	5	0.04	98	1.46	771.4	84	79			50			
10	10	0.04	98	1.47	774.9	87	80			51			
9	15	0.03	97	1.10	778.4	89	81			52	3		
8	20	0.03	97	1.11	781.45	90	82			52			
7	25	0.02	97	0.74	784.5	90	83			53			
6	30	0.02	99	0.74	787.0	91	84			53			
5	35	0.03	99	1.11	789.5	91	84			53			
4	40	0.02	100	0.74	792.6	93	86			53			
3	45	0.02	101	0.74	796.1	93	86			54			
2	50	0.02	106	0.73	797.6	93	86			54			
1	55	0.02	107	0.73	800.1	94	86			54			
	60				802.590								

1055

218

12	0	0.02	108	0.73	802.590	98	87	N/A	N/A	54	3	N/A	N/A
11	5	0.02	109	0.73	805.1	94	88			54	2		
10	10	0.02	110	0.73	807.6	96	88			54			
9	15	0.02	110	0.73	810.1	94	89			55			
8	20	0.02	111	0.73	812.6	96	89			55			
7	25	0.02	111	0.73	815.1	97	90			55			
6	30	0.02	111	0.73	817.6	97	91			55			
5	35	0.02	111	0.73	820.1	98	91			55			
4	40	0.02	111	0.73	822.6	98	91			56			
3	45	0.06	108	2.21	825.1	99	92			56			
2	50	0.07	107	2.59	829.44	101	93			56			
1	55	0.07	107	2.60	831.15	102	94			56			
	60				838.859								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 98

Estimated Stack Temp: 100

Estimated Delta P: 0.04

Estimated Moisture Content: 2

Estimated O2: 20.9

Estimated CO2: 0.05

Equipment Evaluation - OK? Y or N

Ambient Temp.: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

1	2	3	4
DGM Initial:			
Vacuum:			
Leak Rate:			
DGM Final:			

Nozzle Information

Nozzle ID: _____

Nozzle Dia: 0.450

Location: Inlet 1 (inside)

SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION SCAQMD METHOD 1.1

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ████████ CA
 SAMPLING LOCATION Inlet 1
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 13.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 0.0 inches
 DEPTH OF STACK OR DUCT, D: 13.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

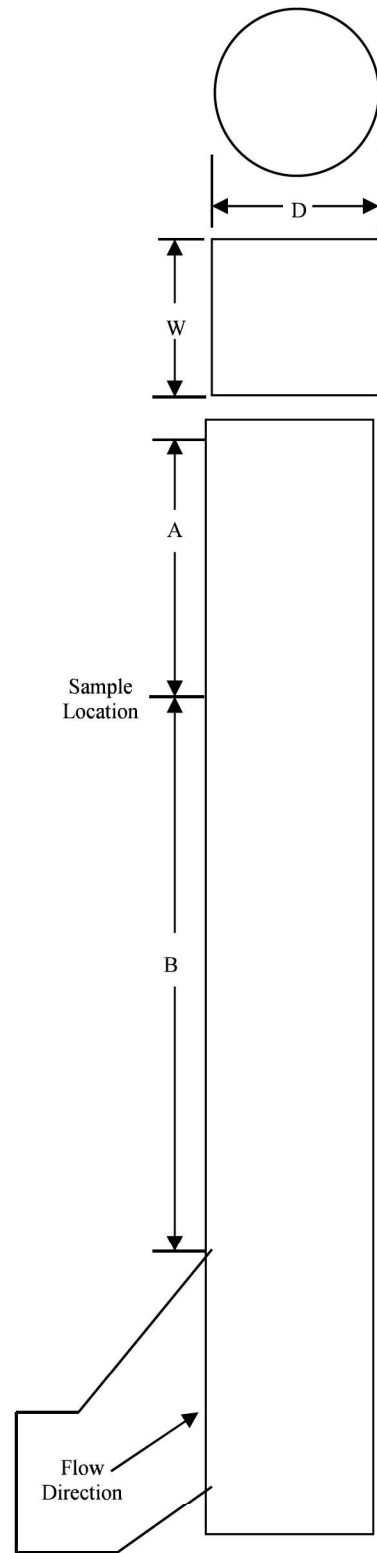
EQUIVALENT DIAMETER
 $De = 2 * (DEPTH) * (WIDTH) / (DEPTH + WIDTH) =$ 13.00 inches

STACK/DUCT AREA = 0.92 sq.feet 132.7 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	<u>B</u>	<u>A</u>
# OF INCHES	>26.0	>6.5
# OF DIAMETERS	>2.00	>0.50

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	0.50	0 1/2
2	6.7	0.87	0 7/8
3	11.8	1.53	1 1/2
4	17.7	2.30	2 1/4
5	25.0	3.25	3 1/4
6	35.6	4.63	4 5/8
7	64.4	8.37	8 3/8
8	75.0	9.75	9 3/4
9	82.3	10.70	10 3/4
10	88.2	11.47	11 1/2
11	93.3	12.13	12 1/8
12	97.9	12.50	12 1/2



DRAWING NOT TO SCALE

Run #:	1	Pilot ID:	85	Impinger #:	Initial	Final	Net	Pilot Leak Check		
Date:	8-14-19	Pilot Coeff.:	0.84	1	721.9	734.4		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMD C	Meter Box #:	A-8	2	535.4	537.1		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Inlet 1	Meter @ Dh:	1.834	3	646.7	648.5		Meter Box Leak Check		
Operator:	DS	Meter Y:	1.0395	4	879.5	887.5		Rate:		"HG
Stack Dia:	13.0"	TC #:	85	5				Initial:	0.00	15"
Amb. Press:	29.90	Start Time:	11:25	H2O Gain =			Final:	0.00	16"	
Static Press:	-1.6	Stop Time:	13:30	Filter:						

Traverse Points	Time (Minute)	Delta P ("H2O)	Stack Temp (F)	Set delta H ("H2O)	Meter Volume (scf)	Mtr. Inlet Temp (F)	Mtr. Outlet Temp (F)	Oven Temp (F)	Probe Temp (F)	Impinger Temp (F)	Pump Vac. ("HG)	TE Cooler Temp (F)	Cyclonic Flow ("H2O)
0	0				515.370								
1	5	.17	128	2.53	519.693	101	101	N/A	N/A	54	5	N/A	
2	10	.15	146	2.17	523.708	102	102			54	5		
3	15	.14	149	2.31	527.856	104	104			54	5		
4	20	.13	150	1.89	531.605	105	105			54	4.5		
5	25	.11	137	1.63	535.103	107	107			54	4.5		
6	30	.10	135	1.49	538.458	108	108			54	4		
7	35	.09	126	1.36	541.664	109	109			54	4		
8	40	.10	127	1.51	545.048	110	110			54	4		
9	45	.12	126	1.82	548.763	111	111			54	4.5		
10	50	.14	126	2.12	552.976	111	111			54	5		
11	55	.13	122	1.99	556.654	111	111			54	4.5		
12	60	.11	120	1.69	560.231	112	112			54	4.5		
0	0				560.231								
1	5	.15	139	2.23	564.336	111	111	N/A	N/A	54	5	N/A	
2	10	.16	138	2.38	568.583	112	112			54	5		
3	15	.14	153	2.06	572.557	119	119			54	5		
4	20	.14	144	2.09	576.569	119	119			54	5		
5	25	.13	144	1.95	580.436	121	121			55	4.5		
6	30	.11	130	1.69	584.093	122	122			55	4		
7	35	.08	131	1.23	587.135	123	123			55	3.5		
8	40	.09	119	1.41	590.448	124	124			55	3.5		
9	45	.11	116	1.73	594.113	123	123			55	4		
10	50	.10	116	1.58	597.614	124	124			55	3.5		
11	55	.08	123	1.25	600.724	123	123			55	3.5		
12	60	.10	113	1.58	604.228	123	123			55	4		

AD
12:25
12:30
st

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 100

Estimated Stack Temp: 130

Estimated Delta P: 0.1

Estimated Moisture Content: 2.0

Estimated O2: 20.8

Estimated CO2: 0.5

Equipment Evaluation - OK? Y or N

Ambient Temp: 81

TC Check:

Pilot Check:

Tedlar Bag: N/A

Pilot Exp Date:

TC Exp Date:

Dry Gas Meter Leak Checks

1	2	3	4

Nozzle Information

Nozzle ID: 85

Nozzle Dia: .348

DGM Initial:

Vacuum:

Leak Rate:

DGM Final:

Run #:	2	Pilot ID:	85	Impinger #	Initial	Final	Net	Pilot Leak Check	
Date:	8-15-19	Pilot Coeff.:	0.84	1	724.1	736.5		Initial:	<input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Client:	SCAGMDC	Meter Box #:	A-8	2	630.0	631.3		Final:	<input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Unit:	Inlet 1	Meter @ Dh:	1.834	3	647.4	649.9		Meter Box Leak Check	
Operator:	DT	Meter Y:	1.0395	4	865.9	902.1		Rate	"HG
Stack Dia:	13.0"	TC #:	85	5				Initial:	0.066 15"
Amb. Press:	29.90	Start Time:	8:10	H2O Gain =				Final:	0.001 16"
Static Press:	-1.5	Stop Time:	10:15	Filter:					

Traverse Points	Time (Minutes)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp. (F)	Mt. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
0	0				604.449								
1	5	.19	122	2.81	608.973	93	93	N/A	N/A	54	4	N/A	
2	10	.18	132	2.62	613.348	93	93			54	4		
3	15	.18	128	2.64	617.745	94	94			54	4		
4	20	.16	104	2.45	621.982	95	95			54	4		
5	25	.14	101	2.16	625.975	97	97			54	4		
6	30	.13	97	2.02	629.842	97	97			54	4		
7	35	.11	94	1.93	633.416	98	98			54	3.5		
8	40	.12	96	1.88	637.148	98	98			54	3.5		
9	45	.10	89	1.58	640.572	98	98			54	3.5		
10	50	.13	88	2.07	644.486	99	99			54	4		
11	55	.15	85	2.40	648.702	100	100			54	4		
12	60	.14	89	2.22	652.768	100	100			54	4		
0	0				652.768								
1	5	.17	114	2.53	657.056	89	89	N/A	N/A	54	4	N/A	
2	10	.18	118	2.67	661.453	90	90			54	4		
3	15	.16	121	2.36	665.591	90	90			54	4		
4	20	.16	119	2.37	669.748	91	91			54	4		
5	25	.11	126	1.61	673.185	92	92			54	3.5		
6	30	.12	131	1.75	676.961	92	93			54	3.5		
7	35	.10	127	1.47	680.048	93	93			54	3.5		
8	40	.10	129	1.46	683.325	93	93			54	3.5		
9	45	.09	132	1.31	686.428	93	93			54	3.5		
10	50	.11	131	1.60	689.852	93	93			54	3.5		
11	55	.13	131	1.89	693.575	93	93			54	3.5		
12	60	.15	137	2.17	697.568	94	94			54	4		

End @ 9:10 St @ 7:15

Isokinetic Factor Setup		Equipment Evaluation, OK? Y or N		Dry Gas Meter Leak Checks				Nozzle Information	
Estimated Dry Gas Meter Temp:	100	Ambient Temp.:	64	1	2	3	4	DGM Initial:	
Estimated Stack Temp:	130	TC Check:	<input checked="" type="checkbox"/>					Vacuum:	
Estimated Delta P:		Pitot Check:	<input checked="" type="checkbox"/>					Leak Rate:	
Estimated Moisture Content:	2.0	Tedlar Bag:	N/A					DGM Final:	
Estimated O2:	20.8	Pitot Exp Date:						Nozzle ID:	#85
Estimated CO2:	05	TC Exp Date:						Nozzle Dia:	0.348

Run #: 3	Pilot ID: 85	Impinger #	Initial	Final	Net	Pilot Leak Check
Date: 8-15-19	Pilot Coef.: 0.84	1	728.9	740.0		Initial: <input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Client: SCARMD C	Meter Box #: A-8	2	749.7	752.5		Final: <input checked="" type="checkbox"/> <input checked="" type="checkbox"/>
Unit: Baghouse - IN1	Meter @ Dh: 1.834	3	640.3	672.1	619.1	
Operator: DJ	Meter Y: 1.0395	4	859.5	877.1		
Stack Dia: 13.0"	TC #: 85	5				
Amb. Press: 29.9	Start Time: 10:53	H2O Gain =			Meter Box Leak Check	
Static Press: -1.4	Stop Time: 12:10	Filter:			Initial: .000 13.1"	
					Final: .000 13.1"	

Traverse Points	Time (Minutes)	Delta P (H2O)	Stack Temp (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp (F)	Mt. Outlet Temp (F)	Oven Temp (F)	Probe Temp (F)	Impinger Temp (F)	Pump Vac. (HG)	TE Cooler Temp (F)	Cyclonic Flow (H2O)
0	0				701.976								
1	5	.18	127	2.70	706.462	105	106	N/A	N/A	54	4	N/A	
2	10	.17	128	2.55	710.845	107	107			54	4		
3	15	.16	125	2.43	715.139	111	111			54	4		
4	20	.14	133	2.11	719.135	113	113			54	4		
5	25	.13	137	1.94	722.978	112	112			54	4		
6	30	.11	138	1.64	726.505	112	112			54	3.5		
7	35	.10	140	1.49	729.873	113	113			54	3.5		
8	40	.11	138	1.64	733.406	112	112			54	3.5		
9	45	.13	126	1.98	737.271	112	112			54	4		
10	50	.12	127	1.82	740.984	112	112			54	3.5		
11	55	.11	131	1.65	744.528	110	110			54	3.5		
12	60	.10	134	1.49	747.883	108	108			54	3.5		
0	0				747.883								
1	5	.17	149	2.44	752.136	101	101	N/A	N/A	54	4	N/A	
2	10	.16	149	2.30	756.268	101	101			54	4		
3	15	.15	154	2.15	760.294	104	104			54	4		
4	20	.13	154	1.86	764.006	104	104			54	3.5		
5	25	.12	155	1.72	767.592	105	105			54	3.5		
6	30	.10	156	1.43	770.894	106	106			54	3.5		
7	35	.10	155	1.43	774.152	106	106			54	3.5		
8	40	.09	156	1.29	777.275	107	107			54	3		
9	45	.10	152	1.44	780.579	107	107			54	3.5		
10	50	.11	152	1.59	784.035	107	107			54	3.5		
11	55	.10	154	1.44	787.321	107	107			55	3.5		
12	60	.12	154	1.73	790.926	107	107			55	3.5		

They did the leak opening for 15 min.

End @ 11:55

Start @ 12:10

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp:	100
Estimated Stack Temp:	130
Estimated Delta P:	
Estimated Moisture Content:	2.0
Estimated O2:	20.9
Estimated CO2:	.05

Equipment Evaluation, OK? Y or N

Ambient Temp:	70
TC Check:	✓
Pilot Check:	✓
Tedar Bag:	N/A
Pilot Exp Date:	
TC Exp Date:	

Dry Gas Meter Leak Checks

	1	2	3	4
DGM Initial:				
Vacuum:				
Leak Rate:				
DGM Final:				

Nozzle Information

Nozzle ID:	6185
Nozzle Dia:	0.348

Location: Inlet 2 (Upstream to Baghouse)

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ████████ CA
 SAMPLING LOCATION Inlet 2
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 22.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 6.00 inches
 DEPTH OF STACK OR DUCT, D: 16.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

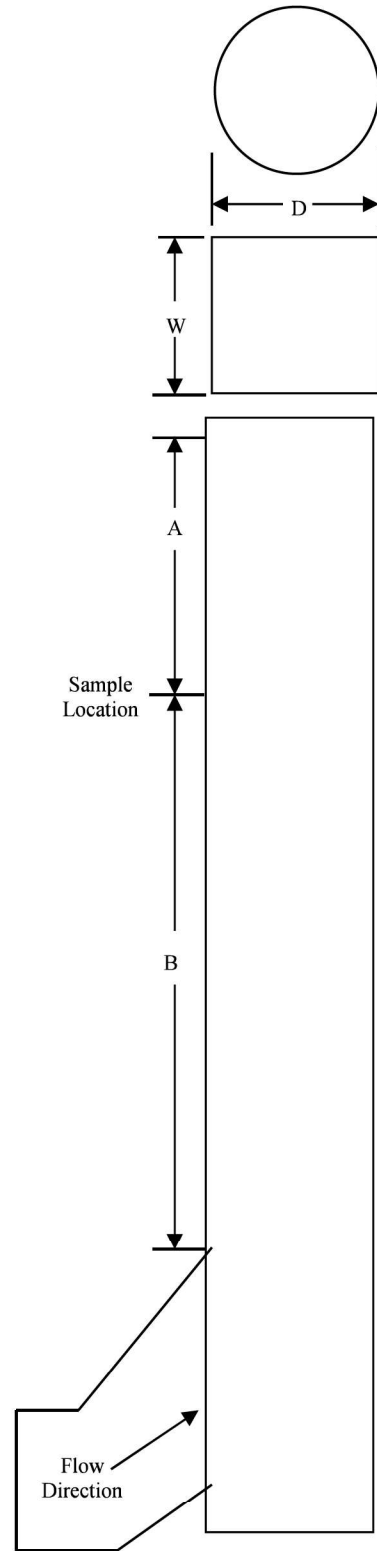
EQUIVALENT DIAMETER
 $De = 2 * (DEPTH) * (WIDTH) / (DEPTH + WIDTH) =$ 16.00 inches

STACK/DUCT AREA = 1.40 sq.feet 201.1 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	<u>B</u>	<u>A</u>
# OF INCHES	42.00	196.00
# OF DIAMETERS	2.63	12.25

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	0.50	6 1/2
2	6.7	1.07	7 1/8
3	11.8	1.89	7 7/8
4	17.7	2.83	8 7/8
5	25.0	4.00	10
6	35.6	5.70	11 3/4
7	64.4	10.30	16 1/4
8	75.0	12.00	18
9	82.3	13.17	19 1/8
10	88.2	14.11	20 1/8
11	93.3	14.93	20 7/8
12	97.9	15.50	21 1/2



DRAWING NOT TO SCALE

Run #:	1	Pilot ID:	28	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-14-19	Pilot Coeff.:	0.84	1	743.0	757.2		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMD C	Meter Box #:	4-6	769.02	668.5	773.2		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Inlet 2	Meter @ Dh:	1.789	3	678.0	630.9		Meter Box Leak Check		
Operator:	WB	Meter Y:	1.0376	4	825.3	841.3		Rate	"HG	
Stack Dia:	16.0"	TC #:	28	5				Initial:	15	0.001
Amb. Press:	29.9	Start Time:	1125	H2O Gain =				Final:	15	0.000
Static Press:	-4.2	Stop Time:	1530	Filler:						

Traverse Points	Time (Minutes)	Delta P (H2O)	Stack Temp (F)	Set delta H (H2O)	Meter Volume (scf)	Mtr. Inlet Temp (F)	Mtr. Outlet Temp (F)	Oven Temp (F)	Probe Temp (F)	Impinger Temp (F)	Pump Vac. (HG)	TE Cooler Temp (F)	Cyclonic Flow (H2O)
12	0	1.90	108	2.25	291.055	91	91	NA	NA	54	11		
11	5	1.80	110	2.10	295.11	92	92			54	11		
10	10	1.90	111	2.25	299.10	93	93			56	11		
9	15	1.90	113	2.25	303.20	94	94			56	11		
8	20	1.75	111	2.05	307.35	96	96			57	10		
7	25	2.50	113	2.95	311.29	98	98			56	14		
6	30	1.70	111	2.00	316.11	100	100			57	10		
5	35	1.20	109	1.40	320.00	101	101			58	9		
4	40	1.00	106	1.15	323.33	103	103			59	8		
3	45	1.00	104	1.15	326.32	103	103			57	8		
2	50	1.05	107	1.25	329.33	104	104			57	8		
1	55	1.00	107	1.15	332.53	104	104			58	8		
12	60	1.95	118	2.30	335.57	104	104			50	12		
11	65	2.00	110	2.35	339.76	104	104			51	12		
10	70	2.25	115	2.65	344.09	105	105			53	13		
9	75	2.15	112	2.50	348.52	106	106			52	13		
8	80	1.90	114	2.25	353.07	108	108			54	12		
7	85	2.30	123	2.70	357.16	109	109			54	14		
6	90	1.80	119	2.10	361.83	110	110			56	11		
5	95	1.60	122	1.90	365.82	110	110			58	11		
4	100	1.30	116	1.55	369.75	111	111			60	9		
3	105	1.20	113	1.40	373.12	111	111			60	9		
2	110	1.05	115	1.25	376.58	110	110			60	9		
1	115	1.10	108	1.30	379.76	110	110			61	9		
END	120				382.967								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: _____

Estimated Stack Temp: _____

Estimated Delta P: _____

Estimated Moisture Content: _____

Estimated O2: _____

Estimated CO2: _____

Equipment Evaluation, OK? Y or N

Ambient Temp: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

	1	2	3	4
DGM Initial:				
Vacuum:				
Leak Rate:				
DGM Final:				

Nozzle Information

Nozzle ID: 4620

Nozzle Dia: 0.181

Run #:	2	Pitot ID:	28	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-15-19	Pitot Coeff.:	0.28	1	745.1	763.9		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCARMDC	Meter Box #:	A-6	2	645.1	650.7		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Inlet 2	Meter @ Dh:	1.789	3	628.7	630.8		Meter Box Leak Check		
Operator:	WB	Meter Y:	1.0376	4	797.7	816.2		Rate	"HG	
Stack Dia:	16.0"	TC #:	28	5				Initial:	2.0	0.001
Amb. Press:	29.9	Start Time:	0810	H2O Gain =			Final:	0	0.000	
Static Press:	-4.3	Stop Time:	1015	Filter:						

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mtr. Inlet Temp. (F)	Mtr. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	1.90	88	2.45	388.315	67	67	N/A	N/A	52	5		
11	5	2.50	89	3.20	387.18	68	68			60	5		
10	10	2.60	88	3.30	391.91	69	69			53	5		
9	15	2.45	87	3.15	396.71	71	71			54	5		
8	20	1.90	86	2.45	401.34	74	74			56	4		
7	25	2.80	85	3.60	405.47	75	75			57	5		
6	30	1.90	86	2.45	410.53	77	77			57	4		
5	35	1.50	86	1.95	414.60	79	79			57	4		
4	40	1.40	84	1.80	418.35	80	80			56	3		
3	45	1.10	77	1.40	412.91	81	81			56	3		
2	50	1.20	74	1.55	425.12	81	81			55	3		
1	55	1.20	75	1.55	428.43	82	82			55	3		
12	60	1.80	87	2.30	431.84	81	81			66	4		
11	65	2.15	88	2.75	435.86	81	81			51	5		
10	70	2.20	88	2.80	440.29	83	83			54	5		
9	75	2.35	89	3.00	444.87	84	84			55	5		
8	80	1.70	90	2.15	449.53	85	85			55	4		
7	85	1.90	91	2.45	453.48	86	86			55	4		
6	90	2.00	92	2.55	457.66	87	87			55	5		
5	95	1.50	92	1.90	462.04	89	89			55	4		
4	100	1.25	89	1.60	465.75	89	89			55	4		
3	105	1.15	87	1.45	469.14	90	90			54	4		
2	110	1.10	85	1.40	472.43	91	91			55	4		
1	115	1.10	85	1.40	475.67	91	91			55	4		
END	120				478.870								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: _____

Estimated Stack Temp: _____

Estimated Delta P: _____

Estimated Moisture Content: _____

Estimated O2: _____

Estimated CO2: _____

Equipment Evaluation, OK? Y or N

Ambient Temp: _____

TC Check: _____

Pitot Check: _____

Tedlar Bag: _____

Pitot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

	1	2	3	4
DGM Initial:				
Vacuum:				
Leak Rate:				
DGM Final:				

Nozzle Information

Nozzle ID: 61.70

Nozzle Dia: 0.181

Run #: 3	Pilot ID: 28	Impinger #	Initial	Final	Net	Pilot Leak Check	
Date: 8-14-19	Pilot Coeff.: 0.84	1	748.6	762.4		Initial:	<input checked="" type="checkbox"/>
Client: SCAQMD C	Meter Box #: A-6	2	689.3	694.1		Final:	<input checked="" type="checkbox"/>
Unit: Inlet 2	Meter @ Dh: 1.789	3	665.7	666.4		Meter Box Leak Check	
Operator: WB	Meter Y: 1.0376	4	789.3	805.3		Rate	"HG
Stack Dia: 16.0"	TC #: 28	5				Initial:	20 0.001
Amb. Press: 29.9	Start Time: 1055	H2O Gain =				Final:	19 0.000
Static Press: -4.3	Stop Time: 1310	Filter:					

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp. (F)	Set delta H (H2O)	Meter Volume (scf)	Mtr. Inlet Temp. (F)	Mtr. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (HG)	TE Cooler Temp. (F)	Cyclonic Flow (H2O)
12	0	2.10	98	2.70	479.057	84	84	NA	NA	56	6		
11	5	2.45	98	3.15	483.48	85	85			51	7		
10	10	2.50	97	3.20	488.26	86	86			53	7		
9	15	2.60	97	3.30	493.10	88	88			55	7		
8	20	1.85	99	2.35	497.94	91	91			57	5		
7	25	2.60	97	3.30	501.92	92	92			58	7		
6	30	1.80	97	2.30	506.89	94	94			58	5		
5	35	1.40	97	1.80	510.88	95	95			60	5		
4	40	1.20	96	1.55	514.48	96	96			59	5		
3	45	1.10	93	1.40	517.81	97	97			60	5		
2	50	1.10	94	1.40	520.94	98	98			58	5		
1	55	1.10	84	1.40	524.12	99	99			59	5		
12	60	1.70	101	2.15	527.29	98	98			54	6		
11	65	2.05	102	2.60	531.25	97	97			55	6		
10	70	2.25	103	2.90	535.53	98	98			56	7		
9	75	1.90	104	2.45	540.17	100	100			58	6		
8	80	1.65	103	2.10	544.35	101	101			60	6		
7	85	2.00	105	2.55	548.18	102	102			58	6		
6	90	1.70	105	2.15	552.40	103	103			60	6		
5	95	1.15	106	1.45	556.35	104	104			60	5		
4	100	1.10	88	1.40	559.56	104	104			59	5		
3	105	1.10	85	1.40	562.73	104	104			58	5		
2	110	1.10	92	1.40	565.93	105	105			59	5		
1	115	1.10	88	1.40	569.12	105	105			60	5		
END	120				572.316								

Isokinetic Factor Setup Estimated Dry Gas Meter Temp: _____ Estimated Stack Temp: _____ Estimated Delta P: _____ Estimated Moisture Content: _____ Estimated O2: _____ Estimated CO2: _____	Equipment Evaluation, OK? Y or N Ambient Temp: _____ TC Check: _____ Pitot Check: _____ Tedlar Bag: _____ Pitot Exp Date: _____ TC Exp Date: _____	Dry Gas Meter Leak Checks <table border="1"> <tr><th>1</th><th>2</th><th>3</th><th>4</th></tr> <tr><td></td><td></td><td></td><td></td></tr> <tr><td></td><td></td><td></td><td></td></tr> <tr><td></td><td></td><td></td><td></td></tr> <tr><td></td><td></td><td></td><td></td></tr> </table> DGM Initial: _____ Vacuum: _____ Leak Rate: _____ DGM Final: _____	1	2	3	4																	Nozzle Information Nozzle ID: <u>6L 20</u> Nozzle Dia: <u>0.187</u>
1	2	3	4																				

APPENDIX D3

CHROMIUM EMISSIONS (HEX/TOTAL) – LABORATORY DATA

M425 Lab Data Summary

				Hex Chrome			Total Chrome		
				Inlet 1	Inlet 2	Outlet	Inlet	Inlet	Outlet
				Inside	Outside		1	2	
Run 1	Rinse	C1	ug	0.068	0.29	<0.22	240	59	<0.31
	Impingers	C2	ug	0.75	2.60	0.092	2300	410	<0.24
	Total		ug	0.818	2.89	<0.31	2540	469	<0.55
Run 2	Rinse	C1	ug	0.90	0.20	<0.0095	50	14	<0.35
	Impingers	C2	ug	21	5.10	<0.022	280	56	<0.24
	Total		ug	21.90	5.30	<0.0315	330	70	<0.59
Run 3	Rinse	C1	ug	0.21	1.9	<0.009	27	110	<0.36
	Impingers	C2	ug	21	2.00	0.037	980	170	<0.24
	Total		ug	21.21	3.9	<0.0460	1007	280	<0.60
Run FB	Rinse	C1	ug		<0.009			<0.36	
	Impingers	C2	ug		<0.021			<0.25	
	Total		ug		<0.030			<0.61	
Run RB	Rinse	C1	ug		< 0.010			< 1	
	Impingers	C2	ug		0.020			< 1	
	Total		ug		< 0.030			< 2	
AVG	Total		ug	14.64	4.03	<0.13	1292.333	273	<0.58



WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Project Number: In (I)/In (O)/Out

Reported:
06/24/2019 14:29

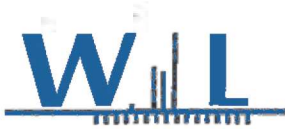
Project Manager: Almega Environmental & Technical Services

Sample Summary

Table with 6 columns: Sample Name, Sampled By, Lab ID, Matrix, Sampled, Qualifiers. Lists 22 samples with details like '10562 - M425 - C1 - In(O) - FB' and 'AOMD Facility A - M425 - RB - Filter'.

Analyses Accreditation Summary

Table with 4 columns: Analyte, CAS #, Not By NELAP, By ANAB. Row for 'CARB 425 in Filter Chromium 6+' with CAS # 18540-29-9 and a green checkmark in the Not By NELAP column.



Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Project Number: In (I)/In (O)/Out
Project Manager: Almega Environmental & Technical Services

Reported:
06/24/2019 14:29

Sample Results

(Continued)

Sample: 10562 - M425 - C1 - Out - R3
9E30014-19 (Filter) Sampled 05/23/19 8:25 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425 Chromium 6+	Batch ID: W9F0120 Instr: LC13 ND	Prepared: 06/04/19 11:45 0.050	ug/filter	5	Analyst: jna 06/04/19 23:22	
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020 Chromium, Total	Batch ID: W9F0440 Instr: ICPMS03 ND	Prepared: 06/10/19 09:31 1.0	ug/filter	5	Analyst: ALN 06/12/19 15:25	M-04

Sample: 10562 - M425 - C2 - Out - R3
9E30014-20 (Filter) Sampled 05/23/19 8:25 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020 Chromium, Total	Batch ID: W9F0440 Instr: ICPMS03 ND	Prepared: 06/10/19 09:31 1.0	ug/filter	5	Analyst: ALN 06/12/19 15:27	M-04

Sample: 10562 - M425 - C2 - Out - R3
9E30014-20RE1 (Filter) Sampled 05/23/19 8:25 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425 Chromium 6+	Batch ID: W9F0369 Instr: LC13 ND	Prepared: 06/06/19 11:40 0.022	ug/filter	1	Analyst: jna 08/08/19 15:00	

Sample: AQMD Facility A - M425 - RB
9E30014-21 (Filter) Sampled 05/23/19 11:30 by Client

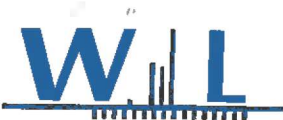
Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020 Chromium, Total	Batch ID: W9F0444 Instr: ICPMS03 ND	Prepared: 06/10/19 09:39 1.0	ug/filter	5	Analyst: ALN 06/12/19 15:55	M-04

Sample: AQMD Facility A - M425 - RB
9E30014-21RE1 (Filter) Sampled 05/23/19 11:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425 Chromium 6+	Batch ID: W9F0369 Instr: LC13 ND	Prepared: 06/06/19 11:40 0.010	ug/filter	1	Analyst: jna 06/06/19 15:12	

Sample: AQMD Facility A - M425 - RB - Filter
9E30014-22 (Filter) Sampled 05/23/19 11:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Metals (Non-Aqueous) by EPA 6000/7000 Series Methods						
Method: EPA 6020 Chromium, Total	Batch ID: W9F0444 Instr: ICPMS03 ND	Prepared: 06/10/19 09:39 1.0	ug/filter	5	Analyst: ALN 06/12/19 15:58	M-04



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Project Number: In (I)/In (O)/Out

Project Manager: Almega Environmental & Technical Services

Reported:
06/24/2019 14:29

Sample Results

(Continued)

Sample: AQMD Facility A - M425 - RB - Filter
9E30014-22RE1 (Filter)

Sampled: 05/23/19 11:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425 Chromium 6+	Batch ID: W9F0369 Instr: LC13 ND	Prepared: 06/06/19 11:40 0.020	ug/filter	1	Analyst: jna 06/06/19 15:24	

Work Orders: 9H20010

Report Date: 10/09/2019

Project: 10566 Baghouse SCAQMD-C

Received Date: 8/20/2019

Turnaround Time: Normal

Phones: (714) 889-4000

Fax: (714) 889-7030

P.O. #: 10566

Attn: Almega Environmental & Technical Services

Billing Code:

Client: Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630


ELAP-CA #1132 • EPA-UCMR #CA00211 • Guam-EPA #17-008R • HW-DOH # • ISO 17025 #L2457.01 • LACSD #10143 •
NELAP-CA #04229CA • NELAP-OR #4047 • NJ-DEP #CA015 • NV-DEP #NAC 445A • SCAQMD #93LA1006

This is a complete final report. The information in this report applies to the samples analyzed in accordance with the chain-of-custody document. Weck Laboratories certifies that the test results meet all requirements of TNI unless noted by qualifiers or written in the Case Narrative. This analytical report must be reproduced in its entirety.

Dear Almega Environmental & Technical Services,

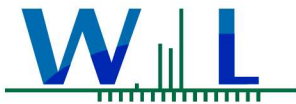
Enclosed are the results of analyses for samples received 8/20/19 with the Chain-of-Custody document. The samples were received in good condition, at 5.1 °C. All analyses met the method criteria except as noted in the case narrative or in the report with data qualifiers.

Reviewed by:



Brandon Gee
Operations Manager/Senior PM





WECK LABORATORIES, INC.

Almega Environmental & Technical Services
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Certificate of Analysis

Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:
10/09/2019 12:54

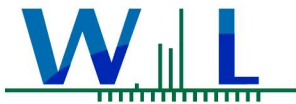
Project Manager: Almega Environmental & Technical Services

Sample Summary

Sample Name	Sampled By	Lab ID	Matrix	Sampled	Qualifiers
10566-M425-FB-C1	Client	9H20010-01	Filter	08/14/19 07:30	
10566-M425-FB-C2	Client	9H20010-02	Filter	08/14/19 07:30	
10566-M425-I1-R1-C1	Client	9H20010-03	Filter	08/14/19 13:30	
10566-M425-I1-R1-C2	Client	9H20010-04	Filter	08/14/19 13:30	
10566-M425-I2-R1-C1	Client	9H20010-06	Filter	08/14/19 13:30	
10566-M425-I2-R1-C2	Client	9H20010-07	Filter	08/14/19 13:30	
10566-M425-O-R1-C1	Client	9H20010-09	Filter	08/14/19 13:30	
10566-M425-O-R1-C2	Client	9H20010-10	Filter	08/14/19 13:30	
10566-M425-I1-R2-C1	Client	9H20010-11	Filter	08/15/19 10:15	
10566-M425-I1-R2-C2	Client	9H20010-12	Filter	08/15/19 10:15	
10566-M425-I2-R2-C1	Client	9H20010-14	Filter	08/15/19 10:15	
10566-M425-I2-R2-C2	Client	9H20010-15	Filter	08/15/19 10:15	
10566-M425-O-R2-C1	Client	9H20010-17	Filter	08/15/19 10:15	
10566-M425-O-R2-C2	Client	9H20010-18	Filter	08/15/19 10:15	
10566-M425-I1-R3-C1	Client	9H20010-19	Filter	08/15/19 13:10	
10566-M425-I1-R3-C2	Client	9H20010-20	Filter	08/15/19 13:10	
10566-M425-I2-R3-C1	Client	9H20010-22	Filter	08/15/19 13:10	
10566-M425-I2-R3-C2	Client	9H20010-23	Filter	08/15/19 13:10	
10566-M425-O-R3-C1	Client	9H20010-25	Filter	08/15/19 13:10	
10566-M425-O-R3-C2	Client	9H20010-26	Filter	08/15/19 13:10	

Analyses Accreditation Summary

Analyte	CAS #	Not By NELAP	By ANAB
CARB 425 in Filter Chromium 6+	18540-29-9	✓	



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Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:

10/09/2019 12:54

Project Manager: Almega Environmental & Technical Services

Sample Results

Sample: 10566-M425-FB-C1
9H20010-01 (Filter) Sampled: 08/14/19 7:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna	
Chromium 6+	ND	0.0090	ug/filter	1	08/26/19 13:06

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln	
Chromium, Total	ND	0.36	ug/filter	1	10/06/19 14:59

Sample: 10566-M425-FB-C2
9H20010-02 (Filter) Sampled: 08/14/19 7:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna	
Chromium 6+	ND	0.021	ug/filter	1	08/26/19 13:18

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln	
Chromium, Total	ND	0.25	ug/filter	1	10/06/19 15:00

Sample: 10566-M425-I1-R1-C1
9H20010-03 (Filter) Sampled: 08/14/19 13:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna	
Chromium 6+	0.068	0.0085	ug/filter	1	08/26/19 13:30

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln	
Chromium, Total	240	38	ug/filter	100	10/06/19 15:02

Sample: 10566-M425-I1-R1-C2
9H20010-04 (Filter) Sampled: 08/14/19 13:30 by Client

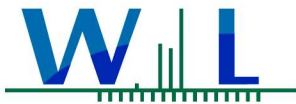
Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna	
Chromium 6+	0.75	0.043	ug/filter	1	08/26/19 13:41

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln	
Chromium, Total	2300	100	ug/filter	500	10/06/19 15:04



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Almega REPORT
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Reported:
10/09/2019 12:54

Project Manager: Almega Environmental & Technical Services

Sample Results

(Continued)

Sample: 10566-M425-I2-R1-C1
9H20010-06 (Filter) Sampled: 08/14/19 13:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna
Chromium 6+	0.29	0.0089	ug/filter	1 08/26/19 13:53

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln
Chromium, Total	59	3.6	ug/filter	10 10/06/19 15:06

Sample: 10566-M425-I2-R1-C2
9H20010-07 (Filter) Sampled: 08/14/19 13:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna
Chromium 6+	2.6	0.041	ug/filter	1 08/26/19 14:05

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln
Chromium, Total	410	20	ug/filter	100 10/06/19 15:07

Sample: 10566-M425-O-R1-C1
9H20010-09 (Filter) Sampled: 08/14/19 13:30 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna	
Chromium 6+	ND	0.22	ug/filter	20 08/26/19 15:04	M-05

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln
Chromium, Total	ND	0.31	ug/filter	1 10/06/19 15:09

Sample: 10566-M425-O-R1-C2
9H20010-10 (Filter) Sampled: 08/14/19 13:30 by Client

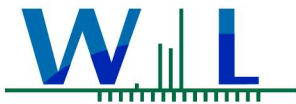
Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
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Hexavalent Chromium by IC

Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna
Chromium 6+	0.092	0.022	ug/filter	1 08/26/19 14:29

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln
Chromium, Total	ND	0.24	ug/filter	1 10/06/19 15:11



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Project Number: 10566 Baghouse SCAQMD-C

Reported:
10/09/2019 12:54

Project Manager: Almega Environmental & Technical Services

Sample Results

(Continued)

Sample: 10566-M425-I1-R2-C1
9H20010-11 (Filter) Sampled: 08/15/19 10:15 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	0.90	0.011	ug/filter	1	08/26/19 14:40	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	50	3.1	ug/filter	10	10/06/19 15:13	

Sample: 10566-M425-I1-R2-C2
9H20010-12 (Filter) Sampled: 08/15/19 10:15 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	21	0.043	ug/filter	1	08/26/19 14:52	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	280	20	ug/filter	100	10/06/19 15:15	

Sample: 10566-M425-I2-R2-C1
9H20010-14 (Filter) Sampled: 08/15/19 10:15 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	0.20	0.0095	ug/filter	1	08/26/19 16:11	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

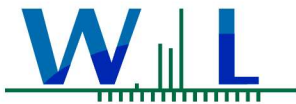
Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	14	1.7	ug/filter	5	10/06/19 17:08	

Sample: 10566-M425-I2-R2-C2
9H20010-15 (Filter) Sampled: 08/15/19 10:15 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	5.1	0.053	ug/filter	1	08/26/19 16:23	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	56	2.0	ug/filter	10	10/06/19 16:45	



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ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:
10/09/2019 12:54

Project Manager: Almega Environmental & Technical Services

Sample Results

(Continued)

Sample: 10566-M425-O-R2-C1
9H20010-17 (Filter) Sampled: 08/15/19 10:15 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	ND	0.0095	ug/filter	1	08/26/19 16:35	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	ND	0.35	ug/filter	1	10/06/19 16:47	

Sample: 10566-M425-O-R2-C2
9H20010-18 (Filter) Sampled: 08/15/19 10:15 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	ND	0.022	ug/filter	1	08/26/19 16:47	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	ND	0.24	ug/filter	1	10/06/19 16:49	

Sample: 10566-M425-I1-R3-C1
9H20010-19 (Filter) Sampled: 08/15/19 13:10 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	0.21	0.0090	ug/filter	1	08/26/19 16:58	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

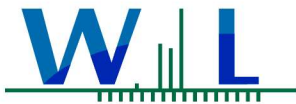
Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	27	3.6	ug/filter	10	10/06/19 16:51	

Sample: 10566-M425-I1-R3-C2
9H20010-20 (Filter) Sampled: 08/15/19 13:10 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	21	0.044	ug/filter	1	08/26/19 17:10	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	980	20	ug/filter	100	10/06/19 16:53	



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Almega REPORT
ENVIRONMENTAL

Project Number: 10566 Baghouse SCAQMD-C

Reported:

10/09/2019 12:54

Project Manager: Almega Environmental & Technical Services

Sample Results

(Continued)

Sample: 10566-M425-I2-R3-C1
9H20010-22 (Filter) Sampled: 08/15/19 13:10 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	1.9	0.0095	ug/filter	1	08/26/19 17:22	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	110	3.5	ug/filter	10	10/06/19 16:54	

Sample: 10566-M425-I2-R3-C2
9H20010-23 (Filter) Sampled: 08/15/19 13:10 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	2.0	0.042	ug/filter	1	08/26/19 17:34	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	170	20	ug/filter	100	10/06/19 16:56	

Sample: 10566-M425-O-R3-C1
9H20010-25 (Filter) Sampled: 08/15/19 13:10 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	ND	0.0090	ug/filter	1	08/26/19 17:46	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

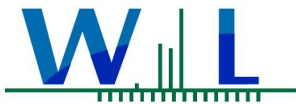
Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	ND	0.36	ug/filter	1	10/06/19 16:58	

Sample: 10566-M425-O-R3-C2
9H20010-26 (Filter) Sampled: 08/15/19 13:10 by Client

Analyte	Result	MRL	Units	Dil	Analyzed	Qualifier
Hexavalent Chromium by IC						
Method: CARB 425	Batch ID: W9H1418	Instr: LC13	Prepared: 08/26/19 09:40	Analyst: jna		
Chromium 6+	0.037	0.022	ug/filter	1	08/26/19 17:57	

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Method: EPA 6020	Batch ID: W9H1709	Instr: ICPMS03	Prepared: 08/29/19 15:58	Analyst: aln		
Chromium, Total	ND	0.24	ug/filter	1	10/06/19 17:00	



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Project Number: 10566 Baghouse SCAQMD-C

Reported:

10/09/2019 12:54

Project Manager: Almega Environmental & Technical Services

Quality Control Results

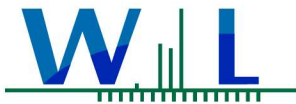
Hexavalent Chromium by IC

Analyte	Result	MRL	Units	Spike Level	Source Result	%REC	Limits	RPD	RPD Limit	Qualifier
Batch: W9H1418 - CARB 425										
Blank (W9H1418-BLK1)										
Chromium 6+	ND	0.00010	ug/filter							
LCS (W9H1418-BS1)										
Chromium 6+	0.00508	0.00010	ug/filter	0.00500		102	90-110			
Matrix Spike (W9H1418-MS1)										
Chromium 6+	0.493	0.0090	ug/filter	0.450	ND	109	85-117			
Matrix Spike (W9H1418-MS2)										
Chromium 6+	4.52	0.042	ug/filter	2.12	2.02	118	85-117			MS-05
Matrix Spike Dup (W9H1418-MSD1)										
Chromium 6+	0.443	0.0090	ug/filter	0.450	ND	98	85-117	11	20	
Matrix Spike Dup (W9H1418-MSD2)										
Chromium 6+	6.14	0.042	ug/filter	2.12	2.02	194	85-117	31	20	MS-05

Quality Control Results

Metals (Non-Aqueous) by EPA 6000/7000 Series Methods

Analyte	Result	MRL	Units	Spike Level	Source Result	%REC	Limits	RPD	RPD Limit	Qualifier
Batch: W9H1709 - EPA 6020										
Blank (W9H1709-BLK1)										
Chromium, Total	ND	0.20	ug/filter							
LCS (W9H1709-BS1)										
Chromium, Total	4.83	0.20	ug/filter	5.00		97	80-120			
LCS Dup (W9H1709-BSD1)										
Chromium, Total	5.04	0.20	ug/filter	5.00		101	80-120	4	20	



WECK LABORATORIES, INC.

Almega Environmental & Technical Services
10602 Walker St
Cypress, CA 90630

Project Number: 10566 Baghouse SCAQMD-C

Project Manager: Almega Environmental & Technical Services

Certificate of Analysis

Almega REPORT
ENVIRONMENTAL

Reported:
10/09/2019 12:54



Notes and Definitions

Item	Definition
M-05	Due to the nature of matrix interferences, sample was diluted prior to analysis. The MDL and MRL were raised due to the dilution.
MS-05	The spike recovery and/or RPD were outside acceptance limits for the MS and/or MSD due to possible matrix interference. The LCS and/or LCSD were within acceptance limits showing that the laboratory is in control and the data is acceptable.
% Rec	Percent Recovery
Dil	Dilution
dry	Sample results reported on a dry weight basis
MDA	Minimum Detectable Activity
MDL	Method Detection Limit
MRL	The minimum levels, concentrations, or quantities of a target variable (e.g., target analyte) that can be reported with a specified degree of confidence. The MRL is also known as Limit of Quantitation (LOQ)
ND	NOT DETECTED at or above the Method Reporting Limit (MRL). If Method Detection Limit (MDL) is reported, then ND means not detected at or above the MDL.
NR	Not Reportable
RPD	Relative Percent Difference
Source	Sample that was matrix spiked or duplicated.
TIC	Tentatively Identified Compound (TIC) using mass spectrometry. The reported concentration is relative concentration based on the nearest internal standard. If the library search produces no matches at, or above 85%, the compound is reported as unknown.

Any remaining sample(s) will be disposed of one month from the final report date unless other arrangements are made in advance.

An Absence of Total Coliform meets the drinking water standards as established by the California State Water Resources Control Board (SWRCB)

All results are expressed on wet weight basis unless otherwise specified.

All samples collected by Weck Laboratories have been sampled in accordance to laboratory SOP Number MIS002.

9H2-0010



CHAIN OF CUSTODY RECORDS

INVOICE TO: _____
REPORT TO: _____
PO # 10566
ALMEGA Environmental & Technical Services
 10602 Walker St.
 Cypress, CA 90630
 (714) 889-4000 Fax (714) 889-7030
 lab@almegaenv.com
ATTN: Cheryl

Job #	10566	Unit #	Baghouse	Client	SCAQMD - C	Location: Inlet & Outlet	ANALYSIS REQUESTED			Return or Dispose	REMARKS	Turnaround Time
							Standard:	Other:	Other:			
Project Manager: Morgan Nguyen Unit Information: Type Of Sample: LIQUID GAS SOLID No of Containers: _____ Lab Sample # _____ Rush: _____ Depends on # of Samples: 5-10 days 3-7 days <u>8/26/19</u>												
8/15/2019	8:10 - 10:15			10566-M425-11-R2-C1		X			1			110 mL
				10566-M425-11-R2-C2		X			1			215 mL
				10566-M425-11-R2-C3		X			1			213 mL
8/15/2019	8:10 - 10:15			10566-M425-12-R2-C1		X			1			95 mL
				10566-M425-12-R2-C2		X			1			259 mL
				10566-M425-12-R2-C3		X			1			270 mL
8/15/2019	8:10 - 10:15			10566-M425-O-R2-C1		X			1			95 mL
				10566-M425-O-R2-C2		X			1			220 mL

Relinquished by: _____
Date: 8/16/2019 **Time:** 11:30
Received by: _____
Date: 8/19/19 **Time:** 13:45

Relinquished by: _____
Date: 8/16/2019 **Time:** 11:40
Received by: _____
Date: 8/19/19 **Time:** 13:45

Relinquished by: _____
Date: 8/16/2019 **Time:** 14:25
Received by: _____
Date: 8/19/19 **Time:** 13:45

Relinquished by: _____
Date: 8/16/2019 **Time:** 14:25
Received by: _____
Date: 8/19/19 **Time:** 13:45

91420010



PO # 10566
 C.N. Bi-Carb

REPORT TO:
 ALMEGA Environmental & Technical Services
 10602 Walker St.
 Cypress, CA 90630
 (714) 889-4000 Fax (714) 889-7030
 lab@almegaenv.com
 Contact:

INVOICE TO:
 Client: SCAQMD - C
 Location: Inlet & Outlet
 Unit Information:

Almega ENVIRONMENTAL
 CHAIN OF CUSTODY RECORDS

Job #	10566	Unit #	Baghouse	Client	SCAQMD - C	Location: Inlet & Outlet	Type Of Sample			No of Containers	ANALYSIS REQUESTED			Return or Dispose	REMARKS	Turnaround Time
							LIQUID	GAS	SOLID		LAB	MS	TOTAL			
8/15/2019	10:55 - 13:10			Morgan Nguyen	Sample Identification	Lab Sample #										
					10566-M425-11-R3-C1		X		1		X	✓			90ml	
					10566-M425-11-R3-C2		X		1		X	✓			215ml	Combi
					10566-M425-11-R3-C3		X		1		X	✓			230ml	
8/15/2019	10:55 - 13:10				10566-M425-12-R3-C1		X		1		X	✓			95ml	
					10566-M425-12-R3-C2		X		1		X	✓			225ml	Combi
					10566-M425-12-R3-C3		X		1		X	✓			200ml	
8/15/2019	10:55 - 13:10				10566-M425-O-R3-C1		X		1		X	✓			90ml	
					10566-M425-O-R3-C2		X		1		X	✓			220ml	
Relinquished by: [Signature]																
Date:	8/16/2019	Time:	11:30	Date:	8/16/19	Time:	11:40	Date:	8/19/19	Time:	13:45	Date:	8/19/19	Time:	13:45	
Relinquished by: [Signature]																
Date:	8/17/19	Time:	14:25	Date:	8/19/19	Time:	14:25	Date:	8/19/19	Time:	14:25	Date:	8/19/19	Time:	14:25	

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5-1' T-022

APPENDIX E

SCAQMD METHOD 5.1 – PARTICULATE MATTER (PM)

APPENDIX E1

PARTICULATE MATTER (PM) – RESULTS AND CALCULATIONS

Location: Baghouse Outlet

TEST RESULTS

SCAQMD Method 5.1 (Particulate Matter)

Facility: AQMD Facility C

City: ██████████ CA

Source: Baghouse

Location: Outlet

Run Number	1	
Run Date	08/16/19	
Run Start Time	7:40	
Run Stop Time	8:56	
Test Train Parameters		AVERAGE
Volume of Dry Gas Sample, SCF*	39.73	39.73
Flue Gas Parameters		
CO2, Percent By Volume, Dry**	< 0.30	< 0.30
O2, Percent By Volume, Dry**	20.90	20.90
Temperature, Degrees F	87.6	87.6
Moisture, %	1.93	1.93
Air Flow Rate, Wet ACFM	6,705	6,705
Air Flow Rate, Dry SCFM*	6,240	6,240
Total Particulate		
Catch, mg	6.57	6.57
Concentration, Gr/DSCF	0.002552	0.002552
Emission Rate, lb/hr	0.136	0.136

Notes:

* 60 Degrees F and 29.92 Inches of Mercury

** O2/CO2 was sampled in Tedlar bag and analyzed via SCAQMD Method 10.1 by GC.

ISOKINETIC SAMPLING TRAIN RESULTS - METHOD: METHOD 5.1

Client Name	Facility C	Operator	NC
Plant Name	Metal Melting facility	Project #	10566
Sampling Location	Outlet	Standard Temperature, °F	60

USE IN AVERAGE OF RUN SET? 1 or 0 =>	1			SET AVERAGE
Run Number	1			
Run Date	08/16/19			
Run Start Time	hh:mm 7:40			
Run Stop Time	hh:mm 8:56			
Meter Calibration Factor	Y 1.0379			
Pitot Tube Coefficient	C _p 0.84			
Actual Nozzle Diameter	in 0.450			
Sample Volume	ft ³ 39.14			39.14
Total Sampling Time	min 72			72
Average Meter Temperature	°F 72.3			72.3
Average Stack Temperature	°F 87.6			87.6
Barometric Pressure	in Hg 29.90			29.9
Stack/Duct Static Pressure	in H ₂ O -0.02			-0.02
Absolute Stack/Duct Pressure	in Hg 29.9			29.9
Average Delta H	in H ₂ O 0.90			0.90
Absolute Meter Pressure	in Hg 30.0			30.0
Avg Differential Pressure (Delta P)	in H ₂ O 0.024			0.024
Total Water Volume Collected	mL 16.9			16.9
Volume of Water vapor @ STP	SCF 0.783			0.783
Volume Metered @ STP	DSCF 39.735			39.735
Calculated Stack Moisture	% H ₂ O 1.93			1.9
Saturated Stack Moisture	% H ₂ O 4.4			4.4
Reported Stack Moisture Content	% H ₂ O 1.93			1.93
Carbon Dioxide Percentage	% CO ₂ 0.30			0.30
Oxygen Percentage	% O ₂ 20.90			20.90
Carbon Monoxide Percentage	% CO 0.000			0.000
Nitrogen Percentage	% N ₂ 78.8			78.8
Dry Mole Fraction	decimal 0.981			0.981
Dry Gas Molecular Weight	lb/lb-mole 28.88			28.88
Wet Stack Gas Molecular Weight	lb/lb-mole 28.67			28.67
Flue Gas Density	lb/ft ³ 0.0744			0.0744
Stack Cross-Sectional Area	in ² 1809.6			1809.6
Stack Cross-Sectional Area	ft ² 12.57			12.57
Percent of Isokinetic Rate	% ISO 100.7			100.7

Air Flow Rate Results

Average Stack Gas Velocity	ft/sec	8.89		8.89
Actual Stack Flow/Minute	ACFM	6,705		6,705
Dry Standard Stack Flow/Minute	DSCFM	6,240		6,240

	Water 1	Water 2	Empty	SG
Initial	617.0	732.1	650.9	866.4
Final	621.6	734.9	652.2	874.6
H2O gain	4.60	2.80	1.30	8.20
Total H2O	16.9			

Cumul. Percent ISO	Point Percent ISO	Square Root DP (in H ₂ O) ^{1/2}	Local Stack Velocity ft/sec	Cumulative Meter Volume scf	Point Meter Volume scf
98.6	98.6	0.173	9.9	1.844	1.844
100.0	101.2	0.200	11.5	4.030	2.185
100.3	100.8	0.200	11.5	6.208	2.177
100.4	100.7	0.200	11.5	8.381	2.173
100.4	100.6	0.200	11.5	10.550	2.169
100.4	100.5	0.200	11.5	12.719	2.169
100.5	101.1	0.141	8.1	14.258	1.543
100.6	101.4	0.141	8.1	15.803	1.546
100.6	101.3	0.141	8.1	17.345	1.545
100.7	101.4	0.141	8.1	18.889	1.545
100.7	101.4	0.141	8.1	20.432	1.545
100.7	99.7	0.141	8.1	21.948	1.518
100.6	99.6	0.141	8.1	23.466	1.517
100.5	98.8	0.141	8.1	24.971	1.505
100.5	101.3	0.141	8.1	26.513	1.543
100.6	101.1	0.141	8.1	28.052	1.541
100.6	101.1	0.141	8.1	29.592	1.541
100.6	101.2	0.141	8.1	31.133	1.542
100.6	101.2	0.141	8.1	32.674	1.542
100.7	101.1	0.141	8.1	34.214	1.541
100.7	101.2	0.141	8.1	35.753	1.540
100.7	101.1	0.141	8.1	37.292	1.539
100.7	101.1	0.141	8.1	38.830	1.539
100.7	99.8	0.141	8.1	40.346	1.517
100.7	99.8	Final Values		40.346	1.517
		0.155	8.9		

EXAMPLE CALCULATIONS, RUN 1

ABSOLUTE PRESSURE, INCHES OF MERCURY

$$\begin{aligned} P_s &= P_{bar} + P_g/13.6 \\ &= 29.90 + -0.02/13.6 \\ &= 29.90 \end{aligned}$$

VOLUME OF WATER VAPOR, STANDARD CUBIC FEET

$$\begin{aligned} V_{wstd} &= 0.002667 * [(T_{std} + 460) / P_{std}] * V_{lc} \\ &= 0.002667 * [(60 + 460) / 29.92 * 16.9 \\ &= 0.783 \end{aligned}$$

SAMPLED VOLUME OF SOURCE GAS, DRY STANDARD CUBIC FEET

$$\begin{aligned} V_{mstd} &= [(T_{std} + 460)/P_{std}] * Y * V_m * (P_{bar} + \Delta H/13.6) / (460 + t_m) \\ &= [(60 + 460)/ 29.92] * 1.0379 * 39.144 * (29.90 + 0.900/13.6) / (460 + 72) \\ &= 39.735 \end{aligned}$$

MOISTURE CONTENT, PERCENT BY VOLUME

$$\begin{aligned} \%H_2O &= V_{wstd} / (V_{wstd} + V_{mstd}) \\ &= 0.783 / (0.783 + 39.735) \\ &= 1.93 \end{aligned}$$

DRY MOLE FRACTION, LB-MOLE/LB-MOLE

$$\begin{aligned} M_{fd} &= 1 - \%H_2O/100 \\ &= 1 - 1.93/100 \\ &= 0.981 \end{aligned}$$

DRY MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_d &= 44*(\%CO_2/100) + 32*(\%O_2/100) + 28*\{[100-(\%CO_2+\%O_2)]/100\} \\ &= 44*(0.3/100) + 32*(20.9/100) + 28*\{[100-(0.3+20.9)]/100\} \\ &= 28.88 \end{aligned}$$

WET MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_s &= M_d * M_{fd} + 18.0 * \%H_2O/100 \\ &= 28.88 * 0.981 + 18.0 * 1.93/100 \\ &= 28.67 \end{aligned}$$

FUEL FACTOR

$$\begin{aligned} F_o &= (20.9 - \%O_2) / \%CO_2 \\ &= (20.9 - 20.9) / 0.3 \\ &= 0.000 \end{aligned}$$

ISOKINETIC SAMPLING RATE, PERCENT

$$\begin{aligned} \%I &= P_{std}/(T_{std} + 460) * (100/60) * V_{mstd} * (t_s + 460) / [P_s * v_s * M_{fd} * \theta * (\pi * D_{ia} * D_{ia} / 576)] \\ &= 29.92 / (60 + 460) * (100/60) * 39.735 * (88 + 460) / [29.90 * 8.89 * 0.981 * 72.00 * (\pi * 0.450 * 0.450 / 576)] \\ &= 100.7 \end{aligned}$$

VELOCITY, FEET PER SECOND

$$\begin{aligned} v_s &= 85.49 * C_p * \text{SQRT}[\Delta p * (460 + t_s) / P_s / M_s] \\ &= 85.49 * 0.84 * \text{SQRT}[0.0240 * (460 + 88) / 29.90 / 28.67] \\ &= 8.89 \end{aligned}$$

VOLUMETRIC FLOW RATE, ACTUAL CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{aw} &= (60/144) * v_s * A \\ &= (60/144) * 8.89 * 1810 \\ &= 6705 \end{aligned}$$

VOLUMETRIC FLOW RATE, DRY STANDARD CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{sd} &= (60/144) * M_{fd} * v_s * A * (T_{std} + 460) / (t_s + 460) * (P_s / P_{std}) \\ &= (60/144) * 0.981 * 8.89 * 1810 * (60 + 460) / (88 + 460) * (29.90 / 29.92) \\ &= 6240 \end{aligned}$$

EXAMPLE CALCULATIONS, RUN 1

TOTAL PARTICULATE CONCENTRATION, GRAINS PER DRY STANDARD CUBIC FOOT

$$\begin{aligned} \text{gr/DSCF} &= (\text{Catch/Conversion}) * 7,000 / 453.592 / \text{Vmstd} \\ &= (6.57/1000) * 7,000 / 453.592 / 39.735 \\ &= 0.00255 \end{aligned}$$

TOTAL PARTICULATE EMISSION RATE, POUNDS PER HOUR

$$\begin{aligned} \text{lb/hr} &= 60 * (\text{Catch/Conversion}) * \text{Qsd} / 453.592 / \text{Vmstd} \\ &= 60 * (6.57/1000) * 6240 / 453.592 / 39.735 \\ &= 0.136 \end{aligned}$$

Location: Inlet 1 (inside)

TEST RESULTS

SCAQMD Method 5.1 (Particulate Matter)

Facility: AQMD Facility C

City: ██████████ CA

Source: Baghouse

Location: Inlet 1

Run Number	1	
Run Date	08/16/19	
Run Start Time	7:40	
Run Stop Time	8:56	
Test Train Parameters		AVERAGE
Volume of Dry Gas Sample, SCF*	53.50	53.50
Flue Gas Parameters		
CO2, Percent By Volume, Dry**	< 0.30	< 0.30
O2, Percent By Volume, Dry**	20.80	20.80
Temperature, Degrees F	100.8	100.8
Moisture, %	1.80	1.80
Air Flow Rate, Wet ACFM	1,147	1,147
Air Flow Rate, Dry SCFM*	1,040	1,040
Total Particulate		
Catch, mg	105.57	105.57
Concentration, Gr/DSCF	0.0305	0.0305
Emission Rate, lb/hr	0.271	0.271

Notes:

* 60 Degrees F and 29.92 Inches of Mercury

** O2/CO2 was sampled in Tedlar bag and analyzed via SCAQMD Method 10.1 by GC.

ISOKINETIC SAMPLING TRAIN RESULTS - METHOD: METHOD 5.1

Client Name	Facility C	Operator	DJ
Plant Name	Metal Melting facility	Project #	10566
Sampling Location	Inlet 1	Standard Temperature, °F	60

USE IN AVERAGE OF RUN SET? 1 or 0 =>	1			SET AVERAGE
Run Number	1			
Run Date	08/16/19			
Run Start Time	hh:mm 7:40			
Run Stop Time	hh:mm 8:56			
Meter Calibration Factor	Y 1.0395			
Pitot Tube Coefficient	C _p 0.84			
Actual Nozzle Diameter	in 0.348			
Sample Volume	ft ³ 54.02			54.02
Total Sampling Time	min 72			72
Average Meter Temperature	°F 87.9			87.9
Average Stack Temperature	°F 100.8			100.8
Barometric Pressure	in Hg 29.90			29.9
Stack/Duct Static Pressure	in H ₂ O -1.50			-1.50
Absolute Stack/Duct Pressure	in Hg 29.8			29.8
Average Delta H	in H ₂ O 1.94			1.94
Absolute Meter Pressure	in Hg 30.0			30.0
Avg Differential Pressure (Delta P)	in H ₂ O 0.127			0.127
Total Water Volume Collected	mL 21.1			21.1
Volume of Water vapor @ STP	SCF 0.978			0.978
Volume Metered @ STP	DSCF 53.495			53.495
Calculated Stack Moisture	% H ₂ O 1.80			1.8
Saturated Stack Moisture	% H ₂ O 6.6			6.6
Reported Stack Moisture Content	% H ₂ O 1.80			1.80
Carbon Dioxide Percentage	% CO ₂ 0.30			0.30
Oxygen Percentage	% O ₂ 20.80			20.80
Carbon Monoxide Percentage	% CO 0.000			0.000
Nitrogen Percentage	% N ₂ 78.9			78.9
Dry Mole Fraction	decimal 0.982			0.982
Dry Gas Molecular Weight	lb/lb-mole 28.88			28.88
Wet Stack Gas Molecular Weight	lb/lb-mole 28.68			28.68
Flue Gas Density	lb/ft ³ 0.0744			0.0744
Stack Cross-Sectional Area	in ² 132.7			132.7
Stack Cross-Sectional Area	ft ² 0.92			0.92
Percent of Isokinetic Rate	% ISO 99.7			99.7

Air Flow Rate Results

Average Stack Gas Velocity	ft/sec	20.74		20.74
Actual Stack Flow/Minute	ACFM	1,147		1,147
Dry Standard Stack Flow/Minute	DSCFM	1,040		1,040

EXAMPLE CALCULATIONS, RUN 1

ABSOLUTE PRESSURE, INCHES OF MERCURY

$$\begin{aligned} P_s &= P_{bar} + P_g/13.6 \\ &= 29.90 + -1.50/13.6 \\ &= 29.79 \end{aligned}$$

VOLUME OF WATER VAPOR, STANDARD CUBIC FEET

$$\begin{aligned} V_{wstd} &= 0.002667 * [(T_{std} + 460) / P_{std}] * V_{lc} \\ &= 0.002667 * [(60 + 460) / 29.92] * 21.1 \\ &= 0.978 \end{aligned}$$

SAMPLED VOLUME OF SOURCE GAS, DRY STANDARD CUBIC FEET

$$\begin{aligned} V_{mstd} &= [(T_{std} + 460)/P_{std}] * Y * V_m * (P_{bar} + \Delta H/13.6) / (460 + t_m) \\ &= [(60 + 460)/29.92] * 1.0395 * 54.021 * (29.90 + 1.943/13.6) / (460 + 88) \\ &= 53.495 \end{aligned}$$

MOISTURE CONTENT, PERCENT BY VOLUME

$$\begin{aligned} \%H_2O &= V_{wstd} / (V_{wstd} + V_{mstd}) \\ &= 0.978 / (0.978 + 53.495) \\ &= 1.80 \end{aligned}$$

DRY MOLE FRACTION, LB-MOLE/LB-MOLE

$$\begin{aligned} M_{fd} &= 1 - \%H_2O/100 \\ &= 1 - 1.80/100 \\ &= 0.982 \end{aligned}$$

DRY MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_d &= 44 * (\%CO_2/100) + 32 * (\%O_2/100) + 28 * \{[100 - (\%CO_2 + \%O_2)]/100\} \\ &= 44 * (0.3/100) + 32 * (20.8/100) + 28 * \{[100 - (0.3 + 20.8)]/100\} \\ &= 28.88 \end{aligned}$$

WET MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_s &= M_d * M_{fd} + 18.0 * \%H_2O/100 \\ &= 28.88 * 0.982 + 18.0 * 1.80/100 \\ &= 28.68 \end{aligned}$$

FUEL FACTOR

$$\begin{aligned} F_o &= (20.9 - \%O_2) / \%CO_2 \\ &= (20.9 - 20.8) / 0.3 \\ &= 0.333 \end{aligned}$$

ISOKINETIC SAMPLING RATE, PERCENT

$$\begin{aligned} \%I &= P_{std}/(T_{std} + 460) * (100/60) * V_{mstd} * (t_s + 460) / [P_s * v_s * M_{fd} * \theta * (\pi * D_{ia} * D_{ia} / 576)] \\ &= 29.92 / (60 + 460) * (100/60) * 53.495 * (101 + 460) / [29.79 * 20.74 * 0.982 * 72.00 * (\pi * 0.348 * 0.348 / 576)] \\ &= 99.7 \end{aligned}$$

VELOCITY, FEET PER SECOND

$$\begin{aligned} v_s &= 85.49 * C_p * \text{SQRT}[\Delta p * (460 + t_s) / P_s / M_s] \\ &= 85.49 * 0.84 * \text{SQRT}[0.1271 * (460 + 101) / 29.79 / 28.68] \\ &= 20.74 \end{aligned}$$

VOLUMETRIC FLOW RATE, ACTUAL CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{aw} &= (60/144) * v_s * A \\ &= (60/144) * 20.74 * 133 \\ &= 1147 \end{aligned}$$

VOLUMETRIC FLOW RATE, DRY STANDARD CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{sd} &= (60/144) * M_{fd} * v_s * A * (T_{std} + 460) / (t_s + 460) * (P_s / P_{std}) \\ &= (60/144) * 0.982 * 20.74 * 133 * (60 + 460) / (101 + 460) * (29.79 / 29.92) \\ &= 1040 \end{aligned}$$

EXAMPLE CALCULATIONS, RUN 1

TOTAL PARTICULATE CONCENTRATION, GRAINS PER DRY STANDARD CUBIC FOOT

$$\begin{aligned} \text{gr/DSCF} &= (\text{Catch/Conversion}) * 7,000 / 453.592 / \text{Vmstd} \\ &= (105.57/1000) * 7,000 / 453.592 / 53.495 \\ &= 0.03045 \end{aligned}$$

TOTAL PARTICULATE EMISSION RATE, POUNDS PER HOUR

$$\begin{aligned} \text{lb/hr} &= 60 * (\text{Catch/Conversion}) * \text{Qsd} / 453.592 / \text{Vmstd} \\ &= 60 * (105.57/1000) * 1040 / 453.592 / 53.495 \\ &= 0.271 \end{aligned}$$

Location: Inlet 2 (Upstream to Baghouse)

TEST RESULTS

SCAQMD Method 5.1 (Particulate Matter)

Facility: AQMD Facility C

City: ██████████ CA

Source: Baghouse

Location: Inlet 2

Run Number	1	
Run Date	08/16/19	
Run Start Time	7:40	
Run Stop Time	8:56	
Test Train Parameters		AVERAGE
Volume of Dry Gas Sample, SCF*	55.51	55.51
Flue Gas Parameters		
CO2, Percent By Volume, Dry**	< 0.30	< 0.30
O2, Percent By Volume, Dry**	20.80	20.80
Temperature, Degrees F	93.2	93.2
Moisture, %	2.26	2.26
Air Flow Rate, Wet ACFM	6,412	6,412
Air Flow Rate, Dry SCFM*	5,825	5,825
Total Particulate		
Catch, mg	45.22	45.22
Concentration, Gr/DSCF	0.0126	0.0126
Emission Rate, lb/hr	0.628	0.628

Notes:

* 60 Degrees F and 29.92 Inches of Mercury

** O2/CO2 was sampled in Tedlar bag and analyzed via SCAQMD Method 10.1 by GC.

ISOKINETIC SAMPLING TRAIN RESULTS - METHOD: METHOD 5.1

Client Name	Facility C	Operator	WB
Plant Name	Metal Melting facility	Project #	10566
Sampling Location	Inlet 2	Standard Temperature, °F	60

USE IN AVERAGE OF RUN SET? 1 or 0 =>	1			SET AVERAGE
Run Number	1			
Run Date	08/16/19			
Run Start Time	hh:mm 7:40			
Run Stop Time	hh:mm 8:56			
Meter Calibration Factor	Y 1.0376			
Pitot Tube Coefficient	C _p 0.84			
Actual Nozzle Diameter	in 0.181			
Sample Volume	ft ³ 54.82			54.82
Total Sampling Time	min 72			72
Average Meter Temperature	°F 75.3			75.3
Average Stack Temperature	°F 93.2			93.2
Barometric Pressure	in Hg 29.90			29.9
Stack/Duct Static Pressure	in H ₂ O -4.30			-4.30
Absolute Stack/Duct Pressure	in Hg 29.6			29.6
Average Delta H	in H ₂ O 2.26			2.26
Absolute Meter Pressure	in Hg 30.1			30.1
Avg Differential Pressure (Delta P)	in H ₂ O 1.740			1.740
Total Water Volume Collected	mL 27.7			27.7
Volume of Water vapor @ STP	SCF 1.284			1.284
Volume Metered @ STP	DSCF 55.513			55.513
Calculated Stack Moisture	% H ₂ O 2.26			2.3
Saturated Stack Moisture	% H ₂ O 5.3			5.3
Reported Stack Moisture Content	% H ₂ O 2.26			2.26
Carbon Dioxide Percentage	% CO ₂ 0.30			0.30
Oxygen Percentage	% O ₂ 20.80			20.80
Carbon Monoxide Percentage	% CO 0.000			0.000
Nitrogen Percentage	% N ₂ 78.9			78.9
Dry Mole Fraction	decimal 0.977			0.977
Dry Gas Molecular Weight	lb/lb-mole 28.88			28.88
Wet Stack Gas Molecular Weight	lb/lb-mole 28.63			28.63
Flue Gas Density	lb/ft ³ 0.0743			0.0743
Stack Cross-Sectional Area	in ² 201.1			201.1
Stack Cross-Sectional Area	ft ² 1.40			1.40
Percent of Isokinetic Rate	% ISO 103.5			103.5

Air Flow Rate Results

Average Stack Gas Velocity	ft/sec	76.54		76.54
Actual Stack Flow/Minute	ACFM	6,412		6,412
Dry Standard Stack Flow/Minute	DSCFM	5,825		5,825

	Water 1	Water 2	Empty	SG
Initial	757.4	727.8	670.2	741.9
Final	776.3	732.2	671.9	744.6
H2O gain	18.9	4.40	1.70	2.70
Total H2O	27.7			

Cumul. Percent ISO	Point Percent ISO	Square Root DP (in H ₂ O) ^{1/2}	Local Stack Velocity ft/sec	Cumulative Meter Volume scf	Point Meter Volume scf
105.4	105.4	1.643	95.7	2.968	2.968
105.4	105.5	1.673	97.4	5.996	3.028
105.9	106.7	1.643	95.5	9.007	3.011
105.4	103.8	1.628	94.7	11.906	2.900
105.3	105.0	1.378	80.6	14.374	2.472
105.7	108.3	1.396	81.2	16.969	2.598
105.2	101.4	1.304	75.8	19.234	2.271
105.2	105.9	1.140	66.5	21.294	2.068
104.8	100.9	1.049	61.3	23.090	1.807
104.6	102.3	1.049	60.5	24.940	1.858
104.5	105.7	1.000	57.6	26.765	1.833
104.4	103.1	0.990	56.9	28.529	1.772
104.1	100.8	1.378	80.1	30.916	2.387
104.0	103.3	1.414	82.3	33.424	2.507
104.2	106.0	1.517	88.5	36.178	2.751
104.1	103.4	1.517	88.4	38.864	2.684
104.1	102.9	1.449	84.4	41.420	2.555
104.0	102.6	1.578	92.2	44.191	2.767
103.9	101.9	1.378	80.4	46.596	2.406
103.8	102.1	1.095	63.7	48.507	1.919
103.6	100.9	1.265	73.4	50.700	2.196
103.7	105.2	1.072	61.9	52.643	1.949
103.6	103.1	1.049	60.6	54.504	1.868
103.6	103.0	1.049	60.5	56.367	1.870
103.6	103.0	Final Values		56.367	1.870
		1.319	76.7		

EXAMPLE CALCULATIONS, RUN 1

ABSOLUTE PRESSURE, INCHES OF MERCURY

$$\begin{aligned} P_s &= P_{bar} + P_g/13.6 \\ &= 29.90 + -4.30/13.6 \\ &= 29.58 \end{aligned}$$

VOLUME OF WATER VAPOR, STANDARD CUBIC FEET

$$\begin{aligned} V_{wstd} &= 0.002667 * [(T_{std} + 460) / P_{std}] * V_{lc} \\ &= 0.002667 * [(60 + 460) / 29.92 * 27.7 \\ &= 1.284 \end{aligned}$$

SAMPLED VOLUME OF SOURCE GAS, DRY STANDARD CUBIC FEET

$$\begin{aligned} V_{mstd} &= [(T_{std} + 460)/P_{std}] * Y * V_m * (P_{bar} + \Delta H/13.6) / (460 + t_m) \\ &= [(60 + 460)/ 29.92] * 1.0376 * 54.824 * (29.90 + 2.263/13.6) / (460 + 75) \\ &= 55.513 \end{aligned}$$

MOISTURE CONTENT, PERCENT BY VOLUME

$$\begin{aligned} \%H_2O &= V_{wstd} / (V_{wstd} + V_{mstd}) \\ &= 1.284 / (1.284 + 55.513) \\ &= 2.26 \end{aligned}$$

DRY MOLE FRACTION, LB-MOLE/LB-MOLE

$$\begin{aligned} M_{fd} &= 1 - \%H_2O/100 \\ &= 1 - 2.26/100 \\ &= 0.977 \end{aligned}$$

DRY MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_d &= 44*(\%CO_2/100) + 32*(\%O_2/100) + 28*\{[100-(\%CO_2+\%O_2)]/100\} \\ &= 44*(0.3/100) + 32*(20.8/100) + 28*\{[100-(0.3+20.8)]/100\} \\ &= 28.88 \end{aligned}$$

WET MOLECULAR WEIGHT, LB/LB-MOLE

$$\begin{aligned} M_s &= M_d * M_{fd} + 18.0 * \%H_2O/100 \\ &= 28.88 * 0.977 + 18.0 * 2.26/100 \\ &= 28.63 \end{aligned}$$

FUEL FACTOR

$$\begin{aligned} F_o &= (20.9 - \%O_2) / \%CO_2 \\ &= (20.9 - 20.8) / 0.3 \\ &= 0.333 \end{aligned}$$

ISOKINETIC SAMPLING RATE, PERCENT

$$\begin{aligned} \%I &= P_{std}/(T_{std} + 460) * (100/60) * V_{mstd} * (t_s + 460) / [P_s * v_s * M_{fd} * \Theta * (\pi * D_{ia} * D_{ia} / 576)] \\ &= 29.92 / (60 + 460) * (100/60) * 55.513 * (93 + 460) / [29.58 * 76.54 * 0.977 * 72.00 * (\pi * 0.181 * 0.181 / 576)] \\ &= 103.5 \end{aligned}$$

VELOCITY, FEET PER SECOND

$$\begin{aligned} v_s &= 85.49 * C_p * \text{SQRT}[\Delta p * (460 + t_s) / P_s / M_s] \\ &= 85.49 * 0.84 * \text{SQRT}[1.7397 * (460 + 93) / 29.58 / 28.63] \\ &= 76.54 \end{aligned}$$

VOLUMETRIC FLOW RATE, ACTUAL CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{aw} &= (60/144) * v_s * A \\ &= (60/144) * 76.54 * 201 \\ &= 6412 \end{aligned}$$

VOLUMETRIC FLOW RATE, DRY STANDARD CUBIC FEET PER MINUTE

$$\begin{aligned} Q_{sd} &= (60/144) * M_{fd} * v_s * A * (T_{std} + 460) / (t_s + 460) * (P_s / P_{std}) \\ &= (60/144) * 0.977 * 76.54 * 201 * (60 + 460) / (93 + 460) * (29.58 / 29.92) \\ &= 5825 \end{aligned}$$

EXAMPLE CALCULATIONS, RUN 1

TOTAL PARTICULATE CONCENTRATION, GRAINS PER DRY STANDARD CUBIC FOOT

$$\begin{aligned} \text{gr/DSCF} &= (\text{Catch/Conversion}) * 7,000 / 453.592 / \text{Vmstd} \\ &= (45.22/1000) * 7,000 / 453.592 / 55.513 \\ &= 0.01257 \end{aligned}$$

TOTAL PARTICULATE EMISSION RATE, POUNDS PER HOUR

$$\begin{aligned} \text{lb/hr} &= 60 * (\text{Catch/Conversion}) * \text{Qsd} / 453.592 / \text{Vmstd} \\ &= 60 * (45.22/1000) * 5825 / 453.592 / 55.513 \\ &= 0.628 \end{aligned}$$

APPENDIX E2
PARTICULATE MATTER (PM) – FIELD DATA

Location: Baghouse Outlet

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ████████ CA
 SAMPLING LOCATION: Outlet
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 54.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 6.00 inches
 DEPTH OF STACK OR DUCT, D: 48.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

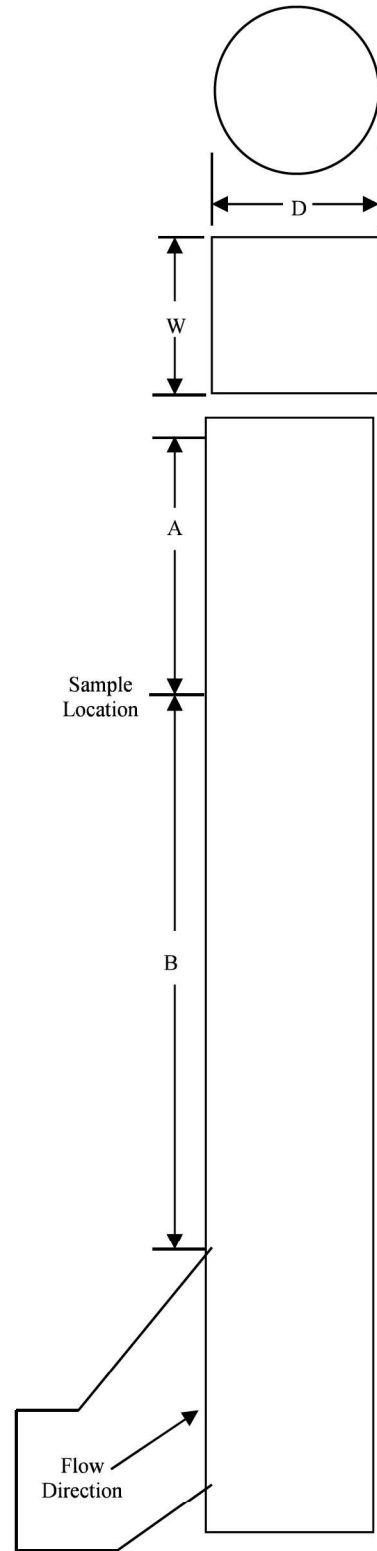
EQUIVALENT DIAMETER
 $De = 2*(DEPTH)*(WIDTH)/(DEPTH+WIDTH) =$ 48.00 inches

STACK/DUCT AREA = 12.57 sq.feet 1809.6 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	<u>B</u>	<u>A</u>
# OF INCHES	126.00	50.00
# OF DIAMETERS	2.63	1.04

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	1.01	7
2	6.7	3.22	9 1/4
3	11.8	5.66	11 5/8
4	17.7	8.50	14 1/2
5	25.0	12.00	18
6	35.6	17.09	23 1/8
7	64.4	30.91	36 7/8
8	75.0	36.00	42
9	82.3	39.50	45 1/2
10	88.2	42.34	48 3/8
11	93.3	44.78	50 3/4
12	97.9	46.99	53



DRAWING NOT TO SCALE

ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW

Run #:	1	Pilot ID:	3	Impinger #	Initial	Final	Net	Pilot Leak Check		
Date:	8-11-19	Pilot Coeff.:	0.84	1	617.0	621.6		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMD 1	Meter Box #:	A-3	2	732.1	731.9		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Outlet	Meter @ Dh:	1.583	3	670.9	652.2		Meter Box Leak Check		
Operator:	NC	Meter Y:	1.0229	4	966.4	874.6		Rate	7HG	
Stack Dia:	48.0" I	TC #:	73	5				Initial:	0.00	12
Amb. Press:	29.9	Start Time:	0740	H2O Gain =				Final:	0.00	12
Static Press:	-0.02	Stop Time:	0856	Filter:		000491				

Transverse Points	Time (Minutes)	Delta P (7HG)	Stack Temp. (F)	Set data H (7HG)	Meter Volume (scf)	Mt. Inlet Temp. (F)	Mt. Outlet Temp. (F)	Oven Temp. (F)	Probe Temp. (F)	Impinger Temp. (F)	Pump Vac. (7HG)	TE Cooler Temp. (F)	Cyclonic Flow (7HG)	
76A	12	0	0.03	85	1.09	839.136	65	65	N/A	N/A	51	3	N/A	N/A
	11	3	0.04	86	1.46	840.9	71	65			50	2		
	10	6	0.04	86	1.46	843.0	75	65			50			
	9	9	0.04	86	1.47	845.1	76	66			51			
	8	12	0.04	87	1.47	847.2	77	67			52			
	7	15	0.04	86	1.47	849.3	77	67			53			
	6	18	0.02	86	0.74	851.4	78	68			53			
	5	21	0.02	87	0.73	852.9	76	68			53			
	4	24	0.02	87	0.73	854.4	77	68			53			
	3	27	0.02	88	0.73	855.9	77	68			53			
	2	30	0.02	88	0.73	857.4	77	68			53			
	1	33	0.02	89	0.73	858.9	77	69	↓	↓	53	↓	↓	↓
		36				869.375								
816	12	0	0.02	88	0.73	860.375	70	69	N/A	N/A	53	2	N/A	N/A
	11	3	0.02	88	0.73	861.84	75	69			54			
	10	6	0.02	88	0.73	863.3	77	69			54			
	9	9	0.02	88	0.74	864.8	78	70			55			
	8	12	0.02	88	0.74	866.3	78	70			54			
	7	15	0.02	88	0.74	867.8	77	70			54			
	6	18	0.02	88	0.73	869.3	77	70			54			
	5	21	0.02	88	0.74	870.8	77	71			54			
	4	24	0.02	89	0.73	872.3	77	71			54			
	3	27	0.02	89	0.73	873.8	78	71			54			
	2	30	0.02	89	0.73	875.3	78	71			55			
	1	33	0.02	90	0.73	876.8	79	71	↓	↓		↓	↓	↓
		36				878.280								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 80

Estimated Stack Temp: 90

Estimated Delta P: 0.04

Estimated Moisture Content: 2

Estimated O2: 20.8

Estimated CO2: 0.05

Equipment Evaluation, OK? Y or N

Ambient Temp.: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

	1	2	3	4
DGM Initial:				
Vacuum:				
Leak Rate:				
DGM Final:				

Nozzle Information

Nozzle ID: _____

Nozzle Dia: 0.450

Location: Inlet 1 (inside)

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ██████████, CA
 SAMPLING LOCATION Inlet 1
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

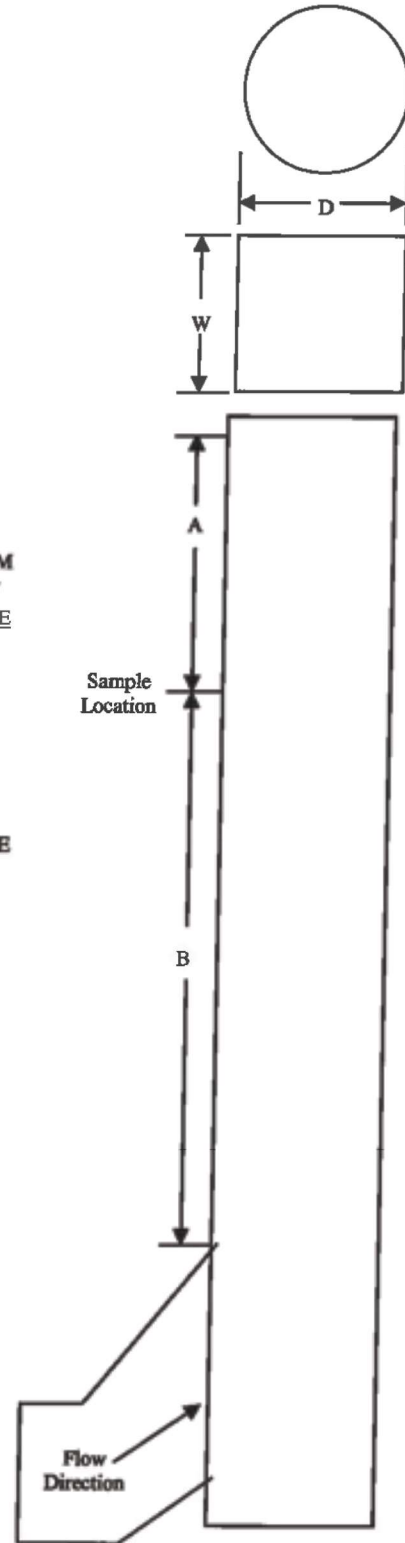
DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 13.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 0.0 inches
 DEPTH OF STACK OR DUCT, D: 13.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

EQUIVALENT DIAMETER
 $De = 2*(DEPTH)*(WIDTH)/(DEPTH+WIDTH) = 13.00$ inches
 STACK/DUCT AREA = 0.92 sq.feet 132.7 sq.inches

	DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
		B	A
	# OF INCHES	>26.0	>6.5
	# OF DIAMETERS	>2.00	>0.50

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	0.50	0 1/2
2	6.7	0.87	0 7/8
3	11.8	1.53	1 1/2
4	17.7	2.30	2 1/4
5	25.0	3.25	3 1/4
6	35.6	4.63	4 5/8
7	64.4	8.37	8 3/8
8	75.0	9.75	9 3/4
9	82.3	10.70	10 3/4
10	88.2	11.47	11 1/2
11	93.3	12.13	12 1/8
12	97.9	12.50	12 1/2



DRAWING NOT TO SCALE

Run #:	1	Pilot ID:	85	Impinger #:	Initial	Final	Net	Pilot Leak Check		
Date:	8-16-11	Pilot Coeff.:	0.84	1	650.7	653.7		Initial:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Client:	SCAQMD C	Meter Box #:	A-8	2	354.0	356.8		Final:	<input checked="" type="checkbox"/>	<input checked="" type="checkbox"/>
Unit:	Booth 150 - TN7	Meter @ Dh:	1834	3	639.2	640.6		Meter Box Leak Check		
Operator:	DJ	Meter Y:	10395	4	828.7	839.8		Rate	7HG	
Stack Dia:	13.0"	TC #:	85	5				Initial:	.000	18"
Amb. Press:	29.9	Start Time:	7:46	H2O Gain =			009192	Final:	.800	18"
Static Press:	-1.5	Stop Time:	8:56	Filter:						

Traverse Point	Time (Minutes)	Delta P (7100)	Stack Temp (F)	Std Delta H (7100)	Meter Volume (scf)	Mt. Inlet Temp (F)	Mt. Outlet Temp (F)	Oven Temp (F)	Probe Temp (F)	Impinger Temp (F)	Pump Vac (7103)	TE Cooler Temp (F)	Cyclonic Flow (7100)
0	0				791.707								
1	3	.16	115	2.35	794.173	82	82	N/A	N/A	54	3.5	N/A	
2	6	.15	114	2.21	796.568	83	83	/	/	54	3.5	/	
3	9	.15	114	2.21	798.964	83	83	/	/	54	3.5	/	
4	12	.13	113	1.92	801.203	84	84	/	/	54	3.0	/	
5	15	.12	109	1.79	803.368	85	85	/	/	54	3.0	/	
6	18	.10	108	1.50	805.343	86	86	/	/	54	3	/	
7	21	.11	105	1.66	807.429	86	86	/	/	54	3	/	
8	24	.13	104	1.96	809.692	87	87	/	/	54	3	/	
9	27	.14	107	2.11	812.044	88	88	/	/	54	3.5	/	
10	30	.15	103	2.27	814.426	88	88	/	/	54	3.5	/	
11	33	.14	101	2.13	816.851	89	89	/	/	54	3.5	/	
12	36	.11	94	1.70	818.964	89	89	/	/	54	3	/	
0	0				818.964								
1	3	.15	103	2.27	821.403	88	88	N/A	N/A	54	3.5	N/A	
2	6	.16	105	2.42	823.928	89	89	/	/	54	3.5	/	
3	9	.14	105	2.12	826.283	89	89	/	/	54	3.5	/	
4	12	.15	98	2.30	828.738	89	89	/	/	54	3.5	/	
5	15	.13	96	2.00	831.026	89	89	/	/	54	3.5	/	
6	18	.11	95	1.70	833.142	90	90	/	/	54	3	/	
7	21	.10	95	1.54	835.156	90	90	/	/	54	3	/	
8	24	.12	90	1.87	837.379	90	90	/	/	54	3	/	
9	27	.11	89	1.72	839.503	91	91	/	/	54	3	/	
10	30	.10	84	1.58	841.548	91	91	/	/	54	3	/	
11	33	.11	85	1.73	843.684	91	91	/	/	54	3	/	
12	36	.10	88	1.57	845.788	92	92	/	/	54	3	/	

END @ 8:16
st @ 8:20

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: 100

Estimated Stack Temp: 130

Estimated Delta P: _____

Estimated Moisture Content: 2.40%

Estimated O2: 20.8

Estimated CO2: 0.05

Equipment Evaluation, OK? Y or N

Ambient Temp.: 64

TC Check:

Pilot Check:

Tedar Bag: N/A

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

1	2	3	4

Nozzle Information

DGM Initial: _____

Vacuum: _____

Leak Rate: _____

DGM Final: _____

Nozzle ID: # 85

Nozzle Dia: .348

Location: Inlet 2 (Upstream to Baghouse)

**SAMPLING AND VELOCITY TRAVERSE POINT DETERMINATION
SCAQMD METHOD 1.1**

CLIENT: AQMD Facility C
 PLANT NAME: Metal Melting Facility
 CITY, STATE: ██████████ CA
 SAMPLING LOCATION Inlet 2
 TYPE OF TESTING: Metals/Particulate

NO. OF PORTS AVAILABLE: 2
 NO. OF PORTS TO BE USED: 2
 PORT INSIDE DIAMETER: 3 inches

DISTANCE FROM FAR WALL TO OUTSIDE OF PORT: 22.00 inches
 NIPPLE LENGTH AND/OR WALL THICKNESS: 6.00 inches
 DEPTH OF STACK OR DUCT, D: 16.00 inches
 STACK OR DUCT WIDTH (IF RECTANGULAR), W: #N/A inches

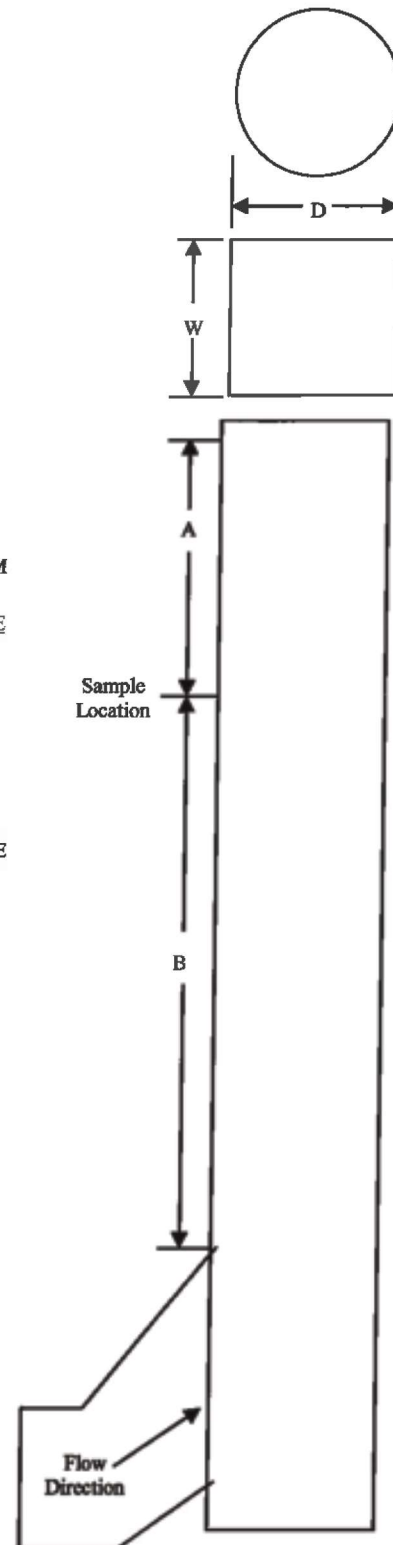
EQUIVALENT DIAMETER
 $De = 2*(DEPTH)*(WIDTH)/(DEPTH+WIDTH) =$ 16.00 inches

STACK/DUCT AREA = 1.40 sq.feet 201.1 sq.inches

DISTANCE OF TEST PORT LOCATION:	UPSTREAM FROM FLOW DISTURBANCE	DOWNSTREAM FROM FLOW DISTURBANCE
	B	A
# OF INCHES	42.00	196.00
# OF DIAMETERS	2.63	12.25

MINIMUM NUMBER OF TRAVERSE POINTS: 24

POINT NO.	% OF DUCT DEPTH	DISTANCE FROM INSIDE WALL (in.)	DISTANCE FROM OUTSIDE OF PORT (in.)
1	2.1	0.50	6 1/2
2	6.7	1.07	7 1/8
3	11.8	1.89	7 7/8
4	17.7	2.83	8 7/8
5	25.0	4.00	10
6	35.6	5.70	11 3/4
7	64.4	10.30	16 1/4
8	75.0	12.00	18
9	82.3	13.17	19 1/8
10	88.2	14.11	20 1/8
11	93.3	14.93	20 7/8
12	97.9	15.50	21 1/2



DRAWING NOT TO SCALE



ISOKINETIC DATA FORM, TE COOLER & CYCLONIC FLOW



Run #: 2	Pilot ID: 28	Impinger #	Initial	Final	Net	Pilot Leak Check
Date: 8-16-19	Pilot Coeff.: 0.84	1	757.4	776.3		Initial: <input checked="" type="checkbox"/>
Client: SCARMDL	Meter Box #: A-6	2	727.8	752.7		Final: <input checked="" type="checkbox"/>
Unit: TALETT	Meter @ Dh: 1.75	3	670.2	671.9		
Operator: WJB	Meter Y: 1.037	4	741.9	744.6		
Stack Dia: 14.0"	TC #: 28	5				
Amb. Press: 29.9	Start Time: 0740	H2O Gain = 009499			Meter Box Leak Check	
Static Press: -4.5	Stop Time: 0858	Filter: 009499			Rate	"HG
					Initial: 19	0.001
					Final: 10	0.000

Traverse Points	Time (Minute)	Delta P (H2O)	Stack Temp (F)	Set delta H (H2O)	Meter Volume (scf)	Mt. Inlet Temp (F)	Mt. Outlet Temp (F)	Oven Temp (F)	Probe Temp (F)	Impinger Temp (F)	Pump Vols (MG)	TE Cooler Temp (F)	Cyclonic Flow (H2O)
12	0	2.70	96	3.40	572.522	64	64	NA	NA	52	4		
11	3	2.80	95	3.55	575.34	65	65			52	4		
10	6	2.70	94	3.40	578.22	66	66			53	4		
9	9	2.65	95	3.35	581.09	69	69			55	4		
8	12	1.90	100	2.40	583.87	70	70			54	3		
7	15	1.95	94	2.45	586.25	72	72			55	3		
6	18	1.70	94	2.15	588.76	73	73			57	3		
5	21	1.30	97	1.65	590.96	74	74			59	3		
4	24	1.10	100	1.40	592.97	75	75			58	3		
3	27	1.10	85	1.40	594.73	75	75			56	3		
2	30	1.00	83	1.25	596.54	76	76			56	2		
1	33	0.98	82	1.25	598.33	76	76			54	2		
12	36	1.90	93	2.40	600.06	75	75			56	3		
11	39	2.00	95	2.55	602.38	76	76			52	3		
10	42	2.30	98	2.90	604.82	77	77			51	3		
9	45	2.30	97	2.90	607.50	78	78			52	3		
8	48	2.10	96	2.65	610.12	79	79			54	3		
7	51	2.40	99	3.05	612.62	80	80			55	3		
6	54	1.90	97	2.40	615.33	80	80			56	3		
5	57	1.20	95	1.50	617.69	81	81			56	3		
4	60	1.60	92	2.05	619.58	81	81			57	3		
3	63	1.15	87	1.45	621.74	81	81			56	3		
2	66	1.10	87	1.40	623.66	81	81			56	3		
1	69	1.10	85	1.40	625.50	82	82			57	3		
END	72				627.346								

Isokinetic Factor Setup

Estimated Dry Gas Meter Temp: _____

Estimated Stack Temp: _____

Estimated Delta P: _____

Estimated Moisture Content: _____

Estimated O2: _____

Estimated CO2: _____

Equipment Evaluation, OK? Y or N

Ambient Temp: _____

TC Check: _____

Pilot Check: _____

Tedlar Bag: _____

Pilot Exp Date: _____

TC Exp Date: _____

Dry Gas Meter Leak Checks

1	2	3	4

Nozzle Information

Nozzle ID: 51.20

Nozzle Dia: 0.181

APPENDIX E3

PARTICULATE MATTER (PM) – LABORATORY DATA


LABORATORY REPORT
SCAQMD M5.1

Lab Report No. A 085
Client Name: AQMD
Unit Tested: Facility C

Project No.: e10566
Date Sampled: 16-Aug-19
Analyst: DW

Client ID	Run #1	Run #2	Run #3	Field Blank
Container No 1 (Filter)	1	1	1	1
Client ID No.:	10566-M5.1-11-R1-C1	10566-M5.1-12-R1-C1	10566-M5.1-13-R1-C1	10566-M5.1-FB-C1
Lab ID No.:	A 085 - R1 - C1	A 085 - R2 - C1	A 085 - R3 - C1	A 085 - FB - C1
Filter ID #	9492	9494	9491	9493
Filter wt., total, mg ($m_{f,t}$)	35.20	7.20	0.90	0.20
Filter Acid, mg	ND	NA	NA	NA
Filter SO ₄ , mg	0.00	NA	NA	NA
Filter wt. net, mg ($m_{f,n}$)	35.20	7.20	0.90	0.20
Container No 2 (Impinger) - Water org	2	2	2	2
Client ID No.:	10566-M5.1-11-R1-C2	10566-M5.1-12-R1-C2	10566-M5.1-13-R1-C2	10566-M5.1-FB-C2
Lab ID No.:	A 085 - R1 - C2 org	A 085 - R2 - C2 org	A 085 - R3 - C2 org	A 085 - FB - C2 org
Volume, ml (V_{vol})	100	100	100	100
Impinger Catch, total, mg ($m_{i,t}$)	46.70	20.65	0.15	0.10
Methylene Chloride Blank, mg (W_{cl})	0.03	0.03	0.03	0.03
Impinger Catch, net, mg ($m_{i,n}$) ($m_{i,t} - m_{cl} - W_{cl}$)	46.67	20.62	0.12	0.07
Container No 2 (Impinger) - Water sr	2	2	2	2
Client ID No.:	10566-M5.1-11-R1-C2	10566-M5.1-12-R1-C2	10566-M5.1-13-R1-C2	10566-M5.1-FB-C2
Lab ID No.:	A 085 - R1 - C2 sr	A 085 - R2 - C2 sr	A 085 - R3 - C2 sr	A 085 - FB - C2 sr
Volume, L (V_{vol})	650	715	625	450
Impinger Catch, total, mg ($m_{i,t}$)	23.70	17.40	5.55	0.15
DI Water Blank, mg (W_{di})	0.00	0.00	0.00	0.00
Impinger Acid, mg ($m_{i,acid}$)	ND	ND	ND	ND
Impinger SO ₄ , mg ($m_{i,SO4}$)	0.00	0.00	3.29	0.00
Impinger Catch, net, mg ($m_{i,n}$) ($m_{i,t} - m_{di} - m_{i,acid} - W_{di}$)	23.70	17.40	5.55	0.15
Total Particulate mass, net, mg (m_T)	105.60	45.25	6.60	0.45
Blank correction weight of PM, mg ($m_{T,b}$)	105.57	45.22	6.57	0.42
$m_T = m_{f,n} + m_{i,n} + m_{T,b}$				

Checked by:



SUMMARY
SCAQMD M5.1



Laboratory: Almaga
Project: AQMD
Unit Tested: Facility C
Lab. ID No.: A.085

Project No.: c10566
Filter, Beaker Wt. Log Page(s): #40, #31-32

Sample Number	Lab ID	Tare Wt. (avg. g)	Final Wt. (avg. g)	Net Change (mg)	Volume ml	Blank mg	Comments
10566-M5.1-I1-R1-C1	A 085 - R1 - C1	0.3947	0.4299	35.20	-		Inlet - 1
10566-M5.1-I1-R1-C2	A 085 - R1 - C2 org	29.4022	29.4489	46.70	100	0.03	Inlet - 1
10566-M5.1-I1-R1-C2	A 085 - R1 - C2 sr	28.8027	28.8264	23.70	650	0.00	Inlet - 1
10566-M5.1-I2-R1-C1	A 085 - R2 - C1	0.3934	0.4006	7.20	-		Inlet - 2
10566-M5.1-I2-R1-C2	A 085 - R2 - C2 org	29.1778	29.1985	20.65	100	0.03	Inlet - 2
10566-M5.1-I2-R1-C2	A 085 - R2 - C2 sr	42.1259	42.1433	17.40	715	0.00	Inlet - 2
10566-M5.1-O-R1-C1	A 085 - R3 - C1	0.3917	0.3926	0.90	-		Outlet
10566-M5.1-O-R1-C2	A 085 - R3 - C2 org	29.2838	29.2840	0.15	100	0.03	Outlet
10566-M5.1-O-R1-C2	A 085 - R3 - C2 sr	29.1118	29.1174	5.55	625	0.00	Outlet
10566-M5.1-FB-C1	A 085 - FB - C1	0.3939	0.3941	0.20	-		Field Blank
10566-M5.1-FB-C2	A 085 - FB - C2 org	29.1975	29.1976	0.10	100	0.03	Field Blank
10566-M5.1-FB-C2	A 085 - FB - C2 sr	29.1218	29.1220	0.15	450	0.00	Field Blank
Reagent Blank		28.6642	28.6641	-0.05	500		DI Water
Reagent Blank		28.7205	28.7207	0.15	500		Methylene Chloride

CALCULATIONS

$$C_A = \frac{m_A}{(V_A * \rho_A)}$$

Where:

C_A - Blank Concentration

m_A - Mass of residue of after evaporation, mg

V_A - Volume of blank, ml

ρ_A - Density, g/ml

$$W_A = C_A * V_{WA} * \rho_A$$

Where:

W_A - Weight of residue, mg

V_{WA} - Volume of liquid use, ml

Reagent Blank

Methylene Chloride

Density of methylene chloride ρ_M , g/ml = 1.3550
Methylene Chloride blank volume V_M , ml = 500
Methylene Chloride blank concentration C_M , mg/g = 0.0002

MeCl Lot No. 186645 Fisher Scientific Optima

DI Water

Density of Water ρ_W , g/ml = 0.998
Water blank volume V_W , ml = 500
Water blank concentration C_W , mg/g = 0.0000

DI Water System - Pure Water Tech - WaterLogic Co.

DW

SULFURIC ACID & SULFUR OXIDES - LABORATORY DATA SHEET

Client: AQMD Project #: c10566 Checked by: DW
 Site Location: NA Unit Tested: Facility C
 Analyst: DW Date Analyzed: 12-Sep-19

Sample No.	Sample		Factor. F = V/A	Sample Titration			Acid, as H ₂ SO ₄ *2H ₂ O mg	Sulfate, as H ₂ SO ₄ *2H ₂ O mg
	Total, V (mL)	Aliquot, A (mL)		T1 (mL)	T2 (mL)	Avg. V (mL)		
ANALYSIS FOR ACID								
A 085 - R1 - C1	50	10	5	0.00	0.00	0.00	ND	
A 085 - R1 - C2 sr	50	10	5	0.00	0.00	0.00	ND	
A 085 - R2 - C2 sr	50	10	5	0.00	0.00	0.00	ND	
A 085 - R3 - C2 sr	50	10	5	0.00	0.00	0.00	ND	
A 085 - FB - C2 sr	50	10	5	0.00	0.00	0.00	ND	
ANALYSIS FOR SULFATE								
A 085 - R1 - C1	50	10	5	0.02	0.02	0.02		0.00
A 085 - R1 - C2 sr	50	10	5	0.02	0.02	0.02		0.00
A 085 - R2 - C2 sr	50	10	5	0.02	0.02	0.02		0.00
A 085 - R3 - C2 sr	50	10	5	1.00	1.00	1.00		3.29
A 085 - FB - C2 sr	50	10	5	0.02	0.02	0.02		0.00

No.	Sodium Hydroxide Titration		Barium Chloride Titration		Detection Limit
	KHP (mg)	Volume, V's (mL)	Aliquot, V1 (10 mL)	Volume, V2 (mL)	
Blank	-	0.00	-	0.02	Sulfate, as
1	0.00000		4	4.02	H ₂ SO ₄ *2H ₂ O, mg
2	0.00000		4	4.02	Acid, as
Avg.	0.10000			0.01003	H ₂ SO ₄ *2H ₂ O, mg

Sulfuric Acid Concentration 0.01000N
 Rieca Lot 4610D98 Exp Sept 2019
 Sodium Hydroxide Solution 0.100 N
 BDH Lot 18J1156571 Exp Sept 2021

Sulfate as SO₄, mg = (V_s - V_{bl}) x N_B x 134.11/2 x F
 Acid as SO₄, mg = (V_s - V_{bl}) x N_S x 134.11/2 x F

CALCULATIONS: N_S = (mg KHP/203.44)/(V_s-V_{bl})
 N_B = (V₁ x N₁₂₃₀₄)/(V₁-V_{TB})

Lot # AG 85



Almega
ENVIRONMENTAL
CHAIN OF CUSTODY
RECORDS

INVOICE TO: _____
REPORT TO: _____
PO # _____

ALMEGA Environmental & Technical Services
10602 Walker St.
Cypress, CA 90630
(714) 889-4000 Fax (714) 889-7030
lab@almegaenv.com
Contact: _____

Standard: X
Other: _____
Rush: _____
Depends on # of Samples
5 - 10 days _____
3 - 7 days _____
Return or Dispose
REMARKS

Job #	10566	Unit #	Baghouse	Client:	SCAQMD - C	Location:	Inlet & Outlet	ANALYSIS REQUESTED			Turnaround Time
								Lab Sample #	Type Of Sample	No of Containers	
Sample Date	Sample Time	Sample Identification	Lab Sample #	LIQUID	GAS	SOLID	ORGANIC	INORGANIC	Metals	Sulfides	Diesel PM
8/16/2019	7:00	10566-M5.1-FB-C1	AG85 53-C1			X					
		10566-M5.1-FB-C2	-C2		X						
8/16/2019	7:40 - 8:56	10566-M5.1-I1-R1-C1	R1-C1			X					
		10566-M5.1-I1-R1-C2	-C2		X						
8/16/2019	7:40 - 8:56	10566-M5.1-I2-R1-C1	R2-C1			X					
		10566-M5.1-I2-R1-C2	-C2		X						
8/16/2019	7:40 - 8:56	10566-M5.1-O-R1-C1	R3-C1			X					
		10566-M5.1-O-R1-C2	-C3		X						

Relinquished by: _____ Date: 8/16/2019 Time: 11:30
Received by: _____ Date: 8/16/19 Time: 11:40

Relinquished by: _____ Date: _____ Time: _____
Received by: _____ Date: _____ Time: _____

Relinquished by: _____ Date: _____ Time: _____
Received by: _____ Date: _____ Time: _____

Standard Receipt
Sample LOG in Checklist

Project No: 210266

Method: 110.1, 25.1

Lab ID: A085

Sampling Date: 8/13 - 8/16

Location: AQMD-C Int: _____

Date & Time Rcd: 8/16/19 11:40

Location: LAB Int: DN

Arrived By: (circle) FedEx UPS Drop Off (int) OK Other _____

Condition of Package(s): (comment): OK Package Type: Box Cooler Other: _____

Number of Sample Container(s): 8, 3 Correct Containers (per Method): Y N

Preservation: (circle) ICE DryICE ICEPacks None

Sample Conditions:

Sample Temp (C): 21

Ambient Temp (C): 21

Sample Temp (C): _____

Filter Condition: OK - Dirty

PH: _____

Components Sealed: Y N

Sample Recovery Completed On: (date & time) _____

Recovered In: (circle) Field Lab Other _____

Silica Gel Condition: _____

Tedlar Bags -

Condensation: Y N

Comments:

Container(s) Requested: Glass _____ Plastic _____

Additional Comments:

A085-22-C2 = hard to extract, black residue stuck to bottle
medly used to collect it. Separation is

Beakers Weight Record

Laboratory: **Almeida**
 Project: **SCAQMD**
 Project No.: **610566**
 Unit Tested: **Facility C**
 Lab. ID No.: **A.085**

Pretest

(page of)
 Balanced ID: **ADDERJEDA**
 Serial No.: **4102866**
 Last Calibration: **12-Jan-19**
 Beaker Weight Log Page(s): **0031-32**

Sample Number	Lab ID	Beaker ID	Beaker Weights (g)				Volume (ml)	Comments
			Date/Time	By	Wt. 1	Wt. 2		
10566-MS.1-Q1-R1-C2	A.085 - R1 - C2 org	6699	8/19/19 11:00	DW	29.4021	29.4023	100	Inlet - 1
10566-MS.1-Q1-R1-C2	A.085 - R1 - C2 sr	7965	8/28/19 11:00	DW	28.8027	28.8026	650	Inlet - 1
10566-MS.1-Q2-R1-C2	A.085 - R2 - C2 org	8365	8/19/19 11:00	DW	29.1777	29.1779	100	Inlet - 2
10566-MS.1-Q2-R1-C2	A.085 - R2 - C2 sr	3023	8/28/19 11:00	DW	42.1258	42.1259	715	Inlet - 2
10566-MS.1-Q-R1-C2	A.085 - R3 - C2 org	8302	8/19/19 11:00	DW	29.2858	29.2858	100	Outlet
10566-MS.1-Q-R1-C2	A.085 - R3 - C2 sr	8027	8/28/19 11:00	DW	29.1118	29.1118	625	Outlet
10566-MS.1-FB-C2	A.085 - FB - C2 org	7928	8/19/19 11:00	DW	29.1974	29.1975	100	Field Blank
10566-MS.1-FB-C2	A.085 - FB - C2 sr	4013	8/28/19 11:00	DW	29.1218	29.1218	450	Field Blank
Reagent Blank		4321	9/24/19 17:00	DW	28.6641	28.6642	500	DI Water
Reagent Blank		7965	11/1/18 11:00	DW	28.7206	28.7204	500	Mercuric Chloride

3

Beakers Weight Record

Laboratory: Almega
 Project: SCAQMD
 Project No.: 10566
 Unit Tested: Facility C
 Lab. ID No.: A.085

Balanced ID: JMD ER: 123
 Serial No.: 4302666
 Last Calibration: 12-Jan-19
 Beaker Weight Log Page(s): #31-32

Sample Number	Lab ID	Beaker ID	Beaker Weights (g)				D.Wt. (mg)	Volume ml	Comments
			Date/Time	By	Wt. 1	Wt. 2			
10566-M5.1-I-R1-C2	A.085 - R1 - C2 org	6699	9/5/19 11:00	DW	29.4488	29.4490	-0.20	100	Inlet - 1
10566-M5.1-I-R1-C2	A.085 - R1 - C2 sr	7795	9/5/19 11:00	DW	28.8262	28.8265	-0.30	650	Inlet - 1
10566-M5.1-Q-R1-C2	A.085 - R2 - C2 org	8305	9/5/19 11:00	DW	29.1983	29.1986	-0.30	100	Inlet - 2
10566-M5.1-Q-R1-C2	A.085 - R2 - C2 sr	8027	9/5/19 11:00	DW	42.1434	42.1433	0.30	71.5	Inlet - 2
10566-M5.1-O-R1-C2	A.085 - R3 - C2 org	8302	9/3/19 11:00	DW	29.2839	29.2840	-0.10	100	Outlet
10566-M5.1-O-R1-C2	A.085 - R3 - C2 sr	8027	9/5/19 11:00	DW	29.1173	29.1174	-0.10	62.5	Outlet
10566-M5.1-FB-C2	A.085 - F8 - C2 org	7928	9/5/19 11:00	DW	29.1976	29.1975	0.10	100	Field Blank
10566-M5.1-FB-C2	A.085 - F8 - C2 sr	4013	9/5/19 11:00	DW	29.1219	29.1220	-0.10	450	Field Blank
Reagent Blank		4321	6/11/19 11:00	DW	28.6641	28.6641	0.00	500	DI Water
Reagent Blank		7965	11/15/18 11:00	DW	28.7207	28.7206	0.10	500	Methylene Chloride

3

Filter Weight Record

x _____ Pretest (page ___ of ___)

Laboratory: Almega
 Project: AQMD
 Project No.: 10566
 Unit Tested: Facility C
 Lab. ID No.: A 085

Balanced ID: A&D ER-182A
 Serial No.: 4702866
 Last Calibration: 12-Jun-19
 Filter Weight Log Page(s): #40

Client Sample No.	Lab ID	Filter ID	Filter Weights (g)				D WL (mg)	Comments	
			Date/Time	By	WL 1	WL 2			
10566-M5.1-11-R1-C1	A 085 - R1 - C1	9492	7/29/19 11:00	DW	0.3947	0.3947	0.3947	0.00	Inlet - 1
10566-M5.1-12-R1-C1	A 085 - R2 - C1	9494	7/29/19 11:00	DW	0.3933	0.3934	0.3934	-0.10	Inlet - 2
10566-M5.1-O-R1-C1	A 085 - R3 - C1	9491	7/29/19 11:00	DW	0.3916	0.3917	0.3917	-0.10	Outlet
10566-M5.1-FB-C1	A 085 - FB - C1	9493	7/29/19 11:00	DW	0.3938	0.3939	0.3939	-0.10	Field Blank

DN

Filter Weight Record

x _____ Post-test (page ___ of ___)

Laboratory: Almega
 Project: AQMD
 Project No.: ε10566
 Unit Tested: Facility C
 Lab. ID No.: A 085

Balanced ID: A&D ER-182A
 Serial No.: 4702866
 Last Calibration: 12-Jun-19
 Filter Weight Log Page(s): #40

Client Sample No.	Lab ID	Filter ID	Filter Weights (g)				D Wt. (mg)	Comments			
			Date/Time	By	Wt. 1	Wt. 2			Average		
10566-M5.1-11-R1-C1	A 085 - R1 - C1	9492	9/5/19 10:00	DW	0.4299	9/6/19 11:00	DW	0.4299	0.4299	0.00	Inlet - 1
10566-M5.1-12-R1-C1	A 085 - R2 - C1	9494	9/5/19 10:00	DW	0.4006	9/6/19 11:00	DW	0.4005	0.4006	0.10	Inlet - 2
10566-M5.1-Q-R1-C1	A 085 - R3 - C1	9491	9/5/19 10:00	DW	0.3925	9/6/19 11:00	DW	0.3926	0.3926	-0.10	Outlet
10566-M5.1-FB-C1	A 085 - FB - C1	9493	9/5/19 10:00	DW	0.3941	9/6/19 11:00	DW	0.3940	0.3941	0.10	Field Blank

R3

CLOSED TITRATION
Acids mS.l

No	Sample ID	Date	Sample Volume		DF (S/A)	mL used	Note
			ml (S)	aliquot (A)			
1	A085 21-C1	9/12	50	10	5	0.00	0.1N NaOH
2	2P		"	"	"	0.00	↓
3	21-C2-SF		"	"	"	0.00	
4	2P		"	"	"	0.00	
5	22-C2-SF		"	"	"	0.00	
6	2P		"	"	"	0.00	
7	23-C2-SF		"	"	"	0.00	
8	2P		"	"	"	0.00	
9	F3-C2-SF		"	"	"	0.00	
10	2P		"	"	"	0.00	
11							
12							
13							
14							
15							
16							
17							
18							
19							
20							
21							

DF = Dilution Factor

Comments 0.1N NaOH Lot# 1851156571 Exp. Oct 2021 VWR-BDH

c10566

TITRATION

Sulfates mS.l

No	Sample ID	Date	Sample Volume		DF (S/A)	mL used	Note
			ml (S)	aliquot (A)			
1	0.01N H ₂ SO ₄	9/12	4	4	1	4.02	0.01N BaCl ₂
2	D.P		"	"	"	4.02	
3	DA BK		100	100	1	.02	
4	D.P		"	"	"	.02	
5	A085 RI-C1		50	10	5	.02	
6	D.P		"	"	"	.02	
7	R1-C2-S		"	"	"	.02	
8	D.P		"	"	"	.02	
9	R2-C2-S		"	"	"	.02	
10	D.P		"	"	"	.02	
11	R3-C2-S		"	"	"	1.00	
12	D.P		"	"	"	1.00	
13	F8-C2-S		"	"	"	0.02	
14	D.P		"	"	"	0.02	
15							
16							
17							
18							
19							
20							
21							

DF = Dilution Factor

Comments * 0.01N Sulfuric Acid Lot# 4610298 Exp Sept 2019 Ricca

APPENDIX F
COLLECTION/CAPTURE EFFICIENCY TEST

APPENDIX G
QUALITY ASSURANCE AND QUALITY CONTROL (QA/QC)
TEST EQUIPMENT CALIBRATION DATA

	Reported Inclined H2O	Electronic ADM
	0.06	0.0781
	0.07	0.0759
	0.07	0.0755
	0.06	0.0643
	0.05	0.0545
	0.04	0.0365
	0.04	0.0406
	0.03	0.0422
	0.03	0.0446
	0.03	0.0525
	0.04	0.0514
	0.05	0.0541
	0.02	0.0254
	0.03	0.0292
	0.03	0.0303
	0.02	0.0250
	0.03	0.0340
	0.04	0.0463
	0.03	0.0432
	0.05	0.0623
	0.05	0.0732
	0.06	0.0783
	0.07	0.0814
	0.07	0.0593
Average	0.0446	0.0524
Sqrt of the average	0.211	0.229
% difference from RM (ADM)	7.8%	
Biased	Low	

TYPE S PITOT TUBE SEMIANNUAL INSPECTION SHEET

CAL DATE: 6/14/2019
NEXT DUE DATE: 12/13/2019
PITOT ID: 28

<p>Degree indicating level position for determining α_1 and α_2</p> <p>Degree indicating level position for determining β_1 and β_2</p> <p>Degree indicating level position for determining θ</p> <p>Degree indicating level position for determining Y, then calculating Z.</p>	Parameter	Values	Allowable Range
	Level and Perpendicular?	Yes OR No	Yes
	Obstruction?	Yes OR No	No
	Damaged?	Yes OR No	No
	α_1	0	$-10^\circ \leq \alpha_1 \leq +10^\circ$
	α_2	0	$-10^\circ \leq \alpha_2 \leq +10^\circ$
	β_1	0	$-5^\circ \leq \beta_1 \leq +5^\circ$
	β_2	0	$-5^\circ \leq \beta_2 \leq +5^\circ$
	γ	0	NA
	θ	0	NA
	$Z = A (\tan \gamma)$	0.000	≤ 0.125 in.
	$W = A (\tan \theta)$	0.000	≤ 0.031 in.
	Dt	0.372	$0.188 \leq Dt \leq 0.375$
	A	0.937	NA
$A/2/(Dt)$	1.26	$1.05 \leq PA/Dt \leq 1.5$	

Certification:

I certify that this pitot tube meets or exceeds all specifications, criteria and/or applicable design features and is hereby assigned a pitot tube calibration factor C_p of 0.84.

Certified By: William Bryant **Date:** 6/14/2019

TYPE S PITOT TUBE SEMIANNUAL INSPECTION SHEET

CAL DATE: 6/14/2019

NEXT DUE DATE: 12/13/2019

PITOT ID: 73

	Parameter	Values	Allowable Range
<p>Degree indicating level position for determining α_1 and α_2</p>	Level and Perpendicular?	Yes OR No	Yes
<p>Degree indicating level position for determining β_1 and β_2</p>	Obstruction?	Yes OR No	No
<p>Degree indicating level position for determining θ</p>	Damaged?	Yes OR No	No
<p>Degree indicating level position for determining Z</p>	α_1	0	$-10^\circ \leq \alpha_1 \leq +10^\circ$
<p>Degree indicating level position for determining W</p>	α_2	0	$-10^\circ \leq \alpha_2 \leq +10^\circ$
<p>Degree indicating level position for determining D_t</p>	β_1	0	$-5^\circ \leq \beta_1 \leq +5^\circ$
<p>Degree indicating level position for determining A</p>	β_2	0	$-5^\circ \leq \beta_2 \leq +5^\circ$
<p>Degree indicating level position for determining Z and γ, then calculating Z</p>	γ	0	NA
	θ	0	NA
	$Z = A (\tan \gamma)$	0.000	≤ 0.125 in.
	$W = A (\tan \theta)$	0.000	≤ 0.031 in.
	D_t	0.374	$0.188 \leq D_t \leq 0.375$
	A	0.875	NA
	$A/2(D_t)$	1.17	$1.05 \leq PA/D_t \leq 1.5$

Certification:



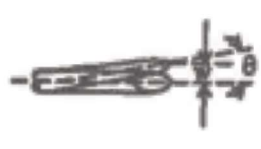
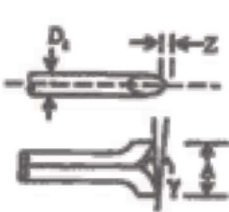
I certify that this pitot tube meets or exceeds all specifications, criteria and/or applicable design features and is hereby assigned a pitot tube calibration factor C_p of 0.84.

Certified By: William Bryant Date: 6/14/2019

W. Bryant

TYPE S PITOT TUBE SEMIANNUAL INSPECTION SHEET

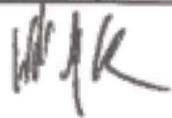
CAL DATE: 6/14/2019
NEXT DUE DATE: 12/13/2019
PITOT ID: 85

	Parameter	Values	Allowable Range
 <p style="font-size: small;">Degree indicating level position for determining α_1 and α_2</p>	Level and Perpendicular?	Yes OR No	Yes
 <p style="font-size: small;">Degree indicating level position for determining β_1 and β_2</p>	Obstruction?	Yes OR No	No
 <p style="font-size: small;">Degree indicating level position for determining θ</p>	Damaged?	Yes OR No	No
 <p style="font-size: small;">Degree indicating level position for determining γ, then calculating Z.</p>	α_1	0	$-10^\circ \leq \alpha_1 \leq +10^\circ$
	α_2	0	$-10^\circ \leq \alpha_2 \leq +10^\circ$
	β_1	0	$-5^\circ \leq \beta_1 \leq +5^\circ$
	β_2	0	$-5^\circ \leq \beta_2 \leq +5^\circ$
	γ	0	NA
	θ	1	NA
	$Z = A (\tan \gamma)$	0.000	≤ 0.125 in.
	$W = A (\tan \theta)$	0.016	≤ 0.031 in.
	Dt	0.375	$0.188 \leq Dt \leq 0.375$
	A	0.917	NA
	$A/2/(Dt)$	1.22	$1.05 \leq PA/Dt \leq 1.5$

Certification:


I certify that this pitot tube meets or exceeds all specifications, criteria and/or applicable design features and is hereby assigned a pitot tube calibration factor C_p of 0.84.

Certified By: William Bryant **Date:** 6/14/2019



ALMEGA ENVIRONMENTAL AND TECHNICAL SERVICES
10602 WALKER STREET
CYPRESS, CA 90630

STACK TEMPERATURE SENSOR SEMI-ANNUAL CALIBRATION

TEMPERATURE SENSOR I.D:	28	REF. DIGITAL NIST TRACEABLE THERMOMETER ID: : 1, 2 & 3
READ OUT I.D:	VA710	ICE BATH: YES
PITOT TUBE I.D:	28	BOILING WATER: YES
PITOT TUBE LENGTH:	37"	HOT OIL: YES
DATE:	6/14/2019	CALIBRATED BY: CH/JO 

ICE BATH				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764570				
Due Date				
11/13/2019				
	31.4	31.5	0.1	0.3
	31.4	31.4	0.0	0.0
	31.4	31.4	0.0	0.0

BOILING WATER				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764579				
Due Date				
11/13/2019				
	212.5	211.9	0.6	0.3
	212.8	212.1	0.7	0.3
	213.9	212.3	1.6	0.7


HOT OIL				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764557				
Due Date				
11/13/2019				
	485.0	483.0	2.0	0.4
	486.0	484.0	2.0	0.4
	486.0	485.0	3.0	0.6

NOTE:
MAXIMUM TOLERANCE BETWEEN ANY TWO MEASUREMENT IS 1.5%.
TAKE READING EVERY ONE MINUTE.

REF. T1 ICE BATH THERMOMETER: -58 - 572 (F)
 REF. T2 BOILING WATER THERMOMETER: -58 - 572 (F)
 REF. T3 HOT OIL THERMOMETER: -58 - 572 (F)

ALMEGA ENVIRONMENTAL AND TECHNICAL SERVICES
10602 WALKER STREET
CYPRESS, CA 90630

STACK TEMPERATURE SENSOR SEMI-ANNUAL CALIBRATION

TEMPERATURE SENSOR I.D:	73	REF. DIGITAL NIST TRACEABLE THERMOMETER ID: : 1, 2 & 3
READ OUT I.D:	VA710	ICE BATH: YES
PITOT TUBE I.D:	73	BOILING WATER: YES
PITOT TUBE LENGTH:	75"	HOT OIL: YES
DATE:	6/14/2019	CALIBRATED BY: CH/JO 

ICE BATH				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764570				
Due Date				
11/13/2019				
	31.4	31.4	0.0	0.0
	31.4	31.4	0.0	0.0
	31.5	31.5	0.0	0.0

BOILING WATER				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764579				
Due Date				
11/13/2019				
	210.1	209.9	0.2	0.1
	210.3	210.0	0.3	0.1
	210.5	210.2	0.3	0.1


ICE BATH				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764557				
Due Date				
11/13/2019				
	441.0	438.0	3.0	0.7
	442.0	439.0	3.0	0.7
	443.0	440.0	3.0	0.7

NOTE:
MAXIMUM TOLERANCE BETWEEN ANY TWO MEASUREMENT IS 1.5%.
TAKE READING EVERY ONE MINUTE.

REF. T1 ICE BATH THERMOMETER: -58 - 572 (F)
 REF. T2 BOILING WATER THERMOMETER: -58 - 572 (F)
 REF. T3 HOT OIL THERMOMETER: -58 - 572 (F)

ALMEGA ENVIRONMENTAL AND TECHNICAL SERVICES
 10602 WALKER STREET
 CYPRESS, CA 90630

STACK TEMPERATURE SENSOR SEMI-ANNUAL CALIBRATION

TEMPERATURE SENSOR I.D:	85	REF. DIGITAL NIST TRACEABLE THERMOMETER ID: : 1, 2 & 3
READ OUT I.D:	VA710	ICE BATH: YES
PITOT TUBE I.D:	85	BOILING WATER: YES
PITOT TUBE LENGTH:	37"	HOT OIL: YES
DATE:	6/14/2019	CALIBRATED BY: CH/JO 

ICE BATH				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764570				
Due Date				
11/13/2019				
	31.5	31.3	0.2	0.6
	31.5	31.4	0.1	0.3
	31.5	31.5	0.0	0.1

BOILING WATER				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764579				
Due Date				
11/13/2019				
	212.3	212.1	0.2	0.1
	212.4	212.1	0.3	0.1
	212.5	212.2	0.3	0.1

ICE BATH				
S/N:	REF. DIGITAL NIST TRACEABLE THERMOMETER TEMPERATURE (°F)	FIELD METER TEMPERATURE (°F)	ABSOLUTE DIFFERENCE TEMPERATURE (°F)	% DIFFERENCE (%)
160764557				
Due Date				
11/13/2019				
	504.0	500.0	4.0	0.8
	505.0	501.0	4.0	0.8
	507.0	503.0	4.0	0.8

NOTE:
 MAXIMUM TOLERANCE BETWEEN ANY TWO MEASUREMENT IS 1.5%.
 TAKE READING EVERY ONE MINUTE.

REF. T1 ICE BATH THERMOMETER: -58 - 572 (F)
 REF. T2 BOILING WATER THERMOMETER: -58 - 572 (F)
 REF. T3 HOT OIL THERMOMETER: -58 - 572 (F)

NOZZLE CALIBRATION FORM

NOZZLE ID #: GL 20

CALIPER ID: 491 568

CALIBRATOR: WB

SIGNATURE: Will M. [Signature]

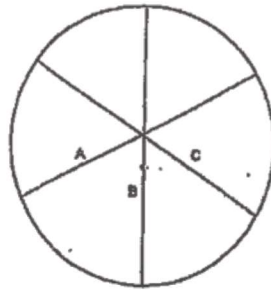
DATE: 6-6-19

Measured Diameter A: 0.181 inch

Measured Diameter B: 0.182 inch

Measured Diameter C: 0.181 inch

Average: 0.181 inch



Inside Diameter

Is the Nozzle Free from Nicks, Dents, or Corrosion?

Yes X

No _____

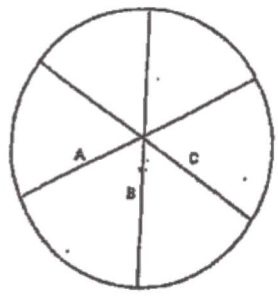
If "No", please describe deviations below:

Nozzle Deviations (if any):

NOZZLE CALIBRATION FORM

NOZZLE ID #: GL 40
CALIPER ID: 491568
CALIBRATOR: WB
SIGNATURE: *[Handwritten Signature]*
DATE: 6-7-19

Measured Diameter A: 0.346 inch
Measured Diameter B: 0.349 inch
Measured Diameter C: 0.350 inch
Average: 0.348 inch



Inside Diameter

Is the Nozzle Free from Nicks, Dents, or Corrosion?

Yes X
No _____

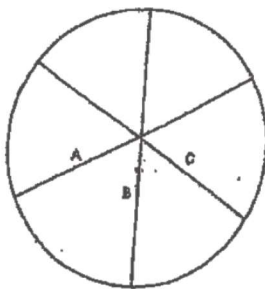
If "No", please describe deviations below:

Nozzle Deviations (if any):

NOZZLE CALIBRATION FORM

NOZZLE ID #: D-13
CALIPER ID: 491568
CALIBRATOR: WB
SIGNATURE: *WB*
DATE: 6-13-19

Measured Diameter A: 0.439 inch
Measured Diameter B: 0.436 inch
Measured Diameter C: 0.436 inch
Average: 0.437 inch



Inside Diameter

Is the Nozzle Free from Nicks, Dents, or Corrosion?

Yes

No

If "No", please describe deviations below:

Nozzle Deviations (if any):

Semi-Annual Field Dry Gas Meter Calibration* Calibration Date: 5/3/2018

Orifice Series: 33-73
 Serial Number: AE/AE2
 Cal Type: Semi-Annual

Calibrated by: Luka Brown
 (signature): [Signature]
 Reviewed by: [Signature]

DRY GAS METER CALIBRATION FACTOR
Y
Yds = 1.0379

ORIFICE CALIBRATION FACTOR
dH@
dH@ = 1.583

DGM INLET				DGM OUTLET				METER READING				ORIFICE READING				QUALITY CONTROL CHECKS						
Initial (°F)	Final (°F)	Initial (°F)	Final (°F)	Initial (cu.ft.)	Final (cu.ft.)	Initial (cu.ft.)	Final (cu.ft.)	Initial (in.H2O)	Final (in.H2O)	Initial (in.H2O)	Final (in.H2O)	(Y _{actual} / Y _{nom}) <	Average Coeff (Y)	dH@ _{avg} <	0.98 <	(Y _{nom} / Y _{act})	0.95 < Y < 1.05	0.10 <=	0.0035	1.035	1.500	
66.0	65.0	64.0	64.0	448.808	454.320	0.110	0.110	0.110	0.110	0.110	0.110	0.0036	PASS	PASS	1.02	0.997	PASS	PASS	1.500	PASS	1.500	PASS
66.0	66.0	65.0	65.0	454.320	459.847	0.110	0.110	0.110	0.110	0.110	0.110	0.0036	PASS	PASS	1.02	0.997	PASS	PASS	1.500	PASS	1.500	PASS
66.0	67.0	66.0	67.0	466.388	471.115	0.680	0.680	0.680	0.680	0.680	0.680	0.0064	PASS	PASS	1.008	1.044	PASS	PASS	1.568	PASS	1.568	PASS
69.0	69.0	68.0	68.0	476.850	482.058	0.680	0.680	0.680	0.680	0.680	0.680	0.0038	PASS	PASS	1.002	1.040	PASS	PASS	1.668	PASS	1.668	PASS
70.0	71.0	69.0	70.0	482.858	487.800	1.700	1.700	1.700	1.700	1.700	1.700	0.0034	PASS	PASS	0.995	1.032	PASS	PASS	1.537	PASS	1.537	PASS
71.0	72.0	70.0	71.0	487.800	493.038	1.700	1.700	1.700	1.700	1.700	1.700	0.0034	PASS	PASS	0.995	1.032	PASS	PASS	1.537	PASS	1.537	PASS
72.0	72.0	71.0	71.0	493.038	498.302	1.700	1.700	1.700	1.700	1.700	1.700	0.0034	PASS	PASS	0.995	1.032	PASS	PASS	1.537	PASS	1.537	PASS
73.0	74.0	72.0	73.0	504.619	510.765	3.300	3.300	3.300	3.300	3.300	3.300	0.0034	PASS	PASS	0.995	1.032	PASS	PASS	1.537	PASS	1.537	PASS
74.0	75.0	73.0	74.0	510.765	517.007	3.300	3.300	3.300	3.300	3.300	3.300	0.0034	PASS	PASS	0.995	1.032	PASS	PASS	1.537	PASS	1.537	PASS

Orifice Series No.	Run Time (min)	CRITICAL ORIFICE				DRY GAS METER				CALCULATIONS				
		Orifice K-factor	Tested Vacuum (in.Hg)	Ambient Temp. (°F)	Orifice dH (in.H2O)	AVG Temp. (°F)	NET Volume (cu.ft.)	Flowrate CFM (SCFM)	Corrected Volume (SCF)	Coefficient Y _{act} (0.95 < Y _{act} < 1.05)	Orifice dH@ (in.H2O)	Flowrate CFM (SCFM)	Corrected Volume (SCF)	Coefficient Y _{act} (0.95 < Y _{act} < 1.05)
33	28	0.1548	25.00	64.0	0.110	64.50	0.2023	0.195	5.484	1.0368	0.195	5.484	1.0368	1.800
33	28	0.1548	25.00	65.0	0.110	65.00	0.202	0.195	5.474	1.0340	0.195	5.474	1.0340	1.502
33	28	0.1548	25.00	65.0	0.110	66.00	0.202	0.198	5.477	1.0333	0.198	5.477	1.0333	1.489
52	12	0.3769	23.50	66.0	0.680	67.00	0.491	0.472	5.658	1.0421	0.472	5.658	1.0421	1.570
52	12	0.3769	23.50	66.0	0.680	68.00	0.491	0.471	5.635	1.0426	0.471	5.635	1.0426	1.567
52	12	0.3769	23.50	67.0	0.680	69.00	0.491	0.466	5.618	1.0455	0.466	5.618	1.0455	1.557
63	7	0.5990	20.50	67.0	1.700	70.00	0.767	0.736	6.163	1.0402	0.736	6.163	1.0402	1.809
63	7	0.5990	20.50	68.0	1.700	71.00	0.768	0.736	6.150	1.0417	0.736	6.150	1.0417	1.809
63	7	0.5990	20.50	68.0	1.700	71.50	0.768	0.738	6.169	1.0380	0.738	6.169	1.0380	1.807
73	6	0.8109	18.00	69.0	3.300	72.75	1.054	1.019	6.115	1.0343	1.019	6.115	1.0343	1.856
73	6	0.8109	18.00	69.0	3.300	73.50	1.054	1.022	6.135	1.0309	1.022	6.135	1.0309	1.856
73	6	0.8109	18.00	70.0	3.300	74.25	1.053	1.020	6.122	1.0321	1.020	6.122	1.0321	1.857

* Critical Orifice used.

Semi-Annual Field Dry Gas Meter Calibration* Calibration Date: 3/19/2019

Office Series: 33-73
 Serial Number: AE/NE
 Call Type: Semi-Annual

Calibrated by: L. Barrow
 (signature)
 Reviewed by:

DRY GAS METER CALIBRATION FACTOR
Y
Y_{ds} = 1.0376

ORIFICE CALIBRATION FACTOR
dH@
dH@ = 1.789

DGM INLET		DGM OUTLET		Meter Reading		Orifice Reading		QUALITY CONTROL CHECKS				
Initial (F)	Final (F)	Initial (F)	Final (F)	Initial (cu.ft.)	Final (cu.ft.)	Initial (in.H2O)	Final (in.H2O)	(Y _{actual} - Y _{target}) < 0.010 **	0.99 < (Y _{act} /Y _{tar}) < 1.02	Average Coeff (Y) (0.95 < Y < 1.05)	dH@ _{avg} = (dH@ ± 0.15)	DGM ID: A-B
N/A	N/A	62.0	63.0	522.972	329.638	0.130	0.130	0.0033	0.966	1.022	1.776	Serial #: 20182666
N/A	N/A	63.0	64.0	529.639	335.123	0.130	0.130	PASS	PASS	PASS	PASS	Model #: XC-622-D
N/A	N/A	64.0	65.0	535.123	340.724	0.130	0.130	PASS	PASS	PASS	PASS	Calibration Interval: X
N/A	N/A	67.0	68.0	541.902	347.626	0.730	0.730	0.0004	1.026	1.044	1.662	Semi-Annual: X
N/A	N/A	68.0	69.0	547.626	353.359	0.730	0.730	PASS	PASS	PASS	PASS	91-monthly: X
N/A	N/A	69.0	70.0	553.359	359.090	0.730	0.730	PASS	PASS	PASS	PASS	Other: X
N/A	N/A	71.0	72.0	561.037	366.288	1.900	1.900	0.0036	1.001	1.039	1.506	Standard Temperature (den.E) Tstd = 60
N/A	N/A	72.0	73.0	566.286	371.518	1.900	1.900	PASS	PASS	PASS	PASS	Barometric Pressure (in.Hg) Inside: 29.59
N/A	N/A	73.0	74.0	571.518	376.762	1.900	1.900	PASS	PASS	PASS	PASS	Final: 29.69
N/A	N/A	74.0	76.0	577.762	383.668	3.800	3.800	PASS	PASS	PASS	PASS	Profile: 29.89
N/A	N/A	75.0	76.0	583.968	390.181	3.800	3.800					
N/A	N/A	76.0	77.0	590.181	396.368	3.800	3.800					

CRITICAL ORIFICE				DRY GAS METER				CALCULATIONS					
Orifice Series No.	Run Time (min)	Orifice K-factor	Treated Vacuum (in.Hg)	Ambient Temp (F)	Flowrate Orifm (SCFM)	Connected Volume (cu.ft.)	NET Volume (cu.ft.)	AVG Temp (F)	Orifice dH (in.H2O)	Flowrate Orifm (SCFM)	Connected Volume (SCF)	Coefficient Y _{ds} (0.95 < Y _{ds} < 1.05)	Orifice dH@ (in.H2O)
33	26	0.1549	27.50	63.0	0.2026	6.870	6.667	62.60	0.130	0.198	5.540	1.0236	1.777
33	26	0.1549	27.50	64.0	0.202	6.865	6.584	63.50	0.130	0.198	5.546	1.0214	1.777
33	26	0.1549	27.50	64.0	0.202	6.865	6.801	64.50	0.130	0.196	5.503	1.0203	1.773
52	12	0.3769	24.50	66.0	0.491	6.898	6.729	67.60	0.730	0.471	6.650	1.0437	1.684
52	12	0.3769	24.50	66.0	0.491	6.898	6.734	68.50	0.730	0.471	6.650	1.0438	1.681
52	12	0.3769	24.50	67.0	0.491	6.891	6.737	69.50	0.730	0.470	6.642	1.0441	1.681
63	7	0.8690	21.00	67.0	0.767	6.370	6.229	71.50	1.900	0.734	6.136	1.0462	1.796
63	7	0.8690	21.00	68.0	0.766	6.366	6.232	72.50	1.900	0.733	6.131	1.0458	1.796
63	7	0.8690	21.00	68.0	0.766	6.366	6.234	73.50	1.900	0.732	6.123	1.0471	1.781
73	6	0.8109	16.00	69.0	1.054	6.326	6.206	74.50	3.800	1.015	6.092	1.0383	1.808
73	6	0.8109	16.00	69.0	1.054	6.325	6.223	75.50	3.800	1.015	6.097	1.0374	1.804
73	6	0.8109	16.00	70.0	1.053	6.319	6.207	76.50	3.800	1.012	6.070	1.0410	1.804

* Critical Orifice used. Note: This Apex Meter Box, Capable Model # XC-622-D does not have a temperature sensor at the inlet. Hence, DGM inlet columns are intentionally left blank.

Semi-Annual Field Dry Gas Meter Calibration* Calibration Date: 4/26/2019

Orifice Series: 33-73
 Serial Number: AE/AE3
 Cal Type: Semi-Annual

Calibrated by: L. Bignow
 (signature)
 Reviewed by:

DRY GAS METER CALIBRATION FACTOR
Y
Yds = 1.0395

ORIFICE CALIBRATION FACTOR
dH@
dH@ = 1.819

DGM INLET		DGM OUTLET		Meter Reading		Orifice Reading		QUALITY CONTROL CHECKS				DGM ID:	
Initial (°F)	Final (°F)	Initial (°F)	Final (°F)	Initial (cu.ft.)	Final (cu.ft.)	Initial (in-H2O)	Final (in-H2O)	(Y _{meas} - Y _{std}) / Y _{std} <	Average Coeff (Y)	dH@ _{meas} <	(dH@ _{meas} - dH@) / dH@	Serial #:	A-S
N/A	N/A	67.0	67.0	359.554	365.083	0.140	0.140	0.010 **	1.02	(0.96 < Y < 1.05)	± 0.15	1612035	
		67.0	67.0	365.083	370.604	0.140	0.140	0.0007	0.999	1.038	1.906	XC-522	
		67.0	68.0	370.604	376.129	0.140	0.140	PASS	PASS	PASS	PASS		
		68.0	69.0	376.149	381.662	0.760	0.760						
		68.0	69.0	381.662	387.175	0.760	0.760	0.0018	1.007	1.047	1.752		
		69.0	69.0	387.175	393.276	0.760	0.760	PASS	PASS	PASS	PASS		
		69.0	69.0	393.276	398.498	1.900	1.900						
		69.0	69.0	398.498	403.736	1.900	1.900	0.0042	1.001	1.041	1.903		
		70.0	70.0	403.739	408.966	1.900	1.900	PASS	PASS	PASS	PASS		
		70.0	70.0	410.470	416.679	3.600	3.600						
		71.0	71.0	416.679	422.871	3.600	3.600	0.0038	0.993	1.033	1.816		
		71.0	71.0	422.871	429.077	3.600	3.600	PASS	PASS	PASS	PASS		

Calibration Interval:
 Semi-Annual: K
 BI-monthly:
 Other:

Standard Temperature (deg.F)
 Tstd = 60

Barometric Pressure (in.Hg)
 Initial: 29.89
 Final: 29.89
 Pbar_{avg}: 29.89

Orifice Series No.	Run Time (min)	CRITICAL ORIFICE				DRY GAS METER				CALCULATIONS			
		Orifice K-factor	Tested Vacuum (in.Hg)	Ambient Temp (°F)	Flowrate Grm (SCFM)	Corrected Volume (cu.ft.)	Orifice dH (in.H2O)	AVG Temp (°F)	NET Volume (cu.ft.)	Flowrate Grm (SCFM)	Corrected Volume (SCF)	Coefficient Y _{std} (0.95 < Y _{std} < 1.05)	Orifice dH@ (in.H2O)
33	28	0.1549	28.50	66.0	0.2021	5.690	0.140	67.00	5.829	0.196	5.456	1.0375	1.905
33	28	0.1549	28.50	66.0	0.202	5.654	0.140	67.00	5.521	0.196	5.447	1.0380	1.908
33	28	0.1549	28.50	66.0	0.202	5.654	0.140	67.50	5.626	0.196	5.466	1.0382	1.908
52	12	0.3769	23.00	66.0	0.491	5.896	0.760	68.00	5.713	0.470	5.635	1.0464	1.752
52	12	0.3769	23.00	66.0	0.491	5.896	0.760	68.00	5.713	0.470	5.635	1.0464	1.752
52	12	0.3769	23.00	67.0	0.491	5.891	0.760	68.50	5.703	0.468	5.620	1.0482	1.753
63	7	0.5890	20.50	67.0	0.767	5.370	1.900	69.00	5.220	0.738	5.153	1.0421	1.803
63	7	0.5890	20.50	67.0	0.767	5.370	1.900	69.00	5.241	0.738	5.174	1.0379	1.803
63	7	0.5890	20.50	67.0	0.767	5.370	1.900	69.50	5.227	0.738	5.155	1.0416	1.802
73	6	0.8109	18.00	68.0	1.055	6.331	3.600	70.00	6.209	1.024	6.143	1.0305	1.818
73	6	0.8109	18.00	68.0	1.055	6.331	3.600	70.50	6.192	1.020	6.121	1.0343	1.818
73	6	0.8109	18.00	68.0	1.055	6.331	3.600	71.00	6.206	1.021	6.129	1.0329	1.814

* Critical Orifice used. Note: This Apex Meter Box, Console Model# XC-522 does not have a temperature sensor at the inlet. Hence, DGM inlet columns are intentionally left blank.

BI-Monthly Field Dry Gas Meter Calibration*

Calibration Date: 7/10/2019

Orifice Series: 62.63
 Serial Number: AE/AE₂
 Cell Type: BI-Monthly

Calibrated by: L. Bernow
 (signature):
 Reviewed by:

SEMI TO BI CHECK		DRY GAS METER CALIBRATION FACTOR	ORIFICE CALIBRATION FACTOR
(±2% of Y)	(±2% of Y)	Y	dH@
1.0587	1.0171	Y _{ds} = 1.0483	dH@ = 1.508
PASS			

DRY GAS METER READINGS									
DGM INLET		DGM OUTLET		Meter Reading		Orifice Reading		QUALITY CONTROL CHECKS	
Initial (°F)	Final (°F)	Initial (°F)	Final (°F)	Initial (cu.ft.)	Final (cu.ft.)	Initial (in.H ₂ O)	Final (in.H ₂ O)	(Y _{in,max} - Y _{in,min}) / Y _{in} < 0.010 **	Average Coeff. Y _{fmj}
75.0	77.0	74.0	78.0	63,915	69,650	0.620	0.620	0.0018	1.046
77.0	78.0	76.0	77.0	69,650	75,411	0.620	0.620	PASS	PASS
78.0	79.0	77.0	78.0	75,411	81,177	0.620	0.620	PASS	PASS
79.0	81.0	78.0	79.0	81,177	88,439	1.700	1.700	0.0051	1.048
81.0	82.0	79.0	80.0	88,439	91,666	1.700	1.700	PASS	PASS
82.0	83.0	80.0	80.0	91,666	96,947	1.700	1.700	PASS	PASS

CRITICAL ORIFICE											
Orifice Series No.	Run Time (min)	Tembed Vacuum (in.Hg)	Ambient Temp. (°F)	Corrected		Orifice dH (in.H ₂ O)	AVG Temp. (°F)	NET Volume (cu.ft.)	Corrected		Coefficient Y _{fmj} (0.85 < Y _{fmj} < 1.05)
				Orifice K-factor	Volume (cu.ft.)				Flowrate Q _{fm} (SCFM)	Volume (SCF)	
52	12	24.0	74.0	0.3769	5,885	0.620	76.50	5,735	0.467	5,807	1.0486
52	12	24.0	74.0	0.3769	5,885	0.620	77.00	5,781	0.468	5,517	1.0478
52	12	24.0	75.0	0.3769	5,880	0.620	78.00	5,766	0.468	5,611	1.0479
63	7	21.5	78.0	0.5890	5,355	1.700	79.25	5,262	0.732	5,122	1.0454
63	7	21.5	76.0	0.5890	5,355	1.700	80.50	5,257	0.728	5,105	1.0488
63	7	21.5	77.0	0.5890	5,360	1.700	81.25	5,251	0.728	5,093	1.0505

* Critical Orifice used.

BI-Monthly Field Dry Gas Meter Calibration*

Calibration Date: 8/2/2019

Office Series: 52,63
 Serial Number: AE/AE₂
 Cal Type: BI-Monthly

Calibrated by: JO
 (signature)
 Reviewed by:

SEMI TO BI CHECK (+2% of Y) 1.0584	(-2% of Y) 1.0168	PASS	DRY GAS METER CALIBRATION FACTOR Y Y _{ds} = 1.0344	ORIFICE CALIBRATION FACTOR dH@ dH@ = 1.589

DRY GAS METER READINGS										
DGM INLET	DGM OUTLET		Meter Reading		Orifice Reading		QUALITY CONTROL CHECKS			
	Initial (°F)	Final (°F)	Initial (cu.ft.)	Final (cu.ft.)	Initial (in.H2O)	Final (in.H2O)	(Y _{fm,max} - Y _{fm,min}) < 0.010 **	0.98 < (Y _{fm} /Y _{fm}) < 1.02	Average Coeff. Y _{fm}	dH@ _{avg} < (dH@) ± U.1b)
N/A	81.0	82.0	149,279	155,103	0.680	0.680				
	82.0	83.0	155,103	160,956	0.680	0.680	0.0042	1.001	1.035	1.571
	83.0	84.0	160,956	166,820	0.680	0.680	PASS	PASS	PASS	PASS
N/A	84.0	85.0	166,820	172,180	1.700	1.700				
	85.0	86.0	172,180	177,529	1.700	1.700	0.0046	0.999	1.033	1.806
	86.0	87.0	177,529	182,865	1.700	1.700	PASS	PASS	PASS	PASS

Orifice Series No.	Run Time (min)	CRITICAL ORIFICE				DRY GAS METER				CALCULATIONS		
		Orifice K-factor	Tested Vacuum (in.Hg)	Ambient Temp. (°F)	Flowrate Q _{fm} (SCFM)	Flowrate Q _{fm} (SCFM)	NET Volume (cu.ft.)	AVG Temp. (°F)	Orifice dH (in.H2O)	Coefficient Y _{fm} < 1.05	Orifice dH@ (in.H2O)	
52	12	0.3769	26.0	81.0	0.484	5.812	81.50	0.680	0.466	5.824	1.0382	1.572
52	12	0.3769	26.0	82.0	0.484	5.806	82.50	0.680	0.468	5.833	1.0340	1.572
52	12	0.3769	26.0	82.0	0.484	5.806	83.50	0.680	0.468	5.864	1.0340	1.589
63	7	0.5890	23.5	82.0	0.756	5.293	84.50	1.700	0.734	5.360	1.0305	1.611
63	7	0.5890	23.5	82.0	0.756	5.283	85.50	1.700	0.731	5.349	1.0345	1.608
63	7	0.5890	23.5	82.0	0.756	5.293	86.50	1.700	0.731	5.358	1.0351	1.605

* Critical Orifice used.



BI-Monthly Field Dry Gas Meter Calibration*

Calibration Date: 7/9/2019

Orifice Series: 52,63
 Serial Number: AE/AE₂
 Cal Type: BI-Monthly

Calibrated by: Will Brown
 (signature):
 Reviewed by:

SEMI TO BI CHECK (+2% of Y)	1.0003	DRY GAS METER CALIBRATION FACTOR Y	ORIFICE CALIBRATION FACTOR dH@
	PASS		
(-2% of Y)	1.0187		
	PASS		

DRY GAS METER READINGS				QUALITY CONTROL CHECKS				DGM ID:
DGM INLET	DGM OUTLET	Meter Reading		Orifice Reading		Average Coeff. Y _{avg}	dH@ _{avg} < (dH@ ± 0.15)	A-3
		Initial (cu.ft.)	Final (cu.ft.)	Initial (in.H2O)	Final (in.H2O)			
Initial (°F)	Final (°F)	Initial (cu.ft.)	Final (cu.ft.)	Initial (in.H2O)	Final (in.H2O)	(Y _{in,max} - Y _{in,min}) < 0.010 **		Serial #: 1612035
N/A	N/A	73.0	74.0	0.770	0.770	1.02		Semi A Yfnc: 1.0395
N/A	N/A	74.0	75.0	0.770	0.770	1.003		Calibration Interval:
N/A	N/A	75.0	76.0	0.770	0.770	PASS		Bi-monthly: x
N/A	N/A	76.0	77.0	0.770	0.770	1.045	1.778	Standard
N/A	N/A	77.0	78.0	0.770	0.770	PASS	PASS	Temperature (deg.F)
N/A	N/A	78.0	79.0	0.770	0.770	0.997	1.803	Told = 60
N/A	N/A	78.0	79.0	0.770	0.770	PASS	PASS	Barometric Pressure (in.Hg)
N/A	N/A	79.0	910.120	1.900	1.900	PASS	PASS	Phar: 30.04

Orifice Series No.	Run Time (min)	CRITICAL ORIFICE				DRY GAS METER				CALCULATIONS	
		Orifice K-factor	Tested Vacuum (in.Hg)	Ambient Temp. (°F)	Orifice dH (in.H2O)	AVG Temp. (°F)	NET Volume (cu.ft.)	Corrected		Coefficient Y _{fsj} (0.85 < Y _{fsj} < 1.05)	Orifice dH@ (in.H2O)
								Flowrate Qfm (SCFM)	Volume (SCF)		
52	12	0.3769	24.0	76.0	0.770	73.50	5.735	0.468	5.828	1.0434	1.761
52	12	0.3769	24.0	76.0	0.770	74.50	5.734	0.468	5.815	1.0453	1.778
52	12	0.3769	24.0	77.0	0.770	75.50	5.742	0.468	5.612	1.0450	1.778
63	7	0.5890	22.0	78.0	1.900	78.50	5.285	0.738	5.150	1.0371	1.808
63	7	0.5890	22.0	78.0	1.900	77.50	5.270	0.735	5.148	1.0360	1.803
63	7	0.5890	22.0	78.0	1.900	78.50	5.285	0.738	5.151	1.0370	1.799

* Critical Orifices used. Note: This Apex Meter Box, Console Model # XC-522-D does not have a temperature sensor at the inlet. Hence, DGM inlet columns are left intentionally blank.

APPENDIX H
FACILITY PROCESS DATA

Facility Process Data

Charge During CARB Method 436 Metals Testing				
Date	Test	Furnace #	Materials	Weight (lbs)
8/13/2019	Metals Run 1	#3 Furnace	25CH	6000
8/13/2019	Metals Run 2	#3 Furnace	25CH	6000
8/14/2019	Metals Run 3	#3 Furnace	25CH	6000
		#4 Furnace	25CH	7000

Charge During CARB Method 425 Chromium Testing				
Date	Test	Furnace #	Materials	Weight (lbs)
8/14/2019	Chromium R1	#3 Furnace	25CH	6000
		#4 Furnace	25CH	7000
8/14/2019	Chromium R2	#3 Furnace	25CH	6000
		#4 Furnace	25CH	7000
8/15/2019	Chromium R3	#3 Furnace	25CH	6000

Charge During SCAQMD Method 5.1 PM Testing				
Date	Test	Furnace #	Materials	Weight (lbs)
8/16/2019	PM Testing	#3 Furnace	25CH	6000
		#4 Furnace	25CH	7000

From: [REDACTED]
 Sent: Monday, December 02, 2019 11:59 AM
 To: Charles Figueroa
 Cc: [REDACTED], Tulasi Gyawali
 Subject: Re: AQMD C Source Testing

In #3 furnace only, the following was melted during the test periods.

- 8/13 three 6000# heats of chrome iron. total 18,000# melted.
- 8/14 three 6000# heats of chrome iron. total 18,000# melted.
- 8/15. four 6000# heats of chrome iron. total 24,000# melted.

Hope this helps.

[REDACTED]
 [REDACTED]
 [REDACTED]
 [REDACTED]
 [REDACTED]

On Mon, Dec 2, 2019 at 9:08 AM Charles Figueroa <Charles@almegaenv.com> wrote:

[REDACTED]

Do you have information as to the loading in Furnace 3 during those test periods ?

8/13	08:50 – 10:55	11:55 – 14:00
8/14	08:25 – 10:30	11:25 – 13:30
8/15	08:10 – 10:15	10:55 – 13:10
8/16	07:40 – 08:56	

How many batches and lbs/batch ?

Thanks

Spectrographic Analysis

Date 8/14/19

Temp: 741
Humid: 70 %
Time: 3:00AM

OPERATOR
signed Matc
signed _____

Furnace #	Alloy	Sample #	Argon		C	Cr	Si	SPECTRO Argon		Mo	Cu	S	P	Released by
			psi (M)	psi (B)				Mn	Ni					
3	25CH	1	3.123	25.826	3.57	596	243	.071	.058	.025	.021	Matc		
4	25CH	2	2.54	25.658	722	503	291	.091	.073	.026	.019	Matc		
3	25CH	3	2.200	25.548	374	557	278	wt: .087	.067	.018	.019	Matc		
4	25CH	4	3.148	26.00	365	672	251	.15	.080	.027	.019	Matc		
4	25CH	5	3.178	25.960	370	598	257	.071	.108	.028	.020	Matc		
4	25CH	6	3.069	26.177	273	493	254	.065	.120	.025	.020	Matc		
3	25CH	7	3.603	26.967	561	617	288	1.547	.181	.016	.025	Matc *		
4	25CH	8	2.158	26.063	872	wt: 577	255	.068	.157	.025	.020	Matc		

END OF SHIFT REMARKS AND SIGNATURE: 6140168 2619°F.

Spectrographic Analysis

Date 8/15/19

Temp: 741 %
Humid: 70 %
Time: 300 min

OPERATOR
signed [Signature]
signed

Furnace #	Alloy	Sample #	Argon		C	Cr	Si	SPECTRO				S	P	Released by
			psi (M)	psi (B)				Mn	Ni	Mo	Cu			
3	25CH	1	3.09	25.969	.500	.501	.264	.188	.077	.074	.055		MAC	
3	25CH	2	3.082	26.767	.168	.570	.277	.101	.099	.077	.087		MAC	
3	25CH	3	3.100	26.138	.382	.848	.266	.121	.070	.076	.044		MAC	
3	25CH	4	2.934	26.000	.364	.177	.279	.106	.084	.026	.035		MAC	

END OF SHIFT REMARKS AND SIGNATURE:



Spectrographic Analysis

Date 8/16/19

OPERATOR

Temp: 741
Humid: 70 %
Time: 3:00:00

signed hmk
signed _____

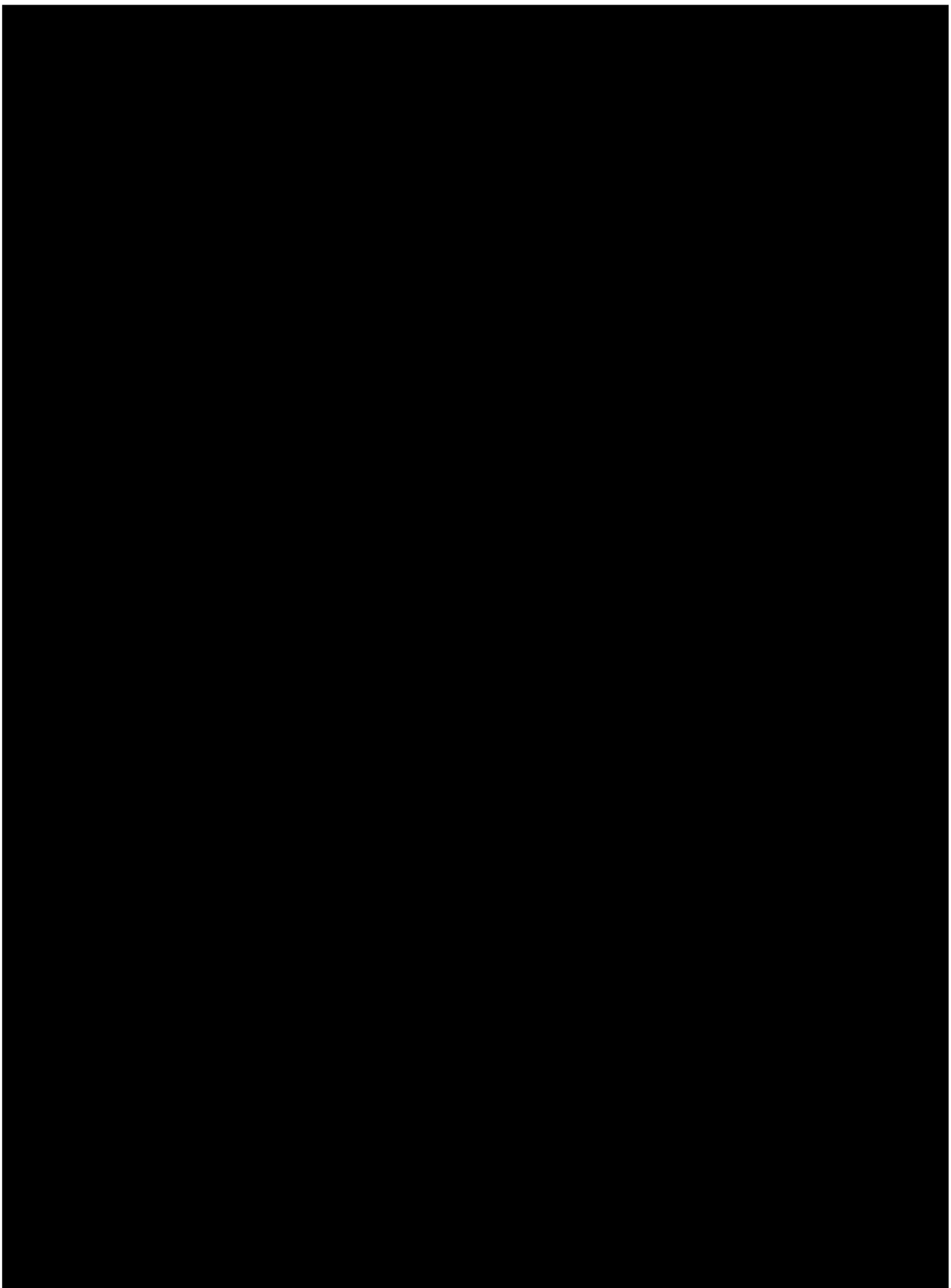
Furnace #	Alloy	Argon		SPECTRO		Argon		psi (M)		psi (B)		S	P	Released by
		Sample #	C	Cr	Si	Mn	Ni	Mo	Cu	psi (M)	psi (B)			
21	K26	1	2,656	26,00	.445	.777	.254	.785	.135	.025	.018			hmk
41	K26	2	2,725	26,178	.451	.767	.285	.402	.124	.028	.018			hmk
3	25CA	3	2,577	25,477	.399	.494	.248	.066	.0124	.025	.021			hmk
3	25CA	4	3,018	25,770	.401	.584	.254	.079	.10	.026	.021			hmk
41	26K	5	2,800	26,282	.267	.775	.290	.184	.111	.028	.019			MAL
3	25CA	6	2,537	25,612	.362	.464	.266	.098	.105	.027	.036			MAL
4	25CM	7	2,484	26,640	.316	.647	.270	.217	.101	.026	.018			MAL
3	25CH	8	3,082	26,100	.367	.504	.262	.067	.114	.029	.031			MAL

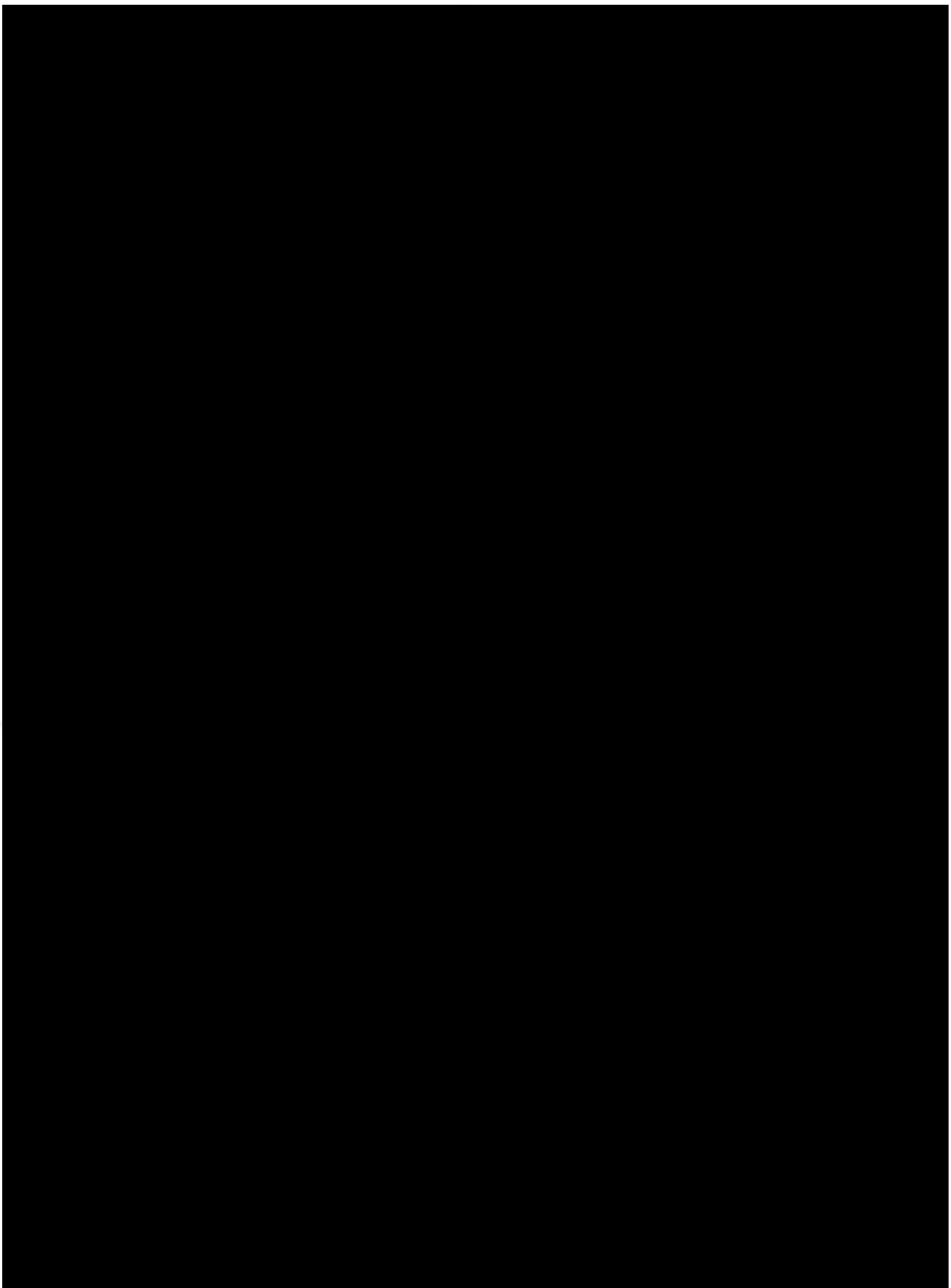
END OF SHIFT REMARKS AND SIGNATURE:

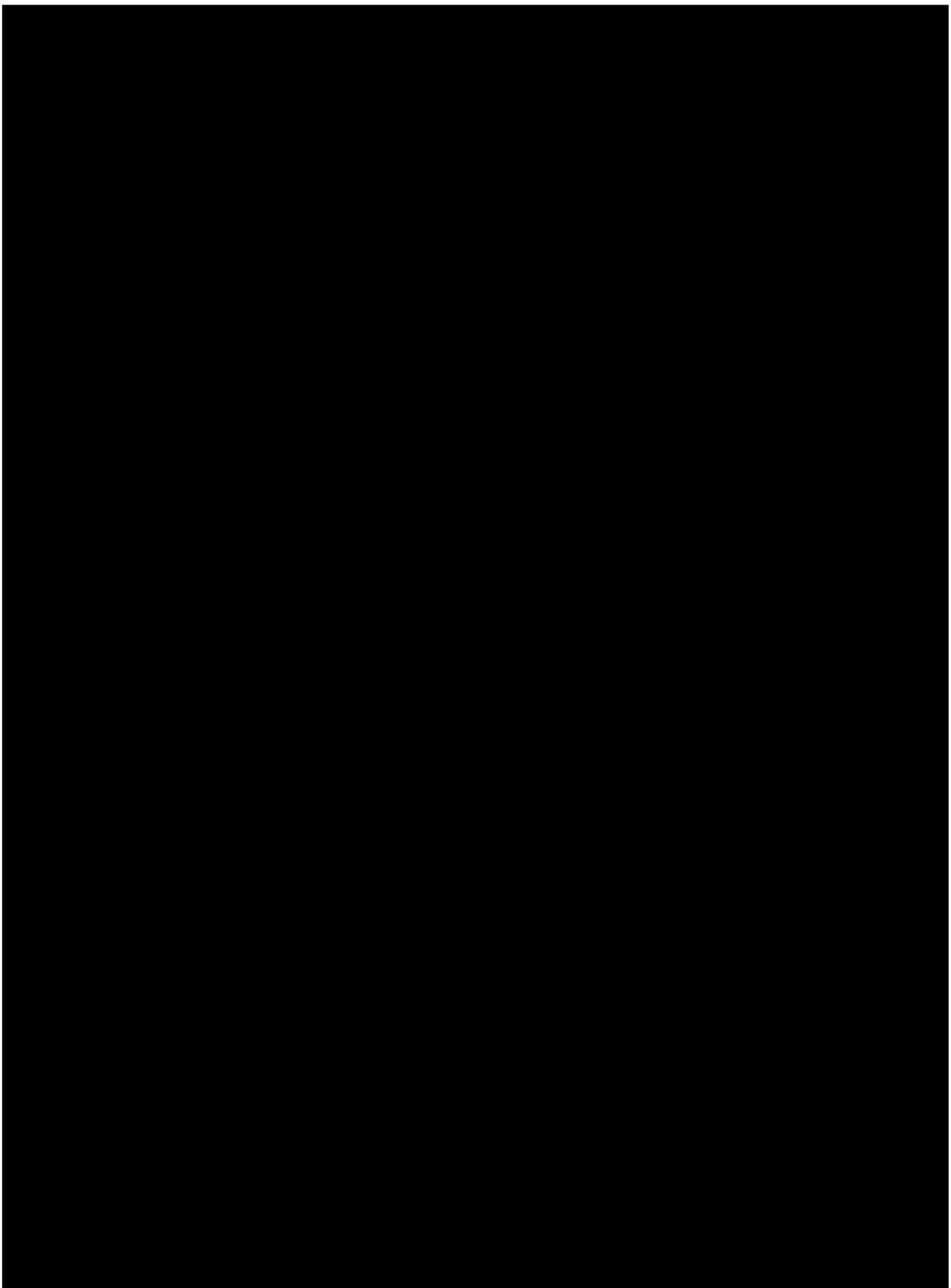
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12	2.80	88
11	2.50	89
10	2.90	88
9	2.90	88
8	2.70	87
7	2.50	88
6	1.40	87
5	0.75	87
4	1.20	87
3	1.60	75
2	1.90	70
1	2.00	69

12	1.90	87
11	2.35	87
10	2.40	87
9	2.50	87
8	2.20	87
7	2.10	87
6	1.60	87
5	1.50	87
4	1.30	85
3	1.45	78
2	1.60	71
1	1.60	70







APPENDIX I
SCAQMD SOURCE TEST PLAN



South Coast Air Quality Management District

21865 Copley Drive, Diamond Bar, CA 91765-4178
(909) 396-2000 • www.aqmd.gov

SOURCE TEST PLAN TO BE CONDUCTED AT

METAL MELTING FACILITY A

METAL MELTING FACILITY B

METAL MELTING FACILITY C

TO DETERMINE PARTICULATE MATTER (PM), ARSENIC, CADMIUM,
NICKEL, CHROMIUM, AND HEXAVALENT CHROMIUM (Cr⁺⁶)
EMISSIONS FROM CHROMIUM ALLOY MELTING OPERATIONS

ISSUED: November 21, 2018

REVISED: March 27, 2019

REVIEWED BY:

A handwritten signature in blue ink, appearing to read "Michael Garibay".

Michael Garibay
Acting Source Testing Manager

SOURCE TEST ENGINEERING BRANCH

SCIENCE & TECHNOLOGY ADVANCEMENT

Creating the air that we breathe...

Metal Melting Test Plan

-2-

Date: 3/27/19

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INTRODUCTION

Ambient monitoring in the city of Paramount in 2016 and 2017 indicated the presence of elevated levels of hexavalent chromium. During an investigation of the emission sources, the SCAQMD identified hexavalent chromium emissions were being generated by sources including heat treating and forging facilities. Screening source tests were performed on heat treating and forging furnaces processing metals or using materials that contained chromium at several facilities. Results showed elevated hexavalent chromium levels in the outlet of the furnaces which were operated between 1,725 to 2100°F. These temperatures are lower than those experienced during metal melting operations.

An internal review was initiated for previously conducted source tests at metal melting facilities. Most of the source tests on file only tested for elemental chromium and did not perform the separate test required to determine hexavalent chromium emissions as they were not suspected from this process. SCAQMD staff was able to identify one metal melting facility which was tested for both total chromium and hexavalent chromium using CARB Method 425. Review of this test indicated that conversion of chromium to hexavalent chromium did occur and result in emissions of hexavalent chromium during the melting operation.

SCAQMD staff initiated the rule development process to amend Rule 1407 to address toxic air contaminant emissions from ferrous metal melting operations and update existing requirements for non-ferrous metal melting operations currently regulated under the rule. Through working group meetings with industry stakeholders it was requested that the rule be separated in to two rules for ferrous and non-ferrous metal melting. After additional input and working group meetings SCAQMD staff decided to bifurcate the rule and reclassify characterization in to non-chromium alloy (Rule 1407) and chromium alloy (Rule 1407.1) metal melting.

Additional data from melting operations of metals with a chromium content greater than 0.5% is needed to quantify the conversion rate of chromium to hexavalent chromium and quantify toxic air contaminant emissions from these facilities to aid in the rulemaking process.

Three facilities have agreed to allow source testing for the purposes of collecting this data. Testing will be performed by a third party source test contractor. The purpose of this test plan is to allow for the source test contractors to provide bids as part of the RFP process, while eliminating the need for multiple contractors to visit the facilities who have volunteered as host sites for the source testing. Testing contractors must be SCAQMD Laboratory Approval Program certified for SCAQMD Methods 1-5 to be able to participate in the RFP process and testing upon award of contract.

Metal Melting Test Plan

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During the source testing at each facility, control system inlet and outlet emissions and associated emission rates will be determined for the following:

- Particulate Matter (PM)
- Total Chromium (Cr)
- Hexavalent Chromium (Cr⁺⁶)
- Arsenic (As)
- Cadmium (Cd)
- Nickel (Ni)

Testing will be performed according to SCAQMD Method 5.1, CARB Method 425, and CARB Method 436. Flow rates will be determined according to SCAQMD Methods 1-4, with the use of EPA Method 5D for the outlet of the HEPA filters at one of the three facilities.

EQUIPMENT AND PROCESS DESCRIPTION

Pursuant to the agreement with the participants to keep the names of the host facilities anonymous, they will be identified as Facilities A, B, and C. [REDACTED]

Metal Melting Facility A

Metal melting Facility A uses electric induction furnaces for the processing of materials including Brass, Zinc, Steel, Stainless Steel, Iron, Aluminum, Cobalt, and Nickel. The facility has eight electric induction furnaces in three sizes as follows:

- 800 lb material capacity with a power rating of 250 kW
- 3,000 lb material capacity with a power rating of 350 kW
- 4,500 lb material capacity with a power rating of 1,000 kW (shared power supply)

[REDACTED] A heat cycle (or “heat”) begins when the metal is placed in the electric induction furnace. Electrical current is applied and the material becomes molten. Testing will be performed during heats of 316 stainless steel. The stainless steel materials are typically melted in one of the 4,500 lb furnaces. Typical temperatures are in the 3000°F range. During the melting process emissions are captured by an exhaust system which mounts to the furnace lid and utilizes a slot design. Suction is provided by the blower which is part of the baghouse and HEPA system. The HEPA filters are mounted in an enclosure above the baghouse and exhaust through two rectangular openings on either side of the enclosure. Because the exhaust does not exit through an exhaust stack special consideration must be given for the outlet testing.

[REDACTED] A typical heat lasts for approximately 2 hours. Each furnace has individual exhaust ducting allowing for testing during a specific heat before being combined in to a common exhaust header. The baghouse and HEPA filter system controls emissions from the eight electric induction furnaces, five casting machines, one Hawley system, four mold spray and coating stations. [REDACTED]

A complete list of process operating parameters to be obtained for the period during testing as well as results reporting requirements is located in **Appendix A**. A basic process flow diagram has been included in **Appendix B**.

Metal Melting Facility B

Metal melting facility B uses electric induction furnaces for the processing of primarily stainless steel. The facility has two 300 lb capacity electric induction furnaces but typically only uses one at a time. The facility makes small precision parts primarily through an investment casting process.

The furnace is loaded with 17-4 PH stainless steel and the heat begins. Electrical current is applied and the material becomes molten. Typical temperatures are in the 3000°F range during the melting process. Castings are placed in an oven which serves the purpose of removing the wax core from the casting while simultaneously preheating the casting to 1600-1800°F to prevent thermal shock during the pouring process. The molten metal from the furnace is poured in to a ladle before being poured in to the casting mold.

Emissions from the furnace are collected by a hood placed directly above each furnace. The hoods have blast gates installed which can be closed during emissions testing to prevent room air dilution from the adjacent non-operational unit. The facility has agreed to install a hood extension on the furnace in use to ensure that all furnace emissions will be captured during the source test operation. Hood emissions are currently routed through a baghouse. The facility is currently in the process of a control system upgrade to install a HEPA filtration downstream of the baghouse for improved emission control. It is anticipated that the HEPA system will be completed around January of 2019.

The facility does approximately 6 heats a day. Each heat follows a repeating cycle of roughly one hour on during the melt followed by a period of roughly one hour with the furnace off.

A complete list of process operating parameters to be obtained for the period during testing as well as results reporting requirements is located in **Appendix A**. A basic process flow diagram has been included in **Appendix B**.

Metal Melting Facility C

Metal melting facility C uses electric induction furnaces for the processing of white iron, cast iron, ductile iron, and stainless steel. The facility has four electric induction furnaces in sizes as follows:

- 7,000 lb material capacity with a power rating of 1,500 kW
- 6,000 lb material capacity with a power rating of 1,500 kW
- 4,000 lb material capacity with a power rating of 1,000 kW
- 2,000 lb material capacity with a power rating of 400 kW

90% of facility operations involve melting of the various irons and approximately 10% percent of operations are stainless steel melts. Raw materials for iron melts are frequently re-runs while the stainless melts tend to be new certified material. The stainless steel processed at the facility is CF8M, CF3M, CF8, and CF3. The facility normally runs 2 furnaces at a time, most frequently the 7,000 lb and 6,000 lb furnaces. Stainless steels are only processed in either the 4,000 lb or 2,000 lb furnace. The furnaces are loaded with the applicable material and the heat begins. Electrical current is applied and the material becomes molten. Typical temperatures are in the 2400-2700°F range during iron melting operations and in the 3000°F range during stainless steel melting operations. Material from the furnace is poured in to pre-heated ladles for transport by forklift to the casting area. All casting at the facility is green sand casting. The casting area is in a separate location within the building.

During the melting process emissions are captured by an exhaust system which mounts to the furnace and utilizes a slot design. Suction is provided by the blower which is part of the baghouse and HEPA system. Each furnace has a closable damper installed which allows for isolation from the system when a furnace is not in use. In the exhaust header there is one non closable exhaust hood which pulls room air in to the system. The HEPA filters are installed between the baghouse and the exhaust stack. The exhaust stack outlet in its current configuration undergoes multiple small angular changes prior to exit to the atmosphere. The facility has agreed to modify the outlet such that a straight run of duct will be provided downstream of the exhaust muffler to meet the requirements of at least two duct diameters downstream and one half of a diameter upstream of any flow disturbances.

The facility does approximately 4-5 heats a day. The iron heats performed in the 7,000 lb and 6,000 lb furnaces take 1.5 – 2 hours. The stainless heats performed in the smaller 4,000 lb and 2,000 lb furnaces take up to 3 hours.

A complete list of process operating parameters to be obtained for the period during testing as well as results reporting requirements is located in **Appendix A**. A basic process flow diagram has been included in **Appendix B**.

SAMPLING AND ANALYTICAL PROCEDURES

Two hour test runs at each location within the system will be performed based on the reference methods described below at the locations specified in Table 1. Refer to **Appendix B** for Facility photos depicting equipment, sample locations, and testing logistical notes.

Sampling times may need to be adjusted on the test days to match the facility's batch time for melting and pouring. It is anticipated these times will end up being close to the proposed two hours per run. Material samples will be collected by the facility and/or source test contractor SCAQMD at each facility corresponding to each heat which occurs during emissions testing. Samples should include all raw materials, molten material, final product, slag, dross, and baghouse catch. If any such samples are un-available at the time of testing, it should be noted in the final test report. The materials shall be properly identified and delivered to the SCAQMD for materials composition testing. Additionally, if the facility has performed in-house analysis for each or any sample(s) it should be provided to the SCAQMD. Results of material analysis conducted by SCAQMD will be provided to the contractor conducting testing (where applicable). Analysis of Weck Laboratory detection limits are satisfactory for meeting the objectives of the contract and the proposed rulemaking efforts. SCAQMD method reporting limits (MRL) will be adjusted to match Weck Laboratory for consistency.

Table 1: Sampling Details

Facility	Sample Location	Test Method	Number of Runs	Sample Ports	Sample Port Access
A	Inlet Header, For 4.5k lb. Furnace for Stainless Melting	SCAQMD Method 5.1	1	To Be Installed by Facility	Accessed by a removable floor grate from ground level.
		CARB Method 425	3		
		CARB Method 436	3		
A	Inlet Header, Upstream of Baghouse	SCAQMD Method 5.1	1	In Place	Can be reached with a ladder.
		CARB Method 425	3		
		CARB Method 436	3		
A	Exhaust Outlet, Downstream of Baghouse/HEPA Filters	SCAQMD Method 5.1	1	No Ports, Use EPA Method 5D	Accessible by facility owned man lift.
		CARB Method 425	3		
		CARB Method 436	3		

Facility	Sample Location	Test Method	Number of Runs	Sample Ports	Sample Port Access
B	Inlet Header, Upstream of Baghouse	SCAQMD Method 5.1	1	To Be Installed by Facility	Accessible from ground level.
		CARB Method 425	3		
		CARB Method 436	3		
B	Exhaust Outlet, Downstream of Baghouse/HEPA Filters	SCAQMD Method 5.1	1	To Be Installed by Facility	Will be accessible by a facility provided man lift.
		CARB Method 425	3		
		CARB Method 436	3		

Facility	Sample Location	Test Method	Number of Runs	Sample Ports	Sample Port Access
C	Inlet Header, Common to 6k, 4k and 2k lb. Furnaces for Stainless Melting	SCAQMD Method 5.1	1	To Be Installed by Facility	Accessible from raised floor.
		CARB Method 425	3		
		CARB Method 436	3		
C	Inlet Header, Common to all Furnaces, Upstream of Baghouse	SCAQMD Method 5.1	1	To Be Installed by Facility	Accessible from facility provided man lift or scaffolding.
		CARB Method 425	3		
		CARB Method 436	3		
C	Exhaust Outlet, Downstream of Baghouse/HEPA Filters	SCAQMD Method 5.1	1	To Be Installed by Facility	Accessible from facility provided man lift.
		CARB Method 425	3		
		CARB Method 436	3		

Gas Flow Rate

The gas velocity will be measured at the inlet duct and outlet duct* in accordance with SCAQMD Methods 1.1 and 2.1. This will be done using an S type Pitot tube, a differential pressure manometer, and a type "K" thermocouple with a digital potentiometer a diagram of this arrangement is presented in Figure 1 below as well as in the appropriate test method. The apparatus will be leak checked both before and after use by introducing a pressure head of at least 80 percent of full scale and blocking the flow at the Pitot tip. An observation of the resulting non diminishing pressure for at least 15 seconds at the manometer should be verified to confirm the absence of leaks in the system.

The velocity measurement location is at least two diameters downstream and one half diameter upstream of any flow disturbances. The sample traverse at each facility will be in accordance with SCAQMD Method 1.1. Traverse sampling is necessary for the determination of stack gas velocity. The number of traverse points must be determined in accordance with SCAQMD Method 1.1 for stacks with diameters greater than 12 inches.

The inlet and outlet* volumetric flow rate is calculated from the duct cross sectional area and average gas velocity. The absence of cyclonic flow conditions must be verified. The flow rate must be corrected to standard conditions using the measured duct temperatures and velocity pressures along with the barometric pressure measured with a calibrated aneroid barometer. The exhaust flow rate must also corrected to dry conditions using the moisture content as determined by SCAQMD Method 4.1 weight gain from the SCAQMD Method 5.1, CARB Method 425, and CARB Method 436 sample trains described in the following sections.

*Facility A does not have an exhaust stack, the HEPA filters are mounted in an enclosure directly on top of the baghouse. Exhaust exits from two rectangular openings in a horizontal direction on either side of the HEPA enclosure (see Figure 2 below for details). Due to the anticipated low velocity pressure exiting the baghouse/HEPA system EPA Method 5D must be used which allows for the velocity and exhaust flow to be determined at the inlet to the baghouse and then applied over the entire area of the exhaust. Isokinetic sampling rates and sampling probe nozzle size will need to be based on these calculations. If it turns out that the velocities can be measured at this location by pitot tube, then isokinetic rate can be set by the measured velocity heads.

Figure 1: Gas Velocity Measurement Apparatus

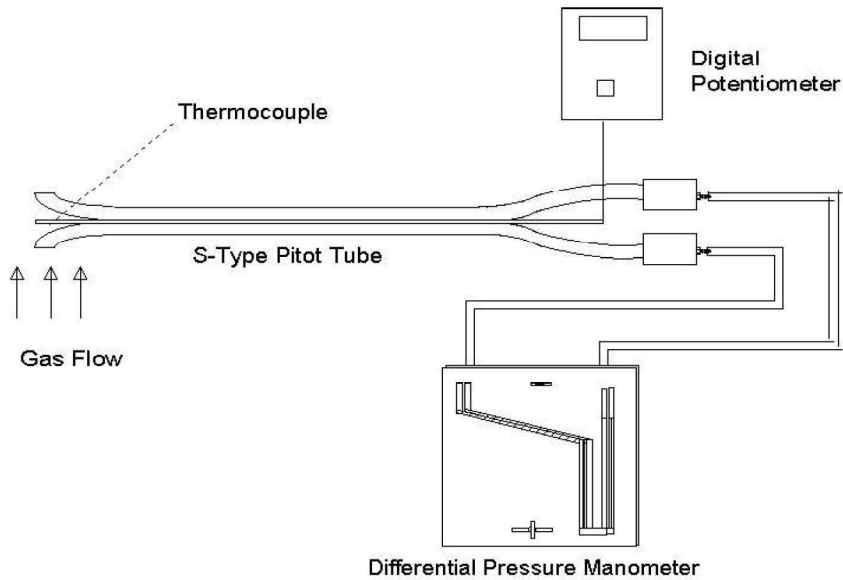
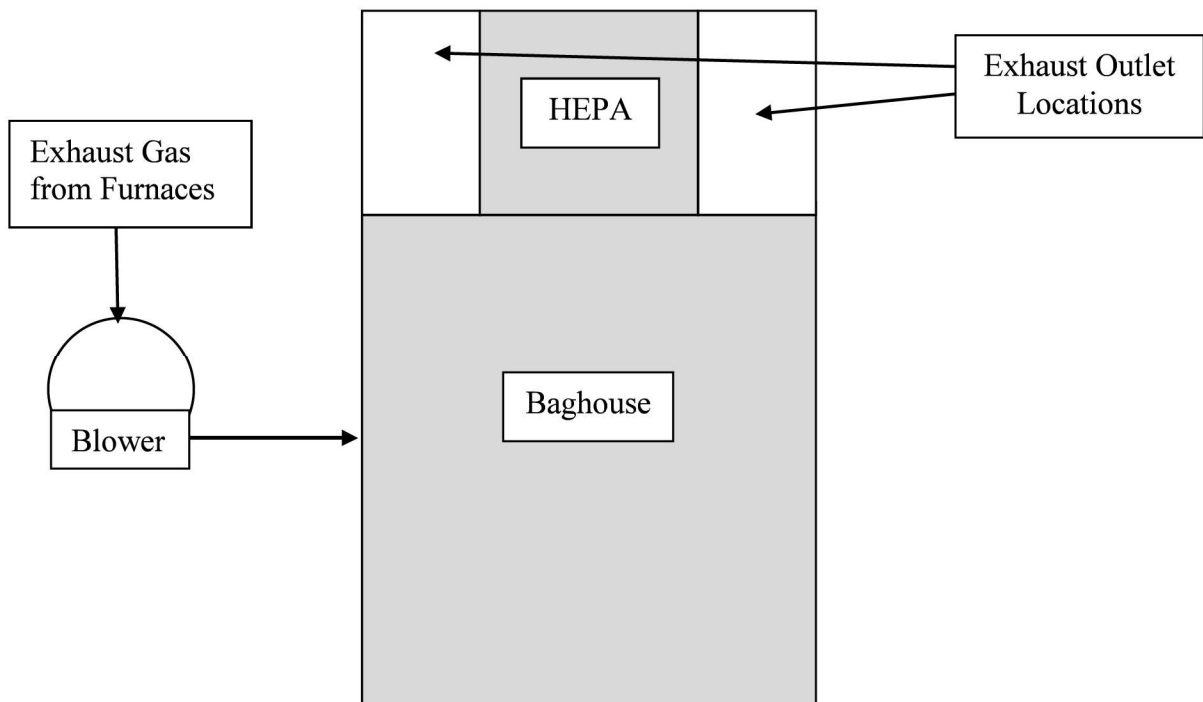


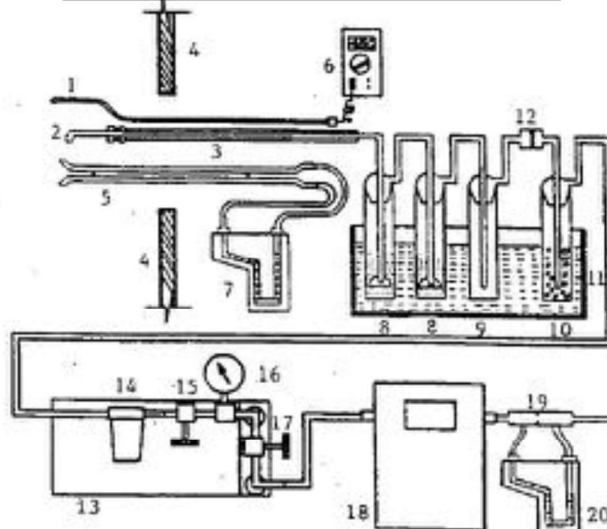
Figure 2: Facility A Exhaust Diagram (EPA Method 5D Required)



Particulate Matter Sampling

Samples are collected using SCAQMD Method 5.1. Particulate matter is withdrawn isokinetically from the source through a sample train by a metering system. Particulate matter is collected in impingers containing deionized water and on a backup filter. The impingers are contained in an ice bath to maintain a sampled gas Temperature of approximately 60°F. The filter is not heated. A diagram of the test apparatus is pictured in Figure 3 below. Total particulate matter mass is defined as the sum of the mass collected in the impingers and the probe, and on the filter after removal of combined water, plus extractable organic matter and sulfuric acid. Samples are analyzed for water gain, PM, acids, sulfates, and organics. For the purposes of this testing, the analysis should include the organic and acid/sulfate traditional analysis. Following analysis, samples shall be retained and made available for 3rd party inspection. This is requested with the understanding that portions of the analytical method are destructive and do not allow for samples to be split. A photograph of residue “inspection” of each sample should be taken prior to analysis. The SCAQMD will reserve the right to physically inspect the samples as necessary, while giving the Contractor ample notice. Although not required by the SCAQMD Method 5.1, optional field blank runs may be performed and analyzed.

Figure 3: Particulate Sampling Train



- | | |
|--|---|
| 1. Temperature Sensor | 11. Ice Bath |
| 2. Nozzle | 12. Filter |
| 3. Glass Lined Stainless Steel Probe | 13. Sealed Pump (Leak Free) |
| 4. S-type Pitot Tube | 14. Filter for Pump |
| 5. Stack Wall | 15. Metering Valve |
| 6. Temperature Sensor Meter | 16. Vacuum Gauge |
| 7. Pitot Tube Inclined Manometer | 17. By-pass Valve |
| 8. Impinger with 100 ml H ₂ O | 18. Temperature Compensated Dry Gas Meter |
| 9. Empty Bubbler | 19. Orifice |
| 10. Bubbler with Silica Gel | 20. Orifice Inclined Manometer |

Hexavalent Chrome Sampling

CARB Method 425 applies to the determination of hexavalent chromium (Cr⁺⁶) and total chromium (Cr) emissions from stationary sources. Emissions are collected from the source in an a sampling train consisting of a glass probe and nozzle connected by non-reactive tubing to the first of two Greenburg-Smith impingers each containing 100 ml of 0.1N sodium bicarbonate (NaHCO₃), an empty bubbler, a Teflon filter, and a bubbler containing tared silica gel desiccant (see Figure 4).

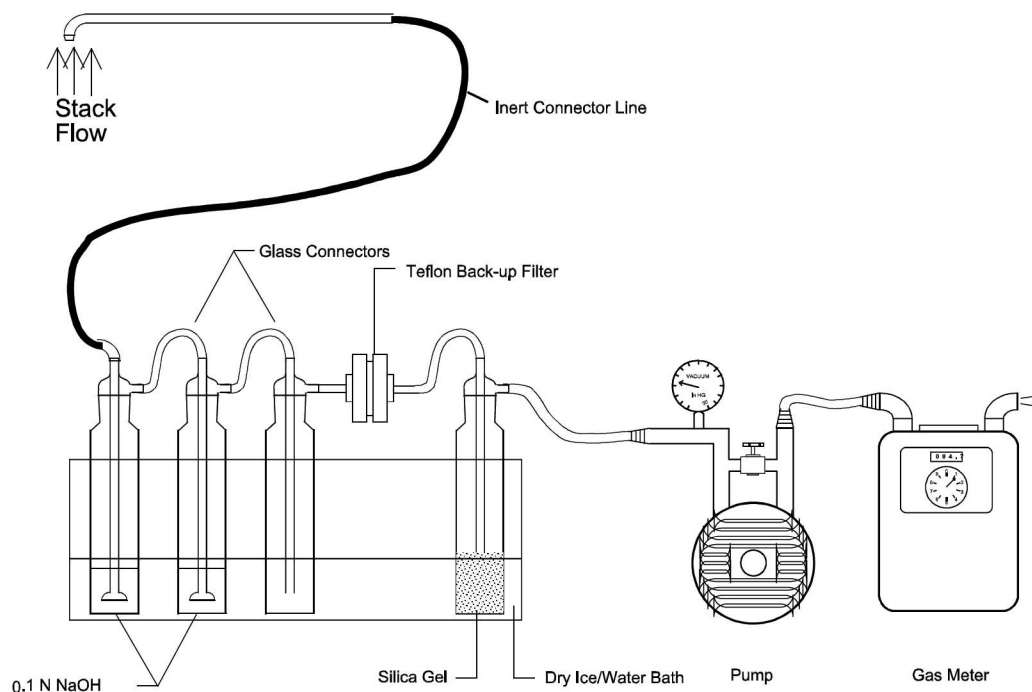
The same batch of 0.1N NaHCO₃ solution shall be used for field blanks, impinger sampling, sample recovery, preparation, extraction, and analysis. One batch of solution should be prepared for each facility. Substituting NaHCO₃ for NaOH is an approved Alternative Test Method as outlined in Sections 10 and 21 of CARB Method 425.

The impinger assembly must be connected to a vacuum pump and a calibrated dry gas meter. The sampling apparatus shall be checked for leaks both before and after sampling by blocking the flow at the probe tip. An observation of the resulting decrease in flow at the meter should be less than 0.02 cfm or four percent of the sampling rate indicated an acceptable leak rate. The impinger train must be contained within an ice bath to condense water and other condensable matter present in the sample stream.

The impinger train will be returned to the laboratory for recovery. The pH of the recovered solution must be verified as being greater than 8.0 as specified in CARB Method 425. Hexavalent chromium collected in the nozzle, probe, and impingers will be determined using ion chromatography with post column reactor (IC/PCR). The probe and line rinse shall be separated and itemized by weight separately from the rest of the analysis. For each facility a minimum of one field blank run shall be analyzed. Each blank sample train shall be brought onto the test site, assembled, leak checked, and analyzed as above for quality control purposes. No sampling should occur on the blank train.

Following testing, CARB Method 425 samples must be recovered within 24 hours. Samples should be split with remaining aliquots after primary analysis to be held for possible 3rd party analysis. Holding time for Method 425 following recovery is 14 days if stored at < 4° C.

Figure 4: CARB Method 425 Sample Train



Multiple Metals Sampling

CARB Method 436 applies to the determination of aluminum (Al), antimony (Sb), arsenic (As), barium (Ba), beryllium (Be), cadmium (Cd), chromium (Cr), cobalt (Co), copper (Cu), lead (Pb), manganese (Mn), mercury (Hg), nickel (Ni), phosphorus (P), selenium (Se), silver (Ag), thallium (Tl), vanadium (Vn), and zinc (Zn) stack emissions from stationary sources. For this source test the metals of specific interest are Cr, As, Cd, and Ni. Sampling is conducted using a modified CARB Method 5 sample train. The stack sample is withdrawn isokinetically from the source, with particulate emissions collected in the heated probe and on a heated filter maintained in the temperature range of $248 \pm 25^{\circ}\text{F}$ and gaseous emissions collected in a series of chilled impingers containing an aqueous solution of dilute nitric acid combined with dilute hydrogen peroxide in two impingers (analyzed for metals). If necessary for sampling the vertical port on horizontal ducts, the addition of flexible Teflon tubing between the heated probe and heated filter, or sampling train sections may be allowed; depending on sampling location.

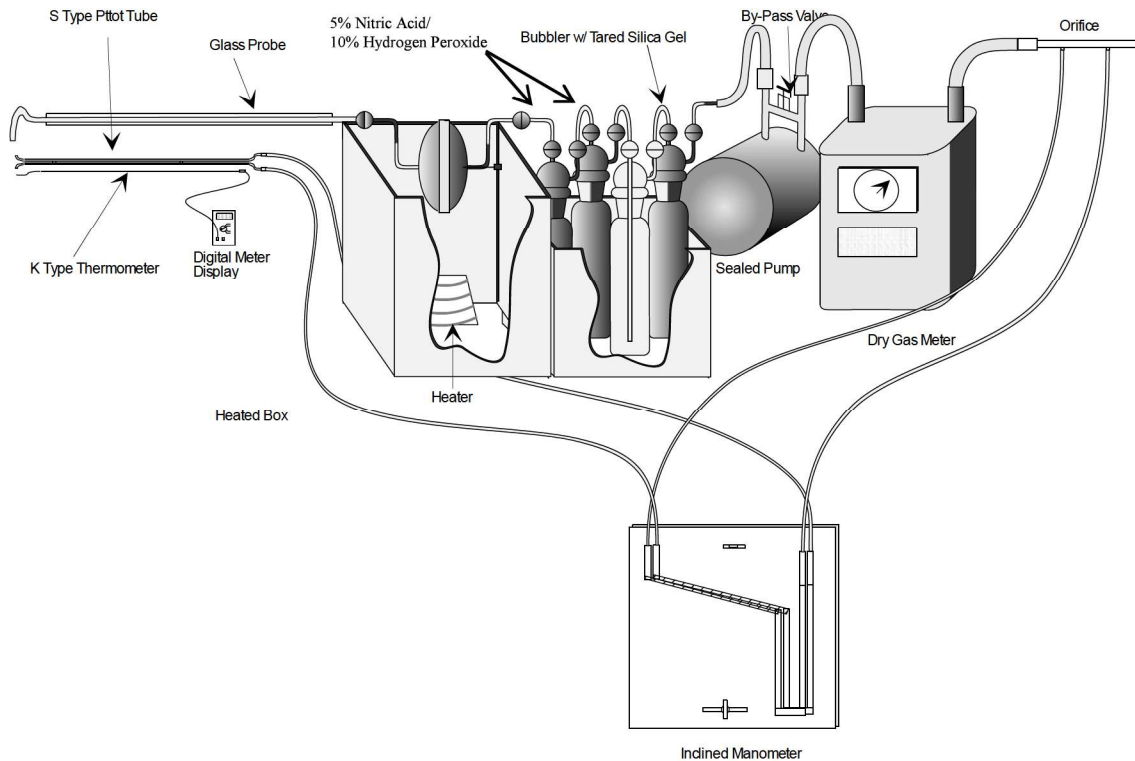
The same batch of 5% HNO₃/10% H₂O₂ solution shall be used for field blanks, impinger sampling, sample recovery, preparation, extraction, and analysis. One batch of solution should be prepared for each facility.

For each facility a minimum of one field blank run shall be analyzed. Each blank sample train shall be brought onto the test site, assembled, leak checked, and analyzed for quality control purposes. No sampling should occur on the blank train.

Sampling train (see Figure 5) components are recovered into separate front and back half fractions and acid digested using conventional Parr^R Bomb or microwave digestion techniques to dissolve inorganics and to remove organic constituents that may create analytical interferences.

Following testing Method 436 samples must be recovered as soon as practical. Samples should be split with remaining aliquots after primary analysis to be held for possible 3rd party analysis. Holding time for Method 436 following recovery is 60 days.

Figure 5: CARB Method 436 Sample Train



After digestion, portions of the probe, filter and nitric acid/hydrogen peroxide digestion solutions are combined into a single front half composite and analyzed for Cr, As, Cd, and Ni. Refer to the test method document for additional details.

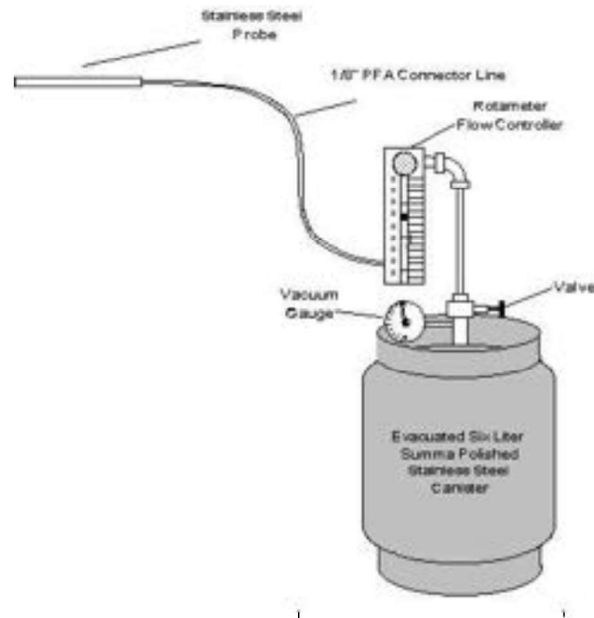
Capture Efficiency

During source testing capture efficiency testing will be performed by SCAQMD personnel (not required for contractor to perform this testing) to determine the efficiency of the collection system. A hot-wire anemometer, vane anemometer, or other device capable of directly measuring air velocity, will quantitatively measure the air velocity at the slots or hood, as applicable, of the furnace emissions collection system. Additionally, a qualitative test shall be performed and photo or video recorded using smoke tubes or smoke sticks. Documentation of these measurements will be provided to the test contractor following measurement.

Integrated Gas Sampling

An integrated gas sample will be taken at each sample location and analyzed for CO, CO₂, and O₂. The sampling procedure shall be according to SCAQMD Method 10.1. The sampling apparatus should consist of a stainless steel probe, a Teflon line, and a 6-liter summa canister (see Figure 6 below for details).

Figure 5: Integrated Gas Sample



Samples will be analyzed for carbon monoxide, carbon dioxide, and oxygen. The gasses should be separated by gas chromatography. Determination shall be by a gas chromatograph with a nickel catalyzed methanizer and flame ionization detector (GC/Ni-FID) for carbon dioxide. Carbon monoxide must be combusted to carbon dioxide and analyzed by SCAQMD Method 25.1. Oxygen will be analyzed by thermal conductivity.

QUALITY ASSURANCE

All applicable pieces of source test and process equipment used directly or indirectly for measurement of source test emission data must be calibrated, and the calibrations included in the final report (this includes gas meters, Pitot tubes, pressure gages, nozzles, temperature devices, calibration gases, fuel usage meters, totalizers, etc.).

All raw data field data sheets, as well as recorder strip charts, must accompany the test report. Additionally, all gas cylinders used to calibrate the analyzers must be certified, and a copy of the gas certificates shall be submitted with the report.

Where laboratory instrument analysis is required, instrument raw stripcharts, calibrations and standards, and limit of detection must be included in the source test report. This also includes equipment transfer and "chain-of-custody" form clearly describing all equipment and laboratory ID

numbers, dates and times, required analysis, and the signature/initials of persons involved in transfers.

The terms “non-detect” or “non-detectable” are no longer used for emission reporting purposes. Instead, non-detectable results are reported with respect to the limit of detection of the analytical instrument or method (e.g. report “<10 ppm”, if detection limit is 10 parts per million). Non-detectable emission results must have supporting documentation to show that acceptable sample volume was collected pursuant to rule or permit limits and analytical method limit of detection.

Equipment used by the source testing contractors must adhere to the Chapter III calibration and maintenance requirements of the District Source Test Manual.

All source testing firms used in monitoring emissions or analyzing samples shall be District LAP contractors in good standing, and must perform testing in accordance with District procedures, as clarified in this evaluation.

FINAL TEST REPORT

The final Source Test Report must include the following information:

- 1) Signed “Statement of Non-Conflict as an Independent Laboratory” (District Rule 304(k)) and CARB Lab Approval or District Lab Approval Program (LAP) document (if applicable).
- 2) A brief opening statement identifying the Facility I.D., the equipment A/N, P/O, or Device I.D. and the reason(s) for testing (applicable rules permit conditions, etc.). Include a copy of the Permit-to-Construct, Permit-to-Operate, or Facility Permit. Also identify the test dates, the personnel on hand for the test, names, titles and phone numbers of responsible test firm and facility personnel.
- 3) A summary of the Source Test results, and properly formatted source test data. Results shall be reported
- 4) A brief process description. Indicate equipment operation during testing; as well as any other information which may influence the final report.
- 5) A “self-critique” of anything that transpired during the test which you feel is useful in the interpretation of the test results.
- 6) A simple schematic diagram of the process, showing the sampling location, with respect to the upstream and downstream flow disturbances. Also include a cross-sectional

diagram of the stack or duct at the sampling location, depicting the sampling points with respect to compass direction.

- 7) The sampling and analytical procedures. Be specific about all aspects of sampling and analysis. Include diagrams of test equipment and methods.
- 8) Complete raw field data, including production data indicative of the testing interval, lab analyses, and the test results (show all calculations).
- 9) Current calibration data regarding all sampling and measuring equipment utilized during testing. This also includes all laboratory calibrations. (see District Source Testing Manual, Chapter III or "Quality Assurance Handbook For Air Pollution Measurement Systems", Vol. III, U.S. EPA-600/4-77-0276).
- 10) All calculations concerning intermediate process, emission, and/or flow information must be shown and included in the final report. This also applies to calculations concerning laboratory analyses.

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APPENDICIES

Metal Melting Test Plan

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APPENDIX A

Process Operating Parameters and Results Reporting Requirements

The following process operating parameters shall be recorded during testing at each location in addition to those specifically required by the applicable source test method:

- 1) Start and End time of each sample run. Note if the sample run must be stopped and restarted due to insufficient sample volume during a single heat.
- 2) Ambient Temperature shall be monitored and recorded before and after each test (°F).
- 3) Ambient Relative Humidity shall be monitored and recorded before and after each test (%).
- 4) Ambient Barometric Pressure shall be monitored and recorded before and after each test (in. Hg).
- 5) Total sampling time for each run (min.).
- 6) Specific material processed during each test run, this should be supported by positive material identification or certification documents.
- 7) Material condition (new/re-run/recycled/etc.).
- 8) Number of heats performed during sampling.
- 9) Total material charged during sampling (lbs.).
- 10) Average baghouse pressure differential during sampling (in. H₂O).
- 11) Average HEPA filter pressure differential during sampling (in. H₂O).
- 12) Stack temperature at sample location shall be monitored and recorded every 15 minutes during sampling (°F).
- 13) Description of all sources venting to the APCS during testing.
- 14) Velocity measurements at capture hood or furnace control system slots (fpm).

Test results summary shall at a minimum document the following:

1. Summary of Process and Test Conditions
2. Summary of Results for Particulate Emissions
 - a) Sample Time
 - b) Exhaust Flow Rate (acfm)
 - c) Exhaust Flow Rate (dscfm)
 - d) Emissions (grains/dscf)
 - e) Mass Emissions (lbs/hr)
3. Summary of Results for Chromium and Hexavalent Chromium
 - a) Sample Time
 - b) Exhaust Flow Rate (acfm)
 - c) Exhaust Flow Rate (dscfm)
 - d) Emissions (µg/dscm)
 - e) Emissions (µg/dscf)
 - f) Mass Emissions (lbs/hr)
4. Summary of Results for Multiple Metals Testing
 - a) Sample Time
 - b) Exhaust Flow Rate (acfm)

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- c) Exhaust Flow Rate (dscfm)
- d) Emissions ($\mu\text{g/dscm}$)
- e) Emissions ($\mu\text{g/dscf}$)
- f) Mass Emissions (lbs/hr)

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APPENDIX B

Facility Process Flow Diagrams & Photos
(Confidential Do Not Distribute)

Figure 6: Facility A - Basic Process Flow Diagram

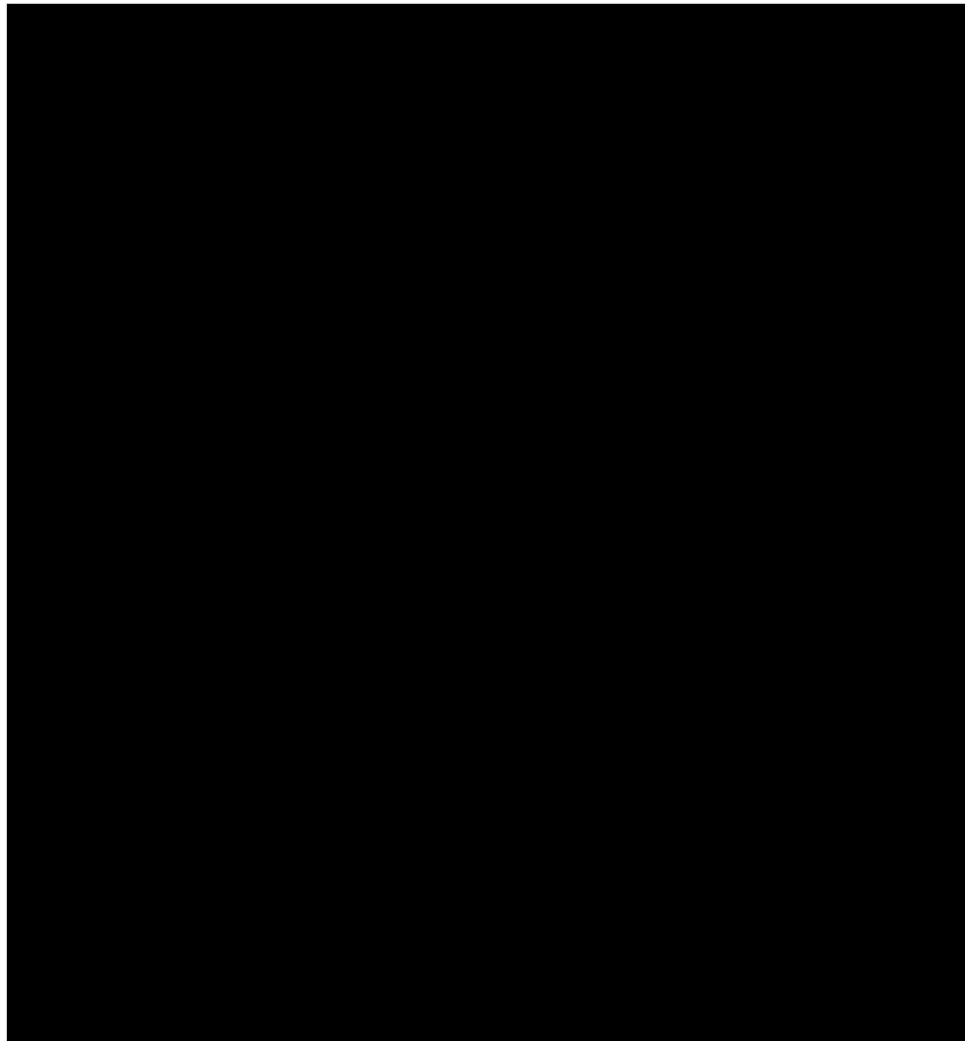
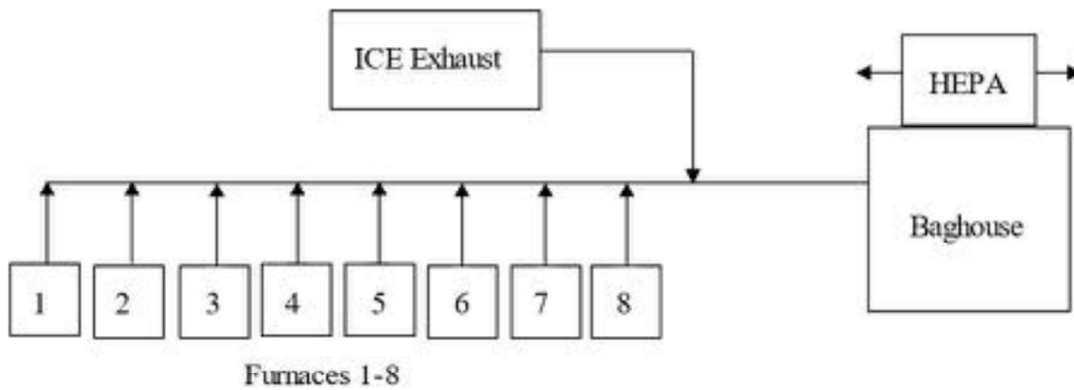


Figure 8: Facility B – Basic Process Flow Diagram

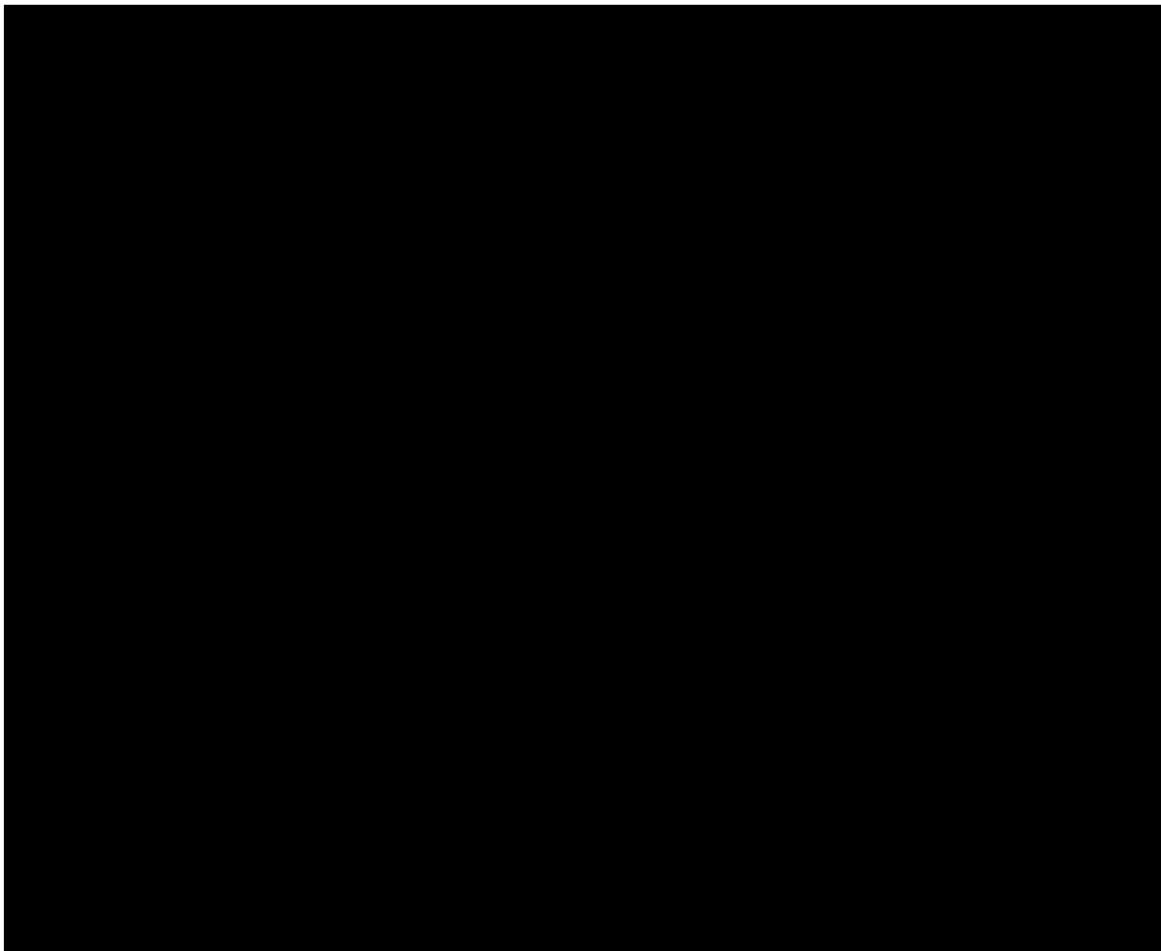
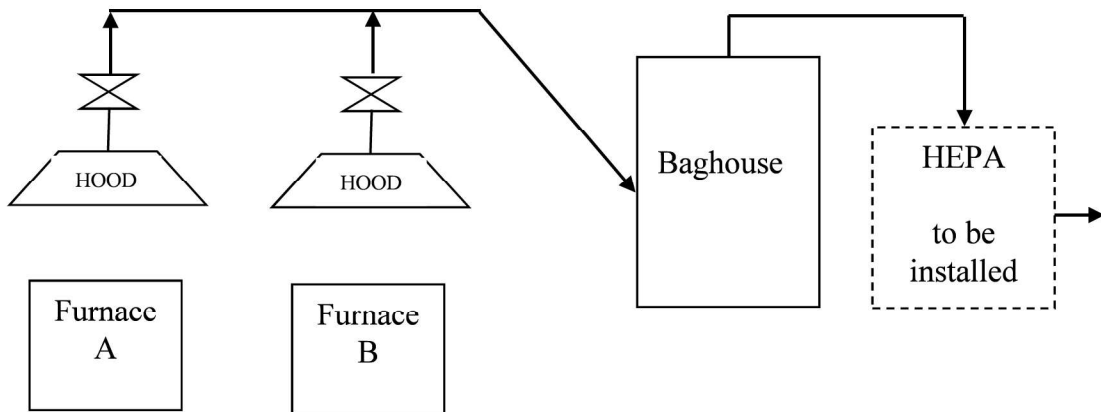
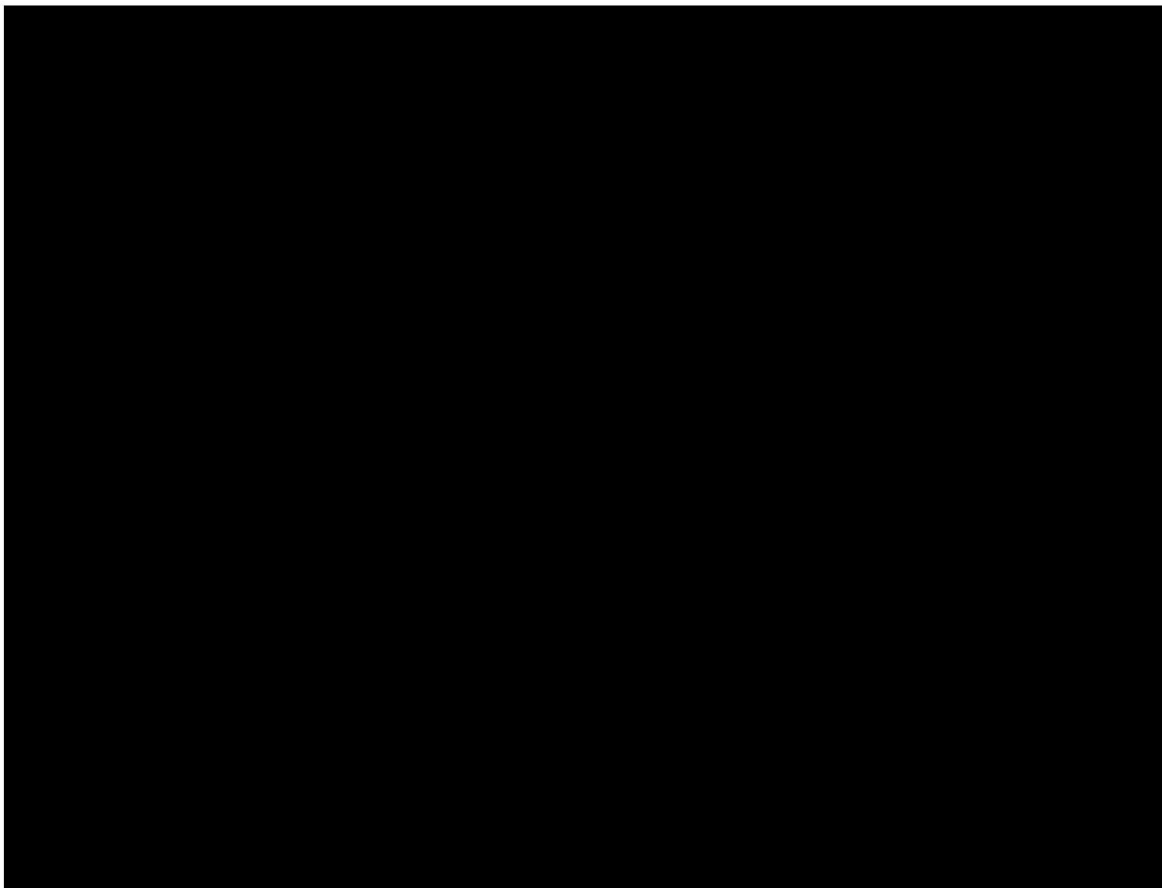
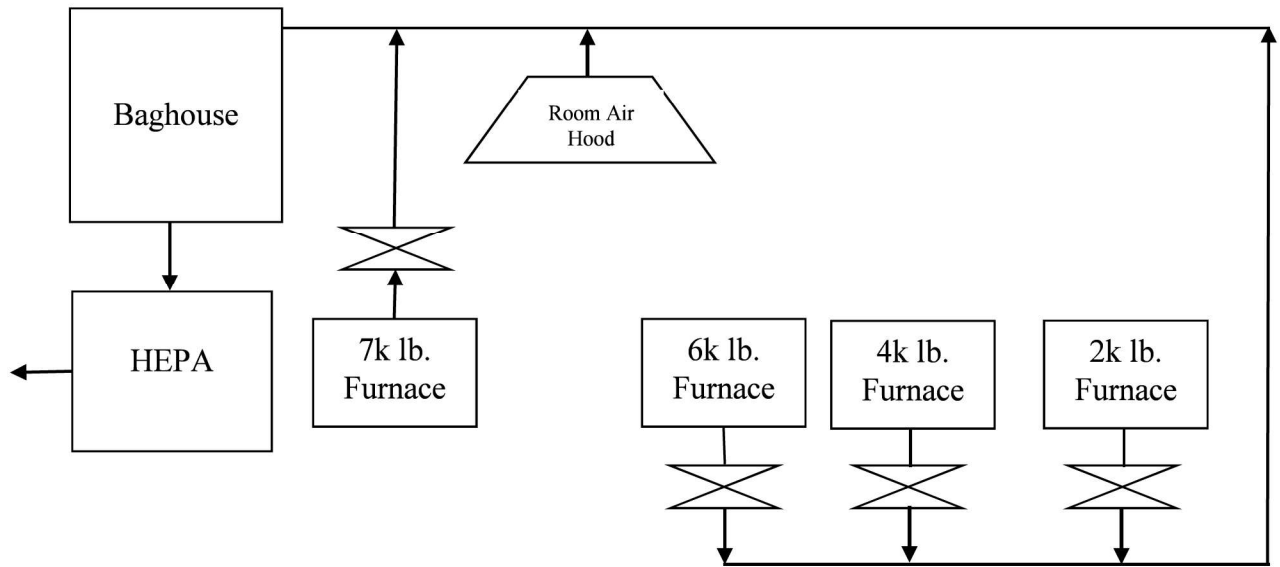


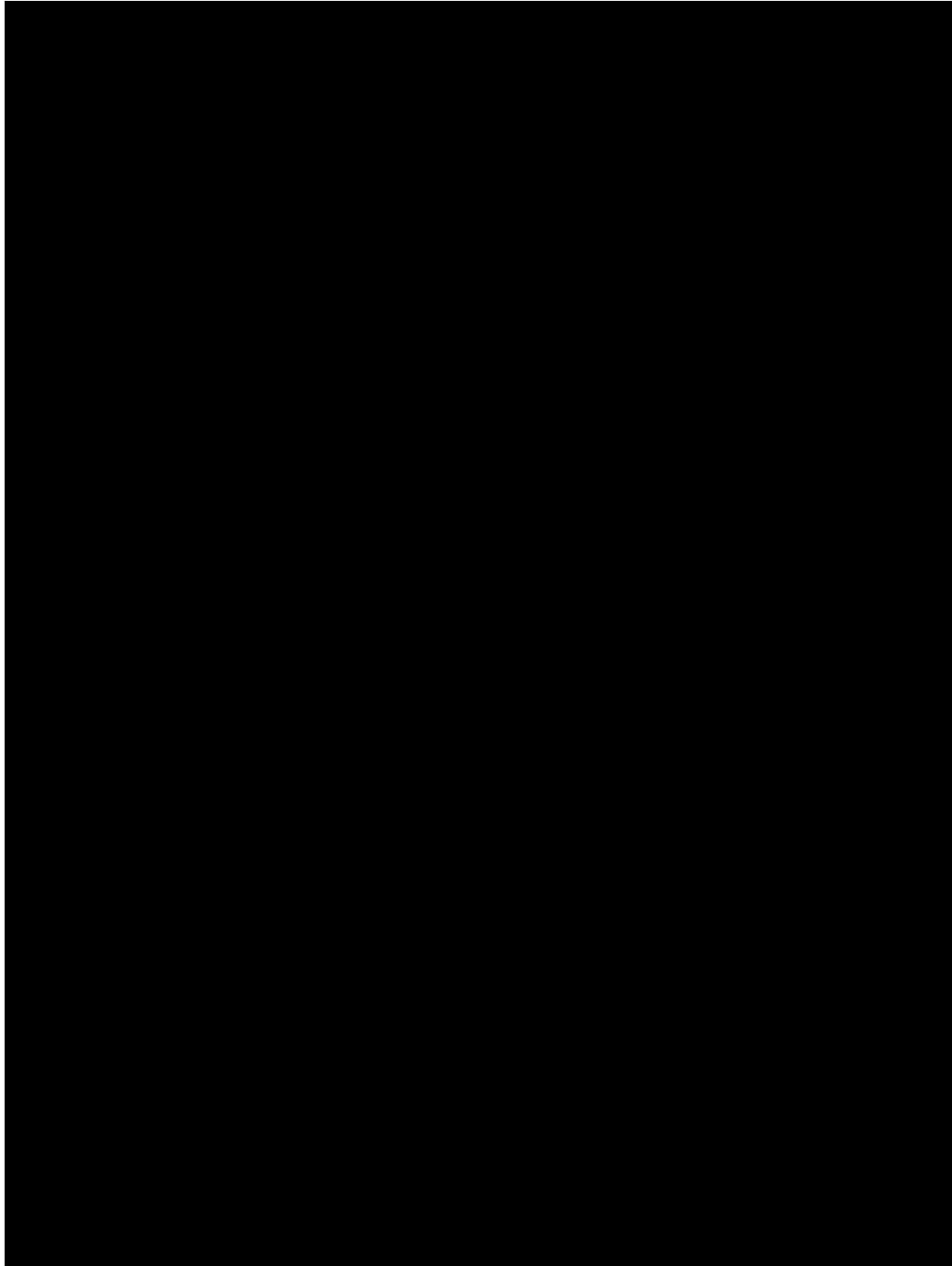
Figure 8: Facility C – Basic Process Flow Diagram



Metal Melting Test Plan

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Date: 3/27/19



APPENDIX J

SCAQMD CHECKLIST FOR SOURCE TEST REPORTS, FORM STR.

SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT

ENGINEERING FORM STR CHECK LIST FOR SOURCE TEST REPORTS

Please check off all the following items to verify that the information is provided in the source test report, and then send the checklist along with the source test report.

- [X] Brief description of the equipment tested.
- [X] Brief process description, including maximum and normal operating temperatures, pressures, through-put, etc.
- [X] Operating conditions under which test was performed.
- [X] Process schematic diagram showing the ports and sampling locations, including the dimensions of the ducts/stacks at the sampling locations, along with upstream and downstream locations, and distances of flow disturbances, (e.g. elbows, tees, fans, dampers) from the sampling locations (upstream and downstream).
- [X] Field and laboratory data forms, strip charts and analyses.
- [X] Brief description of sampling and analytical methods for each gaseous and particulate constituent measured.
- [X] Calculations for volumetric flow rates and emission rates.
- [X] Description of calibration and quality assurance procedures.
- [X] Determination that the testing laboratory qualifies as an “independent testing laboratory” under Rule 304 (no conflict of interest).